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SUPERSONIC FLOW OF CHEMICALLY REACTING GAS-PARTICLE MIXTURES. V--ETC(U)
JAN 76 M M PENNY, S D SMITH, P G ANDERSON NAS9-14517
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LEVEL III

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SUPERSONIC FLOW OF CHEMICALLY REACTING GAS-PARTICLE MIXTURES.

Volume II.

RAMP — A Computer Code for Analysis of Chemically Reacting Gas-Particle Flows.

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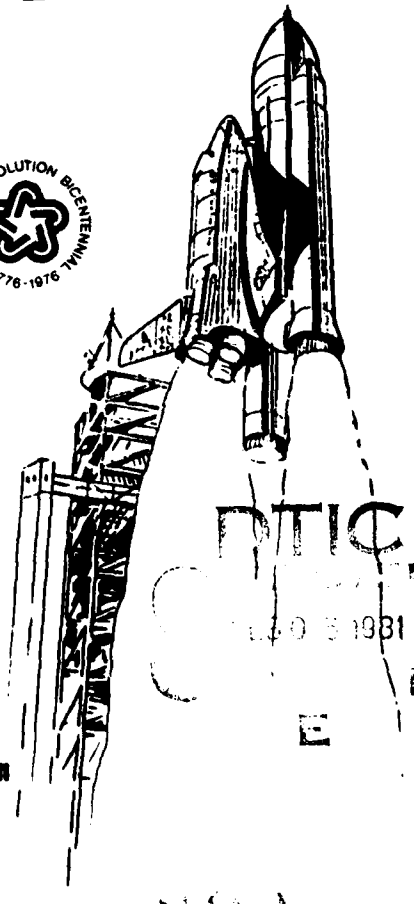

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Johnson Space Center
Houston, TX 77058

FOREWORD

This document is Volume II of a two volume report describing the Reacting and Multi-Phase (RAMP) Computer Code developed by the Advanced Technology Systems Section of Lockheed's Huntsville Research & Engineering Center. Volume II addresses the computer code along with the program input and output. Volume I deals with the theory and numerical solution for the computer code.

Documentation of the computer code was prepared in partial fulfillment of contract requirements (Contract NAS9-14517) with the NASA-Johnson Space Flight Center, Houston, Texas, in support of Space Shuttle related exhaust plume applications. The contracting officer's technical representative for this study was Mr. Barney B. Roberts of the Aerodynamics Systems Analysis Section.

The authors acknowledge the efforts of a number of individuals who contributed to the development of the RAMP code. These include Dr. Terry F. Greenwood and Mr. David C. Seymour of the NASA-Marshall Space Flight Center; and Messrs. Robert J. Prozan, Jon A. Freeman, L. Ray Baker and A. W. Ratliff of Lockheed-Huntsville. Ideas and suggestions for improvement of the analysis are reflected by frequent consultation with these individuals.

Companion documents to this report include a theory and numerical solution document for the RAMP computer code; a report which describes the modifications made to the NASA-Lewis TRAN72 computer code; and documentation of a one-dimensional solution which provides a supersonic startline for the RAMP code. These documentation are, respectively:

- "Supersonic Flow of Chemically Reacting Gas-Particle Mixtures — Volume I — A Theoretical Analysis and Development of the Numerical Solution," LMSC-HREC TR D496555-I.
- "User's Guide for TRAN72 Computer Code Modified for use with RAMP and VOFMOC Flowfield Codes," LMSC-HREC TM D390409.
- "General One-Dimensional Flow of Gas-Particle System," LMSC-HREC TM 390876.

CONTENTS

Section 1
INTRODUCTION AND SUMMARY

Most solid rocket motor propellants contain metal additives which increase the energy content of the system and also suppress combustion pressure instabilities. The presence of these metal additives, however, results in condensed products in the exhaust which can do no expansion work and thereby reduce the effectiveness of the nozzle. Also, the presence of liquid or solid particles in the exhaust will contribute significantly to radiation and plume impingement heating on structures which are either immersed or in proximity to the exhaust plume. It is therefore important to know the physical properties of both the solids and gases throughout the nozzle and exhaust plumes.

This report describes two computer programs which are applicable to the analysis of chemically reacting gas-particle flow fields. The programs are:

- The NASA-Lewis FORTRAN IV Computer Program for Calculation of Thermodynamic and Transport Properties of Complex Chemical Systems (TRAN72)
- The Lockheed Reacting and Multi-Phase Computer Program (RAMP).

These programs are currently operational on the CDC, Univac and IBM computers. To facilitate the use of the codes, they are constructed such that automatic transmission of data to other computer programs is possible via magnetic tapes.

Section 2 presents a description of the modifications made to the TRAN72 computer program to meet the general requirements of Lockheed's RAMP program and provides instructions for operating the modified TRAN72 program. Four example cases are presented which show the required input format

and resultant output for creation of thermodynamic data for typical rocket performance problems. No attempt is made here to report on the program itself since this information is documented in Refs. 1 and 2.

Section 3 of this report discusses the RAMP program. Included are:

- A discussion of the basic capabilities and limitations of the program.
- A user's input guide for the RAMP program.
- A description of the typical input/output for a two-phase chemical equilibrium flow problem; a single phase chemical equilibrium flow problem with free molecular considerations and a single phase finite rate chemistry flow problem.
- A discussion of typical user problems and possible fixes.
- A list of helpful hints and a presentation of example deck set-ups.
- A brief description of each of the basic routines in functional groupings.
- A detailed discussion of each individual routine used in the program.
- Program overlay structure.
- A section of typical example problems including a statement of the problem, accompanying figure and sample input and output.

The gas-particle capability has been incorporated into a streamline-normal method of characteristics computer program (Ref. 3). Choosing this technique provides several important advantages in describing flowfields which contain a gas-particle mixture not found in conventional method of characteristics program (Ref. 4), and at the same time, retains the same sophistication and capabilities of these programs. First, the streamline-normal method allows a data point on a particle limiting streamline to be treated in the same fashion as a data point on a gas streamline. This greatly simplifies the tracing of particle trajectories through the flow field. Also, another important feature is the reduction in computer storage requirement to identify the particle locations. Flow fields containing shock waves (both

right-running and left-running or in combination) can be analyzed in one continuous operation, hence expediting the flowfield description of nozzles and plumes or other complicated geometries.

These computer programs are extremely large and complex so that a complete description of them is not feasible in this report. It is possible, however, to utilize the programs with the information contained herein while total understanding of the methods is made possible by study of the supporting documentation.

The computer programs are available for external distribution. Further information on obtaining the programs is available from the authors.

Section 2

USER'S INPUT/OUTPUT GUIDE FOR THE MODIFIED TRAN72 COMPUTER CODE

The TRAN72 computer program (developed by NASA-Lewis Research Center (Ref. 1)) was synthesized by combining a program for the transport properties calculation with the CEC 71 program (Ref. 2) for the thermodynamic properties calculation. The TRAN72 program was subsequently modified to meet the requirements of Lockheed's reacting and Multi-Phase (RAMP) Computer Program (Ref. 5). The requirements satisfied were: (1) calculation of the theoretical rocket performance (for both equilibrium and frozen compositions) during a "gaseous-only" expansion, after a two-phase combustion chamber calculation; and (2) automated communication of these properties to the RAMP program.

2.1 USE OF THE MODIFIED TRAN72 PROGRAM WITH THE RAMP PROGRAM

Modifications were made to the TRAN72 chemical equilibrium calculational scheme in order to generate thermochemical data consistent with the assumptions utilized in the RAMP program formulation. The assumptions being addressed in the RAMP program are:

- The total mass of the mixture is constant.
- The total energy of the mixture is constant.
- The gas obeys the perfect gas law and is either chemically frozen, in chemical non-equilibrium or in chemical equilibrium.
- There is no mass exchange between the phases.
- The particles are inert.

In the modified TRAN72 calculational scheme, the chamber calculations are performed initially with the condensed species considered. The total mass and total enthalpy of the mixture are then adjusted by removing the mass and

enthalpy associated with the condensed species predicted to exist in the chamber after combustion. The total mass adjustment is made by removing the appropriate amount of mass of each of the elements which comprise the condensed species that exist in the chamber. The total enthalpy is adjusted by removing the enthalpy associated with the condensed species that exist in the chamber. Next, the adjusted elemental mass balance relationships and the adjusted total enthalpy are referenced to the adjusted total mass of the mixture. All condensed species are then removed from the list of possible products being considered by the program. The chamber calculations and subsequent equilibrium chemistry expansion are then made with a gaseous-only composition. When the thermodynamic calculations are completed, the transport properties are calculated in the manner described in Ref. 1. The resultant equilibrium chemistry expansion and corresponding transport properties data are for the case in which there is no heat transfer between the condensed and gaseous species during the equilibirum chemistry expansion process. To account for the effects of the heat transfer that does take place between the condensed and gaseous species during the flowfield calculations, additional thermochemical data are required. To generate the required data, the total enthalpy of the gaseous-only mixture is perturbed (mass is held constant) and the thermochemical data calculational scheme is repeated. The total enthalpy is repeatedly perturbed; the result being an array of equilibrium expansion processes and corresponding transport properties, each with a different degree of heat transfer between the two phases.

Experience in thermodynamical modeling of rocket exhaust flows has indicated that many chemical systems experience a transition from equilibrium to frozen chemistry during the expansion process. The standard TRAN72 program has an option to treat this problem. Under the pressure freeze option the chamber and initial expansion calculations are made assuming equilibrium chemistry. At a predetermined pressure ratio (chamber to local static), the chemistry of the system is frozen and the remainder of the expansion is completed with frozen chemistry. With this option, the transport properties are calculated as outlined in Ref. 1.

The thermochemical and transport data are communicated to the RAMP computer program automatically through the use of a magnetic tape (or rapid access storage, i.e., disk, FASTRAN, etc.). Creation of the data tape (or file) is accomplished by means of an additional subroutine (MOCDAT) added to the TRAN72 program. Logic is provided in this routine for creation of a new data tape (or file) and adding data to an existing Master data list. Each data case must be identified with a unique case name which is subsequently used by the RAMP (see card 8 of RAMP input guide) program to determine if thermodynamic data are available. An additional namelist has been added to the run stream to control use of the options available in the MOCDAT subroutine.

The modified TRAN72 program is used to generate thermodynamic and transport properties of the gaseous phase of the products of combustion being considered in a two-phase flow analysis. Control of the program function for this application is handled through three input groups: the reactant data cards, the $INPT2 namelist, and the $RKTINP namelist. A detailed description of the standard TRAN72 program input is given in Ref. 1. Thermodynamic data required for this application are calculated using the RKT option under the $INPT2 namelist. Selection of this option permits calculation of theoretical rocket performance for both equilibrium and frozen compositions during expansions. The variables MOC2P, PARTHT, QDOTP and NQI have been added to the $INPT2 namelist. The MOC2P variable controls the selection of the two-phase flow analysis option (MOC2P=T). The variables PARTHT, QDOTP and NQI control the selection (PARTHT=T) and use of the variable total enthalpy option when the effects of heat transfer between the condensed and gaseous species are to be determined in a two-phase flow analysis. When PARTHT=T, QDOTP is set equal to the amount by which the total enthalpy of the gaseous only mixture is to be perturbed. NQI is set equal to the number of QDOTP values input. The specific values of the ratio of chamber to local static pressures (P_c/P) at which thermodynamic and transport data are generated are input to the program in the $RKTINP namelist. The pressure freeze option is activated by setting the variable NFZ under the $RKTINP namelist

equal to the number of the pressure ratio at which transition from equilibrium to frozen chemistry is to occur. (The chamber is considered to be number one, the throat number two, etc.). Freeze pressures may be the chamber value or any supersonic pressure. No provision is made for freeze pressures between chamber and throat. The parameters which are generally utilized by the RAMP program are local Mach number, static pressure and temperature, isentropic coefficient (gamma), molecular weight, entropy, Prandtl number, viscosity, specific heat at constant pressure and the total enthalpy (gas only). These parameters, with the exception of the total enthalpy, are calculated for each value of (P_c/P) ratio by the program. A detailed description of the logic involved in the standard TRAN72 program computation is presented in flow chart form in Ref. 1. This information can be consulted for an in-depth understanding of the calculational scheme.

To automatically create a tape for communication with the RAMP program requires that one of the two tape-write options be selected (MOCT=T, or MOCTF=T) under the $INPT2 namelist. The MOCT variable is utilized when the thermochem data are to be run completely under the equilibrium assumption. The MOCTF variable is utilized when the thermochem data are to be run completely or partially frozen. If one of these options is selected an additional namelist, $TAPGEN, must be input to control the tape-write function and the input of the case name card. The $TAPGEN data are input after the $INPT2 data but prior to the case name card and $RKTINP namelist inputs. Table 2-1 summarizes the program variables added to the modified TRAN72 program.

Four example cases showing the required input format and resultant output for creation of thermodynamic data for typical rocket performance problems are presented in Table 2-2. Case 1 is the required input to perform a calculation of theoretical rocket performance for both the equilibrium and frozen composition assumptions during an isentropic expansion. (No tape is generated.) Case 2 is the same as Case 1 except that a tape for communication with other programs is generated for the frozen composition assumption

Table 2-1

ADDITIONAL INPUT VARIABLES FOR MODIFIED* TRAN72 PROGRAM

$INPT2 NAMELIST					
Variable	Dimension	Type	Common Label	Value Before Read	Comment
MOCT	1	L	HREC	F	Selects tape-write option if true for equil. run.
MOC2P	1	L	HREC	F	Selects two-phase flow analysis option if true.
MOCTF	1	L	HREC	F	Selects tape-write option if true for frozen and pressure freeze options.
PARTHT	1	L	TWOPAS	F	Selects variable total enthalpy option if true for two-phase analysis run.
QDOTP**	26	R	TWOPAS	0.0	Set equal to the amount by which the total enthalpy of the gaseous-only mixture is to be perturbed.
NQI	1	I	TWOPAS	0	Set equal to the number of QDOTP values input.
$TAPGEN NAMELIST					
IREAD	1	I	–	1	If equal 0, new data added to master data tape list; if equal 1 data written on new data tape.
IO	1	I	–	8	Tape unit of old master tape list.
IN***	1	I	–	10	Tape unit of new data tape.
Case Name Card Format: 6A4					

*Routines modified from the original TRAN72 program are: LINK, MAIN1 REACT, SEARCH, EQLBRM, ROCKET, RKTOUT, OUT1, TRANSP, OUT.

**The values of QDOTP must always be input in ascending order (from the most negative to the most positive).

***When running multiple cases, the data of the last case must always be placed on tape unit 10 if it is to be communicated automatically to the RAMP or VOFMOC programs.

during expansion (MOCTF=T). Case 3 is the required input format for creation of thermodynamic data for use with the RAMP program (MOC2P=T); a tape is generated for the equilibrium composition assumption during the isentropic expansion (MOCT=T). (The effects of heat transfer between the condensed and gaseous species are not determined.) Finally, Case 4 is the same as Case 3 except that the effects of heat transfer between the condensed and gaseous species are determined (PARTHT=T).

2.2 USE OF THE MODIFIED TRAN72 PROGRAM WITH THE VOFMOC PROGRAM

The TRAN72 program has been modified to meet the requirements of the RAMP computer program. The data tape (or file) created for communication with the RAMP program contains additional data not required by the VOFMOC program (Ref. 6). For that reason, the tape read statement and format statement in subroutines GASTAP and GASRD, respectively, must be modified to read the additional data as "dummy" variables. The following statements must be changed in the above subroutines before the data tape generated by the TRAN72 program can be read correctly by the VOFMOC program.

- Subroutine GASRD

Old Statement: `1 FORMAT(4A6,5X,A3,6X,I2,3X,I2)`

New Statement: `1 FORMAT(6A4,5X,A3,6X,I2,3X,I2)`

- Subroutine GASTAP

Old Statement: `10 READ(10)(BETA(I),I=1,4),IOF,IS`

New Statement: `10 READ(10)(BETA(I),I=1,4),DU,DU,IOF,IS`

No other limitations are placed on the use of the modified TRAN72 program.

Table 2-2

EXAMPLE CASES SHOWING THE REQUIRED INPUT FORMAT FOR CREATION OF THERMODYNAMIC DATA FOR TYPICAL ROCKET PERFORMANCE PROBLEMS

Case 1: Required input to perform a calculation of theroretical rocket performance for both the equilibrium and frozen composition assumptions during expansion. (No tape is generated.)

```
REACTANTS
H  2.00                                          1.00     0.0      G298.15  H
O  2.00                                          1.00     0.0      G298.15  O
                    (Insert Blank Card)
NAMELISTS
 $INPT2
      RKT=T,PSIA=T,KASE=00001,P=200.00,OF=T,MIX=6.0
 $END
 $RKTINP
  PCP=10.,30.,50.,100.,500.,1000.,5000.,50000.,100000.,500000.
 $END
```

Resultant Output for Case 1

```
REACTANTS
H   2.00000      .0000      .0000      .0000      .0000   1.0000            .00  G   298.150  F      .00000
O   2.00000      .0000      .0000      .0000      .0000   1.0000            .00  G   298.150  O      .00000
NAMELISTS
$INPT2
KASE    =              1
T       =   .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
P       =   .20000000E+03,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00
PSIA    =   T
MMHG    =   F
NSQM    =   F
V       =   .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00
RHO     =   .20000000E+03,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00
ERATIO  =   F
OF      =   T
FPCT    =   F
FA      =   F
MIX     =   .80000000E+01,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
            .00000000E+00,  .00000000E+00,  .00000000E+00
TP      =   F
HP      =   F
SP      =   F
TV      =   F
UV      =   F
SV      =   F
RKT     =   T
```

Resultant Output for Case I (Cont'd)

```
SPUCK    =  F
DEIN     =  F
VITO     =  F
LM       =     .0000000E+00
SU       =     .0000000E+00
SU       =     .0000000E+00
IGIS     =  F
IDEBUG   =                +0
TRACE    =     .0000000E+00
SIGNIT   =  F
EUNITS   =  F
TRNSPT   =  T
PRUCH    =  F
PUNCH    =  F
SDUMTA   =  T
DIP      =  F
MOLP     =  F
MOLT     =  F
MOLTP    =  F
MOLZP    =  F
PARINT   =  F
SOUTP    =     .0000000E+00,   .0000000E+00,   .0000000E+00,   .0000000E+00,
               .0000000E+00,   .0000000E+00,   .0000000E+00,   .0000000E+00,
               .0000000E+00,   .0000000E+00,   .0000000E+00,   .0000000E+00,
               .0000000E+00,   .0000000E+00,   .0000000E+00,   .0000000E+00,
               .0000000E+00,   .0000000E+00,   .0000000E+00,   .0000000E+00,
               .0000000E+00,   .0000000E+00,   .0000000E+00,   .0000000E+00,
               .0000000E+00,   .0000000E+00
 ZI      =                +0

SOLV

SPECIES BEING CONSIDERED IN THIS SYSTEM
    J 7/65  H          J 3/64  H02        J 3/61  H2        L11/65  H2O(S)      L11/65  H2O(L)
    J 3/61  H2O        L 2/69  H2O2       J 6/62  O         J12/70  OH          J 9/65  O2
    J 6/61  O3

                    LIST OF CONDENSED SPECIES FROM SEARCH
    H2O(S)      H2O(L)
SMATINP
EWL      =  T
FMWZ     =  T
SUBAX    =     .0000000E+00,   .0000000E+00,   .0000000E+00,   .0000000E+00,
               .0000000E+00,   .0000000E+00,   .0000000E+00,   .0000000E+00,
               .0000000E+00,   .0000000E+00,   .0000000E+00,   .0000000E+00,
               .0000000E+00
SUBAY    =     .0000000E+00,   .0000000E+00,   .0000000E+00,   .0000000E+00,
               .0000000E+00,   .0000000E+00,   .0000000E+00,   .0000000E+00,
               .0000000E+00,   .0000000E+00,   .0000000E+00,   .0000000E+00,
               .0000000E+00
SCL      =     .1000000E+02,   .1000000E+02,   .1000000E+02,   .1000000E+02,
               .5000000E+03,   .1000000E+01,   .1000000E+01,   .5000000E+00,
               .1000000E+00,   .5000000E+00,   .1000000E+00,   .1000000E+00,
               .1000000E+00,   .1000000E+00,   .1000000E+00,   .1000000E+00,
               .1000000E+00,   .1000000E+00,   .1000000E+00,   .1000000E+00,
               .1000000E+00,   .1000000E+00
```

Resultant Output for Case 1 (Cont'd)

```
OF =    0.000000                EFFECTIVE FUEL          EFFECTIVE OXIDANT          MIXTURE
                                  HPP(2)                   HPP(1)                   HSUBO
ENTHALPY                        .00000000                .00000000                .00000000
(KG-MOL)(DEG K)/KG
                                  BOP(1,2)                 BOP(1,1)                  BO(1)
KG-ATOMS/KG                     .99209301+00             .00000000                .14172757+00
      M                         .00000000                .82562343-01             .53571437-01
      O

PT        M         O
 1   -10.016   -10.435     9.000
 2   -10.212   -10.722     3.000
PC/PI= 1.728076    T =   3229.03
 2   -10.212   -10.721     2.000
PC/PI= 1.726724    T =   3229.25
 3   -10.027   -17.681     4.000
 4   -11.100   -18.963     4.000
 5   -11.348   -19.642     4.000
 6   -11.519   -20.621     4.000
 7   -11.000   -24.483     4.000
 8   -12.034   -27.470     3.000
 9   -12.378   -35.461     3.000
10   -12.465   -55.534     2.000
11   -13.250   -64.646     2.000
12   -13.622   -93.855     2.000
```

Resultant Output for Case 1 (Cont'd)

THEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

PC = 2000.0 PSIA

CASE NO. 1

	CHEMICAL FORMULA	WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL	H 2.00000	1.00000	.000	G	298.15	.0000
OXIDANT	O 2.00000	1.00000	.000	G	298.15	.0000

O/F= 6.000 PERCENT FUEL= 14.2857 EQUIVALENCE RATIO= 1.3227 REACTANT DENSITY= .0000

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.7267	10.000	30.000	50.000	100.00	500.00	1000.00	5000.00	10000.0	100000.0	500000.0
MACH NO.	13.409	7.0815	1.3629	.4546	.2722	.1361	.0272	.0136	.0027	.0013	.0001	[illegible]
T, DEG K	3387	3229	2756	2456	2306	2089	1562	1365	995	567	475	331
RHO, G/CC	6.3526-4	3.9127-4	8.2354-5	3.1358-5	2.0152-5	1.1171-5	2.9587-6	1.6896-6	4.7056-7	7.9798-8	4.7254-8	1.4162-8
H, CAL/G	.0	-274.9	-1652.4	-1464.6	-1637.6	-1853.3	-2268.9	-2413.6	-2681.5	-2933.3	-2986.0	-3075.5
S, CAL/(G)(K)	4.5711	4.5711	4.5711	4.5711	4.5711	4.5711	4.5711	4.5711	4.5711	4.5712	4.5711	4.5711
M, MOLE WT	12.969	13.155	13.686	13.931	14.009	14.074	14.111	14.111	14.112	14.112	14.112	14.112
(DL/DLPT)T	-1.04518	-1.03021	-1.01687	-1.00683	-1.00379	-1.00135	-1.00004	-1.00000	-1.00000	-1.00000	-1.00000	-1.00000
(DL/DLTP)	1.0198	1.7271	1.3744	1.1602	1.0982	1.0360	1.0013	1.0002	1.0000	1.0000	1.0000	1.0000
CP, CAL/(G)(K)	3.1639	2.9874	2.0739	1.4322	1.1889	.9561	.7528	.7193	.6516	.5839	.5711	[illegible]
GAMMA (S)	1.1289	1.1269	1.1304	1.1402	1.1429	1.1873	1.2350	1.2435	1.2757	1.3178	1.3273	1.3429
SONIC VEL,M/SEC	1565.7	1516.6	1375.8	1297.3	1261.6	1210.6	1071.1	1007.4	864.7	674.9	622.4	511.3
MACH NUMBER	.000	1.0000	2.157	2.679	2.934	3.253	4.068	4.461	5.478	7.341	8.042	9.926
AS/A1		1.0000	2.9280	5.4053	7.9544	13.469	46.028	78.196	266.21	1500.93	2512.17	8255.61
CSTAR, FT/SEC		7624	7624	7624	7624	7624	7624	7624	7624	7624	7624	7624
CF		.653	1.277	1.506	1.593	1.695	1.875	1.934	2.038	2.132	2.151	2.184
IVAC,LB-SEC/LB		291.9	360.1	399.7	415.2	433.5	466.1	476.8	495.7	512.3	515.7	521.5
ISP, LB-SEC/LB		194.6	302.0	357.0	377.5	401.6	444.3	458.3	483.0	505.2	509.7	517.6

MOLE FRACTIONS

H	.06144	.05369	.02922	.01492	.00933	.00387	.00013	.00002	.00000	.00000	.00000	.00000
HO2	.00002	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
H2	.25264	.24870	.23976	.23429	.24033	.24216	.24392	.24398	.24399	.24399	.24399	.24399
H2O	.63366	.62783	.70389	.73601	.74540	.75254	.75593	.75600	.75601	.75601	.75601	.75601
H2O2	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
O	.00930	.00702	.00181	.00038	.00013	.00002	.00000	.00000	.00000	.00000	.00000	.00000
OH	.06407	.05901	.02314	.00897	.00465	.00139	.00001	.00000	.00000	.00000	.00000	.00000
O2	.00887	.00713	.00216	.00079	.00016	.00002	.00000	.00000	.00000	.00000	.00000	.00000

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .5000E-06 FOR ALL ASSIGNED CONDITIONS

HCO	H2O(L)	O3

(*) WEIGHT FRACTION OF FUEL IN TOTAL FUELS = 1.0000 , TOTAL OXIDANTS

Resultant Output for Case 1 (Cont'd)

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

O/F= 6.0000 PERCENT FUEL= 14.2857 EQUIVALENCE RATIO= 1.3227 CHAMBER PRESSURE= 13.609 ATM

TEMP	VISCOSITY	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
DEG K	POISE	CAL/(CM)(SEC)(K)					CAL/(G)(K)		DIMENSIONLESS		
3367	1027•x10⁻⁶	721•x10⁻⁶	804•x10⁻⁶	1525•x10⁻⁶	5248•x10⁻⁶	6773•x10⁻⁶	•6857	3•1839	•5965	•4627	[illegible]
[illegible]	996•	681•	772•	1452•	4703•	6156•	•6793	2•9674	•6627	•5131	[illegible]
2758	893•	567•	666•	1233•	2440•	3673•	•8550	2•0739	•6193	•4763	[illegible]
2456	819•	503•	590•	1093•	1345•	2438•	•8348	1•4322	•6257	•4013	[illegible]
2366	779•	475•	548•	1023•	847•	1870•	•8230	1•1889	•6273	•4955	[illegible]
2089	719•	436•	485•	921•	364•	1285•	•8038	•9561	•6277	•5353	[illegible]
1562	567•	349•	331•	680•	15•	695•	•7462	•7528	•6216	•6135	[illegible]
1303	503•	314•	272•	586•	2•	587•	•7183	•7193	•6172	•6158	[illegible]
775	371•	240•	160•	400•	0•	400•	•6516	•6516	•6045	•6045	
567	215•	151•	70•	221•	0•	221•	•6839	•6839	•5702	•5762	
[illegible]	160•	129•	54•	164•	0•	164•	•5711	•5711	•5580	•5580	
[illegible]	113•	85•	31•	119•	0•	119•	•5526	•5526	•5253	•5253	

Resultant Output for Case 1 (Cont'd)

THEORETICAL ROCKET PERFORMANCE ASSUMING FROZEN COMPOSITION DURING EXPANSION

PC = 200.0 PSIA

CASE NO. 1

	CHEMICAL FORMULA	WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL	H 2.00000	1.00000	.000	G	298.15	.0000
OXIDANT	O 2.00000	1.00000	.000	G	298.15	.0000

O/F= 6.0000 PERCENT FUEL= 14.2857 EQUIVALENCE RATIO= 1.3227 REACTANT DENSITY= .0000

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.7747	10.000	30.000	50.000	100.00	500.00	1000.00	5000.00	10000.0	50000.0	100000.0
P, ATM	13.609	7.6967	1.3609	.4536	.2722	.1361	.0272	.0136	.0027	.0013	.0001	.0000
T, DEG K	3387	3063	2293	1819	1649	1426	1009	854	574	485	282	17[illegible]
RHO, G/CC	0.3506-4	3.9453-4	9.5694-5	3.9420-5	2.6172-5	1.5600-5	4.2005-6	2.5197-6	7.4008-7	1.3640-7	6.2160-8	2.5[illegible]
H, CAL/G	.0	-269.7	-981.8	-1322.7	-1456.2	-1621.0	-1918.9	-2016.9	-2191.0	-2354.0	-2374.5	-2426.5
S, CAL/(G)(K)	4.5711	4.5711	4.5711	4.5711	4.5711	4.5711	4.5711	4.5711	4.5711	4.5711	4.5711	4.5711
M, MOL WT	12.969	12.969	12.969	12.969	12.969	12.969	12.969	12.969	12.969	12.969	12.969	12.969
CP, CAL/(G)(K)	.8857	.8726	.9224	.7829	.2633	.7351	.6888	.6598	.6212	.5705	.5728	.5[illegible]
GAMMA (S)	1.2692	1.2136	1.2296	1.2953	1.2913	1.2633	1.2772	1.3117	1.3277	1.3519	1.3653	1.3[illegible]
SONIC VEL, M/SEC	1620.3	1543.9	1329.9	1269.1	1190.3	1.749.0	913.0	847.3	722.9	627.0	470.9	3[illegible]
MACH NUMBER	.000	1.000	2.156	2.763	3.042	3.427	4.380	4.649	5.296	6.441	9.307	11.069
AE/AT		1.0000	2.2159	4.5435	6.6605	12.969	35.455	56.827	189.95	1007.57	1069.19	5[illegible]
CSTAR, FT/SEC		7435	7435	7435	7435	7436	7433	7436	7433	7433	7436	7[illegible]
CF		.682	1.206	1.469	1.543	1.626	1.769	1.814	1.891	1.956	1.968	1.[illegible]
IVAC, LB-SEC/LB		2071	3434	3756	3871	4[illegible]9	4249	4325	4454	4562	4586	4[illegible]
ISP, LB-SEC/LB		1574	2923	3393	3562	3756	4680	4189	4366	4516	4545	4[illegible]

MOLE FRACTIONS

H	.36194	HO2	.00202	H2	.25264	H2O	.00366
H2O2	.00001	O	.00936	OH	.06437	O2	.00687

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .50000-05 FOR ALL ASSIGNED CONDITIONS

H2O(S) H2O(L) O3

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

Resultant Output for Case 1 (Cont'd)

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING FROZEN COMPOSITION DURING EXPANSION

O/F= 6.6000 PERCENT FUEL= 14.2657 EQUIVALENCE RATIO= 1.3227 CHAMBER PRESSURE= 13.639 ATM

TEMP	VISCOSITY	MONATOMIC COND	INTERNAL COND	FROZEN COND	CP FROZ	PRANDTL FROZ
DEG K	POISE	----- CAL/(CM)(SEC)(K)			---- CAL/(G)(K)	
3387	1527.x10-6	721.x10-6	804.x10-6	1525.x10-6	.6857	.5965
3003	1362.	667.	748.	1391.	.6726	.5769
2493	1060.	529.	503.	1.31.	.6224	.5949
1819	620.	455.	384.	632.	.7029	.5910
1694	576.	416.	332.	746.	.7030	.5602
1426	516.	372.	271.	642.	.7351	.5035
1064	372.	203.	157.	437.	.6908	.5761
854	316.	244.	122.	366.	.6440	.5669
574	214.	172.	67.	24..	.6042	.5366
315	111.	98.	31.	129.	.5705	.4964
202	67.	62.	24.	100.	.5726	.4665
176	56.	53.	13.	66.	.5076	.4305

Table 2-2 (Continued)

Case 2: Same as Case 1 except that a tape for communication with other programs is generated for the frozen composition assumption during expansion (MOCTF=T).

```
REACTANTS
H  2.00                                          1.00     0.0       G298.15  F
O  2.00                                          1.00     0.0       G298.15  O
                    (Insert Blank Card)
NAMELISTS
 $INPT2
      RKT=T,PSIA=T,KASE=00001,P=200.00,OF=T,MIX=6.0,MOCTF=T
 $END
 $TAPGEN
      IREAD=1,IO=8,IN=10
 $END
 CASE 2
 $RKTINP
  PCP=10.,30.,50.,100.,500.,1000.,5000.,50000.,100000.,500000.
 $END
```

The resultant output for Case 2 is identical to that of Case 1 except for a listing of the data placed on tape for communication with other programs. The following is a listing of that data.

Resultant Output for Case 2

Table 2-2 (Cont'd)

Case 3: Required input for creation of thermodynamic data for use with the RAMP program (MOC2P=T); a tape is generated for the equilibrium composition assumption during expansion (MOCT=T). (The effects of heat transfer between the condensed and gaseous species are not determined.)

```
REACTANTS
AL 1.0                                                  16.      0.0       S298.15  F
C 6.884   H 10.089  O .278   N .264                    12.04    -12000.    S298.15  F
FE2.0     O 3.0                                          .4     -197300.   S298.15  F
C 6.15    H  6.97   O 1.17   N .03                      1.96    -28300.    S298.15  F
N 1.0     H  4.0    O 4.0    CL 1.0                    69.60    -70690.    S298.15  F
                    (Insert Blank Card)
OMIT            AL(S)           AL(L)           ALCL3(S)        ALCL3(L)
OMIT            ALN(S)          ALN             AL2CL6          AL2O2
OMIT            CCL3            CCL4            CH              CH2
OMIT            CH3             CH4             COCL2           C2CL2
OMIT            C2H6            C3O2            C4              C5
OMIT            FE(S)           FE(L)           FECL2(S)        FECL2(L)
OMIT            H2O(S)          H2O(L)
NAMELISTS
 $INPT2
      RKT=T,PSIA=T,KASE=0000,P=554.00,MOC2P=T,MOCT=T
 $END
 $TAPGEN
      IREAD=1,IO=8,IN=10
 $END
 CASE 3
 $RKTINP
  PCP=10.,30.,50.,100.,500.,1000.,5000.,50000.,100000.,500000.
 $END
```

Resultant Output for Case 3

```
              .0000        .0000        .0000        .0000    15.0000            .00  S  298.150  F      .0[illegible]
       H   10.0890   O     .2780   N    .2640        .0000    12.0400      -12000.00  S  298.150  F      .0[illegible]
            3.[illegible]000          .0000        .0000        .0000     [illegible]     -197400.00  S  298.150  F      [illegible]
       H    6.9700   O    1.1700   N    .0300        .0000     1.7600      -28300.00  S  298.150  F      [illegible]
       H    4.0000   O    4.0000   CL  1.0000        .0000    69.0000      -70690.00  S  298.150  F      [illegible]
            AL(S)           AL(L)           ALCL3(S)        ALCL3(L)
            AL[illegible](S)          ALN             AL2CL6          AL2[illegible]
            CCL3            CCL4            CF              CH2
            CH3             CH4             C[illegible]            C2CL2
            C2H2            C3O2            C[illegible]              C[illegible]
            FE(S)           FE(L)           FECL2(S)        FECL2(L)
            H2O(S)          H2O(L)

     =      [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   [illegible]E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   [illegible]E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   [illegible]E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   [illegible]E+00,   .0000000000E+00
            .5[illegible]E+03,   .0000000000E+00,   [illegible]E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            .00[illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00

     =
     =
     =
     =      [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            .00[illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            .00[illegible]E+[illegible]
            .554[illegible]E+03,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            .00[illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            .00[illegible]E+00,   .0000000000E+00,   .00[illegible]E-00,   .0000000000E+00,
            .00[illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            [illegible]E+00,   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            .00[illegible]E+[illegible],   .0000000000E+00,   .0000000000E+00,   .0000000000E+00,
            .[illegible]E+00,   .0000000000E+00
     =   F
     =   F
     =   F
     =   F
            [illegible]   [illegible]   [illegible]   .0000000000E+00,
```

Resultant Output for Case 3 (Cont'd)

```
                .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
                .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
                .00000000E+00,   .00000000E+00,   .00000000E+00,
TL        =  F
HR        =  F
SP        =  F
TV        =  F
.         =  F
.         =  F
.         =  T
CK        =  F
.TN       =  F
.TT       =  F
CK        =      .00000000E+00
SC        =      .00000000E+00
SJ        =      .00000000E+00
TPS       =  F
DEBUG     =                 +0
TRACE     =      .00000000E+00
SILNIT    =  F
EXCITS    =  F
TRNSPT    =  T
FROZN     =  F
PUNCH     =  F
NO DATA   =  T
DIF       =  F
NUCE      =  F
NEXT      =  T
NUCTB     =  F
NUCAP     =  T
PARTNT    =  F
QUOTE     =      .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
                .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
                .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
                .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
                .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
                .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
                .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
                .00000000E+00,   .00000000E+00
...       =                 +0

END

... INPT2 VALUE GIVEN FOR DF, EGRAT, FA, OR FPCT
STARGEN
IREAD     =                 +1
IO        =                 +8
IL        =                +10

SEND

SPECIES BEING CONSIDERED IN THIS SYSTEM
    J12/64  AL              J 6/63  ALM             J 6/70  ALCL            J 6/72  ALCL2             J 6/70  ALCL3
    J 4/73  ALO             J 9/64  ALOCL           J12/67  ALOH            J12/66  ALO2             J12/66  ALO3
    J 4/72  AL2O            J 6/72  AL2O3(S)        J 6/72  AL2O3(L)        J 3/81  C(S)            J 3/81  C
    J12/64  CCL             J12/64  CCL2            J 6/72  CCL3            J 6/72  CCL4            J 6/72  CCL5
    J12/72  C2              J 9/72  C               J 2/81  CCL             J 4/73  CN              J12/64  CO
```

Resultant Output for Case 3 (Cont'd)

```
 3/67  C2H          J 3/61  C2H2         J 9/65  C2H4         J 3/67  C2N          J 3/61  C2N2
 9/68  C2O          J12/69  C3           J 6/72  CL           J 6/66  CLCN         J 6/61  CLO
J 3/61  CLO2        J 9/65  CL2          J12/65  CL2O         J 3/65  FE           J 6/65  FECL
J12/70  FECL2       J 6/65  FECL3(S)     J 6/65  FECL3(L)     J 6/65  FECL3        J 6/65  FEO(S)
J 8/65  FEO(L)      J 9/66  FEO          J 6/66  FEO2H2(S)    J12/66  FEO2H2       J 6/66  FEO3H3(S)
J12/70  FE2CL4      J 6/65  FE2O3(S)     J 6/65  FE3O4(S)     J 9/65  H            J 3/64  HALO
J 9/64  HCL         L12/69  HCN          J12/70  HCO          J12/70  HNCO         J 3/63  HNO
J 8/63  HNO2        J 6/63  HNO3         J 3/64  HO2          J 3/61  H2           J 3/61  H2O
L 2/69  H2O2        J 3/61  N            J12/70  NCO          J12/71  NH           J12/65  NH2
J 9/65  NH3         J 6/63  NO           J12/65  NOCL         J 9/64  NO2          J12/65  NO2CL
J12/64  NO3         J 9/65  N2           J12/65  N2H4         J12/64  N2O          J 9/64  N2O4
J12/70  N3          J 6/62  O            J12/70  OH           J 9/65  O2           J 6/61  O3

                    LIST OF CONDENSED SPECIES FROM SEARCH
AL2O3(S)    AL2O3(L)    C(S)        FECL3(S)    FECL3(L)
FEO(S)      FEO(L)      FEO2H2(S)   FEO3H3(S)   FE2O3(S)
FE3O4(S)
$NITRP
FUEL     =  T
PRIZ     =  T
SUMAR    =     .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
               .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
               .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
               .00000000E+00
SUMAR    =     .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
               .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
               .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
               .00000000E+00
FCF      =     .10000000E+02,  .30000000E+02,  .50000000E+02,  .10000000E+03,
               .50000000E+03,  .10000000E+04,  .50000000E+04,  .50000000E+05,
               .10000000E+06,  .50000000E+06,  .00000000E+00,  .00000000E+00,
               .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
               .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
               .00000000E+00,  .00000000E+00
OFZ      =                +1

$END

OF =     .000000
                          EFFECTIVE FUEL          EFFECTIVE OXIDANT          MIXTURE
ENTHALPY                     HPP(2)                   HPP(1)                  HSUBO
(KG-MOLE)(DEG K)/KG       -.22321037+03             .00000000              -.22321037+03

KG-ATOMS/KG                  BOP(1,2)                 BOP(1,1)                 BO(I)
      AL                   .59299890-02             .00000000              .59299890-02
      C                    .94112869-02             .00000000              .94112869-02
      H                    .37088374-01             .00000000              .37088374-01
      O                    .24331565-01             .00000000              .24331565-01
      N                    .62445374-02             .00000000              .62445374-02
      FE                   .50096372-04             .00000000              .50096372-04
      CL                   .59239498-02             .00000000              .59239498-02

      AL        C         H         O         N        FE        CL
  -13.240  -11.960   -9.063  -13.274  -13.305  -11.197  -21.957   12.000
  -17.498  -13.395   -9.465  -17.699  -13.615  -15.216  -20.292    0.000
```

Resultant Output for Case 3 (Cont'd)

THE VERTICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

P = 554.7 PSIA
CASE NO. 1

	CHEMICAL FORMULA								WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL	AL 1.00000								.16000	.000	S	298.15	.0000
FUEL	C 4.88400	H	10.08900	O	.27800	N	.26400		.12000	-12000.000	S	298.15	.0000
FUEL	FE 2.00000	O	3.00000						.00900	-197300.000	S	298.15	.0000
FUEL	C 4.15000	H	6.97000	O	1.17000	N	.03000		.01900	-28300.000	S	298.15	.0000
FUEL	N 1.00000	H	4.00000	O	4.00000	CL	1.00000		.69000	-75670.000	S	298.15	.0000

O/F= .0000 PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 1.6977 REACTANT DENSITY= .0000

	CHAMBER	THROAT	EXIT
PC/P	1.0000		
P, ATM	37.697		
T, DEG K	3391		
RHO, G/CC	3.534E-3		
H, CAL/G	-443.6		
S, CAL/(G)(K)	2.3005		
M, MOL WT	28.309		
MOLE/GM PRT	-1.01875		
GAMMA/(GAMMA-1)	1.3331		
CP, CAL/(G)(K)	.8697		
GAMMA (S)	1.1383		
V, METERS/SEC	1064.8		

MOLE FRACTIONS

AL	.00010
ALH	.00001
ALCL	.00406
ALCL2	.00140
ALCL3	.00012
AR	.00011
ALOCL	.00152
ALOH	.00037
ALO2	.00003
ALO2H	.00042
ALO	.00001
AL2O3(L)	.07356
CO	.23061
HCL	.00001
CO2	.01614
[illegible]	.01264
[illegible]	.00001
[illegible]	[illegible]
[illegible]	[illegible]

Resultant Output for Case 3 (Cont'd)

FECL	.00005
FECL2	.00072
FE	.00034
FE(OH)2	.00002
H	.03611
HCL	.13260
HCO	.00002
H2	.25637
H2O	.14065
N	.00001
N2	.00001
NH3	.00001
NO	.00067
N2	.08152
C	.00073
OH	.00867
O2	.00016

MASS OF ELEMENTS BEING REMOVED FOR TWO PHASE CALCULATION (KG OF SPECIE/KG OF MIXTURE)

AL	.15136+00	.15136+00
C	.00000	.15136+00
H	.00000	.15136+00
O	.13465+00	.28603+00
N	.00000	.28603+00
FE	.00000	.28603+00
CL	.00000	.28603+00

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .50000-05 FOR ALL ASSIGNED CONDITIONS

AL2O3(S)	C(S)	C	CCL	CCL2	CH2O	CN	CNN	CN2	C2
C2H	C2H2	C2H4	C2N	C2H2	C2O	C3	CLCN	CLO2	CL2O
FECL3(S)	FECL3(L)	FECL3	FEO(S)	FEO(L)	FEO2H2(S)	FEO3H3(S)	FE2CL4	FE2O3(S)	FE3H4(S)
HALO	HCN	H2O	H2O	HNO2	HNO3	HO2	H2O2	NCO	[illegible]
[illegible]	NO2	NO2CL	NO3	N2H4	N2O	N2O4	N3	O3	

[illegible] WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

ADJUSTED VALUE OF HSUBO = .21937+03 (KG-MOL)(DEG K)/KG

[illegible] TOTAL MASS VALUES AFTER TWO PHASE CORRECTION

AL	[illegible]+03
C	[illegible]+01

Resultant Output for Case 3 (Cont'd)

```
H          .5194669-01
O          .2229166-01
N          .6746253-02
FE         .7016621-04
CL         .8297230-02

AL2O3(S)   HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

AL2O3(L)   HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

C(S)       HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FECL3(S)   HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FECL3(L)   HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FEO(S)     HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FEO(L)     HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FEO2H2(S)  HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FEO3H3(S)  HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FE2O3(S)   HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FE3O4(S)   HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS
ADJUSTED LIST OF SPECIES TO BE CONSIDERED IN TWO PHASE SYSTEM
```

AL	ALH	ALCL	ALCL2	ALCL3
ALO	ALOCL	ALOH	ALO2	ALO2H
AL2O	C	CCL	CCL2	CH2O
CN	CNN	CN2	CO	COCL
CO2	C2	C2H	C2H2	C2H4
C2N	C2N2	C2O	C3	CL
CLCN	CLO	CLO2	CL2	CL2O
FE	FECL	FECL2	FECL3	FEO
FEO2H2	FE2CL4	H	HALO	HCL
HCN	HCO	HNCO	HNO	HNO2
HNO3	HO2	H2	H2O	H2O2
N	NCO	NH	NH2	NH3
NO	NOCL	NO2	NO2CL	NO3
N2	N2H4	N2O	N2O4	N3
O	OH	O2	O3	

```
NT      AL        C         H         O         N         FE        CL
 1  -17.488   -13.390   -9.465   -17.899   -13.815   -15.216   -20.292   12.000

NT      AL        C         H         O         N         FE        CL
 1  -17.488   -13.390   -9.465   -17.899   -13.815   -15.216   -20.292   12.000
 2  -17.528   -13.424   -9.599   -18.444   -13.947   -14.668   -20.666    4.000
P(/PT= 1.759304    T =   3141.91
 2  -17.528   -13.424   -9.599   -18.446   -13.948   -14.666   -20.667    2.000
P(/PT= 1.763161    T =   3140.96
 3  -17.68[illegible]  -12.9[illegible]  -9.966   -20.974   -14.357   -17.950   -22.117    4.000
 4  -18.[illegible]  -12.[illegible]  -10.166   -23.476   -14.5[illegible]  -1[illegible]  -23.[illegible]  5.000
    -19.[illegible]  -11.[illegible]  -10.261   -24.960   -14.597   -11.0[illegible]  -21.116    4.00[illegible]
```

Resultant Output for Case 3 (Cont'd)

6	-21.406	-10.502	-10.381	-27.388	-14.717	-10.135	-25.220	4.000
7	-29.265	-6.980	-10.664	-35.203	-15.022	-7.661	-28.541	4.000
8	-33.709	-4.995	-10.802	-39.505	-15.180	-6.507	-30.313	4.000
9	-44.524	.788	-11.187	-51.778	-15.626	-3.956	-35.218	5.000
10	-69.401	11.113	-11.985	-73.344	-16.451	-3.945	-43.520	9.000
11	-73.702	12.186	-12.299	-77.133	-16.754	-4.016	-45.216	5.000
12	-88.629	14.662	-13.034	-89.118	-17.461	-4.682	-50.640	5.000

Resultant Output for Case 3 (Cont'd)

```
        THEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION FOR TWO PHASE MOC CALCULATIONS

PC =    554.0 PSIA
CASE NO.      1
                                                                           WT FRACTION   ENERGY     STATE    TEMP     DENSITY
       CHEMICAL FORMULA                                                    (SEE NOTE)    CAL/MOL             DEG K    G/CC
FUEL   AL 1.00000                                                            .16000          .000     S      298.15   [illegible]
FUEL   C  6.88400   H 10.08900   O   .27800   N   .26400                     .12540   -12990.000      S      298.15   [illegible]
FUEL   FE 2.00000   O  3.00000                                               .00400  -197300.000      S      298.15   [illegible]
FUEL   C  6.15000   H  6.97000   O  1.17000   N   .03000                     .01760   -28300.000      S      298.15   [illegible]
FUEL   N  1.00000   H  4.00000   O  4.00000   CL 1.00000                     .69600   -70690.000      S      298.15   [illegible]

          O/F=    .0000     PERCENT FUEL=100.0000     EQUIVALENCE RATIO=  1.6977     REACTANT DENSITY=    .0000

                     CHAMBER    THROAT     EXIT       EXIT       EXIT       EXIT       EXIT       EXIT       EXIT       EXIT       EXIT       EXIT
PC/P                 1.0000     1.7632     10.000     30.000     50.000     100.00     500.00     1000.00    5000.00    50000.0    100000.0   50[illegible]
P, ATM               37.697     21.381     3.7697     1.2566     .7539      .3770      .0754      .0377      .0075      .0008      .0004      .00[illegible]
T, DEG K             3391       3141       2392       1954       1771       1537       1089       943        687        470        444        373
RHO, G/CC            2.7379-3   1.6949-3   4.0075-4   1.6455-4   1.0917-4   6.2963-5   1.7776-5   1.0272-5   2.8206-6   4.1999-7   2.2630-7   5.5653-8
H, CAL/G             435.9      254.8      -206.5     -432.6     -522.5     -630.6     -827.9     -894.2     -1016.5    -1137.4    -1166.4    -1225.5
S, CAL/(G)(K)        2.8416     2.8416     2.8416     2.8416     2.8416     2.8416     2.8416     2.8416     2.8416     2.8416     2.8416     2.8416

M, MOL WT            20.208     20.431     20.863     20.997     21.042     21.068     21.073     21.073     21.079     21.491     21.867     22.5[illegible]
(DLV/DLP)T           -1.01730   -1.01197   -1.00280   -1.00167   -1.00087   -1.00015   -1.00000   -1.00000   -1.00013   -1.02296   -1.02153   -1.0[illegible]
(DLV/DLT)P           1.2902     1.2133     1.0556     1.0351     1.0204     1.0042     1.0000     1.0001     1.0032     1.5614     1.5495     1.[illegible]
CP, CAL/(G)(K)       .7641      .6497      .5682      .5186      .4084      .4471      .4455      .4599      .4962      1.6848     1.6835     .62[illegible]
GAMMA (S)            1.1799     1.1856     1.2255     1.2404     1.2507     1.2684     1.2685     1.2580     1.2362     1.1247     1.1212     1.21[illegible]7
SON VEL, M/SEC       1283.0     1231.0     1060.6     979.7      935.5      877.1      738.3      684.0      576.6      452.3      434.9      407.7
MACH NUMBER          .000       1.000      2.145      2.752      3.027      3.406      4.405      4.878      6.025      8.022      8.419      9.147

AE/AT                           1.0000     2.2454     4.7030     6.7463     11.069     36.087     60.883     212.18     1369.11    2516.98    10054.3
CSTAR, FT/SEC                   6006       6006       6006       6006       6006       6006       6006       6006       6006       6006       60[illegible]6
CF                              .672       1.267      1.473      1.547      1.632      1.776      1.822      1.904      1.982      2.000      2.037
IVAC, LB-SEC/LB                 231.4      278.4      304.2      314.0      325.3      345.1      351.6      363.4      375.1      378.1      384.[illegible]
ISP, LB-SEC/LB                  125.5      236.4      274.9      286.6      304.6      331.6      340.2      355.5      370.0      373.4      385.2

MOLE FRACTIONS

AL                   .00011     .00006     .00000     .00000     .00000     .00000     .00000     .00000     .00000     .00000     .00000     .[illegible]
ALH                  .00002     .00001     .00000     .00000     .00000     .00000     .00000     .00000     .00000     .00000     .00000     .[illegible]
ALCL                 .02434     .00429     .00302     .00100     .00032     .00003     .00000     .00000     .00000     .00000     .00000     .[illegible]
ALCL2                .[illegible]151     .00168     .00266     .00234     .00135     .00032     .00000     .00000     .00000     .00000     .00000     .[illegible]
ALCL3                .[illegible]     .00019     .00123     .00563     .00737     .00903     .00942     .00943     .00943     .00961     .00976     .[illegible]
[illegible]          .[illegible]12     .00006     .00000     .00000     .00000     .00000     .00000     .00000     .00000     .00000     .00000     .[illegible]
[illegible]          .[illegible]     .00178     .0015[illegible]     .00065     .00033     .00004     .00000     .00000     .00000     .00000     .00000     .[illegible]
[illegible]          .[illegible]     .00037     .0001[illegible]     .00005     .00001     .00000     .00000     .00000     .00000     .00000     .00000     .[illegible]
[illegible]          .[illegible]     .[illegible]2     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .00000     .00000     .[illegible]
[illegible]          .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]
[illegible]          .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]
[illegible]          .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]     .[illegible]
```

Resultant Output for Case 3 (Cont'd)

[illegible]CL	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
C2	.01742	.01872	.02373	.02745	.03335	.04071	.07161	.09716	.14702	.20294	.21692	.24618
C2H4	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00634	.01228	.02376
CL	.01343	.00984	.00158	.00021	.00006	.00001	.00000	.00000	.00000	.00000	.00000	.00000
CL[illegible]	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
CL2	.00002	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FE	.00053	.00040	.00004	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FECL	.00005	.00004	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FECL2	.00078	.00095	.00191	.00147	.00148	.00148	.00148	.00147	.00100	.00001	.00001	.00000
FEC	.00004	.00003	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FEC2H2	.00002	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FEC2CL4	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00024	.00075	.00076	.00079
H	.03894	.02730	.00428	.00054	.00018	.00002	.00000	.00000	.00000	.00000	.00000	.00000
[illegible]	.14313	.14788	.15483	.14945	.14612	.14403	.14362	.14361	.14365	.14646	.14902	.15398
[illegible]	.00004	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
H2	.27673	.28240	.29874	.30959	.31542	.32400	.35537	.37572	.43644	.46672	.46396	.45497
[illegible]	.15182	.15731	.16308	.16066	.15793	.15118	.12017	.09902	.04501	.00561	.00485	.00719
[illegible]	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
[illegible]	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
NH3	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00001	.00005	.00005	.00012
NO	.00072	.00037	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
N2	.08600	.09915	.09123	.09182	.09202	.09213	.09216	.09216	.09218	.09396	.09560	.09875
O	.00079	.00033	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
OH	.00936	.00564	.00042	.00003	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000
O2	.00017	.00007	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .50000-05 FOR ALL ASSIGNED CONDITIONS

C	CCL	CCL2	CH2O	CN	CNN	CN2	C2	C2H	C2H2
C2N	C2N2	C2O	C3	CLCN	CLO2	CL2O	FECL3	HALO	HCN
HCO	HNO	HNO2	HNO3	HO2	H2O2	NCO	NH	NOCL	NO2
[illegible]	NO3	N2H4	N2O	N2O4	N3	O3			

NOTE: WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

Resultant Output for Case 3 (Cont'd)

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

O/F= .0000 PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 1.6977 CHAMBER PRESSURE= 37.697 ATM

TEMP	VISCOSITY	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	C_P FROZ	C_P EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
DEG K	POISE	CAL/(CM)(SEC)(K)					CAL/(G)(K)		DIMENSIONLESS		
[illegible]	931.X10-6	489.X10-6	434.X10-6	923.X10-6	1889.X10-6	2812.X10-6	.4765	.9560	.4802	.3163	2.0328
[illegible]	881.	450.	406.	856.	1923.	2260.	.4723	.8437	.4859	.3260	2.1145
[illegible]	723.	352.	312.	664.	309.	973.	.4553	.5670	.4960	.4216	1.8954
[illegible]	476.	305.	252.	558.	84.	642.	.4415	.5177	.4959	.5053	.8732
1771	584.	287.	227.	514.	44.	558.	.4346	.4862	.4943	.5113	.6970
1537	524.	262.	193.	456.	17.	473.	.4244	.4490	.4920	.5019	.6399
1089	413.	213.	131.	344.	25.	369.	.4013	.4455	.4819	.4980	.6726
543	372.	197.	113.	310.	35.	345.	.3935	.4599	.4728	.4957	.6788
487	295.	167.	87.	254.	49.	303.	.3815	.4962	.4432	.4840	.6356
470	220.	131.	64.	195.	378.	572.	.3669	1.6848	.4155	.6489	.5401
[illegible]	210.	124.	60.	184.	385.	569.	.3622	1.6835	.4124	.6207	.5725
[illegible]	180.	105.	50.	155.	71.	225.	.3485	.6206	.4049	.4949	.5851

Resultant Output for Case 3 (Cont'd)

37.7	.0	.0	.0	.0	.0	.0
AL	ALH	ALCL	ALCL	ALCL	ALO	ALOC
ALOH	ALO2	ALO2	AL2O	CU	COCL	CO2
C2H4	CL	CLO	CL2	FE	FECL	FECL
FEO	FEO2	FE2C	H	HCL	HCO	H2
H2O	N	NH2	NH3	NO	N2	O
OH	O2					
.0	.0	.0	.0	.0	.0	.0
			2	3		L
		H				
						2
	H2	L4				

.4359247+03	.3769732+02	.3390819+04	.2841598+01	.2020825+02	.1179931+01	.0000000
.3163401+00	.9305036-03	.9560249+00	.2812115-02	.4366309+03	.4359248+03	
.1132173-03	.1507067-04	.4379596-02	.1507849-02	.1333928-03	.1187501-03	.1645857-02
.4039977-03	.3112202-04	.6672308-03	.1156668-04	.2489219+00	.9362504-05	.1742090-01
.0000000	.1342891-01	.8596271-05	.2276880-04	.5295636-03	.5376999-04	.7756356-03
.4156609-04	.1687344-04	.0000000	.3698058-01	.1431325+00	.1980204-04	.2767278+00
.1512157+00	.6230679-05	.1003542-04	.8944617-05	.7181847-03	.8799679-01	.7867242-03
.9355125-02	.1720760-03					
.4359247+03	.2136053+02	.3140957+04	.2841598+01	.2043003+02	.1185590+01	.9999910+00
.3259434+00	.8807139-03	.8436730+00	.2279505-02	.2558245+03	.4359248+03	
.6433016-04	.7911510-05	.4493953-02	.1062665-02	.1925566-03	.6466427-04	.1780386-02
.3672676-03	.1789324-04	.6473545-03	.1005036-04	.2505720+00	.4775126-05	.1872234-01
.0000000	.9643804-02	.3314562-05	.1381009-04	.4011297-03	.3900843-04	.9529531-03
.2596958-04	.1402744-04	.0000000	.2729937-01	.1478759+00	.9815456-05	.2823964+00
.1573068+00	.2130557-05	.4938457-05	.6056653-05	.3701068-03	.8915276-01	.3334942-03
.5647358-02	.7476523-04					
.4359247+03	.3769732+01	.2391724+04	.2841598+01	.2086339+02	.1225498+01	.2145372+01
.4216392+00	.7234367-03	.5669603+00	.9727770-03	-.2065394+03	.4359248+03	
.3327863-05	.4170076-06	.3016670-02	.2676543-02	.1231439-02	.2793990-05	.1800881-02
.1863053-03	.8735849-06	.4042951-03	.3451460-05	.2512822+00	.3487737-06	.2373073-01
.0000000	.1581908-02	.3320406-07	.1427471-05	.4411977-04	.4502560-05	.1409896-02
.1168446-05	.3673287-05	.0000000	.4262138-02	.1546307+00	.6745071-06	.2987367+00
.1608855+00	.1586114-07	.3230540-06	.2203549-05	.1428510-04	.9122957-01	.4120498-05
.4215771-03	.9446268-06					
.4359247+03	.1256577+01	.1954051+04	.2841598+01	.2099746+02	.1240437+01	.2751845+01
.5653146+00	.6262552-03	.5177159+00	.6416247-03	-.4326721+03	.4359248+03	
.8201462-07	.1299154-07	.1001670-02	.2341220-02	.5030172-02	.5698880-07	.8454597-03
.4476964-04	.1906093-07	.1250767-03	.3015500-06	.2473266+00	.3410233-07	.2945263-01
.0000000	.2105451-03	.0000000	.1486300-06	.2626275-05	.3346853-06	.1469125-02
.2574562-07	.9247256-06	.0000000	.5627758-03	.1494502+00	.6996303-07	.3095920+00
.1614694+00	.0000000	.4167069-07	.1441550-05	.4986179-06	.9182347-01	.3865033-07
.2773610-04	.0000000					
.4359247+03	.7539963+00	.1770467+04	.2841598+01	.2104202+02	.1250728+01	.3027195+01
.5232286+03	.5882874-03	.4861955+00	.5576625-03	-.5225386+03	.4359248+03	
.0000000	.0000000	.3152707-03	.1346570-02	.7374045-02	.0000000	.3254811-03
.[illegible]-04	.0000000	.3791392-04	.2616569-07	.2444227+00	.1056706-07	.3334641-01
[illegible]	.0[illegible]-04	.0000000	.4133326-07	.4657910-06	.7074326-07	.1475243-02
[illegible]	.4[illegible]-06	.1195370-07	.1749900-03	.1461190+00	.2050243-07	.3154241+00

Resultant Output for Case 3 (Cont'd)

.1579295+00	.0000000	.0000000	.1269936-05	.7063415-07	.9201868-01	.0000000
.5430638-05	.0000000					
.4359247+03	.3769732+00	.1538754+01	.2841598+01	.2106825+02	.1264444+01	.3406137+01
.5018912+00	.5261424-03	.4476[illegible]+00	.4725366-03	-.6306132+03	.4359248+03	
.0000000	.0000000	.4570[illegible]-04	.3429520-03	.9039011-02	.0000000	.3713637-04
.8271668-06	.0000000	.2632328-05	.0000000	.2370037+00	.0000000	.4071111-01
.0000000	.8625673-05	.0000000	.0000000	.2276020-07	.0000000	.1477922-02
.0000000	.1008712-06	.2517976-07	.2499550-04	.1446307+00	.0000000	.3240030+00
.1511102+00	.0000000	.0000000	.1161820-05	.0000000	.9213347-01	.0000000
.3659424-06	.0000000					
.4359247+03	.2539464-01	.1691197+04	.2841598+01	.2197352+02	.1266522+01	.4404794+01
.4962457+00	.4130492-03	.4534695+00	.3694617-03	-.8279437+03	.4359248+03	
.0000000	.0000000	.0000000	.1440776-05	.9424992-02	.0000000	.1180151-07
.0000000	.0000000	.0000000	.0000000	.2057731+00	.0000000	.7181003-01
.0000000	.1591419-07	.0000000	.0000000	.0000000	.0000000	.1477579-02
.0000000	.0000000	.4667664-06	.4563272-07	.1436157+00	.0000000	.3553664+00
.1401745+00	.0000000	.0000000	.1693874-05	.0000000	.9215589-01	.0000000
.0000000	.0000000					
.4359247+03	.3769732-01	.9426276+03	.2841598+01	.2107350+02	.1257964+01	.4877867+01
.4957344+00	.3721051-03	.4594975+00	.3451780-03	-.8942021+03	.4359248+03	
.0000000	.0000000	.0000000	.7020767-07	.9426430-02	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.1856253+00	.0000000	.9215887-01
.0000000	.0000000	.0000000	.0000000	.0000000	.0000000	.1473103-02
.0000000	.0000000	.2699663-05	.0000000	.1436149+00	.0000000	.3757156+00
.9242151-01	.0000000	.0000000	.2303133-05	.0000000	.9215590-01	.0000000
.0000000	.0000000					
.4359247+03	.7539463-02	.6866498+03	.2841598+01	.2107861+02	.1236233+01	.6024976+01
.4939334+00	.2950400-03	.4961691+00	.3025158-03	-.1016549+04	.4359248+03	
.0000000	.0000000	.0000000	.0000000	.9420008-02	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.1305335+00	.0000000	.1470181+00
.0000000	.0000000	.0000000	.0000000	.0000000	.0000000	.9970115-03
.0000000	.0000000	.2409640-03	.0000000	.1436496+00	.0000000	.4306365+00
.4611196-01	.0000000	.0000000	.7234770-05	.0000000	.9217577-01	.0000000
.0000000	.0000000					
.4359247+03	.7539463-03	.4701619+03	.2841598+01	.2159107+02	.1124659+01	.8022327+01
.6467061+00	.2204009-03	.1664817+01	.5722468-03	-.1137387+04	.4359248+03	
.0000000	.0000000	.0000000	.0000000	.9613277-02	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.6764866-01	.0000000	.2029571+00
.5541365-02	.0000000	.0000000	.0000000	.0000000	.0000000	.1495355+04
.0000000	.0000000	.7469476-03	.0000000	.1464606+00	.0000000	.4666955+00
.5513141-02	.0000000	.0000000	.4970353-04	.0000000	.9395832-01	.0000000
.0000000	.0000000					
.4359247+03	.3769732-03	.4437693+03	.2841598+01	.2186660+02	.1121163+01	.8418898+01
.6204756+00	.2096421-03	.1663584+01	.5686409-03	-.1166417+04	.4359248+03	
.0000000	.0000000	.0000000	.0000000	.9781362-02	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.4476555-01	.0000000	.2189200+00
.1277745-01	.0000000	.0000000	.0000000	.0000000	.0000000	.6950650-05
.0000000	.0000000	.7636803-03	.0000000	.1490212+00	.0000000	.4639642+00
.4846624-02	.0000000	.0000000	.5245236-04	.0000000	.9560003-01	.0000000
.0000000	.0000000					
.4359247+03	.7539464-04	.3730417+03	.2841598+01	.2259505+02	.1210653+01	.9146675+01
.4944671+00	.1798081+03	.6206307+00	.2254947-03	-.1225552+04	.4359248+03	
[illegible]	.0000000	[illegible]	[illegible]	.1010710-01	.0000000	.0000000
[illegible]	.0000000	[illegible]	[illegible]	.4133927-02	.0000000	.2461753+00
[illegible]	[illegible]	[illegible]	[illegible]	[illegible]	.0000000	[illegible]
[illegible]	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]
.7[illegible]-02	.0000000	.0000000	.1229451-02	.0000000	.9[illegible]-01	[illegible]
[illegible]	.0000000					

Table 2-2 (Continued)

Case 4: Same as Case 3 except that the effects of heat transfer between the condensed and gaseous species are determined (PARTHT=T).

```
REACTANTS
AL 1.0                                                  16.      0.0       S298.15  F
C 6.884   H 10.089 O .278   N .264                      12.04    -12000.   S298.15  F
FE2.0     O 3.0                                          .4     -197300.  S298.15  F
C 6.15    H  6.97  O 1.17   N .03                        1.96   -28300.   S298.15  F
N 1.0     H  4.0   O 4.0    CL 1.0                      69.60   -70690.   S298.15  F
                    (Insert Blank Card)
OMIT            AL(S)           AL(L)           ALCL3(S)        ALCL3(L)
OMIT            ALN(S)          ALN             AL2CL6          AL2O2
OMIT            CCL3            CCL4            CH              CH2
OMIT            CH3             CH4             COCL2           C2CL2
OMIT            C2H6            C3O2            C4              C5
OMIT            FE(S)           FE(L)           FECL2(S)        FECL2(L)
OMIT            H2O(S)          H2O(L)
NAMELISTS
 $INPT2
      RKT=T,PSIA=T,KASE=00001,P=554.00,MOC2P=T,MOCT=T,PARTHT=T,
      OOOTP=-600.0,-300.0,0.0,100.0,NQ1=4
 $END
 $TAPGEN
      IREAD=1,ID=8,IN=10
 $END
 OOOTP TEST CASE
 $RKTINP
  PCP=10.,30.,50.,100.,500.,1000.,5000.,50000.,100000.,500000.
 $END
```

Resultant Output for Case 4

```
    START2
.    1.0000         .0000         .0000         .0000        .0000   16.0000             .00  S  298.150  F    .00000
     6.9840  H   10.0890  O    .2780  N     .2690        .0000   12.0400       -12000.00  S  298.150  F    .00000
     2.0000  O    3.0000        .0000        .0000        .0000     .4000     -197300.00  S  298.150  F    .00000
C    6.1500  H    6.9700  O   1.1700  N     .0320        .0000    1.9600      -28300.00  S  298.150  F    .00000
N    1.0000  H    4.0000  O   4.0000  CL  1.0000        .0000   69.6000      -70690.00  S  298.150  F    .00000
OMIT             AL(S)           AL(L)           ALCL3(S)        ALCL3(L)
OMIT             ALN(S)          ALN             AL2CL6          AL2O2
OMIT             CCL3            CCL4            CH              CH2
OMIT             CH3             CH4             COCL2           C2CL2
OMIT             C2H6            C3O2            C4              C5
OMIT             FE(S)           FE(L)           FECL2(S)        FECL2(L)
OMIT             H2O(S)          H2O(L)
NAMELISTS
SINPT2
KASE    =          +1
T       =    .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
P       =    .55400000E+03,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00
PSIA    =  T
HPHS    =  F
NSGM    =  F
V       =    .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00
RHO     =    .55400000E+03,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
             .00000000E+00,  .00000000E+00
RATIO   =  F
        =  F
I       =  F
        =  F
        =    .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
```

Resultant Output for Case 4 (Cont'd)

```
                .[illegible]E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
                .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
                .00000000E+09,   .00000000E+09,   .00000000E+00
TP        =  F
[illegible]  =  F
[illegible]  =  F
[illegible]  =  F
[illegible]  =  F
[illegible]  =  F
HAT       =  T
SHOCK     =  F
DETN      =  F
DTTO      =  F
CR        =     .00000000E+00
SO        =     .00000000E+00
SO        =     .00000000E+00
IONS      =  F
IDEBUG    =                +0
TRACE     =     .00000000E+00
SIUNIT    =  F
FUNITS    =  F
TRNSPT    =  T
FROZN     =  F
PUNCH     =  F
NOLATA    =  T
DIF       =  F
[illegible]  =  F
[illegible]  =  T
HOCTP     =  F
HOC2P     =  T
PARTHT    =  T
COCTP     =    -.60000000E+03,  -.30000000E+03,   .00000000E+00,   .10000000E+03,
               .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
               .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
               .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
               .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
               .00000000E+00,   .00000000E+00,   .00000000E+00,   .00000000E+00,
               .00000000E+00,   .00000000E+00
NOI       =                +4

SEND

NO INPT2 VALUE GIVEN FOR OF, EQRAT, FA, OR FPCT

STARGEN
IREAD     =                +1
IO        =                +8
IN        =               +10

SEND

SPECIES BEING CONSIDERED IN THIS SYSTEM
    J12/65  AL          J 6/63  ALH         J 6/70  ALCL        J 6/72  ALCL2       J 6/70  ALCL3
    J 6/70  ALO         J 9/64  ALOCL       J12/67  ALOH        J12/68  ALO2        J12/68  ALO2H
    J 6/72  AL2O        J 6/72  AL2O3(S)    J 6/72  AL2O3(L)    J 3/61  C(S)        J 3/61  C
    J[illegible]/69  CCL        J12/68  CCL2        J 3/61  CH2O        J 6/69  CN          J 6/66  CNN
    J[illegible] 70  CN2        J 9/65  CO          J12/65  COCL       J 9/65  CO2         J12/69  C2
```

Resultant Output for Case 4 (Cont'd)

```
J 3/67  C2H          J 3/61  C2H2         J 9/65  C2H4         J 3/67  C2N          J 3/61  C2N2
J 9/61  C2O          J12/69  C3           J 6/62  CL           J 6/66  CLCN         J 3/61  CLO
J 3/61  CLO2         J 9/65  CL2          J12/65  CL2O         J 3/65  FE           J 6/65  FECL
J12/70  FECL2        J 6/65  FECL3(S)     J 6/65  FECL3(L)     J 6/65  FECL3        J 6/65  FECL4
J 6/65  FEO(L)       J 9/66  FEO          J 6/66  FEO2H2(S)    J12/66  FEO2H2       J 6/66  FE(OH)3(S)
J12/70  FE2CL4       J 6/65  FE2O3(S)     J 6/65  FE3O4(S)     J 9/65  H            J 3/64  H2
J 9/64  HCL          L12/69  HCN          J12/70  HCO          J12/70  HNCO         J 3/63  HNO
J 6/63  HNO2         J 6/63  HNO3         J 3/64  HO2          J 3/61  H2           J 3/61  H2O
L 2/69  H2O2         J 3/61  N            J12/70  NCO          J12/71  NH           J12/65  NO
J 9/65  NH3          J 6/63  NO           J12/65  NOCL         J 9/64  NO2          J12/65  NO2CL
J12/64  NO3          J 9/65  N2           J12/65  N2H4         J12/64  N2O          J 9/64  N2O4
J12/70  N3           J 6/62  O            J12/70  OH           J 9/65  O2           J 6/61  O3
```

LIST OF CONDENSED SPECIES FROM SEARCH

```
AL2O3(S)    AL2O3(L)    C(S)        FECL3(S)    FECL3(L)
FEO(S)      FEO(L)      FEO2H2(S)   FEO3H3(S)   FE2O3(S)
FE3O4(S)
```

```
SOLVE
T1      =  T
P1      =  T
S1      =  .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
           .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
           .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
           .00000000E+00
S1F1    =  .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
           .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
           .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
           .00000000E+00
P1      =  .10000000E+02,  .30000000E+02,  .50000000E+02,  .10000000E+03,
           .50000000E+03,  .10000000E+04,  .50000000E+04,  .50000000E+05,
           .10000000E+06,  .50000000E+06,  .00000000E+00,  .00000000E+00,
           .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
           .00000000E+00,  .00000000E+00,  .00000000E+00,  .00000000E+00,
           .00000000E+00,  .00000000E+00
PFZ     =                  +1

SEND
```

```
OF =    .000000
```

	EFFECTIVE FUEL HPP(2)	EFFECTIVE OXIDANT HPP(1)	MIXTURE HSUBO
ENTHALPY (KG-MOL)(DEG K)/KG	-.22321037+03	.00000000	-.22321037+03

KG-ATOMS/KG	BOP(I,2)	BOP(I,1)	BO(I)
AL	.59299890-02	.00000000	.59299890-02
C	.94112869-02	.00000000	.94112869-02
H	.37088374-01	.00000000	.37088374-01
O	.24331585-01	.00000000	.24331585-01
N	.62445374-02	.00000000	.62445374-02
FE	.50096372-04	.00000000	.50096372-04
CL	.59239498-02	.00000000	.59239498-02

BT	AL	C	H	O	N	FE	CL	
I	-13.240	-11.960	-9.063	-19.674	-13.305	-11.197	-21.957	12.000
J	-17.488	-13.390	-9.465	-17.899	-13.815	-15.214	-20.292	8.000

Resultant Output for Case 4 (Cont'd)

THEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

PC = 554.0 PSIA

CASE NO. 1

	CHEMICAL FORMULA									WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL	AL	1.00000								.16000	.000	S	298.15	.0000
FUEL	C	6.88400	H	10.08900	O	.27800	N	.26400		.12040	-12000.000	S	298.15	.0000
FUEL	FE	2.00000	O	3.00000						.00400	-197300.000	S	298.15	.0000
FUEL	C	6.15000	H	6.97000	O	1.17000	N	.03000		.01960	-28300.000	S	298.15	.0000
FUEL	N	1.00000	H	4.00000	O	4.00000	CL	1.00000		.69600	-70690.000	S	298.15	.0000

O/F= .0000 PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 1.6977 REACTANT DENSITY= .0000

	CHAMBER	THROAT	EXIT
PC/P	1.0000		
P, ATM	37.697		
T, DEG K	3391		
RHO, G/CC	3.8348-3		
H, CAL/G	-443.6		
S, CAL/(G)(K)	2.3005		
M, MOL WT	28.334		
(DLV/DLP)T	-1.01875		
(DLV/DLT)P	1.3331		
CP, CAL/(G)(K)	.8897		
GAMMA (S)	1.1383		
SOUND VEL,M/SEC	1064.8		

MOLE FRACTIONS

AL	.00010
ALH	.00001
ALCL	.00406
ALCL2	.00140
ALCL3	.00012
ALO	.00011
ALOCL	.00152
ALOH	.00037
ALO2	.00003
ALO2H	.00062
AL2O	.00001
AL2O3(L)	.07356
CO	.23061
COCL	.00001
CO2	.01614
CL	.01244
CLO	.00001
CL2	.00002
FE	.00049

Resultant Output for Case 4 (Cont'd)

FECL	.00005
FECL2	.00072
FEO	.00004
FEO2H2	.00002
H	.03611
HCL	.13260
HCO	.00002
H2	.25637
H2O	.14066
N	.00001
NH2	.00001
NH3	.00001
NO	.00067
N2	.08152
O	.00073
OH	.00867
O2	.00016

MASS OF ELEMENTS BEING REMOVED FOR TWO PHASE CALCULATION (KG OF SPECIE/KG OF MIXTURE)

AL	.15138+00	.15138+00
C	.00000	.15138+00
H	.00000	.15138+00
O	.13465+00	.28603+00
N	.00000	.28603+00
FE	.00000	.28603+00
CL	.00000	.28603+00

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .50000-05 FOR ALL ASSIGNED CONDITIONS

AL2O3(S)	C(S)	C	CCL	CCL2	CH2O	CN	CNN	CN2	C2
C2H	C2H2	C2H4	C2N	C2N2	C2O	C3	CLCN	CLO2	CL2O
FECL3(S)	FECL3(L)	FECL3	FEO(S)	FEO(L)	FEO2H2(S)	FEO3H3(S)	FE2CL4	FE2O3(S)	FE3O4(S)
HALO	HCN	HNCO	HNO	HNO2	HNO3	HO2	H2O2	NCO	NH
NOCL	NO2	NO2CL	NO3	N2H4	N2O	N2O4	N3	O3	

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

ADJUSTED VALUE OF HSUBO = .21937+03 (KG-MOL)(DEG K)/KG

ELEMENTAL MASS VALUES AFTER TWO PHASE CORRECTION

AL	.4973149-01
	.1318168-01

Resultant Output for Case 4 (Cont'd)

```
H          .5194689-01
O          .2229186-01
N          .8246253-02
FE         .7016621-04
CL         .8297230-02

AL2O3(S)   HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

AL2O3(L)   HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

C(S)       HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FECL3(S)   HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FECL3(L)   HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FEO(S)     HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FEO(L)     HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FEO2H2(S)  HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FEO3H3(S)  HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FE2O3(S)   HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS

FE3O4(S)   HAS BEEN OMITTED FROM PRODUCTS LIST FOR TWO PHASE CALCULATIONS
ADJUSTED LIST OF SPECIES TO BE CONSIDERED IN TWO PHASE SYSTEM
AL         ALH        ALCL       ALCL2      ALCL3
ALO        ALOCL      ALOH       ALO2       ALO2H
AL2O       C          CCL        CCL2       CH2O
CN         CNN        CN2        CO         COCL
CO2        C2         C2H        C2H2       C2H4
C2N        C2N2       C2O        C3         CL
CLCN       CLO        CLO2       CL2        CL2O
FE         FECL       FECL2      FECL3      FEO
FEO2H2     FE2CL4     H          HALO       HCL
HCN        HCO        HNCO       HNO        HNO2
HNO3       HO2        H2         H2O        H2O2
N          NCO        NH         NH2        NH3
NO         NOCL       NO2        NO2CL      NO3
N2         N2H4       N2O        N2O4       N3
O          OH         O2         O3

PT      AL        C         H         O         N         FE        CL
 1   -17.488   -13.390   -9.465   -17.899   -13.815   -15.216   -20.292   12.000

PT      AL        C         H         O         N         FE        CL
 1   -28.435    -3.033   -7.764   -31.668   -12.109    -8.769   -24.279   14.000
 2   -31.712    -1.571   -7.873   -34.874   -12.230    -7.897   -25.623    4.000
PC/PT= 1.816574    T =   1102.32
 2   -31.699    -1.576   -7.873   -34.862   -12.229    -7.900   -25.618    2.000
PC/PT= 1.812748    T =   1102.81
 2   -31.700    -1.576   -7.873   -34.863   -12.229    -7.900   -25.618    1.000
PC/PT= 1.812791    T =   1102.81
 3   -[illegible]   3.450   -8.257   -45.883   -12.665   -6.358   -30.144    6.000
```

Resultant Output for Case 4 (Cont'd)

4	-49.569	5.640	-8.642	-51.839	-13.050	-6.097	-32.721	5.000
5	-52.281	6.369	-8.843	-54.292	-13.244	-6.025	-33.830	5.000
6	-56.101	7.277	-9.125	-57.676	-13.515	-5.930	-35.372	5.000
7	-67.538	9.431	-9.803	-67.225	-14.153	-6.154	-39.700	5.000
8	-74.692	10.534	-10.110	-72.848	-14.430	-6.489	-42.202	5.000
9	-94.390	13.416	-10.919	-87.969	-15.126	-7.777	-48.840	4.000
10	-123.358	17.710	-12.291	-109.998	-16.278	-10.128	-58.422	3.000

THE TEMPERATURE= .2821+03 IS OUT OF RANGE FOR POINT 10

11	-132.355	19.060	-12.748	-116.779	-16.658	-10.947	-61.351	5.000

THE TEMPERATURE= .2640+03 IS OUT OF RANGE FOR POINT 11

12	-154.765	22.434	-13.914	-133.466	-17.612	-13.184	-68.490	6.000

THE TEMPERATURE= .2281+03 IS OUT OF RANGE FOR POINT 12

Resultant Output for Case 4 (Cont'd)

THEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION FOR TWO PHASE MOC CALCULATIONS

PC = 554.0 PSIA

QDOTP = -600.0 (KG-MOL)(DEG K)/KG

CASE NO. 1

	CHEMICAL FORMULA	WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL	AL 1.00000	.16000	.000	S	298.15	.0000
FUEL	C 6.88400 H 10.08900 O .27800 N .26400	.12040	-12000.000	S	298.15	.0000
FUEL	FE 2.00000 O 3.00000	.00400	-197300.000	S	298.15	.0000
FUEL	C 6.15000 H 6.97000 O 1.17000 N .03000	.01960	-28300.000	S	298.15	.0000
FUEL	N 1.00000 H 4.00000 O 4.00000 CL 1.00000	.69600	-70690.000	S	298.15	.0000

O/F= .0000 PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 1.6977 REACTANT DENSITY= .0000

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.8128	10.000	30.000	50.000	100.00	500.00	1000.00	5000.00	50000.0	100000.0	500000.0
P, ATM	37.697	20.795	3.7497	1.2566	.7539	.3770	.0754	.0377	.0075	.0008	.0004	.0001
T, DEG K	1252	1103	788	682	645	601	500	454	363	282	264	228
RHO, G/CC	7.7355-3	4.8452-3	1.2353-3	4.8714-4	3.1309-4	1.7140-4	4.2894-5	2.4039-5	6.3015-6	8.7581-7	4.7836-7	1.1617-7
H, CAL/G	-756.4	-822.3	-972.0	-1046.5	-1077.3	-1116.0	-1193.0	-1220.9	-1274.4	-1330.9	-1344.8	-1372.7
S, CAL/(G)(K)	2.3169	2.3169	2.3169	2.3169	2.3169	2.3169	2.3169	2.3169	2.3169	2.3169	2.3169	2.3169
M, MOL WT	21.082	21.089	21.181	21.687	21.989	22.406	23.329	23.735	24.909	26.890	27.492	28.833
(DLV/DLP)T	-1.00039	-1.00051	-1.01053	-1.04025	-1.04385	-1.04139	-1.02848	-1.02881	-1.03815	-1.03961	-1.03643	-1.02558
(DLV/DLT)P	1.0024	1.0040	1.1357	1.6013	1.6785	1.6553	1.3986	1.3786	1.5657	1.7373	1.7269	1.5903
CP, CAL/(G)(K)	.4397	.4479	.6478	1.3197	1.4468	1.4141	.9040	.7948	.9963	1.3126	1.3346	1.2172
GAMMA (S)	1.2739	1.2684	1.2140	1.1598	1.1523	1.1500	1.1846	1.2068	1.1878	1.1498	1.1427	1.1333
SON VEL,M/SEC	793.1	742.7	612.7	550.6	530.2	506.3	459.3	437.9	379.5	316.7	302.1	273.8
MACH NUMBER	.000	1.000	2.193	2.830	3.091	3.427	4.162	4.503	5.487	6.929	7.396	8.318
AE/AT		1.0000	2.1686	4.7910	7.0134	12.103	43.889	75.923	274.29	1873.87	3390.26	13691.2
CSTAR, FT/SEC		3482	3482	3482	3482	3482	3482	3482	3482	3482	3482	3482
CF		.700	1.266	1.468	1.544	1.634	1.801	1.858	1.961	2.066	2.090	2.139
IVAC,LB-SEC/LB		135.4	168.5	176.0	182.3	190.0	204.4	209.3	218.2	227.7	228.9	234.5
ISP, LB-SEC/LB		75.7	139.0	158.9	167.1	176.9	194.9	201.1	212.3	223.6	226.3	231.6

MOLE FRACTIONS

ALCL3	.00943	.00943	.00947	.00970	.00984	.01002	.01044	.01062	.01114	.01203	.01230	.01290
CO	.22132	.20755	.15253	.10712	.08587	.05865	.01166	.00334	.00010	.00000	.00000	.00000
CO2	.05656	.07037	.12432	.16062	.17634	.19592	.22432	.22789	.21452	.19771	.19608	.20029
C2H4	.00000	.00000	.00117	.00907	.01383	.02039	.03477	.04081	.05686	.07837	.08316	.08989
FECL2	.00142	.00131	.00035	.00012	.00008	.00004	.00000	.00000	.00000	.00000	.00000	.00000
FE2CL4	.00003	.00008	.00057	.00070	.00073	.00077	.00082	.00083	.00087	.00094	.00096	.00101
HCL	.14367	.14369	.14434	.14780	.14986	.15269	.15899	.16175	.16975	.18325	.18736	.19650
HCN	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
H2	.33970	.35343	.40313	.41432	.41503	.41392	.39827	.37949	.30643	.18611	.15214	.08238
H2O	.13550	.12173	.07099	.05509	.05165	.04698	.05576	.06996	.12613	.20402	.22069	.24216

Resultant Output for Case 4 (Cont'd)

NH3	.00034	.00042	.00099	.00123	.00125	.00129	.00192	.00321	.01054	.03395	.05416	.09755
N2	.09202	.09149	.09213	.09423	.09554	.09734	.10106	.10229	.10366	.09762	.09315	.07732

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .50000-05 FOR ALL ASSIGNED CONDITIONS

AL	ALH	ALCL	ALCL2	ALO	ALOCL	ALOH	ALOO	ALO2H	AL2O
C	CCL	CCL2	CH2O	CN	CNN	CN2	COCL	C2	C2H
C2H2	C2N	C2N2	C2O	C3	CL	CLCN	CLO	CLO2	CL2
CL2O	FE	FECL	FECL3	FEO	FEO2H2	H	HALO	HCO	HNCO
HNO	HNO2	HNO3	HO2	H2O2	N	NCO	NH	NH2	NO
NOCL	NO2	NO2CL	NO3	N2H4	N2O	N2O4	N3	O	OH
O2	O3								

NOTE, WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

Resultant Output for Case 4 (Cont'd)

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

O/F= .0000 PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 1.6977 CHAMBER PRESSURE= 37.697 ATM

TEMP	VISCOSITY	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
DEG K	POISE	CAL/(CM)(SEC)(K)					CAL/(G)(K)		DIMENSIONLESS		
1252	456.X10-6	231.X10-6	153.X10-6	384.X10-6	18.X10-6	402.X10-6	.4102	.4396	.4876	.4990	.6588
1103	417.	214.	133.	347.	26.	373.	.4021	.4674	.4926	.4999	.6621
748	326.	179.	96.	275.	104.	379.	.3857	.6476	.4579	.5576	.5579
682	293.	161.	86.	248.	352.	599.	.3792	1.3197	.4471	.6454	.5731
64[illegible]	261.	154.	82.	237.	402.	639.	.3742	1.4468	.4466	.6359	.5976
601	265.	145.	77.	222.	390.	612.	.3716	1.4191	.4436	.6127	.6259
500	227.	121.	64.	184.	191.	376.	.3579	.9046	.4423	.5465	.6785
454	209.	108.	56.	164.	149.	312.	.3496	.7946	.4435	.5303	.7087
363	168.	79.	38.	117.	206.	323.	.3325	.9963	.4[illegible]	.5199	.8531
282	126.	49.	21.	69.	317.	387.	.2949	1.3124	.5265	.5293	1.3742
[illegible]	117.	42.	17.	59.	334.	394.	.2871	1.3346	.5650	.39	1.5477
[illegible]	97.	30.	11.	41.	315.	355.	.2706	1.2172	.5431	.33[illegible]	2.2014

[illegible] 600.0 AND PC = 37.7 HAS BEEN COMPLETED AND WRITTEN ON TAPE UNIT[illegible]

Resultant Output for Case 4 (Cont'd)

THEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION FOR TWO PHASE MOC CALCULATIONS

PC = 554.0 PSIA

QDOTP = -300.0 (KG-MOL)(DEG K)/KG

CASE NO. 1

	CHEMICAL FORMULA								WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL	AL	1.00000							.16000	.000	S	298.15	.0000
FUEL	C	6.88400	H	10.08900	O	.27800	N	.26400	.12040	-12000.000	S	298.15	.0000
FUEL	FE	2.00000	O	3.00000					.00400	-197300.000	S	298.15	.0000
FUEL	C	6.15000	H	6.97000	O	1.17000	N	.03000	.01960	-28300.000	S	298.15	.0000
FUEL	N	1.00000	H	4.00000	O	4.00000	CL	1.00000	.69600	-70690.000	S	298.15	.0000

O/F= .0000 PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 1.6977 REACTANT DENSITY= .0000

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.7973	10.000	30.000	50.000	100.00	500.00	1000.00	5000.00	50000.0	100000.0	500000.0
P, ATM	37.697	20.974	3.7697	1.2566	.7539	.3770	.0754	.0377	.0075	.0008	.0004	.0001
T, DEG K	2524	2261	1599	1263	1132	978	712	623	510	393	351	285
RHO, G/CC	3.8111-3	2.3735-3	6.0545-4	2.5556-4	1.7109-4	9.8961-5	2.7224-5	1.5546-5	3.9161-6	5.3507-7	3.0400-7	7.8424-8
H, CAL/G	-160.2	-293.1	-603.8	-751.4	-909.0	-877.8	-1004.7	-1048.2	-1131.7	-1225.0	-1247.2	-1299.7
S, CAL/(G)(K)	2.6415	2.6415	2.6415	2.6415	2.6415	2.6415	2.6415	2.6415	2.6415	2.6415	2.6415	2.6415
M, MOL WT	20.934	20.995	21.071	21.074	21.074	21.074	21.083	21.092	21.732	22.869	23.208	24.336
(DLV/DLP)T	-1.00241	-1.00170	-1.00038	-1.00001	-1.00002	-1.00003	-1.00017	-1.00064	-1.02757	-1.01204	-1.01777	-1.03450
(DLV/DLT)P	1.0427	1.0318	1.0020	1.0001	1.0001	1.0004	1.0035	1.0110	1.5890	1.1884	1.2714	1.6242
CP, CAL/(G)(K)	.5364	.5133	.4440	.4382	.4429	.4560	.4955	.5004	1.6026	.6352	.6994	1.2406
GAMMA (S)	1.2345	1.2416	1.2709	1.2743	1.2706	1.2609	1.2367	1.2373	1.1319	1.2212	1.2197	1.1616
SOS VEL,M/SEC	1112.3	1054.4	895.5	796.8	753.2	697.6	589.1	551.4	469.9	417.6	391.5	336.4
MACH NUMBER	.000	1.000	2.152	2.792	3.094	3.513	4.513	4.944	6.068	7.149	7.704	9.139
AC/AT		1.0000	2.1454	4.4022	6.2775	10.319	34.580	59.053	224.13	1566.81	2729.48	10379.7
VSTAR, FT/SEC		5008	5008	5008	5008	5008	5008	5008	5008	5008	5008	5008
CF		.691	1.262	1.457	1.527	1.605	1.742	1.786	1.868	1.956	1.976	2.014
IVAC,LB-SEC/LB		194.1	229.9	249.6	257.1	265.9	281.8	287.2	297.7	309.3	311.8	316.7
ISP, LB-SEC/LB		107.5	196.5	226.8	237.6	249.9	271.1	278.0	290.7	304.4	307.5	313.5

MOLE FRACTIONS

ALCL	.00176	.00092	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
ALCL2	.00335	.00275	.00019	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
ALCL3	.00290	.00493	.00922	.00942	.00943	.00943	.00943	.00943	.00972	.01023	.01038	.01089
ALCCL	.00097	.00060	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
ALH	.00012	.00006	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
ALOH	.00025	.00013	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
CO	.25314	.25151	.23934	.22209	.21161	.19130	.13704	.11526	.06135	.00257	.00030	.00000
[illegible]	.02279	.02523	.03042	[illegible]	[illegible]	[illegible]	[illegible]	.16266	.20490	.24298	.23959	[illegible]
[illegible]	.00000	.00000	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]	.00006	.01011	.02795	.03302	[illegible]
[illegible]	.00088	.00033	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]	.00000	.00000	.00000	.00000	[illegible]

Resultant Output for Case 4 (Cont'd)

FF	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FECL2	.00145	.00146	.00148	.00148	.00147	.00145	.00065	.00020	.00002	.00000	.00000	.00000
FECOH2	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FE2CL4	.00000	.00000	.00000	.00000	.00000	.00001	.00042	.00064	.00075	.00080	.00081	.00085
H	.00247	.00095	.00002	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
HCL	.15177	.14910	.14382	.14362	.14362	.14362	.14368	.14374	.14810	.15585	.15816	.16585
H2	.30023	.30508	.32182	.33924	.35072	.37003	.42449	.44611	.45661	.43808	.41765	.34453
H2O	.16601	.16504	.15353	.13629	.12481	.10550	.05120	.02960	.01331	.02126	.03787	.09501
NH3	.00002	.00001	.00001	.00001	.00001	.00002	.00005	.00010	.00018	.00054	.00194	.00839
NO	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
N2	.09153	.09180	.09214	.09215	.09215	.09215	.09217	.09219	.09495	.09974	.10077	.10223
OH	.00029	.00008	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .50000-05 FOR ALL ASSIGNED CONDITIONS

AL	ALH	ALO	ALO2	AL2O	C	CCL	CCL2	CH2O	CN
CNN	CN2	COCL	C2	C2H	C2H2	C2N	C2N2	C2O	C3
CLCN	CLO	CLO2	CL2	CL2O	FECL	FECL3	FEO	HALO	HCN
HCO	HNCO	HNO	HNO2	HNO3	HO2	H2O2	N	NCO	NH
NH2	NOCL	NO2	NO2CL	NO3	N2H4	N2O	N2O4	N3	O
O2	O3								

NOTE: WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

Resultant Output for Case 4 (Cont'd)

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

O/F= .0000 PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 1.6977 CHAMBER PRESSURE= 37.697 ATM

TEMP	VISCOSITY	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
DEG K	POISE	CAL/(CM)(SEC)(K)					CAL/(G)(K)		DIMENSIONLESS		
2524	753.X10-6	364.X10-6	333.X10-6	698.X10-6	181.X10-6	879.X10-6	.4586	.5352	.4945	.4582	1.5542
2261	696.	338.	297.	635.	94.	729.	.4516	.5124	.4948	.4888	1.1024
1599	543.	269.	202.	471.	12.	483.	.4273	.4440	.4924	.4989	.6525
1263	459.	232.	154.	387.	17.	404.	.4107	.4381	.4877	.4982	.6614
1132	425.	218.	137.	354.	23.	377.	.4037	.4429	.4837	.4982	.6696
978	382.	201.	117.	318.	33.	351.	.3954	.4559	.4756	.4970	.6766
712	303.	171.	89.	260.	49.	309.	.3826	.4955	.4466	.4861	.6435
623	275.	159.	81.	239.	47.	286.	.3786	.5004	.4342	.4799	.6087
510	234.	137.	69.	205.	389.	594.	.3689	1.6026	.4214	.6326	.5663
393	187.	106.	51.	158.	76.	234.	.3486	.6352	.4130	.5066	.5834
351	169.	94.	44.	137.	83.	221.	.3391	.6994	.4158	.5342	.5696
285	136.	69.	30.	99.	194.	293.	.3172	1.2406	.4371	.5760	.6759

CASE FOR 600TR = 300.0 AND PC = 37.7 HAS BEEN COMPLETED AND WRITTEN ON TAPE UNIT10

Resultant Output for Case 4 (Cont'd)

THEORETICAL ROCKET PERFORMANCE ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION FOR TWO PHASE MOC CALCULATIONS

PC = 554.0 PSIA

QDOTP = .0 (KG-MOL)(DEG K)/KG

CASE NO. 1

	CHEMICAL FORMULA								WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL	AL 1.00000								.16000	.000	S	298.15	.0000
FUEL	C 6.88400	H	10.08900	O	.27800	N	.26400		.12040	-12000.000	S	298.15	.0000
FUEL	FE 2.00000	O	3.00000						.00400	-197300.000	S	298.15	.0000
FUEL	C 6.15000	H	6.97000	O	1.17000	N	.03000		.01960	-28300.000	S	298.15	.0000
FUEL	N 1.00000	H	4.00000	O	4.00000	CL	1.00000		.69600	-70690.000	S	298.15	.0000

O/F= .0000 PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 1.6977 REACTANT DENSITY= .0000

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.7631	10.000	30.000	50.000	100.00	500.00	1000.00	5000.00	50000.0	100000.0	500000.0
P, ATM	37.697	21.381	3.7697	1.2566	.7539	.3770	.0754	.0377	.0075	.0008	.0004	.0001
T, DEG K	3391	3141	2392	1954	1771	1537	1089	943	687	470	444	373
RHO, G/CC	2.7379-3	1.6749-3	4.0075-4	1.6455-4	1.0917-4	6.2983-5	1.7778-5	1.0272-5	2.8206-6	4.2000-7	2.2637-7	5.5653-8
H, CAL/G	435.9	254.8	-206.5	-432.6	-522.5	-630.6	-827.9	-894.2	-1016.5	-1137.4	-1166.4	-1225.6
S, CAL/(G)(K)	2.8416	2.8416	2.8416	2.8416	2.8416	2.8416	2.8416	2.8416	2.8416	2.8416	2.8416	2.8416
M, MOL WT	20.208	20.431	20.663	20.997	21.042	21.068	21.073	21.073	21.079	21.491	21.867	22.595
(DLV/DLP)T	-1.01730	-1.01197	-1.00280	-1.00167	-1.00088	-1.00015	-1.00000	-1.00000	-1.00013	-1.02296	-1.02153	-1.00615
(DLV/DLT)P	1.2902	1.2133	1.0556	1.0351	1.0204	1.0042	1.0000	1.0001	1.0032	1.5614	1.5495	1.1275
CP, CAL/(G)(K)	.9641	.8497	.5482	.5186	.4884	.4491	.4455	.4599	.4962	1.6848	1.6836	.6206
GAMMA (S)	1.1799	1.1856	1.2255	1.2409	1.2507	1.2684	1.2685	1.2580	1.2362	1.1247	1.1212	1.2107
SON VEL,M/SEC	1283.0	1231.0	1080.8	979.7	935.5	877.1	738.3	684.0	578.6	452.3	434.9	407.2
MACH NUMBER	.000	1.000	2.145	2.752	3.027	3.406	4.405	4.878	6.025	8.022	8.419	9.147
AE/AT		1.0000	2.2454	4.7030	6.7483	11.089	36.087	60.883	212.17	1369.10	2516.99	10054.2
CSTAR, FT/SEC		6006	6006	6006	6006	6006	6006	6006	6006	6006	6006	6006
CF		.672	1.266	1.473	1.547	1.632	1.776	1.822	1.904	1.982	2.000	2.037
IVAC,LB-SEC/LB		231.4	278.4	304.2	314.0	325.3	345.1	351.6	363.4	375.1	378.1	384.0
ISP, LB-SEC/LB		125.5	236.4	274.9	288.8	304.6	331.6	340.2	355.5	370.0	373.4	390.2

MOLE FRACTIONS

AL	.00011	.00006	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
ALH	.00002	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
ALCL	.00438	.00429	.00302	.00100	.00032	.00003	.00000	.00000	.00000	.00000	.00000	.00000
ALCL2	.00151	.00168	.00268	.00234	.00135	.00032	.00000	.00000	.00000	.00000	.00000	.00000
ALCL3	.00013	.00019	.00123	.00503	.00737	.00903	.00942	.00943	.00943	.00961	.00978	.01011
ALO	.00012	.00006	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
ALOCL	.00165	.00178	.00180	.00035	.00033	.00004	[illegible]	[illegible]	[illegible]	.00000	.00000	.00000
ALOH	[illegible]	[illegible]	[illegible]	[illegible]	.00001	[illegible]	[illegible]	[illegible]	[illegible]	.00000	.00000	.00000
[illegible]	[illegible]	[illegible]	[illegible]	[illegible]	.00000	[illegible]	[illegible]	[illegible]	[illegible]	.00000	.00000	.00000
ALO2H	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]	.00000	.00000	.00000

Resultant Output for Case 4 (Cont'd)

	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.0[illegible]
	.24892	.25057	.25128	.24733	.24402	.23700	.20597	.18563	.13083	.04765	.04477	.0[illegible]
	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.0[illegible]
[illegible]	.01742	.01872	.02373	.02945	.03335	.04071	.07181	.09216	.14702	.20296	.21892	.24[illegible]
[illegible]2H4	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00634	.01228	.02376
CL	.01313	.00964	.00158	.00021	.00006	.00001	.00000	.00000	.00000	.00000	.00000	.00000
CL2	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
CL2	.00002	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
[illegible]	.00003	.00040	.00004	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FECL	.00005	.00004	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FECL2	.00079	.00095	.00141	.00147	.00148	.00148	.00148	.00147	.00100	.00001	.00001	.00000
FEC	.00004	.00003	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FEO2H2	.00002	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FE2CL4	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00024	.00075	.00076	.00079
H	.03898	.02730	.00428	.00058	.00018	.00002	.00000	.00000	.00000	.00000	.00000	.00000
HCL	.14313	.14788	.15483	.14945	.14612	.14403	.14362	.14361	.14365	.14646	.14902	.15398
HCO	.00002	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
H2	.27673	.28240	.29874	.30959	.31542	.32400	.35537	.37572	.43064	.46670	.46396	.45497
H2O	.15182	.15731	.16308	.16066	.15793	.15118	.12017	.09962	.04501	.00561	.00485	.00719
[illegible]	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
HN2	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
HN3	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00001	.00005	.00005	.00012
HO	.00072	.00037	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
HO2	.08800	.08915	.09123	.09182	.09202	.09213	.09216	.09216	.09218	.09396	.09560	.09575
O	.00079	.00033	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
OH	.00936	.00564	.00042	.00003	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000
O2	.00017	.00007	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .50000-05 FOR ALL ASSIGNED CONDITIONS

C	CCL	CCL2	CH2O	CN	CNN	CN2	C2	C2H	C2-2
C2H2	C2H2	C2O	C3	CLCN	CLO2	CL2O	FECL3	HCLO	HCN
HNO	HNO	HNO2	HNO3	HO2	H2O2	NCO	NH	NOCL	NO2
NO3	NO3	N2H4	N2O	N2O4	N3	O3			

WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

Resultant Output for Case 4 (Cont'd)

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

O/F= .0000 PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 1.6977 CHAMBER PRESSURE= 37.697 ATM

TEMP	VISCOSITY	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
DEG K	POISE	CAL/(CM)(SEC)(K)					CAL/(G)(K)		DIMENSIONLESS		
3391	931.X10-6	489.X10-6	434.X10-6	923.X10-6	1889.X10-6	2812.X10-6	.4765	.9560	.4802	.3163	2.0328
3141	881.	450.	406.	856.	1423.	2280.	.4723	.8437	.4859	.3260	2.1145
2372	723.	352.	312.	664.	309.	973.	.4553	.5670	.4960	.4216	1.8954
1954	626.	305.	252.	558.	84.	642.	.4415	.5177	.4959	.5053	.8732
1771	584.	287.	227.	514.	44.	558.	.4346	.4882	.4943	.5113	.6975
1537	528.	262.	193.	456.	17.	473.	.4244	.4490	.4920	.5019	.6399
1089	413.	213.	131.	344.	25.	369.	.4013	.4455	.4819	.4980	.6726
943	372.	197.	113.	310.	35.	345.	.3935	.4599	.4728	.4957	.6788
687	295.	167.	87.	254.	49.	303.	.3815	.4962	.4432	.4840	.6776
470	220.	121.	64.	195.	378.	572.	.3669	1.6849	.4155	.6489	.5801
344	210.	124.	60.	184.	385.	569.	.3622	1.6836	.4124	.6207	.5725
374	180.	105.	50.	155.	71.	225.	.3485	.6206	.4049	.4949	.5851

CALC FOR QDOTR = .0 AND PC = 37.7 HAS BEEN COMPLETED AND WRITTEN ON TAPE UNIT10

Resultant Output for Case 4 (Cont'd)

THEORETICAL ROCKET PERFORMANCE ASSUMING C HILIBRIUM COMPOSITION DURING EXPANSION FOR TWO PHASE MOC CALCULATIONS

PC = 554.0 PSIA

NOTP = 100.0 (KG-MOL)(DEG K)/KG

CASE NO. 1

	CHEMICAL FORMULA							WT FRACTION (SEE NOTE)	ENERGY CAL/MOL	STATE	TEMP DEG K	DENSITY G/CC
FUEL	AL 1.00000							.16000	.000	S	298.15	.0000
FUEL	C 6.88400	H 10.08900	O .27800	N .26400				.12040	-12000.000	S	298.15	.0000
FUEL	FE 2.00000	O 3.00000						.00400	-197300.000	S	298.15	.0000
FUEL	C 6.15000	H 6.97000	O 1.17000	N .03000				.01960	-28300.000	S	298.15	.0000
FUEL	N 1.00000	H 4.00000	O 4.00000	CL 1.00000				.69600	-70690.000	S	298.15	.0000

O/F= .0000 PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 1.6977 REACTANT DENSITY= .0000

	CHAMBER	THROAT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT	EXIT
PC/P	1.0000	1.7555	18.000	30.000	50.000	100.00	500.00	1000.00	5000.00	50000.0	100000.0	500000.0
P, ATM	37.697	21.474	3.7697	1.2566	.7539	.3770	.0754	.0377	.0075	.0008	.0004	.0001
T, DEG K	3577	3338	2624	2175	1979	1736	1239	1069	771	492	458	400
RHO, G/CC	2.5464-3	1.5758-3	3.6265-4	1.4719-4	9.7326-5	5.5685-5	1.5626-5	9.0572-6	2.5109-6	3.9434-7	2.1508-7	5.1266-8
H, CAL/G	634.6	441.0	-63.5	-315.0	-415.7	-537.4	-761.7	-837.0	-975.1	-1110.1	-1140.7	-1203.5
S, CAL/(G)(K)	2.8986	2.8986	2.8986	2.8986	2.8986	2.8986	2.8986	2.8986	2.8986	2.8986	2.8986	2.8986
M, MOL WT	19.829	20.098	20.715	20.906	20.968	21.038	21.073	21.073	21.074	21.134	21.461	22.291
(DLV/DLP)T	-1.02630	-1.01978	-1.00532	-1.00226	-1.00194	-1.00099	-1.00001	-1.00000	-1.00003	-1.00568	-1.02206	-1.01153
(DLV/DLT)P	1.4236	1.3380	1.1077	1.0459	1.0404	1.0234	1.0002	1.0000	1.0006	1.1334	1.5582	1.3120
CP, CAL/(G)(K)	1.1737	1.0562	.6778	.5456	.5298	.4949	.4392	.4470	.4846	.7153	1.7138	1.1485
GAMMA (S)	1.1720	1.1735	1.2024	1.2320	1.2371	1.2483	1.2735	1.2674	1.2419	1.1950	1.1225	1.1391
SON VEL,M/SEC	1325.9	1272.9	1125.4	1032.4	985.4	925.4	789.1	731.1	614.7	481.1	446.5	412.0
MACH NUMBER	.000	1.000	2.148	2.731	3.008	3.384	4.332	4.800	5.971	7.941	8.633	9.519
AE/AT		1.0000	2.2884	4.8343	6.9518	11.502	37.553	63.109	217.66	1331.23	2419.62	9976.24
CSTAR, FT/SEC		6248	6248	6248	6248	6248	6248	6248	6248	6248	6248	6248
CF		.668	1.269	1.480	1.557	1.645	1.795	1.843	1.927	2.006	2.024	2.060
IVAC,LB-SEC/LB		240.4	290.9	318.7	329.3	341.7	363.2	370.1	382.7	394.8	397.7	403.8
ISP, LB-SEC/LB		129.8	246.5	287.5	302.3	319.3	348.6	357.8	374.3	389.6	393.0	399.9

MOLE FRACTIONS

AL	.00021	.00013	.00002	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
ALH	.00002	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
ALCL	.00449	.00451	.00400	.00260	.00155	.00038	.00000	.00000	.00000	.00000	.00000	.00000
ALCL2	.00115	.00125	.00192	.00266	.00256	.00141	.00002	.00000	.00000	.00000	.00000	.00000
ALCL3	.00007	.00009	.00038	.00181	.00372	.00714	.00941	.00943	.00943	.00945	.00960	.00997
ALO	.00022	.00014	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
ALOCL	.00154	.00171	.00209	.00141	.00128	.00041	.00000	.00000	.00000	.00000	.00000	.00000
ALOH	.00043	.00041	.00028	.00014	.00007	.00002	.00000	.00000	.00000	.00000	.00000	.00000
AL2	.00005	.00004	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
AL2H	.00066	.00068	.00056	.00033	.00019	.00005	.00000	.00000	.00000	.00000	.00000	.00000

Resultant Output for Case 4 (Cont'd)

AL2O	.00001	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
CO	.24530	.24753	.25130	.24954	.24744	.24308	.22029	.20359	.15134	.08938	.06814	.05858
COCL	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
CO2	.01604	.01737	.02175	.02603	.02895	.03423	.05749	.07419	.12645	.18779	.20302	.23733
C2H4	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00071	.00586	.01320
CL	.01959	.01550	.00431	.00089	.00033	.00007	.00000	.00000	.00000	.00000	.00000	.00000
CLO	.00002	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
CL2	.00003	.00002	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FE	.00074	.00065	.00017	.00003	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FECL	.00006	.00005	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FECL2	.00051	.00065	.00124	.00144	.00146	.00148	.00148	.00148	.00142	.00003	.00001	.00000
FEO	.00006	.00005	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FEO2H2	.00001	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
FE2CL4	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00003	.00072	.00075	.00078
H	.35881	.04513	.01172	.00238	.00090	.00019	.00000	.00000	.00000	.00000	.00000	.00000
HCL	.13522	.14086	.15400	.15454	.15160	.14650	.14363	.14362	.14362	.14403	.14625	.15191
HCO	.00003	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
H2	.26816	.27394	.29220	.30257	.30791	.31614	.34103	.35775	.41001	.46928	.46828	.46125
H2O	.14167	.14928	.16178	.16163	.16029	.15690	.13449	.11779	.06554	.00617	.00422	.00373
K	.00002	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
KH	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
KH2	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
KH3	.00001	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00003	.00003	.00004
NO	.00129	.00078	.00007	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
N2	.08605	.08749	.09055	.09142	.09169	.09200	.09216	.09216	.09216	.09241	.09383	.09746
O	.00195	.00103	.00004	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000
OH	.01514	.01041	.00153	.00017	.00004	.00001	.00000	.00000	.00000	.00000	.00000	.00000
O2	.00041	.00022	.00001	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000	.00000

ADDITIONAL PRODUCTS WHICH WERE CONSIDERED BUT WHOSE MOLE FRACTIONS WERE LESS THAN .50000-05 FOR ALL ASSIGNED CONDITIONS

	CCL	CCL2	CH2O	CN	CNN	CN2	C2	C2H	C2H2
[illegible]	C2N2	C2O	C3	CLCN	CLO2	CL2O	FECL3	HALO	HCN
[illegible]	HNO	HNO2	HNO3	HO2	H2O2	NCO	NOCL	NO2	NO2CL
[illegible]	N2H4	N2O	N2O4	N3	O3				

NOTE. WEIGHT FRACTION OF FUEL IN TOTAL FUELS AND OF OXIDANT IN TOTAL OXIDANTS

Resultant Output for Case 4 (Cont'd)

TRANSPORT PROPERTIES OF ROCKET EXHAUST ASSUMING EQUILIBRIUM COMPOSITION DURING EXPANSION

O/F= .0000 PERCENT FUEL=100.0000 EQUIVALENCE RATIO= 1.6977 CHAMBER PRESSURE= 37.697 ATM

TEMP	VISCOSITY	MONATOMIC COND	INTERNAL COND	FROZEN COND	REACTION COND	EQUILIBRIUM COND	CP FROZ	CP EQ	PRANDTL FROZ	PRANDTL EQ	LEWIS NUMBER
DEG K	POISE	CAL/(CM)(SEC)(K)					CAL/(G)(K)		DIMENSIONLESS		
3577	966.X10-6	535.X10-6	448.X10-6	983.X10-6	2701.X10-6	3684.X10-6	.4797	1.1614	.4718	.3047	1.9347
3338	920.	491.	424.	915.	2216.	3131.	.4759	1.0468	.4783	.3075	2.0181
2624	773.	381.	342.	723.	733.	1456.	.4613	.6748	.4934	.3584	2.1906
2175	676.	328.	282.	610.	204.	814.	.4489	.5447	.4971	.4521	1.5662
1979	632.	308.	255.	563.	110.	673.	.4424	.5283	.4967	.4963	1.0051
1736	576.	283.	221.	504.	49.	553.	.4331	.4947	.4944	.5147	.6827
1739	453.	230.	151.	381.	18.	399.	.4095	.4392	.4871	.4985	.6610
1069	408.	211.	128.	339.	27.	366.	.4002	.4470	.4810	.4979	.6739
771	321.	178.	95.	272.	47.	319.	.3852	.4846	.4546	.4881	.6460
492	229.	137.	66.	203.	93.	297.	.3706	.7153	.4177	.5530	.4923
458	216.	129.	62.	191.	377.	567.	.3660	1.7139	.4141	.6525	.5354
[illegible]	191.	113.	54.	167.	222.	389.	.3544	1.1485	.4069	.5655	.5942

Resultant Output for Case 4 (Cont'd)

```
14  19
                37.7          .0            .0            .0            .0            .0            .0
                ALCL          CO            CO2           C2H4          FECL          FE2C          HCL
                HCN           H2            H2O           NH3           N2
                  .0            .0            .0            .0            .0            .0            .0
                  3                                                     2             L4
 -.7563738+03   .3769732+02   .1252025+04   .2316876+01   .2108151+02   .1273913+01   .0000000
  .4989933+00   .4563408-03   .4396469+00   .4020671-03  -.7563768+03   .4359248+03
  .9428998-02   .2213171+00   .5656125-01   .6356326-06   .1420590-02   .2818051-04   .1436682+00
  .7031177-05   .3396975+00   .1355033+00   .3444960-03   .9201622-01
 -.7563738+03   .2079518+02   .1102806+04   .2316876+01   .2108425+02   .1268393+01   .1000014+01
  .4999204+00   .4167851-03   .4478939+00   .3734105-03  -.8222937+03   .4359248+03
  .9431178-02   .2075478+00   .7036607-01   .2886612-05   .1310753-02   .8339599-04   .1436865+00
  .4465831-05   .3534276+00   .1217255+00   .4163899-03   .9199360-01
 -.7563738+03   .3769732+01   .7877338+03   .2316876+01   .2118054+02   .1214012+01   .2192553+01
  .5575984+00   .3264648-03   .6477590+00   .3792524-03  -.9720358+03   .4359248+03
  .9424387-02   .1525266+00   .1243209+00   .1173380-02   .3606663-03   .5675932-03   .1443440+00
  .1370478-05   .4031337+00   .7098577-01   .9949192-03   .9212702-01
 -.7563738+03   .1256577+01   .6817608+03   .2316876+01   .2168739+02   .1159792+01   .2830043+01
  .6454377+00   .2931151-03   .1319709+01   .6993245-03  -.1046507+04   .4359248+03
  .9701081-02   .1071182+00   .1606201+00   .9068643-02   .1203698+03   .7006136-03   .1477984+00
  .4477561-06   .4143225+00   .5509359-01   .1228891-02   .9422703-01
 -.7563738+03   .7539463+00   .6453291+03   .2316876+01   .2198938+02   .1152252+01   .3090746+01
  .6359320+00   .2808524-03   .1446776+01   .6389527-03  -.1077336+04   .4359248+03
  .9836150-02   .8586683-01   .1763356+00   .1382713-01   .7687923-04   .7329794-03   .1498565+00
  .2334062-06   .4150332+00   .5164609-01   .1252018-02   .9553624-01
 -.7563738+03   .3769732+00   .6005654+03   .2316876+01   .2240571+02   .1150021+01   .3426542+01
  .6127097+00   .2651319-03   .1414120+01   .6119196-03  -.1115978+04   .4359248+03
  .1002243-01   .5664641-01   .1959207+00   .2038877-01   .4025138-04   .7659185-03   .1526938+00
  .8484318-07   .4139165+00   .4997683-01   .1290444-02   .9733776-01
 -.7563738+03   .7539464-01   .4997360+03   .2316876+01   .2332926+02   .1184618+01   .4161616+01
  .5465525+00   .2272465-03   .9039898+00   .3758624-03  -.1193036+04   .4359248+03
  .1043556-01   .1165654-01   .2263195+00   .3477145-01   .4775039-05   .8160768-03   .1589878+00
  .0000000      .3982703+00   .5575718-01   .1917929-02   .1010628+00
 -.7563738+03   .3769732-01   .4535921+03   .2316876+01   .2373454+02   .1206837+01   .4502552+01
  .5302512+00   .2086584-03   .7948053+00   .3127628-03  -.1220947+04   .4359248+03
  .1061680-01   .3344559-02   .2278921+00   .4081220-01   .1119664-05   .8321213-03   .1617497+00
  .0000000      .3794934+00   .6995832-01   .3011109-02   .1022885+00
 -.7563738+03   .7539463-02   .3631953+03   .2316876+01   .2490873+02   .1187839+01   .5486519+01
  .5198346+00   .1682996-03   .9963067+00   .3225603-03  -.1274390+04   .4359248+03
  .1114206-01   .9685249-04   .2145187+00   .5686166-01   .1924629-07   .8738680-03   .1697518+00
  .0000000      .3064283+00   .1261278+00   .1054005-01   .1036589+00
 -.7563738+03   .7539463-03   .2821073+03   .2316876+01   .2689000+02   .1149841+01   .6923687+01
  .4290227+00   .1264152-03   .1312575+01   .3867612-03  -.1330938+04   .4359248+03
  .1202837-01   .6724682-06   .1977058+00   .7837445-01   .0000000      .9433831-03   .1832539+00
  .0000000      .1861087+00   .2040166+00   .3994983-01   .9761839-01
 -.7563738+03   .3769732-03   .2640326+03   .2316876+01   .2749220+02   .1142715+01   .7345774+01
  .3951660+00   .1165517-03   .1334568+01   .3936224-03  -.1344762+04   .4359248+03
  .1229770-01   .1513244-06   .1960788+00   .8315707-01   .0000000      .9645144-03   .1873590+00
  .0000000      .1521438+00   .2206946+00   .5415713-01   .9314826-01
 -.7563738+03   .7539464-04   .2280598+03   .2316876+01   .2883328+02   .1133297+01   .8318345+01
  .3324584+00   .9707645-04   .1217187+01   .3554134-03  -.1372651+04   .4359248+03
  .1287755-01   .0000000      .2002919+00   .8908997-01   .0000000      .1011566-02   .1964977+00
  .0000000      .6238127-01   .2421631+00   .9735169-01   .7731578-01
```

Resultant Output for Case 4 (Cont'd)

14 29

37.7	.0	.0	.0	.0	.0	.0
ALCL	ALCL	ALCL	ALOC	ALOH	ALOZ	CO
CO2	C2H4	CL	FE	FECL	FEO2	FE2C
H	HCL	H2	H2O	NH3	NO	N2
OH						
.0	.0	.0	.0	.0	.0	.0
	2	3	L	2	H H2	L4
-.1602248+03	.3769732+02	.2523549+04	.2641502+01	.2093427+02	.1234515+01	.0000000
.4582123+00	.7526580-03	.5351739+00	.8790749-03	-.1602746+03	.4359248+03	
.1760368-02	.3348199-02	.2903079+02	.9741932-03	.1206483-03	.2517351-03	.2531436+00
.2279352-01	.0000000	.8806887-03	.1216908-04	.1445723-02	.6134732-06	.3642480-07
.2473379-02	.1517709+00	.3002301+00	.1660690+00	.1931272-04	.1127655-04	.9152944-01
.2693930-03						
-.1602248+03	.2097395+02	.2260741+04	.2641502+01	.2099450+02	.1241601+01	.9999871+00
.4888470+00	.6955243-03	.5124021+00	.7290353-03	-.2730988+03	.4359248+03	
.9205383-03	.2751438-02	.4934754-02	.6011832-03	.5550546-04	.1266052-03	.2515054+00
.2523195-01	.0000000	.3335506-03	.3181922-05	.1464880+02	.2993611-05	.4391096-07
.9452135-03	.1490980+00	.3050812+00	.1650383+00	.1466029-04	.2222073-05	.9160136-01
.7716545-04						
-.1602248+03	.3769732+01	.1598976+04	.2641502+01	.2107104+02	.1270915+01	.2151640+01
.4949496+00	.5432992-03	.4439681+00	.8834306-03	-.6038541+03	.4359248+03	
.7251824-05	.1882156-03	.9219356-02	.9476257-05	.2519392-06	.8251240-06	.2093355+00
.3841538-01	.0000000	.5523370-05	.0000000	.1477434-02	.1540916-06	.1647993-06
.1563639-04	.1438173+00	.3218208+00	.1535342+00	.9859068-05	.0000000	.9214110-01
.2639749-06						
-.1602248+03	.1256577+01	.1262657+04	.2641502+01	.2107357+02	.1274308+01	.2791617+01
.4982400+00	.4590785-03	.4381370+00	.4036996-03	-.7514287+03	.4359248+03	
.2813667-07	.6870379-05	.9419553-02	.7030968-07	.0000000	.0000000	.2228909+00
.5569395-01	.0000000	.1117824-06	.0000000	.1476419-02	.0000000	.9052662-06
.3101619-06	.1436219+00	.3392353+00	.1362902+00	.1096029-04	.0000000	.9215180-01
.0000000						
-.1602248+03	.7539463+00	.1131757+04	.2641502+01	.2107371+02	.1270571+01	.3093501+01
.4982418+00	.4245533-03	.4428848+00	.3773834-03	-.8090325+03	.4359248+03	
.0000000	.1033837-05	.9425557-02	.0000000	.0000000	.0000000	.2106097+00
.6717794-01	.0000000	.1260983-07	.0000000	.1473142-02	.0000000	.2569584-05
.3478363-07	.1436169+00	.3507217+00	.1248074+00	.1279010-04	.0000000	.9215155-01
.0000000						
-.1602248+03	.3769732+00	.9783330+03	.2641502+01	.2107405+02	.1260915+01	.3512634+01
.4969634+00	.3823293-03	.4559489+00	.3507614-03	-.8778451+03	.4359248+03	
.0000000	.5565892-07	.9426679-02	.0000000	.0000000	.0000000	.1913016+00
.8648955-01	.0000000	.0000000	.0000000	.1451504-02	.0000000	.1342216-04
.0000000	.1436184+00	.3700315+00	.1054988+00	.1742310-04	.0000000	.9215072-01
.0000000						
-.1602248+03	.7639464-01	.7115676+03	.2641502+01	.2108328+02	.1236658+01	.4612590+01
.4860838+00	.3029659-03	.4954813+00	.3088231-03	-.1004693+04	.4359248+03	
.0000000	.0000000	.9430871-02	.0000000	.0000000	.0000000	.1370387+00
.1408727+00	.7589053-06	.0000000	.0000000	.6480552-03	.0000000	.4155835-03
.0000000	.1436614+00	.4244850+00	.5120124-01	.5126752-04	.0000000	.9217421-01
.0000000						

Resultant Output for Case 4 (Cont'd)

-.1602248+03	.3769732-01	.6233164+03	.2641502+01	.2109246+02	.1237317+01	.4943952+01
.4798761+00	.2745319-03	.5004125+00	.2862806-03	-.1048229+04	.4359248+03	
.0000000	.0000000	.9434947-02	.0000000	.0000000	.0000000	.1152581+00
.1626640+00	.5602065-04	.0000000	.0000000	.1987182-03	.0000000	.6406098-03
.0000000	.1437441+00	.4461110+00	.2960416-01	.9640264-04	.0000000	.9219179-01
.0000000						
-.1602248+03	.7539463-02	.5098975+03	.2641502+01	.2173222+02	.1131861+01	.6067823+01
.6325566+00	.2344632-03	.1602553+01	.5940016-03	-.1131658+04	.4359248+03	
.0000000	.0000000	.9721170-02	.0000000	.0000000	.0000000	.4134849-01
.2048976+00	.1011067-01	.0000000	.0000000	.2063838-04	.0000000	.7521168-03
.0000000	.1481041+00	.4566094+00	.1330836-01	.1796001-03	.0000000	.9494796-01
.0000000						
-.1602248+03	.7539463-03	.3927007+03	.2641502+01	.2286879+02	.1221243+01	.7148683+01
.5085582+00	.1869840-03	.6351563+00	.2335309-03	-.1225045+04	.4359248+03	
.0000000	.0000000	.1022956-01	.0000000	.0000000	.0000000	.2565656-02
.2429807+00	.2795156-01	.0000000	.0000000	.3700813-06	.0000000	.8021237-03
.0000000	.1558497+00	.4380803+00	.2126156-01	.5407849-03	.0000000	.9973768-01
.0000000						
-.1602248+03	.3769732-03	.3507314+03	.2641502+01	.2320816+02	.1219744+01	.7703991+01
.5342084+00	.1685633-03	.6993554+00	.2206735-03	-.1247245+04	.4359248+03	
.0000000	.0000000	.1038139-01	.0000000	.0000000	.0000000	.3034368-03
.2395880+00	.3301573-01	.0000000	.0000000	.3462150-07	.0000000	.8141979-03
.0000000	.1581625+00	.4176481+00	.3787433-01	.1440391-02	.0000000	.1007720+00
.0000000						
-.1602248+03	.7539464-04	.2851196+03	.2641502+01	.2433566+02	.1161626+01	.9139187+01
.5760464+00	.1358459-03	.1240641+01	.2925737-03	-.1289680+04	.4359248+03	
.0000000	.0000000	.1088580-01	.0000000	.0000000	.0000000	.3642044-05
.2237378+00	.4852166-01	.0000000	.0000000	.0000000	.0000000	.8537706-03
.0000000	.1658463+00	.3445272+00	.9500789-01	.8386152-02	.0000000	.1022298+00
.0000000						

Resultant Output for Case 4 (Cont'd)

37.7	.0	.0	.0	.0	.0	.0
AL	ALH	ALCL	ALCL	ALCL	ALO	ALOC
ALOH	ALO2	ALO2	AL2O	CO	COCL	CO2
C2H4	CL	CLO	CL2	FE	FECL	FECL
FEO	FEO2	FE2C	H	HCL	HCO	H2
H2O	N	NH2	NH3	NO	N2	O
OH	O2					
.0	.0	.0	.0	.0	.0	.0
			2	3		L
		H				
						2
	H2	L4				

.4359247+03	.3769732+02	.3390819+04	.2841597+01	.2020825+02	.1179931+01	.0000000
.3193401+00	.9305038-03	.9560250+00	.2812115-02	.4366310+03	.4359248+03	
.1133123-03	.1507067-04	.4379597-02	.1507848-02	.1333928-03	.1187501-03	.1645867-02
.[illegible]75-03	.3112200-04	.5672310-03	.1156668-04	.2489219+00	.9362496-05	.1742090-01
.[illegible]000	.1342840-01	.3596266-05	.2276880-04	.5295637-03	.5377000-04	.7756351-03
.[illegible]603-04	.1687343-04	.0000000	.3898059-01	.1431325+00	.1980203-04	.2767278+00
.[illegible]57+00	.6230678-05	.1003542-04	.8944619-05	.7181845-03	.6799682-01	.7867240-03
.[illegible]24-02	.1720780-03					
.[illegible]7+03	.2138067+02	.3140961+04	.2841597+01	.2043083+02	.1185590+01	.9099833+00
.3209[illegible]1+00	.8807145-03	.8436760+00	.2279514-02	.2558272+03	.4359248+03	
.[illegible]37-04	.7911599-05	.4293953-02	.1682681-02	.1925552-03	.6466[illegible]-04	.1780386-02
.3672[illegible]3-03	.1789343-04	.6473550-03	.1005034-04	.2505720+00	.4775170-05	.1872230-01
.[illegible]00	.9643867-02	.3314617-05	.1381021-04	.4011326-03	.3900870-04	.9529499-03
.3[illegible]7787-04	.1402728-04	.0000000	.2729957-01	.1478758+00	.9815555-05	.2823984+00
.1673067+00	.2130597-05	.4938507-05	.6056679-05	.3701131-03	.8915273-01	.3334999-03
.5637412-02	.7476643-04					
.4359247+03	.3769732+01	.2391724+04	.2841597+01	.2086339+02	.1225498+01	.2145373+01
.4216390+00	.7234387-03	.5669603+00	.9727776-03	-.2065395+03	.4359248+03	
.3387878-05	.4170093-06	.3018671-02	.2676543-02	.1231441-02	.2793984-05	.1800880-02
.1863053-03	.8735825-06	.4042947-03	.3451480-05	.2512822+00	.3487733-06	.2373070-01
.0000000	.1581906-02	.3528476-07	.1427468-05	.4411977-04	.4502559-05	.1409096-02
.1108444-05	.3873278-05	.0000000	.4282134-02	.1548307+00	.6745069-06	.2987388+00
.1630845+00	.1586111-07	.3230539-06	.2203550-05	.1428507-04	.9122957-01	.4120485-05
.4215762-03	.9446231-06					
.4359247+03	.1256577+01	.1954051+04	.2841597+01	.2099746+02	.1240437+01	.2751845+01
.5053146+00	.6262552-03	.5177160+00	.6416247-03	-.4326720+03	.4359248+03	
.8201477-07	.1299156-07	.1001870-02	.2341220-02	.5030165-02	.5698891-03	.8454601-03
.4790967-04	.1906095-07	.1250767-03	.3015587-06	.2473286+00	.3610234-07	.2945281-01
.0000000	.2105451-03	.0000000	.1466360-06	.2626279-05	.3396954-06	.1469126-02
.2574565-07	.9247267-06	.0000000	.5827761-03	.1494502+00	.6996306-07	.3095920+00
.1606644+00	.0000000	.3167089-07	.1441540-05	.4988180-06	.9182346-01	.3865035-07
.2720610-04	.0000000					
.4359247+03	.7539463+00	.1770970+04	.2841597+01	.2104202+02	.1250728+01	.3027191+01
.5113287+00	.5840877-03	.4881963+00	.5576637-03	-.5225373+03	.4359248+03	
.0000000	.0000000	.3152790-03	.1346595-02	.7374008-02	.0000000	.3254889-03
.1306632-04	.0000000	.3791142-04	.2616711-07	.2440227+00	.1056719-07	.3334634-01
.0000000	.6401082-04	.0000000	.4136392-07	.4657069-06	.7074523-07	.1475244-02
.0000000	.4063055-06	.1196556-07	.1798937-03	.1461190+00	.2050271-07	.3184241+00

Resultant Output for Case 4 (Cont'd)

.1579295+00	.0000000	.0000000	.1269429-05	.7063640-07	.9201865-01	.0000000
.5438782-05	.0000000					
.4359247+03	.3769732+00	.1536764+04	.2841597+01	.2106825+02	.1268444+01	.3406137+01
.5018911+00	.5281425-03	.4490495+00	.4725370-03	-.6306133+03	.4359248+03	
.0000000	.0000000	.2578890-04	.3235589-03	.9034002-02	.0000000	.3713656-04
.8221727-06	.0000000	.2632357-05	.0000000	.2370036+00	.0000000	.4071113-01
.0000000	.8885716-05	.0000000	.0000000	.2278036-07	.0000000	.1477921-02
.0000000	.1008717-06	.2517966-07	.2499562-04	.1440307+00	.0000000	.3240029+00
.1611803+00	.0000000	.0000000	.1181819-05	.0000000	.9213347-01	.0000000
.3659447-06	.0000000					
.4359247+03	.7539464-01	.1089138+04	.2841597+01	.2107342+02	.1268522+01	.4404798+01
.4980436+00	.4130485-03	.4454896+00	.3694616-03	-.8279443+03	.4359248+03	
.0000000	.0000000	.0000000	.1448731-05	.9424993-02	.0000000	.1180094-07
.0000000	.0000000	.0000000	.0000000	.2059728+00	.0000000	.7181018-01
.0000000	.1591363-07	.0000000	.0000000	.0000000	.0000000	.1477579-02
.0000000	.0000000	.4667770-06	.4383116-07	.1436157+00	.0000000	.3553667+00
.1201724+00	.0000000	.0000000	.1643713-05	.0000000	.9215591-01	.0000000
.0000000	.0000000					
.4359247+03	.3769732-01	.9425273+03	.2841597+01	.2107350+02	.1257965+01	.4877887+01
.4957344+00	.3721050-03	.4598876+00	.3451979-03	-.8942023+03	.4359248+03	
.0000000	.0000000	.0000000	.2028718-07	.9426439-02	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.1856252+00	.0000000	.9215891-01
.0000000	.0000000	.0000000	.0000000	.0000000	.0000000	.1473133-02
.0000000	.0000000	.2699704-05	.0000000	.1436149+00	.0000000	.3757159+00
.5782447-01	.0000000	.0000000	.2303138-05	.0000000	.9215589-01	.0000000
.0000000	.0000000					
.4359247+03	.7539463-02	.6866479+03	.2841597+01	.2107861+02	.1236233+01	.6024985+01
.4939732+00	.2950794-03	.4961691+00	.3025153-03	-.1016549+04	.4359248+03	
.0000000	.0000000	.0000000	.0000000	.9428790-02	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.1308331+00	.0000000	.1470185+00
.0000000	.0000000	.0000000	.0000000	.0000000	.0000000	.9977943-03
.0000000	.0000000	.2405710-03	.0000000	.1436497+00	.0000000	.4306370+00
.4901143-01	.0000000	.0000000	.7234971-05	.0000000	.9217582-01	.0000000
.0000000	.0000000					
.4359247+03	.7539463-03	.4701601+03	.2841597+01	.2149112+02	.1124657+01	.8022363+01
.6489039+00	.2203997-03	.1684853+01	.5722589-03	-.1137390+04	.4359248+03	
.0000000	.0000000	.0000000	.0000000	.9613291-02	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.6764592-01	.0000000	.2029589+00
.6342102-02	.0000000	.0000000	.0000000	.0000000	.0000000	.1495248-04
.0000000	.0000000	.7464991-03	.0000000	.1464609+00	.0000000	.4666960+00
.5513191-02	.0000000	.0000000	.4970577-04	.0000000	.9395854-01	.0000000
.0000000	.0000000					
.4359247+03	.3769732-03	.4437711+03	.2841597+01	.2186676+02	.1121162+01	.8418862+01
.6206803+00	.2096428-03	.1683582+01	.5686518-03	-.1166413+04	.4359248+03	
.0000000	.0000000	.0000000	.0000000	.9781344-02	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.4476821-01	.0000000	.2189178+00
.1227722-01	.0000000	.0000000	.0000000	.0000000	.0000000	.6951192-05
.0000000	.0000000	.7636795-03	.0000000	.1490210+00	.0000000	.4639650+00
.4846502-02	.0000000	.0000000	.5244972-04	.0000000	.9559991-01	.0000000
.0000000	.0000000					
.4359247+03	.7539464-04	.3730398+03	.2841597+01	.2259506+02	.1210657+01	.9146692+01
.4948838+00	.1798073-03	.6206126+00	.2254886-03	-.1225553+04	.4359248+03	
.0000000	.0000000	.0000000	.0000000	.1010714-01	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.4133430-02	.0000000	.2461793+00
.2376425-01	.0000000	.0000000	.0000000	.0000000	.0000000	.3509000-06
.0000000	.0000000	.7923300-03	.0000000	.1539842+00	.0000000	.4549716+00
.7194[illegible]-02	.0000000	.0000000	.1229947-03	.0000000	.9874951-01	.0000000
.0000000	.0000000					

Resultant Output for Case 4 (Cont'd)

14 45

37.7	.0	.0	.0	.0	.0	.0
AL	ALH	ALCL	ALCL	ALCL	ALO	ALOC
ALOH	ALO2	ALO2	AL2O	CO	COCL	CO2
C2H4	CL	CLO	CL2	FE	FECL	FECL
FEO	FEO2	FE2C	H	HCL	HCO	H2
H2O	N	NH	NH2	NH3	NO	N2
O	OH	O2				
.0	.0	.0	.0	.0	.0	.0
		H	2	3		L 2
	H2	L4				

.6346412+03	.3769732+02	.3577445+04	.2898596+01	.1982916+02	.1171983+01	.0000000
.2046845+00	.9664749-03	.1161364+01	.3683903-02	.6350372+03	.4359248+03	
.0053037-03	.2367840-04	.4489698-02	.1148701-02	.6957333+04	.2160258-03	.1541295-02
.4310749-03	.5305767-04	.6641428-03	.1330929-04	.2452998+00	.1166047-04	.1603791-01
.0000000	.1958877-01	.1833198-04	.3000517-04	.7366891-03	.6707950-04	.5143083-03
.6376191-04	.1417380-04	.0000000	.5880807-01	.1352194+00	.2556314-04	.2681632+00
.1416669+00	.1507846-04	.5275324-05	.1293186-04	.7713723-05	.1270547-02	.8604562-01
.1750378-02	.1513511-01	.4083972-03				
.6346412+03	.2147409+02	.3337836+04	.2898596+01	.2009782+02	.1173163+01	.1000002+04
.3575168+00	.9197014-03	.1046784+01	.3130653-02	.4414487+03	.4359248+03	
.1120271-03	.1380414-04	.4506430-02	.1252088-02	.9167631-04	.1367556-03	.1709850-02
.4048302-03	.3586662-04	.6772983-03	.1225823-04	.2475255+00	.6392512-05	.1737388-01
.0000000	.1549566-01	.8677156-05	.1997895-04	.6492262-03	.5141590-04	.6476667-03
.4058352-04	.1299312-04	.0000000	.4513150-01	.1408622+00	.1355632-04	.2739400+00
.1492786+00	.6270197-05	.2157114-05	.6831396-05	.5144375-05	.2768576-03	.8748957-01
.1024954-02	.1041049-01	.2239626-03				
.6346412+03	.3769732+01	.2624198+04	.2898596+01	.2071496+02	.1202397+01	.2147775+01
.2584012+00	.7734172-03	.6747985+00	.1456191-02	.6362667+02	.4359248+03	
.1597269-04	.1425760-05	.3997242-02	.1917626-02	.3836486-03	.1417762-04	.2085972-02
.2758803-03	.4278858-05	.5562425-03	.6806218-05	.2513011+00	.6756059-06	.2175425-01
.0000000	.4314948-02	.2677630-06	.3393257-05	.1896533-03	.1399649-04	.1236444-02
.6840326-05	.6223044-05	.0000000	.1172147-01	.153[illegible]68+00	.1319798-05	.2922049+00
.1617807+00	.1348413-06	.5587857-07	.6442764-06	.1673[illegible]33-05	.6646672-04	.9055436-01
.4029394-04	.1533840-02	.9219790-05				
.6346412+03	.1256577+01	.2175088+04	.2898596+01	.2090559+02	.1232027+01	.2730635+01
.4521157+00	.6756653-03	.5446834+00	.8140033-03	-.3149984+03	.4359248+03	
.1217303-05	.1233652-06	.2602509-02	.2655842-02	.1808188-02	.9268012-06	.1805881-02
.1407762-03	.2990067-06	.3311282-03	.2244446-05	.2495366+00	.9511653-07	.2603372-01
.0000000	.8875517-03	.0000000	.5379850-06	.2259043-04	.1907144-05	.1439758-02
.3743496-06	.1978275-05	.0000000	.2384555-02	.1545429+00	.1810615-06	.3025738+00
.1616284+00	.0000000	.0000000	.8450266-07	.9841773-06	.4358066-05	.9141998-01
.9497780-06	.1689164-03	.2169419-05				
.6346412+03	.7539463+00	.1979481+04	.2898596+01	.2096765+02	.1237149+01	.3008470+01
.4962928+00	.6318374-03	.5283412+00	.6726386-03	-.4157422+03	.4359248+03	
.2021826-06	.2341599-07	.1552376-02	.2557092-02	.3723212-02	.1419706-06	.1276696-02
.7439706-04	.4724370-07	.1915195-03	.7161947-06	.2474420+00	.3194120-07	.2894670-01
.0000000	.3296726-03	.0000000	.1788665-06	.5613426-05	.5320516-06	.1463812-02
.5676256-07	.9899146-06	.0000000	.8976531-03	.1515976+00	.6098909-07	.3[illegible]69+00

Resultant Output for Case 4 (Cont'd)

.1602902+00	.0000000	.0000000	.2769061-07	.8204827-06	.8460498-06	.9169325-01
.9647754-07	.4416059-04	.2190551-07				
.6346412+03	.3769732+00	.1735652+04	.2898596+01	.2103770+02	.1248329+01	.3384292+01
.5146682+00	.5757205-03	.4946593+00	.5533381-03	-.5373824+03	.4359248+03	
.0000000	.0000000	.3842927-03	.1410561-02	.7140359-02	.0000000	.4145268-03
.1529001-04	.0000000	.4538077-04	.3712160-07	.2430831+00	.0000000	.3422911-01
.0000000	.6671202-04	.0000000	.3186651-07	.5619659-06	.6683589-07	.1475009-02
.0000000	.3331265-06	.0000000	.1863991-03	.1464963+00	.1171992-07	.3161441+00
.1569016+00	.0000000	.0000000	.0000000	.4880289-06	.6175149-07	.9200010-01
.0000000	.5120585-05	.0000000				
.6346412+03	.7539464-01	.1239137+04	.2898596+01	.2107317+02	.1273544+01	.4332024+01
.4985357+00	.4529474-03	.4391854+00	.3990244-03	-.7616922+03	.4359248+03	
.0000000	.0000000	.2557190-06	.1969111-04	.9405686-02	.0000000	.6774893-05
.0000000	.0000000	.2273234-07	.0000000	.2202908+00	.0000000	.5748200-01
.0000000	.3658016-04	.0000000	.0000000	.0000000	.0000000	.1478378-02
.0000000	.0000000	.7028104-07	.8474228-06	.1436339+00	.0000000	.3410337+00
.1344906+00	.0000000	.0000000	.0000000	.7334871-06	.0000000	.9215527-01
.0000000	.0000000	.0000000				
.6346412+03	.3769732-01	.1068909+04	.2898596+01	.2107340+02	.1267394+01	.4799935+01
.4979248+00	.4075329-03	.4469675+00	.3658262-03	-.8369689+03	.4359248+03	
.0000000	.0000000	.0000000	.1368479-05	.9425067-02	.0000000	.1249697-07
.0000000	.0000000	.0000000	.0000000	.2035910+00	.0000000	.7419196-01
.0000000	.1418848-07	.0000000	.0000000	.0000000	.0000000	.1477919-02
.0000000	.0000000	.3143899-06	.3905330-07	.1436155+00	.0000000	.3577492+00
.1177905+00	.0000000	.0000000	.0000000	.9321324-06	.0000000	.9215621-01
.0000000	.0000000	.0000000				
.6346412+03	.7539463-02	.7711565+03	.2898596+01	.2107407+02	.1241940+01	.5970672+01
.4880897+00	.3213768-03	.4845871+00	.3190706-03	-.9750578+03	.4359248+03	
.0000000	.0000000	.0000000	.0000000	.9426750-02	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.1513421+00	.0000000	.1264495+00
.0000000	.0000000	.0000000	.0000000	.0000000	.0000000	.1418790-02
.0000000	.0000000	.2991052-04	.0000000	.1436188+00	.0000000	.4100142+00
.6553907-01	.0000000	.0000000	.0000000	.2432948-05	.0000000	.9215836-01
.0000000	.0000000	.0000000				
.6346412+03	.7539463-03	.4924284+03	.2898596+01	.2113407+02	.1195000+01	.7941334+01
.5530473+00	.2292583-03	.7153479+00	.2965378-03	-.1110051+04	.4359248+03	
.0000000	.0000000	.0000000	.0000000	.9453577-02	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.8937745-01	.0000000	.1877870+00
.7090097-03	.0000000	.0000000	.0000000	.0000000	.0000000	.3457162-04
.0000000	.0000000	.7241634-03	.0000000	.1440277+00	.0000000	.4692845+00
.6166081-02	.0000000	.0000000	.0000000	.2802303-04	.0000000	.9240794-01
.0000000	.0000000	.0000000				
.6346412+03	.3769732-03	.4584027+03	.2898596+01	.2146061+02	.1122473+01	.8632748+01
.6525379+00	.2160705-03	.1713851+01	.5674959-03	-.1140703+04	.4359248+03	
.0000000	.0000000	.0000000	.0000000	.9599661-02	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.6813972-01	.0000000	.2030182+00
.5864667-02	.0000000	.0000000	.0000000	.0000000	.0000000	.1302474+04
.0000000	.0000000	.7463916-03	.0000000	.1462531+00	.0000000	.4682766+00
.4221504-02	.0000000	.0000000	.0000000	.3448310-04	.0000000	.9383268-01
.0000000	.0000000	.0000000				
.6346412+03	.7539464-04	.3995016+03	.2898596+01	.2229051+02	.1139060+01	.9519825+01
.5655087+00	.1913325-03	.1148547+01	.3885959-03	-.1203464+04	.4359248+03	
.0000000	.0000000	.0000000	.0000000	.9970897-02	.0000000	.0000000
.0000000	.0000000	.0000000	.0000000	.1858052-01	.0000000	.2372927+00
.1897670-01	.0000000	.0000000	.0000000	.0000000	.0000000	.1700275-05
.0000000	.0000000	.7811695-03	.0000000	.1519087+00	.0000000	.4612544+00
.3731506-02	.0000000	.0000000	.0000000	.4497508-04	.0000000	.9745668-01
.0000000	.0000000	.0000000				

Section 3
REACTING AND MULTIPHASE (RAMP) COMPUTER PROGRAM

A precise knowledge of local flow properties in nozzles and exhaust plumes is necessary for performance, radiation, attenuation, heat transfer and impingement analyses. The reacting and multiphase (RAMP) computer program is designed to give detailed flowfield information in the supersonic region of a reacting multiphase two-dimensional or axisymmetric flow field. The boundaries of the flow field may be solid such as in a nozzle or "free" such as in a plume. The analysis may be utilized therefore to predict performances as well as plume characteristics of a given engine system. A printed record of the program results is given for user inspection while a binary tape is provided for subsequent manipulation by other analyses. A transonic solution taken from Ref. 7 is also provided internal to the program.

The flow of a gas-particle mixture is described by the equations for conservation of mass, conservation of momentum and conservation of energy. In the gaseous phase the state variables P, ρ, R and T are related by the equation of state while for the particulate phase the equations are for the particle drag, particle heat balance and the particle equation of state. Development of these equations is based on the following assumptions:

1. The particles are spherical in shape.
2. The particle internal temperature is uniform.
3. The gas and particles exchange thermal energy by convection and radiation (optional).
4. The gas obeys the perfect gas law and is either frozen and/or in chemical equilibrium, or is in chemical non-equilibrium.
5. The pressure of the gas and the drag of the particles contribute to the force acting on the control volume.

6. The gas is inviscid except for the drag it exerts on the particles.

7. There are no particle interactions.

8. The volume occupied by the particles is negligible.

9. There is no mass exchange between the phases.

10. A discrete number of particles, each of different size or chemical species, is chosen to represent the actual continuous particle distribution.

11. The particles are inert.

The supersonic two-phase solution accepts the starting line provided by the internally calculated transonic solution as well as other pertinent data supplied through the read function. The equations of motion under the assumptions just listed are hyperbolic and permit the use of a forward marching scheme; a streamline/normal grid structure is employed where the step lengths in the axial and radial directions are under program control. Both BCD (printer) and unformatted binary output tapes are produced. A Prandtl-Meyer expansion of the gas phase and a free boundary calculation are employed to treat the plume flow solution. The run is terminated when prespecified problem limits are reached.

The two-phase flow analysis will treat an extremely wide range of operating conditions. With few exceptions the limitations are imposed by the theory rather than numerical considerations. In this discussion dimension statement sizes which are arbitrarily set are not considered a limitation. The true limitations are:

- Supersonic regions influenced by embedded subsonic regions.
- Vacuum or limiting expansion limitation — a small region of the expansion fan for a vacuum expansion cannot be treated where the Mach number is so large that treatment by continuous flow assumptions becomes meaningless (this limitation is both numerical and theoretical).

- For two-phase flow the lower boundary can only be horizontal (i.e., nozzle centerline).

A complete derivation of the governing equations are available in Volume I of this report. The characteristic equations employed in this analysis are given in Table 3-1a and 3-1b, and a list of symbols is provided in Table 3-2.

A free molecular flow calculation has been provided as an option which permits treatment of the rarefied regions of the plume. As the gas expands it first freezes out the vibrational and rotational modes. During this transition the characteristic equations continue to be employed but the equation of state is modified. At translational freezing, however, the solution switches to an effective source solution. The stream lines are considered straight and the velocity constant. Conservation of mass then determines the density while other properties are found from the equation of state.

Each of the subroutines comprising the RAMP program is listed in Table 3-3. The subroutines which call and are called by the particular routine as well as a brief statement regarding the function of the routine are also included in the table. Routines which have an asterisk in the description column are taken from the Ref. 7 analysis.

Tables 3-4a and 3-4b present a flow chart of the main routines in functional groupings for the equilibrium and finite rate versions. To attempt to completely flow chart the entire program would probably transmit less information than that given in Table 3-4 since it would be extremely complex and bulky. The functional flow chart in conjunction with Table 3-3 and the program listing is felt to be the most appropriate method for presenting the information.

Table 3-1a

ENTHALPY-ENTROPY-VELOCITY FORM OF THE COMPATIBILITY EQUATIONS FOR GAS-PARTICLE FLOW (FOR CHEMICAL EQUILIBRIUM AND/OR FROZEN FLOW APPLICATIONS)

- The variables $q, \theta, H, S, \rho^j, u^j, v^j, h^j$ completely define the gas-particle flow at a given location in the flow field.
- The slope of the gas streamline, θ, is given by

$$\frac{dy}{dx} = \tan\theta \tag{3.1}$$

and the compatibility equations which apply along gas streamlines are:

$$dH - T\,dS + \frac{1}{\rho}\sum_{j=1}^{NP} \rho^j A^j \left[(u - u^j) + \tan\theta\,(v - v^j)\right] dx = 0 \tag{3.2}$$

$$T\,dS - \frac{(C_p - R)}{q\cos\theta\,\rho R}\sum_{j=1}^{NP} \rho^j A^j B_1^j\,dx = 0 \tag{3.3}$$

where

$$B_1^j = \frac{1}{C_p/R - 1}\left\{\vec{q}\cdot\Delta\vec{q}^{\,j} - \vec{q}^{\,j}\cdot\Delta\vec{q}^{\,j} + \frac{2}{3}C^j\,(T^j - T) + \frac{3\sigma}{A^j m^j r^j}\left[\varepsilon^j\,(T^j)^4 - \alpha^j\,T^4\right]\right\} \tag{3.4}$$

$$A^j = \frac{9}{2}\left[\frac{\nu f^j}{m^j\,(r^j)^2}\right] \tag{3.5}$$

and

$$C^j = \frac{k\,G^j}{\nu f^j} \tag{3.6}$$

- The slope of the Mach lines is given by

$$\frac{dy}{dx} = \tan(\theta \mp \alpha) \tag{3.7}$$

and the compatibility equations which apply along each Mach line are:

$$d\theta \pm \frac{\cot\alpha}{q}\,dq \pm \frac{\sin\alpha\,\cos\alpha\,dS}{\gamma R} \mp \frac{\cot\alpha\,dH}{q^2} \mp \frac{\delta\,\sin\theta\,\sin\alpha\,dx}{y\cos(\theta \mp \alpha)}$$

$$\pm \frac{dx}{\rho q^2\cos(\theta \mp \alpha)}\sum_{j=1}^{NP} \rho^j A^j \left[\pm (v - v^j)\cos(\theta \mp \alpha) \mp (u - u^j)\sin(\theta \mp \alpha) + \frac{B_1^j}{q\sin\alpha}\right] = 0 \tag{3.8}$$

- The particle streamline direction, θ^j, is given by

$$\frac{dy}{dx} = \frac{v^j}{u^j} = \tan\theta^j \quad j = 1, NP \tag{3.9}$$

and the compatibility equations which apply along particle streamlines are:

$$u^j\,du^j = A^j\,(u - u^j)\,dx \quad j = 1, NP \tag{3.10}$$

$$u^j\,dv^j = A^j\,(v - v^j)\,dx \quad j = 1, NP \tag{3.11}$$

$$u^j\,dh^j = -\left[\frac{2}{3}A^j C^j\,(T^j - T) + \frac{3\sigma}{m^j r^j}\left[\varepsilon^j\,(T^j)^4 - \alpha^j\,T^4\right]\right] dx \quad j = 1, NP \tag{3.12}$$

- One additional equation for particle density is derived using the integral equation for particle mass conservation

$$d\dot{m}^j = (2\pi)^\delta\,\rho^j\left\{u^j\,(y^j)^\delta\,dy^j - v^j\,(y^j)^\delta\,dx^j\right\} \tag{3.13}$$

and δ takes on the values

δ = 0 for 2 dimensional flow
1 for axisymmetric flow

Table 3-1b

PRESSURE-DENSITY-VELOCITY FORM OF THE COMPATIBILITY EQUATIONS FOR GAS-PARTICLE FLOW (FOR CHEMICAL NON-EQUILIBRIUM AND TRANSITION FLOW APPLICATIONS)

- The variables $q, \theta, P, \rho, \rho^j, u^j, v^j, h^j$ completely define the gas-particle flow at a given location in the flow field

- The slope of the gas streamline, θ, is given by

$$\frac{dy}{dx} = \tan\theta \tag{3.1}$$

and the compatibility equations which apply along gas streamlines are:

$$q\,dq + \frac{dP}{\rho} + \frac{1}{\rho}\sum_{j=1}^{NP} \rho^j A^j \left[(u - u^j) + \frac{v}{u}(v - v^j)\right] dx = 0 ,$$

$$dP - a^2 d\rho + \frac{\psi_1}{u} dx - \frac{1}{u}\sum_{j=1}^{NP} \rho^j A^j B_1^j \, dx = 0 \tag{3.14}$$

and

$$\rho u \, dX_i - \dot{w}_i \, dx = 0 \qquad i = 1, NG \tag{3.15}$$

- The slope of the Mach lines (*left running characteristics and right running characteristics*) is given by

$$\frac{dy}{dx} = \tan(\theta \mp \alpha) \tag{3.7}$$

and the compatibility equations which apply along each Mach line are:

$$d\theta \mp \cot\alpha \frac{dP}{\rho q^2} \mp \frac{\delta \sin\theta \sin\alpha \, dx}{y \cos(\theta \mp \alpha)} \pm \frac{dx}{\rho q^2 \cos(\theta \mp \alpha)} \sum_{j=1}^{NP} \rho^j A^j \left[\pm (v - v^j) \cos(\theta \mp \alpha)\right.$$

$$\left. \mp (u - u^j) \sin(\theta \mp \alpha) + \frac{B_1^j}{q \sin\alpha}\right] \mp \frac{\dfrac{dx}{C_p/R - 1} \displaystyle\sum_{i=1}^{NG} \mu_i \dot{X}_1}{q^3 \sin\alpha \cos(\theta \mp \alpha)} = 0 .$$

- The particle streamline direction, θ^j, is given by

$$\frac{dy}{dx} = \frac{v^j}{u^j} = \tan\theta^j \qquad j = 1, NP \tag{3.9}$$

and the compatibility equations which apply along particle streamlines are:

$$u^j du^j = A^j (u - u^j) \, dx \qquad j = 1, NP \tag{3.10}$$

$$u^j dv^j = A^j (v - v^j) \, dx \qquad j = 1, NP \tag{3.11}$$

$$u^j dh^j = -\left[\frac{2}{3} A^j C^j (T^j - T) + \frac{3\sigma}{m^j r^j}\left[\varepsilon^j (T^j)^4 - \alpha^j T^4\right]\right] dx \qquad j = 1, NP \tag{3.12}$$

- One additional equation for particle density is derived using the integral equation for particle mass conservation

$$d\dot{m}^j = (2\pi)^\delta \rho^j \left[u^j (y^j)^\delta \, dy^j - v^j (y^j)^\delta \, dx^j\right] \tag{3.13}$$

and δ takes on the values

$\delta = 0$ for 2 dimensional flow
$ 1$ for axisymmetric flow

Table 3-2

LIST OF SYMBOLS

Symbol	English	Metric	Description
A^j	1/sec	1/sec	Defined in Table 3-1
B_1^j	ft^2/sec^2	m^2/sec^2	Defined in Table 3-1
C^j	$ft^2/sec^2/^oR$	$m^2/sec^2/^oK$	Defined in Table 3-1
C_p	$ft^2/sec^2/^oR$	$m^2/sec^2/^oK$	Gas specific heat at constant pressure
ϵ^j	None	None	Emissivity
f^j	None	None	Drag coefficient parameter $(C_D/C_{D_{Stokes}})$
G^j	None	None	Nusselt number parameter (Nu/Nu_{Stokes})
H	ft^2/sec^2	m^2/sec^2	Total Enthalpy
h^j	ft^2/sec^2	m^2/sec^2	Particle enthalpy
m^j	$slug/ft^3$	kg/m^3	Mass density of a jth particle
NP, NG	None	None	Number of particle sizes, number of gaseous species
Pr	None	None	Prandtl number
q	ft/sec	m/sec	Velocity
R	$ft^2/sec^2/^oR$	$m^2/sec^2/^oK$	Gas "constant" (universal gas constant/molecular weight)
r^j	ft	m	Radius of a jth particle
S	$ft^2/sec^2/^oR$	$m^2/sec^2/^oK$	Entropy
T	^oR	^oK	Static temperature
T^j	^oR	^oK	Particle temperature
u	ft/sec	m/sec	Gas axial velocity component
v	ft/sec	m/sec	Gas radial velocity component
u^j	ft/sec	m/sec	Particle axial velocity
v^j	ft/sec	m/sec	Particle radial velocity
y, x	ft	m	Radial, axial coordinates

LIST OF SYMBOLS (Continued)

Symbol	English	Metric	Description
T_o	^oR	^oK	Local total temperature
T_{o_R}	^oR	^oK	Reference total temperature
α	rad	rad	Mach angle
$\tilde{\alpha}^j$	None	None	Accommodation coefficient
γ	None	None	Isentropic exponent
$\Delta\bar{q}^j$	ft/sec	m/sec	$\bar{q} - \bar{q}_j$
δ	None	None	0 – two-dimensional, 1 – axisymmetric
θ	rad	rad	Flow Angle
ν	lbf-sec/ft^2	kg/m sec	Gas viscosity
ρ	slug/ft^3	kg/m^3	Density
ρ^j	slug/ft^3	kg/m^3	Particle density (j^{th} particle size)
σ	ft^2/sec^3	m^2/sec^3	Stefan-Boltzmann constant
μ_i	Not used	cal/gm	Chemical potential of specie i
χ_i	Not used	gm/gm	Mass fraction of specie i

Table 3-3

RAMP PROGRAM SUBROUTINE LIST

Subroutines No.	Name	Calls Following Routine(s)	Called by Following Routine(s)	Description
1	ABCALC	–	27	*
2	ALGINT	–	18, 31	log-log interpolation routine
3	AOASTR	82, 98, 116, 44, 22	74	iterative solution of area ratio as a function of Mach number
4	AVERAG	98, 21, 106, 83, 94	95	determines flow regime from Knudsen number
5	BLKDAT	–	–	block data routine
6	BOUND	47	7, 30, 49, 55, 70, 71, 74, 95	provides radial dimension and angle of bounding wall at given axial station
7	BOUNDA	41, 6, 23, 46	70, 72, 92	locates wall point when a shock wave is near a wall
8	CARCTR	77, 98, 12, 84, 114	72, 89, 91, 92	solves an interior point compatibility equation for a downstream shock wave point
9	CCALC	–	27	*
10	CHECK	93, 69, 35, 31	70, 95	adds points to or deletes points from the solution as necessary
11	CHEM	102, 85, 88	56	computes the species net rates of production as functions of temperature, density and gas composition
12	COEFEQ	–	8, 55, 95	computes coefficients used in solution of the two-phase compatibility equations
13	COEFF3	35, 69, 41, 77, 31	55, 95	computes the particle flow properties
14	DELTAF	–	24, 115	computes the turning angle through an oblique shock wave
15	DMDXSI	–	–	dummy routine not presently used
16	DOTPRD	–	112	computes the dot product of two vectors
17	DRAGCP	–	31, 77	computes the drag coefficient for the solid particle using Kliegel
18	DRAGMR	2	31, 60, 65, 77, 107	computes the drag coefficient for the solid particle using Crowe
19	DRIVER	40, 74, 108, 70	51	driving routine for main program flow
20	EMOFP	–	81	calculates Mach number from pressure and entropy
21	EMOFV	106	4, 24, 26, 31, 34, 52, 63, 65, 70, 73, 77, 78, 81, 82, 87, 89, 91, 109, 111, 115	computes Mach number from velocity
22	ENTROP	–	3, 24, 115	computes entropy rise across gas shock wave
23	ERRORS	–	7, 33, 34, 41, 52, 55, 70, 72, 81, 82, 89, 90, 91, 92, 100, 106, 109, 110	routine prints various error messages as for the appropriate flag from the calling routine
24	ESHOCK	98, 21, 75, 83, 22, 14, 115	61, 63, 90, 91, 92, 109	computes properties downstream of shock wave
25	EXPCOR	55, 41, 93, 77, 61	70	computes the flowfield points near an expansion corner
26	FABLE	96, 118, 106, 75, 21	98	routine used in determination of local dependent state properties
27	FCALC	1, 9, 68	45	*
28	FIND11	–	60, 65, 107	*
29	FNEWTN	–	34, 55, 95	determines the Newtonian impact pressure on plume free boundary
30	FREEMC	6, 43, 41, 117, 35, 69, 61, 62	70	computes flowfield properties in the free molecular flow regime
31	GAPPBI	2, 69, 98, 111, 106, 21, 75, 97, 18, 17	10, 13, 71, 95	interpolates for flow properties between two data points
32	GASRD	33, 37, 38, 36, 96, 118	74	subroutine which reads gas properties from cards

Table 3-3 (Continued)

Subroutines No.	Name	Calls Following Routine(s)	Called by Following Routine(s)	Description
33	GASTAP	36, 23, 39	32	subroutine which reads gas properties from tape and outputs on tape
34	HYPER	98, 75, 21, 29, 63, 44, 100, 105, 23	70	determines hypersonic back pressure at corner
35	IDMPFP	85	10, 13, 30, 55, 66, 70, 78, 79, 95	function to compute the particle storage location within the PFPARY array
36	IDMTAB	–	32, 33, 73	function to compute gas property storage locations within the TABB array
37	IDMXSI	–	32	function to compute gas interpolation parameter storage locations within XSIDIM array
38	IDTAPE	96	32	writes ideal gas properties on data tape
39	IMPUT	93	33	reads chemistry input data for finite rate case
40	INITP	–	40	initializes data arrays and control variables, sets convergent criterion
41	INRSCT	23	7, 13, 25, 30, 55, 70, 71, 72, 79, 89, 91, 92, 95	solves for the intersection of two straight lines
42	INTEGR	69, 112	53	integrates conservation equations along normal
43	ITERM	–	30, 70	decides whether line should be terminated due to problem limits being exceeded
44	ITSUB	–	3, 34, 52, 58, 63, 71, 76, 81, 82, 87, 89, 90, 91, 92, 100, 104, 105, 109	general purpose iteration control routine solves function of one variable
45	JAMES	27, 57	65	*
46	KIKOFF	–	7, 106, 110	provides proper termination – card reads, tape writes for internally detected errors
47	LAGRNG	–	6	interpolates for r, θ as a function of x when wall points are input
48	LEGS	–	57	*
49	LIMITS	6	70	determines whether current boundary equation still applicable
50	LIPIN	82, 111, 98	74	prepares initial data surface for simple options
51	MAIN	19	–	driver program
52	MASCON	82, 21, 83, 44, 23	74	determines startline data from mass conservation, linear Mach number variation
53	MASSCK	42, 69	70	integrates mass flow, determines cumulative error in mass flow
54	MAXTIM	–	62, 70	Univac 1108 system routine for checking run time against input variable for cutting off run before maxtime is reached
55	MOCSOL	77, 69, 35, 105, 75, 41, 6, 84, 13, 56, 29, 81, 113, 12, 111, 23, 93	25	solves the characteristic equations in continuous regions, calling arguments control type of solution i.e., upper boundary, lower boundary, interior, single phase only
56	NEWENT	11	55, 95	computes entropy and enthalpy/OF change along a streamline
57	NEWT	48	45	*
58	NORSCK	104, 44	61	calculates pitot total pressure for finite rate case
59	NUSNUP	–	–	dummy routine presently not used
60	ONED	28, 18	65	*
61	OUT	64, 58, 24, 98, 75, 77, 112, 69, 93	25, 30, 70, 91	performs bulk of printed output function; outputs are flowfield data points
62	OUTBIN	54, 69, 97	30, 70	performs unformatted binary output of flowfield data on a magnetic tape

Table 3-3 (Continued)

Subroutines No.	Name	Calls Following Routine(s)	Called by Following Routine(s)	Description
63	OVEREX	98, 21, 24, 75, 44, 111, 69, 35	34	computes corner condition for over-expanded flow situation
64	PAGE	–	61, 65, 67, 73	writes page headings
65	PARTIL	60, 45, 80, 28, 18, 114, 107, 64, 93, 98, 21, 106	108	*
66	PARTIN	82, 110, 103, 75, 93, 98, 35, 69	74	reads gas and particle flow properties from tape or cards
67	PARTPH	64	74	reads input and sets up data table of particle T versus h
68	PCALC	–	27	*
69	PFP	85	10, 13, 30, 31, 42, 53, 55, 61, 62, 63, 66, 70, 71, 73, 77, 78, 79, 95, 101	computes the particle property data storage location and retrieves data from the PFPARY array
70	PHASE1	93, 77, 61, 53, 101, 62, 6, 109, 21, 103, 75, 92, 95, 54, 49, 7, 69, 35, 41, 91, 19, 30, 98, 111, 43, 79, 78, 25, 34, 81, 113, 100, 23	19	this subroutine performs the overall control for the entire flowfield solution, selectively calling those calculations which are pertinent to the particular mesh construction as well as the highest level logic routine combining point or limited region solutions into an entire field solution
71	PHYSOL	69, 46, 98, 44, 31, 77, 6, 111	89, 91, 92, 95	computes intersection of physical characteristics with a "normal" data line
72	PHYZOL	7, 41, 23, 98, 111, 8	92	computes intersection of characteristics with "normal" at a downstream shock point
73	PLMOUT	64, 96, 36, 98, 21, 69	74	this routine outputs the input data
74	PLUMIN	73, 32, 86, 6, 3, 52, 50, 66, 67	19	this routine provides the control for all input functions by selectively calling pertinent input routines and/or calls transonic solution
75	POFEM	–	24, 26, 31, 34, 55, 61, 63, 66, 70, 77, 78, 81, 83, 87, 89, 91, 115	computes pressure as a function of Mach number and entropy
76	POFH	44	105	computes pressure as a function of velocity and enthalpy
77	PPATPT	98, 106, 21, 75, 69, 97, 17, 18	8, 13, 25, 55, 61, 70, 71, 79, 92, 95	calculates and stores gas and particle dependent variables as a function of the independent flow variables
78	PRANDT	98, 100, 111, 21, 106, 75, 105, 93, 69, 35	70	provides overall control of Prandtl-Meyer corner calculation
79	PRFRBD	69, 41, 35, 77	70	computes flow properties at a particle limiting intersection with a plume boundary
80	PROP	–	65, 107, 114	*
81	RGMOFP	98, 96, 113, 20, 75, 21, 44, 23	55, 70, 95	iterative solution for Mach number as a function of pressure
82	RGVOFM	98, 96, 113, 21, 44, 23	3, 50, 52, 66	iterative solution velocity as a function of Mach number
83	RHOFEM	75	4, 24, 52, 115	density as a function of Mach number
84	ROTERM	-	8, 55, 95	rotational term in method of characteristics equation
85	RWU	–	11, 35, 69, 93	Univac 1108 machine language routine to access temporary storage
86	SETHTG	102, 98	74	computes 1-dimensional startline properties for a constant startline property finite rate case
87	SITER	96, 21, 75, 44	65	computes entropy as a function of pressure, total enthalpy and velocity
88	SLDP	–	11	solves a set of N simultaneous linear equations using the Gauss-Gordan reduction algorithm with the diagonal pivot strategy
89	SLPLIN	41, 71, 8, 75, 21, 44, 23	91, 95	performs the slip line calculations

Table 3-3 (Continued)

Subroutines No.	Name	Calls Following Routine(s)	Called by Following Routine(s)	Description
90	SOKFLX	24, 44, 23, 98, 111	–	computes the flow properties downstream of a reflected shock
91	SOKINT	21, 41, 95, 23, 61, 24, 111, 109, 75, 44, 71, 8, 89, 98	70	computes the flow properties at the intersection of shock waves of the opposite family
92	SOKSOL	41, 95, 111, 24, 98, 72, 71, 8, 44, 7, 23, 77	70	provides control for a shock point solution
93	SPCTX	85	10, 25, 39, 55, 61, 65, 66, 70, 78, 95	reads from or writes on data files the species mole fraction for each point (finite rate version only)
94	STGMOD	–	4	computes gas thermodynamic properties in the transition flow regime
95	STRNOR	93, 69, 35, 77, 111, 41, 89, 71, 31, 13, 84, 56, 12, 29, 4, 81, 113, 10, 6	70, 91, 92	this subroutine provides the regional control for the streamline/normal solution. It has a lower level of logical control than PHASE1 (70) being interested only in determining the location and flow properties of a single new mesh point
96	TAB	–	26, 32, 38, 73, 81, 82, 98, 108	computes the thermodynamic data storage location and retrieves data from the TABB array
97	TEMTAB	–	31, 62, 77	performs table lookup for particle T = f(h) or h = f(T)
98	THERMO	96, 26, 99	3, 4, 8, 24, 31, 34, 50, 61, 63, 65, 66, 70, 71, 72, 73, 77, 78, 81, 82, 86, 87, 90, 91, 92, 100, 109, 115	provides control of interpolation of gas thermodynamic and transport properties
99	THERM1	102, 105	98	computes gas properties as a function of total enthalpy, velocity, temperature and species mole fractions
100	THETPM	98, 106, 105, 44, 23	34, 70, 78	this subroutine evaluates Prandtl-Meyer equation
101	THRUST	69, 112	70	starting line integration and wall pressure integration are performed here
102	TKEY	–	11, 86, 99, 104, 105	computes and interpolates thermodynamic properties from thermodynamic tables which are input
103	TOFEM	–	66, 70, 113	computes temperature as a function of Mach number
104	TOFENH	102, 44	58	computes temperature as a function of total enthalpy and velocity
105	TOFH	102, 44, 76	35, 55, 78, 99, 100	computes temperature as a function of total enthalpy, velocity and species mole fractions
106	TOFV	23, 46	4, 21, 26, 31, 65, 77, 78, 100	computes temperature as a function of velocity
107	TRACE	80, 28, 18	65	*
108	TRANS	96, 65	19	*
109	TURN	98, 21, 110, 24, 44, 111, 23	70, 91	computes shock angle and downstream properties for known turning angle
110	UOFEM	23, 46	66, 109, 111	Mach angle as a function of Mach number
111	UOFV	110, 21	8, 31, 50, 55, 63, 70, 71 72, 78, 90, 91, 92, 95, 109	Mach angle as a function of velocity
112	VEMAG	16	42, 61, 101	computes magnitude of a vector
113	VOFEM	103	55, 70, 81, 82, 95	computes velocity as a function of Mach number
114	WDGI	80	65	*
115	WEAK	98, 21, 75, 83, 22, 14	24	computes properties downstream of an ideal gas shock wave

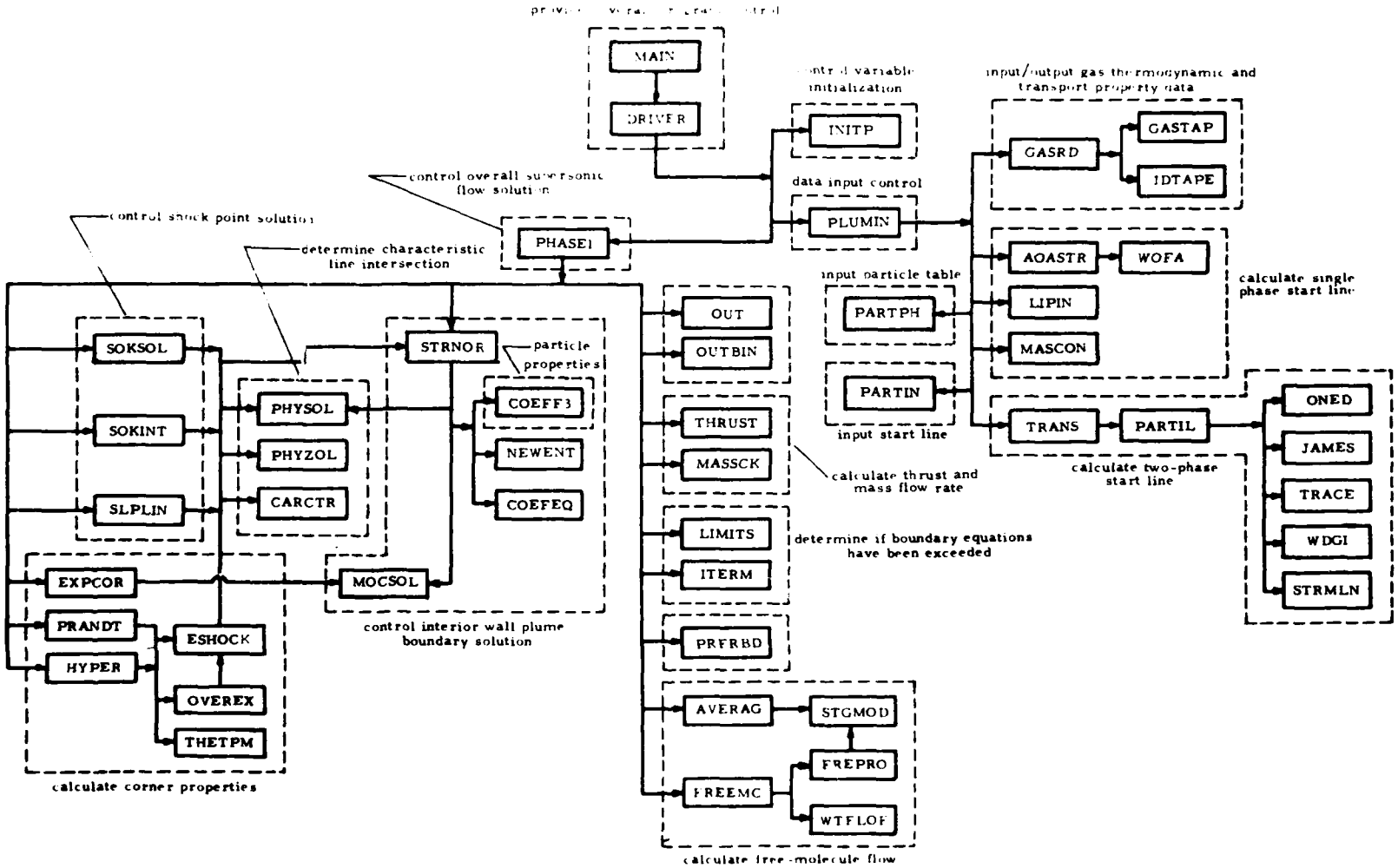
Table 3-3 (Concluded)

Subroutines No.	Name	Calls Following Routine(s)	Called by Following Routine(s)	Description
116	WOFA	–	3, 24	one-dimensional mass flow as a function of area relation
117	WTFLOF	–	30	computes area bounded by two data points
118	XSI	–	26, 32	computes storage location and retrieves data from the XSIDIM array

*Reference 7

Table 3-4a

BASIC RAMP FLOW CHART BROKEN DOWN INTO FUNCTIONAL GROUPINGS FOR THE EQUILIBRIUM CHEMISTRY VERSION



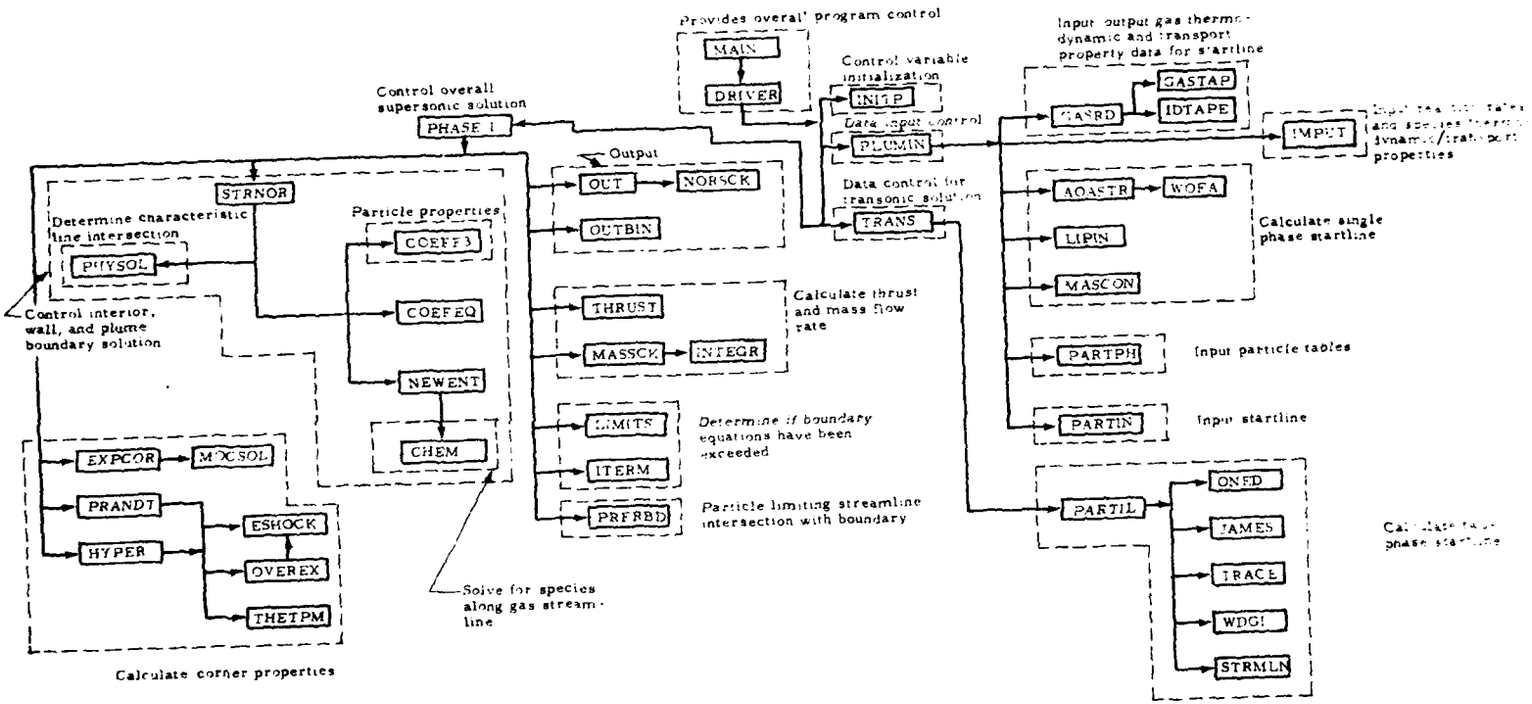


Table 3-4b - Basic RAMP Flow Chart Broken Down into Functional Groupings for the Finite Rate Chemistry Version

3.1 CAPABILITIES AND LIMITATIONS

The RAMP computer program described in this document can be used to solve a wide variety of problems associated with real gas, supersonic, compressible flow. Some of the more important, basic capabilities of the existing program are outlined below:

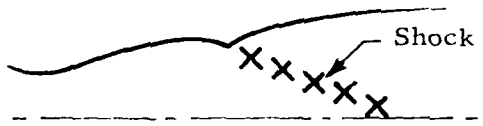
- The gas may be ideal or real. If the gas is real; frozen, equilibrium, or non-equilibrium chemistry assumptions can be made. The effects of oxidizer/fuel gradients may be considered.
- Two-dimensional or axisymmetric flow problem geometries can be used.
- Both upper and lower boundaries can be solid or free. (A solid boundary can be approximated by either a conic or polynomial equation.) (Two-phase problems require the nozzle centerline as a lower boundary).
- A nozzle wall may be curve fit with discrete points.
- Compression corners on the upper wall can be calculated.
- Any number of expansion corners can be considered on either the upper or lower wall.
- Various methods for obtaining an initial start line are utilized.
    1. The program will calculate a one-dimensional start line anywhere in the nozzle.
    2. The program will calculate a start line at points within the nozzle necessary to conserve mass.
    3. Data on a normal surface can be input at points across the flow field within the nozzle or in the plume.
    4. An exit plane startline can be punched.
    5. The program can be restarted from the startline punched in 4 above.
- Hypersonic or quiescent approach flow options may be used.
- Exit to ambient pressure ratios from over-expanded to highly under-expanded are possible.
- Displacement of the axis of symmetry from the center of flow (i.e., the plug nozzle flow field) is possible (for gas only cases).

- Due to computer core size limitations the code presently consists of two versions: (1) an equilibrium chemistry version, and (2) a finite rate chemistry version. The finite rate version has all the capabilities of the equilibrium programs with the following exceptions:

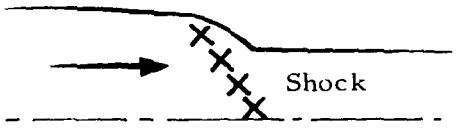
  1. Free molecular flow
  2. Shock Waves

  It is anticipated that one version will be released at a later date.

- The equilibrium version which accompanies this documentation will handle only attached (over-expanded nozzles or compression corners) right-running shocks (see sketch below). The logic for calculating left-running shocks, and coalescing shocks is in the code but has not been thoroughly checked out. When check out is completed, the program modifications will be forwarded to users.



Over-Expanded Nozzle with Right-Running Shock



Attached Right-Running Shock

- There is presently a maximum of 100 points on a normal and 50 input points.

- Reacting gas solutions which are in chemical equilibrium have been facilitated by modifying the TRAN72 computer program as described in Section 2 to provide binary tape and punched output of its equilibrium or frozen real gas calculations at any desired O/F ratio(s). The RAMP program has the capability for selecting the proper case from a large set of real gas properties cases stored on a master tape. The method of generating this master tape is outlined in Table 3-5. Cases stored are uniquely identified by some characteristic of the particular gas under consideration. For example, a LOX/LH_2 system may be identified by the following:

Gas Type	Mixture Ratio	Chamber Pressure
O2/H2	O/F = 1.5 - 8.0	PC = 546.0

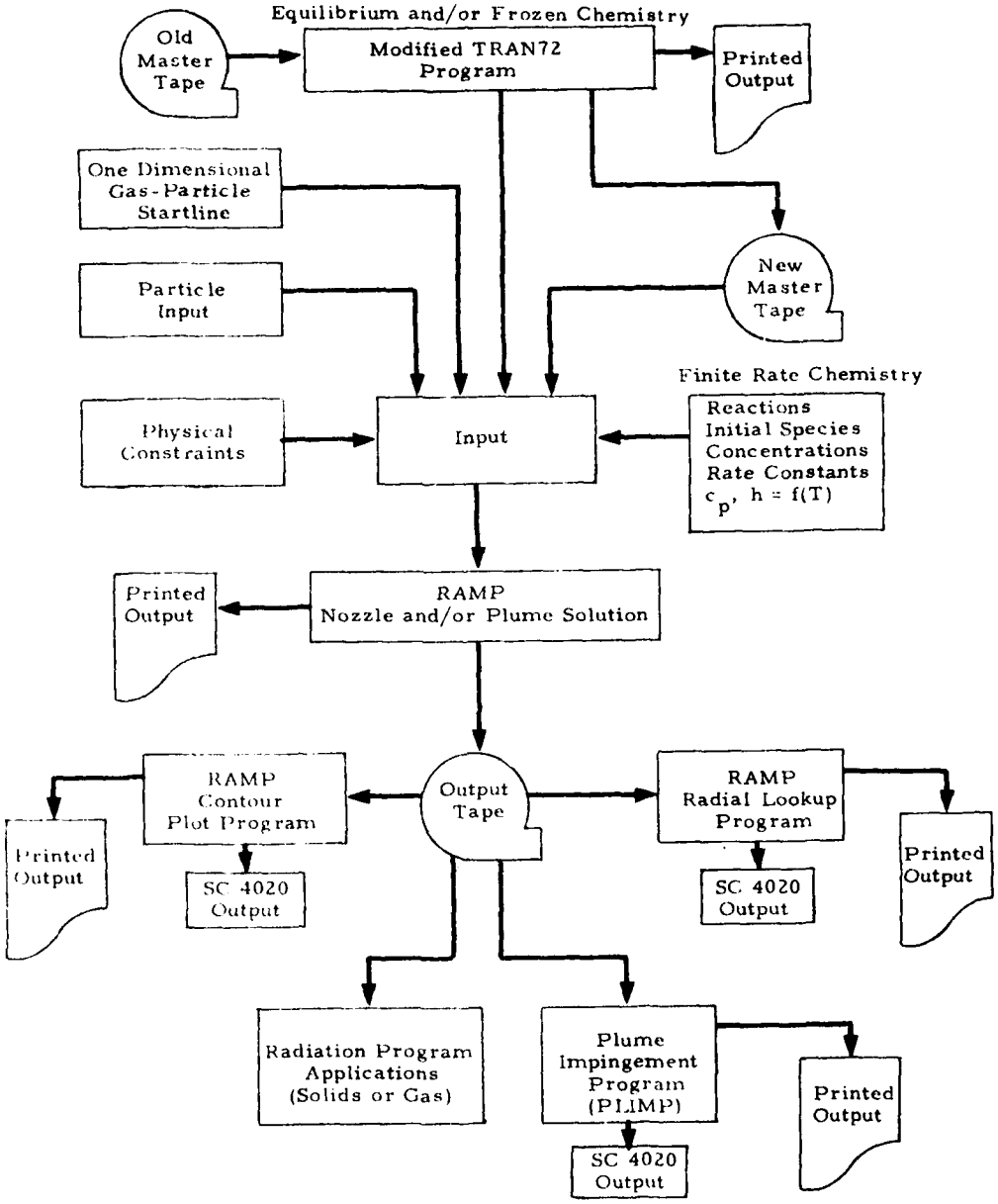
New cases of general interest may be added to the master tape; however, ad hoc cases should be prepared on a separate tape. Tape preparation sequence and communication with the RAMP program is diagrammed in Table 3-5.

- Once the gas-particle flowfield solution has been obtained, the output tape may be used by the RAMP Radial Lookup Program (described in Appendix A) which determines the radial variations of flowfield properties across the nozzle and plume flowfields at constant axial stations. The Plume Impingement Program (PLIMP) (Ref. 9) may also be run to determine the effects of the rocket exhaust plume on objects immersed in the plume. Sequencing and communication of auxiliary programs with the RAMP program is shown in Table 3-5.

- Two-dimensional or axisymmetric solutions are selected by simply loading a control word in the program input data. This integer (0 or 1) is then multiplied by the term containing (1/r) in the governing differential equation. By appropriate description of the flow boundaries, it is possible to change from a solid to free boundary on either the upper or lower walls. Conversely, it is not possible to change from a free to a solid boundary on either wall.

Table 3-5

SEQUENCING AND COMMUNICATION OF AUXILIARY PROGRAMS WITH THE RAMP PROGRAM



3.2 USER'S INPUT GUIDE FOR THE RAMP PROGRAM

This section outlines in detail the procedures for using the Reacting and Multi-Phase (RAMP) Computer Program. Each card and its use is explained in Section 3.2.1. The program magnetic tape assignments are given in Table 3-6.

3.2.1 RAMP Program Input Information

The input data are organized into sections determined by their use. The description of these cards is given below.

RAMP Computer Program Input Instructions

Cards 1-3 — Problem Description Required — Format 3(20A4)

Column	Parameter	Description
1-240	HEADER	Problem description may be put on three cards; however only the first 120 columns will be printed while all 240 characters will be written on the data tape. All three cards must be present even if biank.

Card 4 — Run Control Card Required — Format 16I5 (Right Adjusted)

Column	Parameter	Value	Description
5	ICON(1) Gaseous thermodynamic data control parameter	1	The gas composition is either chemically frozen and/or in chemical equilibrium. The gas properties are read directly from cards 8, 9, 10 and 11.
		2	Same as ICON(1)=1 except gas properties are read directly from a data tape mounted on FORTRAN unit 10.
		3	The gas composition is in chemical non-equilibrium. The gas properties are determined, as a function of temperature in thermodynamic data tables input on cards 13.

Card 4

Column	Parameter	Value	Description
5	ICON(1)	4	Same as ICON(1)=3 except gas composition is chemically frozen.
8-9	NTAPE	N	If ICON(2)=2, tape unit number for startline if not input from cards. The program defaults to unit 5 (read cards) for ICON(2)=2. If ICON(2)≠2 and a two-phase transonic solution is being performed NTAPE is the unit on which the transonic startline will be written. In this case the program defaults to unit 8.
10	ICON(2) Start line control parameter for gas only solution	0	Generate straight startline with Mach number given.
		1	Generate source startline with A/A^* given
		2	Startline input from cards or tape.
	or	3	Generate startline by conservation of mass using a linear Mach number distribution.
	Startline control parameter for gas-particle solution	0	Generate startline using transonic approximation.
		2	Startline input from cards.
13	ICON(3) Control manner in which points along the startline are spaced	0	Points are spaced according to a sine distribution.
		1	Points are evenly spaced (recommended)
		2	Points are evenly spaced on a circular arc based on the input value of the upper limit of the startline (card 18.CORLIP(2))
			NOTE: This option is necessary only if program is to set up its own gaseous startline.
14, 15	ICON(3)		Number of startline points. Maximum of 50 (right adjust)**

**NOTE: If particles are present and supersonic startline is generated by transonic approximation then total number of points on startline may be adjusted by transonic program depending on particle distributions.

Card 4 (Continued)

Column	Parameter	Value	Description
16-20	ICON(4) Number of upper boundary equations		Upper boundary specification indicator. If specifying upper boundary by equations, set equal to number of equations to be used. Maximum of 100. Right adjust.

Option for ICON(4) when upper boundary is described by individual points and slopes

ICON(4)

1N000 + Number of discrete points (no boundary equation following last point) (slope at each point in radians)

2N000 + Number of discrete points + 1 (an upper boundary equation follows last point) (slope at each point in radians)

3N000 + Number of discrete points (no boundary equation following last point) (slope at each point in degrees)

4N000 + Number of discrete points + 1 (an upper boundary equation follows last point) (slope at each point in degrees)

N ~ number of points to use for Lagrangian Integration (5 max).

If N is set to zero, a linear assumption will be made.

NOTE: If a nozzle is being run the throat must also be specified by discrete points.

Column	Parameter	Value	Description
21-25	ICON(5) Number of lower boundary equations		Lower boundary specification indicator. Same description and option as ICON(4).
30	ICON(6)	0	Not presently used
35	ICON(7) Flow type option	0	Two-dimensional flow problem geometry.
		1	Axisymmetric flow problem geometry.
38	INOZ	2	Calculations terminated at nozzle exit.
39	ICON(8) Data output control, used in conjunction with ICON(16)	0	Full printout
		1	Print only boundary, shock, input, Prandtl-Meyer, and particle limiting streamline points.

Card 4 (Continued)

Column	Parameter	Value	Description
40	ICON(8)	1	Print 1 line (R, X, M, θ, S and shock angle)
		2	Print above plus Mach angle, P, ρ, T, V.
		3	Print all of above plus MWT, γ, TO*, PO*, S*.
42	MORFT Compliments ICON(9)		For English system of units.
		0	Dimensions are in feet.
		1	Dimensions are in inches.
			For metric system of units.
		2	Dimensions are in centimeters.
		3	Dimensions are in meters
		4	System of units specified by user.
43	ICON(9) Units indicator	0	Use English system of units.
		1	Use metric system of units.
			This option controls the units in which the flow field is calculated. The program assumes that the boundary equations are input in the same units as the units indicator (ICON(9)). This option will not override the units specification on cards 8 and 30 but will convert the units of the gas and particle thermodynamics to correspond to the units of this indicator.
44-45	ISPECS		Number of discrete particle sizes used to represent particle distribution (10 max). If gaseous only flow set equal to 0 (right adjust).
48-50	ICON(10)		Maximum iterations allowable for each point in flow field. If set to 0 program assumes value of 100. Right adjust.
51-55	ICON(11)		Case number printed at top of each page.
60	ICON(12)	0	Calculate shock wave.
		1	No rotation option.
61	ICON(13)	0	Flowfield data will be output on FORTRAN unit 3.
		1	Data will not be written on tape.

Card 4 (Concluded)

Column	Parameter	Value	Description
65	ICON(13)	0	Free molecular calculations will not be considered.
		1	Free molecular calculations will be considered.
68-70	ICON(14)	0	No intermediate printout in solution iteration.
		N	Print intermediate results for N^{th} line. Right adjust.
71-75	ICON(15)	0	No intermediate printout.
		M	Print intermediate results from M^{th} point on each line from the Nth (ICON(14)) line on. Right adjust.
76	ICON(16)	0	No punched cards output.
		1	Punch data line at nozzle exit
77-78	ICON(16)	0	Print every line.
		N	Print every N^{th} line (use with ICON(8)). Put 0 in column 77 if N < 10.
79-80	ICON(16)*		Time (SEC) before end of allotted run time when new startline is to be punched. Put 0 in column 79 if time less than 10 seconds.

Card 5 — Finite Rate Chemistry Run Control Card (Required if ICON(1)>2) — Format 8I5 (Right Adjusted)

Column	Parameter	Value	Description
1-5	NT		Number of temperature points in thermodynamic data tables.
6-10	NS		Number of gaseous species (excluding 3rd bodies)
11-15	NM		Number of 3rd bodies.
16-20	NR		Number of reactions specified.
25	NPRINT	0	No intermediate printout in chemistry calculations.
		1	Echo print of input data.
		2	Print intermediate results of chemistry calculations.

*NOTE: Applicable for Univac 1108 only.

Card 5 (Continued)

Column	Parameter	Value	Description
30	ICTAPE	0	Species concentrations for start-line read directly from cards.
		1	Species concentrations read directly from a data tape mounted on FORTRAN unit 10.
35	KGUP	≥ 2	Number of normals calculated before finite rate chemistry contributes to dS and dH.
40	IDIDO	0	Uniform species concentrations along startline.
		1	Non-uniform species concentrations along startline.

Card 6 Upper Boundary Description Required

If ICON(4) < 10000 use following format (I1, 3X, I1, 5X, 6E10.6).

Column	Parameter	Value	Description
1	IWALL(K, 2)	1	Conic equation $R = A[(B+CX+DX^2)^{1/2}+E]$ Represents throat region. (See page 3-27 for an example and description.)
		2	Polynomial equation $R = AX^4+BX^3+CX^2+DX+E$
		3	Free boundary equation $P = P_\infty(1+E_\infty X)(1+\gamma_\infty(M_\infty \sin(\theta_B-\theta_\infty))^2)$ (See page 3-27 for an example and description.)
		6	Same as IWALL=3 except oblique shock solution for plume boundary. Use if $1.5 < M_\infty < 5.5$.
5	ITRAN(K, 2)	0	No discontinuity follows this equation.
		1	Expansion corner follows.
		2	Compression corner follows.

Card 6 (Continued)

Column	Parameter	Value	Description
11-20	WALLCO(K, 1, 2)		Coefficient A or P_∞ (psfa or N/m^2). (Units must be consistent with R in ft or m.)
21-30	WALLCO(K, 2, 2)		B or γ_∞
31-40	WALLCO(K, 3, 2)		C or M_∞
41-50	WALLCO(K, 4, 2)		D or θ_∞ (deg)
51-60	WALLCO(K, 5, 2)		E or E_∞
61-70	WALLCO(K, 6, 2)		Maximum value of X applicable to equation (feet if ICON(9)=0 meters if ICON(9)=1).
71-80	RSTAR		Throat radius (ft or m) required only on card for last equation. This is required for two-phase transonic solution only.

If 10000 < ICON(4) < 20000 use following format (I5, 5X, 3E10.6, I5, 5X, 3E10.6).

Column	Parameter	Value	Description
5	ITRANS(K, 2)		Same as before.
11-20	WALLCO(K, 3, 2)		Axial displacement (X) of point K (ft or m).
21-30	WALLCO(K, 1, 2)		Radial displacement (R) of point K (ft or m).
31-40	WALLCO(K, 2, 2)		Wall angle (θ) at point K (rad).
45	ITRANS(K+1, 2)		Same as before.
51-60	WALLCO(K+1, 3, 2)		X at point K+1 (ft or m).
61-70	WALLCO(K+1, 1, 2)		R at point K+1 (ft or m).
71-80	WALLCO(K+1, 2, 2)		θ at point K+1 (rad).

NOTE: Card 6, in the above format, is repeated for each equation until all necessary equations have been input. That is, repeat Card 6, in succession in order of increasing XMAX, for K=1, 2, . . . , ICON(4). All units for lengths for two-phase calculations are consistent with ICON(9), otherwise units for lengths are input at user's discretion.

Repeat Card 6, in above format, in succession, and in order of increasing X, until all required points have been input.

If 20000 < ICON(4) < 30000 the above format is used except the last segment of the upper boundary is input via an equation. The equation is input with the format for ICON(4) < 10000 except the throat radius RSTAR is not required.

If 40000 < ICON(4) < 50000, the format for 20000 < ICON(4) < 30000 is used except θ is input in dimension of degrees.

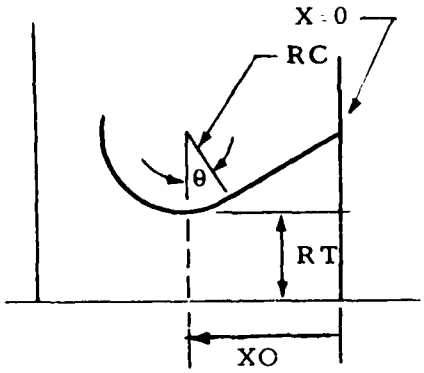
Card 6a Format E10.6

Card 6a is used only when running a two-phase case where the upper boundary (nozzle wall) is specified by discrete points (ICON(4) > 10000). Do not input this card for any other cases.

Column	Parameter	Value	Description
1-10	RSTAR		Throat radius (ft or m).

Card 7 Lower Boundary Description Required

The formats and options for Card 7 are controlled by ICON(5) and are the same as for Card 6 (Upper Boundary) with the following exceptions: (1) the distance from the nozzle throat to the center (X=0) of the coordinate system for the wall equations is read in place of RSTAR. This is only necessary for two-phase cases where a transonic solution is desired and where $X \neq 0$ at the nozzle throat. This distance is positive if the center of the coordinate system is downstream of the throat and negative if the center of the coordinate system is upstream of the throat. It is not possible to run a two-phase case with the lower boundary specified by points, therefore there is no Card 7a; (2) the indices of the parameters are (–, –, 1) instead of (–, –, 2), e.g., WALLCO(K, 1, 1) instead of WALLCO(K, 1, 2). A nozzle throat region showing the coefficients of a circular throat and free boundary are shown in the sketch on the following page.



RC = radius of curvature of the circular arc of the throat
RT = throat radius
XO = axial distance from the origin of the coordinate system to the throat
θ = throat divergence angle corresponding to the maximum value for which the throat conic equation applies

The conic equation for this case would have the following form:

A = -1 for an upper equation, +1 for a lower equation (-1 for this case)

$B = RC^2 - XO^2$

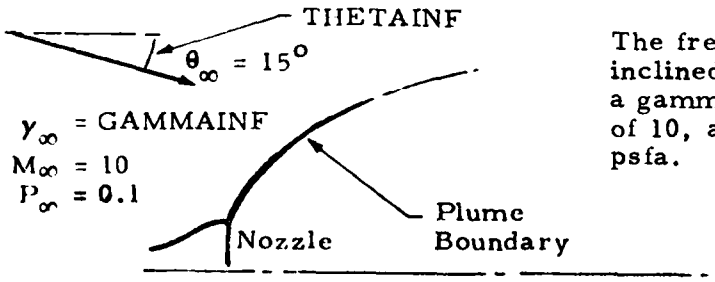
$C = 2XO$

$D = -1$

$E = -(RC + RT)$

$Xmax = RC \sin\theta + XO$

An example of a free boundary is shown in the sketch below.



The freestream approach flow is inclined at 15 deg to the plume with a gamma (γ) of 1.4, a Mach number of 10, and a static pressure of 0.1 psfa.

PINF = 0.1 (psfa)
E = 0 (No pressure variation with axial distance)
GAMMAINF = 1.4
MINF = 10
THETAINF = -15°

Card 8 Gas Property Control Format 6A4, 5X, A3, 6X, I2, 3X, I2

This card is required whether gas data input by cards or tape.

Column	Parameter	Description
1-24	ALPHA(I)	Gas name for real gas on tape (see Section 2, page 3). If inputting gas data via cards, may be any name.
30-32	UNITS (Independent of ICON(9))	ENG Input gas data with English units (cards only). MKS Metric units (cards or tape).
39-40	IOF	Number of O/F tables for gaseous only solution or number of gas total enthalpy tables for two-phase solution
44-45	IS	Number of entropy tables per IOF entry, 1 for gas, 2 maximum for gas chemical equilibrium solution.

Card 9 Mixture Ratio or Total Enthalpy (This card is not used if ICON(1)$\geq$2) Format E10.6, 8X, I2

Column	Parameter	Description
1-10	OFRAT(M)	For gaseous only flow input O/F ratio, for particle flow input gas total enthalpy (cal/gm for metric, Btu/lbm for English, units specified by Card 8).

Card 10 Entropy (This card is not used if ICON(1)$\geq$2) Format E10.6, 8X, I2

Column	Parameter	Description
1-10	STAB(M, I)	Entropy of gas (cal/gm-^{o}K or Btu/lbm-^{o}R, units specified by Card 8).
19-20	IVTAB(M, I)	Number of Mach numbers for this entropy value (13 max).

Card 11 — Gas Properties (This card is not used if ICON(1)$\geq$2; units specified by Card 8) — Format 8E10.6

Column	Parameter	Description
1-10	XSIDIM(1)	Mach number associated with above entropy.
11-20	XSIDIM(2)	Molecular weight of gas (gm/g-mole or lbm/lb-mole).
21-30	XSIDIM(3)	Gamma (C_p/C_v)
31-40	XSIDIM(4)	Temperature (^oK or ^oR)
41-50	XSIDIM(5)	Pressure (atm)
51-60	XSIDIM(6)	Prandtl number (dimensionless)
61-70	XSIDIM(7)	Absolute viscosity (poise)
71-80	XSIDIM(8)	Ideal gas (1 velocity cut per table) — viscosity temperature exponent. Real gas — C_p (cal/gm-^oK or Btu/lbm-^oR).

To illustrate the arrangement of Cards 9, 10 and 11, let IOF=2 and IS=2; then the proper arrangement is:

```
Card 9
     10
     11  (1-13 such cards)
     10
     11  (1-13 such cards)
      9
     10
     11  (1-13 such cards)
     10
     11  (1-13 such cards)
```

Card 12 — Gas Properties (This card is required if ICON(1)>2) — Format 3E10.6

Column	Parameter	Default Value	Description
1-10	PR	0.7	Prandtl number (dimensionless).
11-20	VISO	1.0E-04	Absolute Viscosity (poise).

Card 12 (Continued)

Column	Parameter	Default Value	Description
21-30	EX	0.6	Viscosity temperature exponent.

Cards 13 Gas Thermodynamic Data (The following cards are required if ICON(1)>2)

The following set of cards contain species thermodynamic data. The first card contains the species name, molecular weight and heat of formation. The second and remaining cards contain the temperature and corresponding specific heat, entropy and enthalpy for that species. Two temperatures and corresponding thermodynamic data are placed on each card. The input table can contain up to a maximum of 30 temperature points. The data are input exactly as presented in the JANAF tables (Ref. 10) with the temperature points being the same for all species. Cards 13.1, 13.2, 13.3, etc., are repeated for each species.

Card	Column	Description	Format
13.1	1-6	Name of first species	A6
	7-16	Molecular weight	E10.3
	17-26	Heat of formation, h_{298_i} (kcal/mole)	E10.3
13.2	1-10	First temperature point (^oK)	F10.4
	11-20	c_{p_i} (cal/mole-^oK)	F10.4
	21-30	S_i (cal/mole-^oK)	F10.4
	31-40	$h_i - h_{298_i}$ (kcal/mole)	F10.4
	41-50	Second temperature point (^oK)	F10.4
	51-60	c_{p_i} (cal/mole-^oK)	F10.4
	61-70	S_i (cal/mole-^oK)	F10.4
	71-80	$h_i - h_{298_i}$ (kcal/mole)	F10.4
13.3	1-10	Third temperature point	F10.4
		⋮	
		etc.	

Cards 14 Catalytic Species Weighting Factor Data
(The following cards are required if ICON(1)>2 and NM>0)

The following set of cards specify the catalytic species (M1, M2, M3, . . .) and their respective composition in terms of the species participating in the reactions. Weighting factors must be read in the same order in which the thermodynamic data sets are read.

Card	Column	Description	Format
14.1.1	1-6	AID(NS+1) — Name of first catalytic species (e.g., M1)	A6
14.1.2	1-5	WF(1, 1) — Weighting factor of first species (for first catalytic species). Set weighting factor to zero for any reactant which does not contribute to the respective catalytic species.	16F5.2
	6-10	WF(1, 2) — Weighting factor of second species contributing to first catalytic species.	
	⋮		
	75-80	WF(1, 16) — Weighting factor of 16th species contributing to first catalytic species.	
14.1.3	1-5	WF(1, 17) — Weighting factor of 17th species contributing to first catalytic species, etc.	16F5.2
14.2.1	1-6	AID(NS+2) — Name of second catalytic	A6
14.2.2	1-5	WF(2, 1) — Weighting factor of first species contributing to second catalytic species, etc.	16F5.2
14.NM.1	1-6	AID(NS+NM) — Name of last catalytic species, etc.	A6

Cards 15 Chemical Reaction Mechanisms
(The following cards are required if ICON(1)>2 and NR>2)

The following set of cards specifies the chemical reaction mechanisms for a particular problem, one card for each reaction. No particular order is required.

Card	Column	Description	Format
15.1	1-6	Species A	A6
	7	+ sign	
	8-13	Species B (or M)	A6

AD-A094 633 LOCKHEED MISSILES AND SPACE CO INC HUNTSVILLE AL HUN--ETC F/G 21/8.2
SUPERSONIC FLOW OF CHEMICALLY REACTING GAS-PARTICLE MIXTURES. V--ETC(U)
JAN 76 M M PENNY, S D SMITH, P G ANDERSON NAS9-14517
UNCLASSIFIED LMSC-HREC-TR-D496555-2 NL

2 OF 5
AD
A094633

Cards 15 (Continued)

Card	Column	Description	Format
15.1	14	+ sign	
	15-20	Blank (or M)	6x(A6)
	21	= sign	
	22-27	Species C	A6
	28	+ sign (if needed)	
	29-34	Species D (or M)	A6
	35	+ sign (if needed)	
	36-41	Species E (or M)	A6
	42-48	Blank	
	49-50	Reaction type, 1 to 12	I2
	51	Rate constant type, 1 to 5	I1
	52-59	A, pre-exponential factor (cm-particle-sec units)	E8.2
	60-64	N, temperature exponent	F5.2
	65-74	B, activation energy (cal/mole)	F10.1
	75-80	M, temperature exponent	F6.2
15.2		Next reaction	
15.NR		Last reaction	

Cards 16 Startline Data (The following cards are required if ICON(1)>2 and ICTAPE=0) Format 7E10.3

The following cards contain the species mole fractions on the startline. Mole fractions must be read in the same order in which the thermodynamic sets are read.

Card	Column	Description
16.1	1-10	Mole fraction of first species at the first point on the startline.
	⋮	
	61-70	Mole fraction of seventh species at the first point on the startline.

Cards 16 (Continued)

Card	Column	Description
16.2	1-10	Mole fraction of eighth species at the first point on the startline.
	⋮	
	61-70	Mole fraction of the fourteenth species at the first point on the startline.
		⋮
		etc.

Cards 16.1 and 16.2, etc., are repeated for each point on the startline. For a uniform startline (IDIDO=0), mole fractions are read for 1 point only.

Card 17 Chamber Condition Data (This card is used if ICON(1)>2 and ICTAPE=0) Format 2E10.3

Column	Parameter	Description
1-10	PC	Chamber pressure (atm)
11-20	TC	Chamber temperature (^{o}K)

Card 18 Startline Data (This card is not used if ICON(2)=2 or for gas particle flow). Format 8E10.6

Use Card 18a if ICON(1)$\leq$2. Use Card 18b if ICON(1)>2.

Card	Column	Parameter	Description
18a*	1-10	CORLIP(2)	Axial coordinate of upper limit of startline (ft or m, see Fig. 3-1a)
	11-20	CORLIP(6)	Axial coordinate of lower limit of startline (ft or m, see Fig. 3-1a). (If ICON(3) point spacing option = 2 this value is recalculated using CORLIP(2)).
	21-30	CORLIP(4)	Mach number (ICON(2)=0) or A/A^* (ICON(2)=1) for startline
	31-40	CORLIP(5)	Entropy of startline (cal/gm/^{o}K or Btu/lbm/^{o}R)
	41-50	CORLIP(8)	Mixture ratio (O/F) of startline

*Card 18a is used to input the gas startline information when the gas chemical equilibrium, frozen or ideal gas option is utilized in the solution.

Card 18 (Continued)

Card	Column	Parameter	Description
18b*	1-10	CORLIP(2)	Axial coordinate of upper limit of start-line (ft or m, see Fig. 3-1a)
	11-20	CORLIP(6)	Axial coordinate of lower limit of start-line (ft or m, see Fig. 3-1a)
	21-30	CORLIP(4)	Mach number (ICON(2)=0) or A/A^* (ICON(2)=1) for startline
	31-40	P	Pressure for startline (atm)
	41-50	T	Temperature for startline (^oR or ^oK)

Card 19 Startline Data Format 6E13.7

Do not use this card if ICON(2)$\neq$2 or for gas-particle flow. Use feet if ICON(9)=0, meters if ICON(9)=1. Use Card 19a if ICON(1)$\leq$2. Use Card 19b if ICON(1)>2.

Repeat this card in succession and in order of increasing R for I=1, 2, . . . , ICON(3).

Card	Column	Parameter	Description
19a**	1-13	R	Radial coordinate (R) of point I on startline (ft or m)
	14-26	X	Axial coordinate (X) of point I (ft or m)
	27-39	EM	Mach number at point I (dimensionless)
	40-52	THETA	Flow angle at point I (deg)
	53-65	S	Entropy at point I (cal/gm/^oK or Btu/lbm/^oR)
	66-78	OF	Mixture ratio at point I (O/F)
19b*	1-13	R	Radial coordinate (R) of point I on start-line (ft or m)
	14-26	X	Axial coordinate (X) of point I (ft or m)
	27-39	EM	Mach number at point I (dimensionless)
	40-52	THETA	Flow angle at point I (deg)
	53-65	T	Temperature at point I (^oR or ^oK)
	66-78	P	Pressure at point I (atm)

*This card is used to input the gas startline information when the gas chemical non-equilibrium option is utilized in the solution.

**See footnote on previous page.

Card 20 Cutoff Limits Data Format 8E10.6

Required (See Fig. 3-1b)

Column	Parameter	Description
1-10	CUTDAT(1)	Radial coordinate defining upper limit of calculation regime (ft or m)
11-20	CUTDAT(2)	Axial coordinate defining upstream cutoff limit (ft or m)
21-30	CUTDAT(3)	Angle upper limit of calculation regime makes with horizontal (deg)
31-40	CUTDAT(4)	Radial coordinate defining downstream cutoff limit (ft or m)
41-50	CUTDAT(5)	Axial coordinate defining downstream cutoff limit (ft or m)
51-60	CUTDAT(6)	Angle downstream cutoff line makes with horizontal (deg)

Card 21 Mesh Control Fromat 8E10.6

Required (See Section 3.5.1)

Column	Parameter	Description
1-10	STEP(3)	Interior point insertion criteria (ft or m). See Section 3.5.1.
11-20	STEP(6)	Axis point insertion criteria (ft or m). See Section 3.5.1.
21-30	STEP(9)	Particle limiting streamline insertion criteria.
31-40	STEP(7)	Point deletion criteria.
41-50	STEP(1)	Prandtl-Meyer integration step size (deg).
51-60	STEP(8)	Interpolation factor for calculating lower wall.

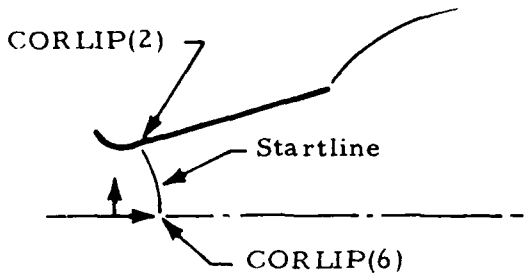
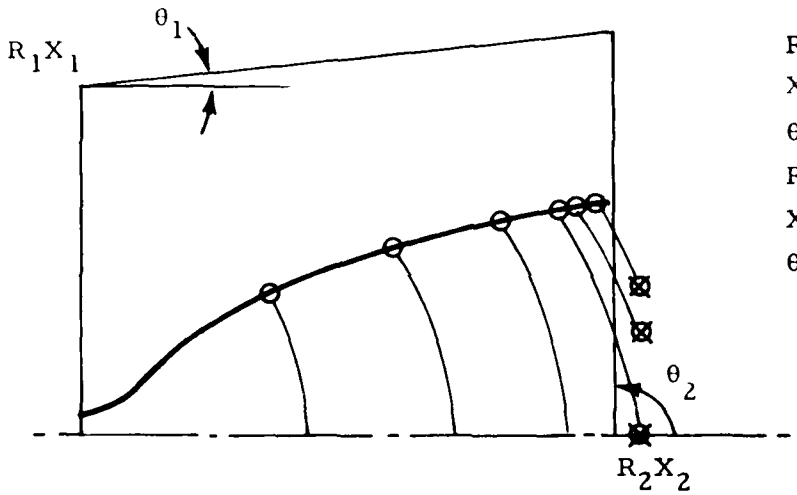


Fig. 3-1a - Startline Geometric Set-Up



R_1	CUTDAT(1)
X_1	CUTDAT(2)
θ_1	CUTDAT(3)
R_2	CUTDAT(4)
X_2	CUTDAT(5)
θ_2	CUTDAT(6)

⊠ Normal terminated by downstream cutoffs.

⊙ Normal terminated by plume boundary.

NOTE: The normals must terminate on an upper boundary. Therefore, R_1, X_1, θ_1 must have values such that the cutoff box will always be above the plume or solid boundary. The code will attempt to fill up the cutoff box with normals until fewer than six points remain on the normal.

Fig. 3-1b - Cutoff Limits

Card 22 Free-Molecular Control Variables Format 6E10.6
(This card is not used if ICON(13)=0)

Column	Parameter	Description
1-10	VIBNO	Reciprocal of the Knudsen number at which the vibrational energy mode thermally freezes.
11-20	ROTNO	Reciprocal of the Knudsen number at which the rotational energy mode thermally freezes.
21-30	TRANNO	Reciprocal of the Knudsen number at which the translational energy mode thermally freezes.
31-40	CHARL	Characteristic length used in the Knudsen number calculation (nomally the nozzle exit radius).
41-50	VISCC	Reference viscosity (poise) if not input in thermo tables.
51-60	CONMM	Viscosity relation temperature exponent if not input in thermo tables.

Cards 23 through 35 are input only for two-phase solution.

Card 23 Particle Solution Control Format 16I5
(Use only if ISPECS >0)

Column	Parameter	Value	Description
4	IZO	0	Nozzle wall equations are referenced to the nozzle throat.
		1	Nozzle wall equations are referenced to the nozzle exit plane.
5	IWRITE (particle print flag)	0	1 line of print for each particle ($V, \theta, \Delta M$, h, P, T)
		1	Above plus Re, ΔV, ΔT, viscosity, C_p, Pr
		2	All of above plus T_o, P_o, C_D/C_{DS}, Nu/Nus, A, B
6-10	IDRAG	0	Use drag table coded in Kliegel program (Ref. 7).
		1	Use C. J. Crowe drag table coded internal to program (Ref. 11).

Card 23 (Continued)

Column	Parameter	Value	Description
14-15	NSETS	0	Startline calculated by program (ICON(2)≠2)
		N	Number of startline points at which particles are present for given startline. ICON(2)=2, N ≤ ICON(3). Right adjust.
18	IPCHS	0	No punch.
		1	Punch startline from transonic program.
24	JTEM(1)		The elements of the JTEM(M) arrary indicate which temperature/enthalpy table is to be used for particle species M. The value of JTEM(1) is always set equal to 1 for particle species 1.
25, 30	JTEM(M) M = 2, ISPECS	0	Indicates that the particle species M temperature/enthalpy table will be the same as that for particle species 1. Cards 30, 31 and 32 are not required for particle species M.
. . . 65		M	Indicates that the particle species M temperature/enthalpy table will be input on Cards 30, 31 and 32 as Table M.
		N	Indicates that the particle species N temperature/enthalpy table will be the same as that for particle species M. (N < M). Cards 30, 31 and 32 are not required for particle species N.

Card 24 Particle Format 8E10.6

Column	Parameter	Description
1-10	XMASSP	Ratio of particle total mass flow rate to gas mass flow rate.

Card 25 Particle Mass Flow Rate Fractions (Use only if ISPECS > 0) Format 8E10.6

Column	Parameter	Description
1-10	PERTG(1)	Ratio of particle No. 1 mass flow rate to total particle mass flow rate.

Card 25 (Continued)

Column	Parameter	Description
11-20	PERTG(2)	Ratio of particle No. 2 mass flow rate to total particle mass flow rate.
.	.	.
.	.	.
.	.	.
	PERTG(ISPECS)	Ratio of particle No. ISPECS mass flow rate to total particle mass flow rate.

Card 26	Particle Size Data (Use only if ISPECS>0)	Format 8E10.6
Column	Parameter	Description
1-10	PSP(2, 1)	Radius of particle No. 1 (microns).
.	.	.
.	.	.
.	.	.
	PSP(2, ISPECS)	Radius of particle No. ISPECS (microns).

Card 27	Particle Mass Density (Use only if ISPECS>0)	Format 8E10.6
Column	Parameter	Description
1-10	PSP(1, 1)	Mass density of particle No. 1 (lbm/ft^3, or kg/m^3)
.	.	.
.	.	.
.	.	.
	PSP(1, ISPECS)	Mass density of particle No. ISPECS (lbm/ft^3, or kg/m^3).

Card 28	Emissivity Data* (Use only if ISPECS>0) (ϵ in Eq. (3.6))	Format 8E10.6
Column	Parameter	Description
1-10	EMISS(1)	Emissivity of particle No. 1.
.	.	.
.	.	.
.	.	.
	EMISS(ISPECS)	Emissivity of particle No. ISPECS

*The emissivity and accommodation coefficients are used to determine the local energy exchange between the gas and particles via radiation. They normally produce negligible affects on solution and usually are set to 0 (zero).

Card 29	Accommodation Coefficients* (Use only if ISPECS>0) (α in Eq. (3.6)	Format 8E10.6

Column	Parameter	Description
1-10	ACC(1)	Accommodation coefficient of particle No. 1.
.	.	.
.	.	.
.	.	.
	ACC(ISPECS)	Accommodation coefficient of particle No. 1 ISPECS.

Card 30	Particle Equation of State (Use only if ISPECS>0)	Format 4A6, I3, A6

Column	Parameter	Description
1-24	ALPHA	Particle name (any name).
28-33	UNIT (Independent of ICON(9))	ENG Data input in English units MKS Use metric units

Card 31	Particle Data (Use only if ISPECS>0)	Format I3, 12A6

Column	Parameter	Description
1-3	NPTM(I)	Number of temperature-enthalpy data points for this particle. If equal to 1, input liquid and solid heat capacities (see Card 32). Right adjust.

Card 32	Particle Enthalpy Data (Use only if ISPECS>0; units specified by Card 30).	Format 7E10.6

Column	Parameter	Description
1-10	TM(I)	Melting point temperature of particle No. I (^{o}R in English units, ^{o}K in MKS units).

*The emissivity and accommodation coefficients are used to determine the local energy exchange between the gas and particles via radiation. They normally produce negligible affects on solution and usually are set to 0 (zero).

Card 32 (Continued)

Column	Parameter	Description
11-20	HS(I)	Enthalpy of solid phase of particle No.I at melting point temperature (Btu/lbm or cal/gm).
21-30	HM(I)	Enthalpy of liquid phase of particle No.I at melting point temperature (Btu/lbm or cal/gm)
	If NPTM(I)=1, use following format.	
31-40	APHO(1, 1, I)	Heat capacity of liquid phase of particle No.I (Btu/lbm-^{o}R or cal/gm-^{o}K).
41-50	APHO(1, 2, I)	Heat capacity of solid phase of particle No.I (Btu/lbm-^{o}R or cal/gm-^{o}K).
	If NPTM(I) > 1 use following format.	
31-40	APHO(1, 1, I)	Temperature for T-H table for particle No.I (^{o}R or ^{o}K).
41-51	APHO(1, 2, I)	Enthalpy for T-H table for particle No.I (Btu/lbm or cal/gm).
51-60	APHO(2, 1, I)	Second temperature in T-H table for particle No.I (^{o}R or ^{o}K).
61-70	APHO(2, 2, I)	Second enthalpy in T-H table for particle No.I.

The above format (APHO(J, 1, I), APHO(J, 2, I)) is continued on successive cards of format 7E10.6 for J=1, 2, . . . , NPTM(I).

There are as many sets of cards 30, 31, 32 as there are different chemical species.

Card 33 Input Startline Format 6E13.7
(The following cards are required if ICON(2)=2 and ISPECS > 0).

Use Card 33a if ICON(1) $\leq$ 2. Use Card 33b if ICON(1) > 2.
Repeat this card for I=1, 2, . . . , ICON(3) starting at point on nozzle axis.

Card 33a*

Column	Parameter	Description
1-13	R	Radial coordinate of startline point I (ft or m).
14-26	X	Axial coordinate of startline point I (ft or m).

*This card is used when gas chemical equilibrium, frozen or ideal gas option is selected.

Card 33a (Continued)

Column	Parameter	Description
27-39	EM	Mach number at point I.
40-52	THETA	Flow angle at point I (deg).
53-65	S	Entropy at point I (Btu/lbm-^{o}R or cal/gm-^{o}K).
66-78	OF	Gas total enthalpy (Btu/lbm or cal/gm).

Card 33b*

Column	Parameter	Description
1-13	R	Radial coordinate of startline point I (ft or m).
14-26	X	Axial coordinate of startline point I (ft or m).
27-39	EM	Mach number at point I.
40-52	THETA	Flow angle at point I (deg).
53-65	T	Temperature at point I (^{o}R or ^{o}K)
66-78	P	Pressure at point I (atm).

Card 34 Startline Particulate Data Format I5, 5X, 4E13.7
(The following cards are required if ICON(2)=2 and ISPECS>0).

Use Card 34a if ICON(1) $\leq$ 2. Use Card 34b if ICON(1) > 2.

Card 34a

Column	Parameter	Description
5	J1	Particle number
11-23	H1	Particle enthalpy at point I (Btu/lbm or cal/gm).
14-36	RHO1	Particle density at point I (slug/ft^3 or kg/m^3).
37-49	U1	Particle axial velocity at point I (ft/sec or m/sec).
50-62	V1	Particle radial velocity at point I (ft/sec or m/sec).

*This card is used when the gas chemical non-equilibrium option is selected.

Card 34b

Column	Parameter	Description
5	J1	Particle number.
11-23	H1	Particle enthalpy at point I (Btu/lbm or cal/gm.
14-36	RHO1	Particle density at point I (slug/ft^3 or kg/m^3).
37-49	V_p	Particle velocity at point (I) (ft/sec or m/sec).
50-62	Θ_p	Particle flow angle at point I (deg).

Card 34 is repeated for each discrete particle size at each point on the start line where particles are present, starting at the nozzle wall and going toward the axis (reverse order of Card 33).

Card 35 Transonic Flow Data (Use only if ISPEC > 0 and ICON(2) ≠ 2) Format: Namelist

Although there are many parameters that may be input via the namelist DATA, most of these have already been assigned values in the previous 32 input cards; and some of the parameters do not apply to the transonic calculation. Only those namelist parameters that could have a significant effect on the program are included below. The namelist data begins in Column 2 with $DATA. The last card begins in Column 2 and contains only $END.

Parameter		Assumed Value
THID	Throat inlet half angle (deg)	None
THFD	Fairing angle (deg) (If THFD > THID no fairing)	5.0
THJD	Angle defining farthest downstream zone in transonic region (deg)	9.0
THIW	Angle where start line intersects nozzle wall (deg)	12.0
RRT	Throat wall radius of curvature divided by throat radius (> 2.0)	None

Card 35 (Continued)

Parameter		Assumed Value
ZAX	Value of X where startline intersects nozzle axis, normalized by throat radius (If ZAX is not input the program will calculate a value.)	None

(See Fig. 3-2 for an illustration of above parameters.)

ZI	Number of zones into which the upstream portion of transonic zone is divided*.	3.0
ZJ	Number of zones into which the downstream portion of transonic zone is divided*	2.0

*See Ref. 7.

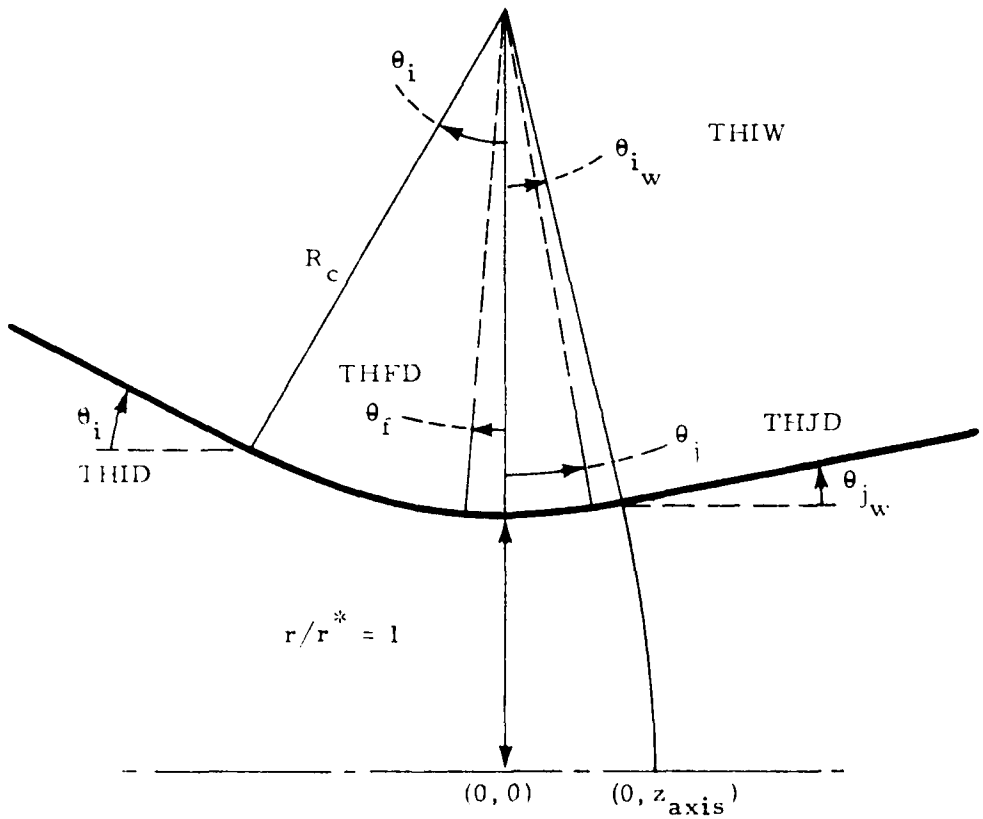


Fig. 3-2 - Inlet and Throat Parameters for a Gas-Particle Transonic Solution (see Ref. 7)

Table 3-6

MAGNETIC TAPE ASSIGNMENTS FOR THE RAMP PROGRAM

Where Required	Tape Units U-1108	Tape Unit Function
GASTAP – Uses TRAN72 data to set up equilibrium thermodynamic data tables or uses TRAN72 data to get species distribution on startline if finite rate option is selected.	10	Gas properties data generated by the TRAN72 program (input data)
GASTAP, IDTAPE and OUTBIN – Outputs input data and flowfield results on unit 3 for use with other auxiliary programs	3	Flowfield data generated by the RAMP program (output data)
PARTIL – Arranges two phase transonic solution output in the form used by the data acquisition routines.	NTAPE*	Ordered startline data generated internally by the two-phase transonic solution (input data)
PARTIN – Reads startline information necessary to initiate a flowfield solution.	NTAPE*	Variable tape unit number on which startline data calculated external to program is stored (input data).
IDMPFP and PFP – Store and retrieve particle data for each point in the flow field.	2	Stores particle data calculated internally by the RAMP program at each point in the flow field.
SPCTX – Stores and retrieves chemical species data for each point in the flow field.	1	Stores chemical species data calculated internally by the RAMP program at each point in the flow field.

*Set internally to 8 if ICON(2) = 0, NSPECS > 0 and not input on card 4. Set internally to 5 if ICON(2) = 2 (start line data read from cards) and not input on card 4.

3.2.2 Control Card Set-Up for Univac 1108 Exec 8 and Program Overlay Structures

A typical run stream set-up for the Univac 1108 Exec 8 computer is presented in this section. Also included are two tables which give the overlay structures for the two versions of the RAMP program.

Control Card Set-Up for the Univac 1108 Exec 8

```
∇FIN
∇FIN
DATA DECK
∇XQT GO
∇PRT, T
∇FREE A
∇COPIN A., TPF$.
∇REWIND A
∇USE 10, GAS
∇ASG, T 2, F
∇ASG, T 1, F
∇ASG, T GAS, T, 2415          Assign data tape containing
                              thermodynamic data (if required).
∇ASG, T TPF$. F///1000        Assign sufficient computer
                              storage for program.
∇FREE TPF$
∇ASG, T A, T, 17003           Assigns program tape
∇USE 13, FLOW
∇ASG, T FLOW, T, SAVE         Output data tape
∇RUN CONTROL CARD
```

NOTE: This schematic is typical of a run control scheme for the Univac 1108 Exec 8 computer. It is presented to acquaint the user with magnetic tape and scratch area assignments.

The data deck has been described in Section 3.2.1 and will be presented first in flow chart form and the listed for several example problems in Section 3.7.

Tables 3-7a and 3-7b give the program overlay structure for the equilibrium and finite rate chemistry versions of the RAMP program. The equilibrium version requires 63.3K octal storage locations while the finite rate version requires 62.4K octal storage locations.

Table 3-7a

RAMP OVERLAY STRUCTURE FOR EQUILIBRIUM CHEMISTRY VERSION OF PROGRAM

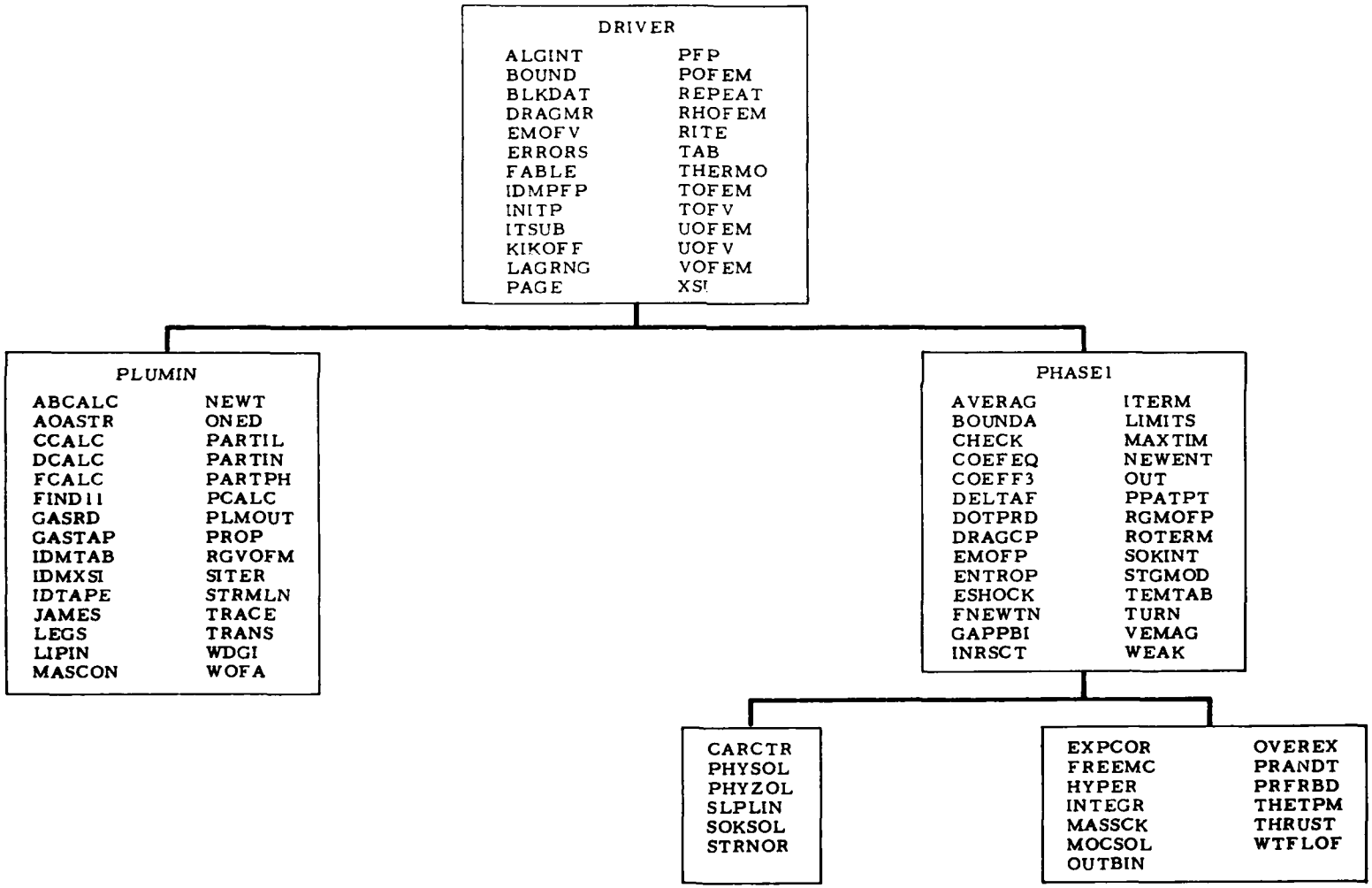
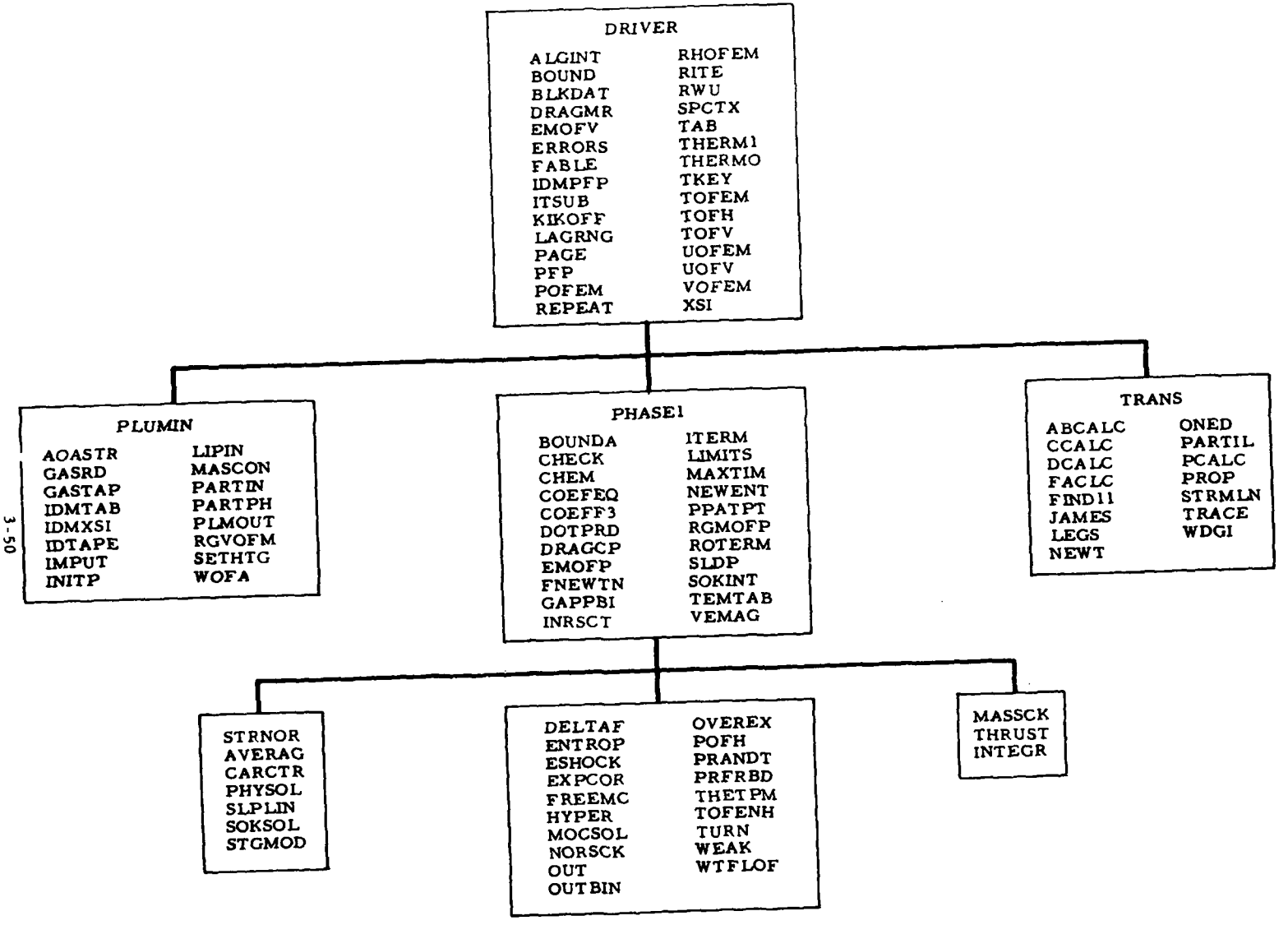


Table 3-7b

RAMP OVERLAY STRUCTURE FOR FINITE RATE VERSION OF PROGRAM



3.3 OUTPUT FORMAT

This section describes the printed output as well as the binary tape output for the RAMP code.

3.3.1 Description of Printed Output

The program output is organized so that the initial pages contain the input data and the initial data surface. Each data surface thereafter is constructed along a "normal" to the streamlines which have been chosen to represent the flow expansion of the nozzle and exhaust plume. The computer code will treat a chemical equilibrium and/or frozen or chemical non-equilibrium flow expansion with or without the presence of particles; consequently typical printouts for each case are presented to demonstrate the output for each case. Numbered flags on the example printout sheets correspond to the numbered comments in the following description of the printout. The calculations are performed in either the English or metric system of units; hence units for both are given.

GROUP 1 – IDENTIFICATION

(1) Computer code identification

(2) Identifies gas-particle flow solution; does not occur for gaseous only case.

(3) Case Number: Appears on each page – may be a maximum of five digits.

(4) Problem Title: Identifies particular solution, appears on each page and may be 120 spaces.

GROUP 2 – PROGRAM CONTROL

(5) These 16 parameters control the execution of program according to the options selected. (See Card 4 of the Input Guide for an explanation of the individual parameters.)

GROUP 3 – BOUNDARY EQUATIONS (See input guide for a detailed description)

(6) Type Equation: Identifies the type of boundary equation selected.

(7) ITRANS: Indicates whether a discontinuity follows this equation.

(8) Equation Coefficients: Apply to upper and lower boundary equations.

(9) MAX: Maximum value of x for which this equation applies.

GROUP 4 – GAS-PARTICLE MIXTURE IDENTIFICATION

(10) Total Enthalpy (appears for gas-particle flow): Gas total enthalpy before it is perturbed (see page 2-2).

(11) Indicates number of discrete particles used to represent the particle distribution.

(12) Gas Identification: Name (24 characteristics max.) which identifies the gas. If the gas data is stored on a magnetic tape, this is the name which is used to locate the gas data on the data tape (see Card 8 of the Input Guide).

GROUP 5 – GAS PROPERTIES

(13) Total Enthalpy (appears for gas-particle flow): Gas total enthalpy for this table.

(13) O/F Ratio (appears for gaseous only solution): O/F for this table.

(14) Entropy: May be two maximum for each O/F or total enthalpy.

(15) Gas Thermodynamics Data Velocity: May be 13 maximum for each entropy (ft/sec or m/sec).

(16) Gas Constant: Value associated with particular velocity, etc., ($ft^2/sec^2/^oR$ or $m^2/sec^2/^oK$).

(17) Isentropic Exponent: Value associated with particular velocity, etc.

(18) Temperature: Value associated with particular velocity, etc., (^oR or ^oK).

(19) Pressure: Value associated with particular velocity, etc., (lbf/ft^2 or N/m^2).

Gas Transport Data: (does not appear for gaseous only solution).

(20) Prandtl Number: Value associated with particular value of velocity, etc.

(21) Viscosity: Value associated with particular value of velocity, etc.

(22) Specific Heat at Constant Pressure: This parameter appears for real gas with multiple velocity values. If only one velocity is used the parameter printed is the viscosity exponent for the equation $\mu = \mu_o (T/T_o)^{exp}$.

GROUP 6 – PROBLEM LIMIT INFORMATION (see input guide)

(23) R: Radial coordinate of upper cutoff (units consistent with boundary equations).

(24) X: Axial coordinate of upper cutoff (units consistent with boundary equations).

(25) THETA: Angle of upper cutoff line (deg)

(26) R: Radial coordinate of lower cutoff (units consistent with boundary equations).

(27) X: Axial coordinate of lower cutoff (units consistent with boundary equations.

(28) Theta: Angle of lower cutoff line (deg).

GROUP 7 – PARTICLE DESCRIPTION (does not appear for gaseous only solution)

(29) Particle Number: Number assigned to particular particle (10 max).

(30) Particle Radius: Radius of the particle in microns.

(31) Mass Density: Particle density (lbm/ft^3 or kg_m/m^3).

(32) Emissivity: Coefficient of emmisivity for particle radiation to the surrounding medium.

(33) Accommodation Coefficient: Accommodation coefficient for radiation from the surrounding medium to the particle.

(34) $\sum_{j=1}^{N} \dot{\omega}_p^j / \dot{\omega}g$: Particle percent loading relative to the gas.

(35) $\dot{\omega}_p^j / \sum_{j=1}^{N} \dot{\omega}_p^j$: Individual particle percentage relative to the total mass flow rate

(36) UNITS: Units with which the particle temperature-enthalpy table will be input (see the input guide).

(37) TMELT: Temperature of the particle during the phase change from liquid to solid (^oR or ^oK).

(38) HSOLID: Value of enthalpy at which the particle becomes a solid (ft^2/sec^2 or M^2/sec^2).

(39) HLIQUID: Value of enthalpy at which the particle begins the transition from liquid to solid phase (ft^2/sec^2 or M^2/sec^2) constant specific heat analysis.

(40) CPMELT: Value of the specific heat at constant pressure for the particle in the liquid state ($ft^2/sec^2/^oR$ or $m^2/sec^2/^oK$).

(41) CPSOLID: Value of the specific heat at constant pressure for the particle in the solid state ($ft^2/sec^2/^oR$ or $m^2/sec^2/^oK$).

(40) TP: Value of the particle temperature (^oR or ^oK) (50 max.).

(41) HP: Value of particle enthalpy corresponding to (40) (50 max.)

(42) Re: Particle Reynolds number (28 max.).

(43) DRAG COEF: Particle drag coefficient parameter, f^j, corresponding to (42) .

GROUP 8 – GAS START LINE INFORMATION

(44) R: Radial coordinate of the data point (units consistent with boundary equations).

(45) X: Axial coordinate of the data point (units consistent with boundary equations).

(46) M: Local value of the Mach number (must be > 1.0).

(47) THETA: Local flow deflection angle (deg).

(48) S: Local value of entropy level ($ft^2/sec^2/^oR$ or $m^2/sec^2/^oK$).

(49) MACH ANGLE: Local value corresponding to M (deg).

(50) Shock Angle: Local value of shock angle if point is a downstream shock point (deg).

(51) H-TOTAL (gas-particle flow): Gas total enthalpy level (ft^2/sec^2 or m^2/sec^2).

(51) O/F (gas only flow): local value of O/F.

GROUP 9 – PARTICLE START LINE INFORMATION (does not appear for gaseous only solution)

(52) POINT: Data point at which this particle is present.

(53) SPECIE: Particle number for this data point.

(54) u: Particle axial component of velocity (ft/sec or m/sec).

(55) V: Particle radial component of velocity (ft/sec or m/sec).

(56) θ: Particle streamline deflection angle (rad)

(57) h: Particle enthalpy level (ft^2/sec^2 or m^2/sec^2)

(58) ρ: Local particle concentration ($slug/ft^3$ or kg_m/m^3)

GROUP 10 — MESH CONTROL CRITERIA (see input guide)

(59) DLI: Point insert criteria for the nozzle-plume interior solution (units consistent with boundary equations).

(60) DXA: Line insert criteria along the axis (units consistent with boundary equations).

(61) DLM: Insert criteria near a particle limiting streamline (units consistent with the boundary equations).

(62) DLD: Point delete criteria (units consistent with the boundary equations).

(63) DEGPM: Incremental angle to be used in the numerical integration to define the Prandtl-Meyer expansion fan (deg).

(64) F: Interpolation factor used in the axis point solution.

GROUP 11 — DATA LINE FLOW PROPERTIES

NOTE: The output format for all data surfaces are the same with each point type on the line being identified. Several different lines are shown to indicate typical line constructions.

(65) Line: Line number; lines are numbered in ascending order.

(66) Point: Indicates point number on the line.

(67) Description: Indicates point type and flow regime. These options are:

Point Type	Output Format	Flow Regime	Output Format
a. Input	INPUT POINT	a. Continuum	CONTIN
b. Interior	INTER	b. Vibrationally Frozen	VIBFRZ
c. Wall	WALL	c. Rotationally Frozen	ROTFRZ
d. Free Boundary	FREEBD	d. Transitionally Frozen	TRNFRZ
e. Prandtl-Meyer	PRN-MR		
f. Upstream	UP-SHK		
g. Downstream Shock	DWNSHK		
h. Shock Interaction	SOKINT		
i. Slipline	SLIP		

NOTES: The point type and flow regime will appear in the appropriate combination to completely describe the data point.

Items (70) through (81) refer to gas conditions.

(68) R: Radial coordinate of the data point (units consistent with the boundary equations)

(69) X: Axial coordinate of the data point (units consistent with the boundary equations)

(70) M: Local value of the Mach number

(71) θ: Local flow deflection angle of the gas streamline (deg)

(72) S: Local entropy level of the gas ($ft^2/sec^2/^oR$ or $m^2/sec^2/^oK$)

(73) V: Local magnitude of the velocity (ft/sec or m/sec)

(74) H-TOTAL (gas-particle flow): Gas total enthalpy level (ft^2/sec^2 of m^2/sec^2)

(74) O/F (gas only flow): Local value of O/F

(75) Mach Angle: Mach angle corresponding to the Mach number (deg)

(76) P: Local pressure (lb_f/in^2 or N/m^2)

(77) ρ: Local density ($slug/ft^3$ or kgm/m^3)

(78) T: Local static temperature (^oR or ^oK)

(79) GAS CONST: Local value of the gas constant ($ft^2/sec^2/^oR$ or $m^2/sec^2/^oK$)

(80) LOCAL GAMMA: Local value of the isentropic exponent

(81) SHOCK ANGLE: Local value of the downstream shockwave angle (deg)

NOTE: Items (82) through (87) refer to the particle properties. This printout does not appear for gas only flow.

(82) V: Local magnitude of particle velocity (ft/sec or m/sec)

(83) θ: Local particle streamline deflection angle (deg)

(84) DM: Difference in Mach number between the gas and particle

(85) h: Local particle enthalpy level (ft^2/sec^2 or m^2/sec^2)

(86) ρ: Local particle concentration ($slug/ft^3$ or kgm/m^3)

(87) T: Local particle temperature (^oR or ^oK)

(88) Indicates the data point is on a particle limiting streamline

GROUP 12 – INTEGRATED GAS AND PARTICLE MASS FLOW RATES

NOTE: The units of the flow rates depend on the units of the boundary equation. For the following units perform the indicated operation.

Units	Factor	$\dot{\omega}$
in.	1/144	slug/sec
ft	1	slug/sec
M	1	kg_m/sec
None	$(\text{Ref. length})^2$	slug/sec or kg_m/sec

(89) Gas mass flow rate

(90) Particle total mass flow rate

(91) Sum of the gas and particle mass flow rate

(92) Particle percent loading relative to the gas (numerical integration results)

(93) Particle percent loading relative to mixture

GROUP 13 – MOMENTUM INTEGRATION RESULTS

(94) This is a calculation of the component of the net thrust due to the gas and particle momentum across the starting line.

FORCEX, FORCEY: Net axial and radial component of the thrust vector (lb_f or N)

TORQZ: Net torque resulting from the thrust (ft-lb_f or m-N)

ISP: Specific impulse corresponding to FORCEX (lb_f-sec/lb_m)

(95) This is the incremental gas and particle contribution to the thrust and torque vector

DELFXG, DELFYG: Net gaseous axial and radial component of the thrust vector (lb_f or N)

TORQZG: Net torque resulting from the gaseous contribution to the thrust vector (ft-lb_f or m-N)

DELFXP, DELFYP: Particle momentum contribution to the thrust vector (lb_f or N)

TORQZP: Net torque resulting from the particle contribution to the thrust vector (ft-lb_f or m-N)

Problem Solution Iteration Control

(96) ITR: Number of iterations required for this point to converge within the convergence criteria

GROUP 14 – PRESSURE INTEGRATION RESULTS

(97) This calculation is the thrust and torque resulting from the gas pressure acting on the nozzle wall.

FORCEX, FORCEY: Axial and radial component of the thrust (lb_f or N). This thrust vector includes the momentum and pressure contribution.

TORQZ: Net torque resulting from the thrust (ft-lb_f or m-N)

DELFX, DELFY: Incremental force in the axial and radial directions resulting from the pressure acting on the nozzle wall (lb_f or N)

ISP: Specific impulse corresponding to FORCEX (lb_f-sec/lb_m)

GROUP 15 – PERCENT CHANGE IN MASS FLOW RATE, MOMENTUM, ENERGY, AND ISP

NOTE: This is a comparison of the mass flow rate, momentum, energy and ISP relative to the mass flow rate, momentum, energy and ISP through the input (starting line) surface. The percent change should be near zero; any variation from zero is an indication of accumulated error in the numerical solution.

(98) Percent change in the mass flow rate of the gas

(99) Percent change in the mass flow rate of the particles

(100) Percent change in the mass flow rate of the mixture

(101) Percent change in the momentum of the gas

(102) Percent change in the momentum of the particles

(103) Percent change in the momentum of the mixture

(104) Percent change in I_{sp}

(105) Percent change in the energy of the gas

(106) Percent change in the energy of the particles

(107) Percent change in the energy of the mixture.

GROUP 16 – FREE MOLECULAR CONTROL PARAMETERS

108 VIBNO: Reciprocal of the Knudsen number at which the vibrational energy mode thermally freezes.

109 ROTNO: Reciprocal of the Knudsen number at which the rotational energy mode thermally freezes.

110 TRANNO: Reciprocal of the Knudsen number at which translational energy mode thermally freezes.

111 CHARL: Characteristic length used in the mean free path calculation used to compute the local value of the Knudsen number (units consistent with the boundary equations).

112 GAMV: Value of the isentropic exponent to be used in the vibrationally frozen flow calculations.

113 GAMR: Value of the isentropic exponent to be used in the rotationally frozen flow calculations.

NOTE: Items 112 and 113 are the gas species data to be used in the calculation of parameters used in the Knudsen number calculation (10 max. may be used).

GROUP 17 – SPECIES THERMODYNAMIC AND REACTION DATA

114 These 7 parameters control the execution of the finite rate chemistry calculations according to the options selected. (See Card 5 of the Input Guide for an explanation of the individual parameters.)

115 Prandtl number of the gas (dimensionless)

116 Absolute viscosity of the gas (poise)

117 Viscosity temperature exponent

118 Reaction number

119 Reaction being considered

120 A: Pre-exponential factor (cm-particle-sec)

121 N: Temperature exponent

122 B: Activation energy (cal/mole)

123 M: Temperature exponent

124 R-Type: Reaction type

(125) K-Type: Rate constant type

(126) Catalytic species being considered. (See Card(s) 14 for an explanation.)

GROUP 18 – SPECIES MOLE FRACTIONS ON THE STARTLINE

(127) Point: Indicates the point number on the startline

(128) Corresponding species mole fractions at the point (127)

(129) Chamber pressure (atm)

(130) Chamber temperature (^{o}K)

(131) Species mole fractions at a point on the data surface

Sample Printout
for Two-Phase Chemical Equilibrium Flow

Sample Printout for Two-Phase Chemical Equilibrium Flow

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SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM (1)
GAS-PARTICLE FLOW SOLUTION (2)
CASE NO.  1 (3)                                                                    PAGE  1
SHUTTLE SEP MOTOR NOZZLE (4)
                                                                                                  Group 1

                                RUN CONTROL PARAMETERS (5)
ICON(1)   ICON(2)   ICON(3)   ICON(4)   ICON(5)   ICON(6)   ICON(7)   ICON(8)
   2         0        25         3         1         0         1         2

ICON(9)   ICON(10)  ICON(11)  ICON(12)  ICON(13)  ICON(14)  ICON(15)  ICON(16)
   0        25         1         1         0         0         0       11510

FLOW CALCULATIONS ARE IN ENGLISH UNITS WITH THE R,X COORDINATES IN FEET
THE FLOWFIELD DATA WILL BE WRITTEN ON TAPE                                                        Group 2

                                UPPER BOUNDARY
(6) TYPE  ITRANS (7)   A (8)      B (8)      C (8)      D (8)      E (8)      MAX (9)
  1        0        -.10000+01  .15340+00   .00000    -.10000+01 -.52225+00  .14672+00
  2        1         .10000+01  .51561+01   .21824+01 -.10000+01 -.21796+01  .74059+00
  3        0         .49290+01  .00000      .00000     .00000     .00000     .10000+04
                                                                                                  Group 3
                                LOWER BOUNDARY
TYPE  ITRANS   A        B        C        D        E        MAX
  2     0     .00000   .00000   .00000   .00000   .00000   .10000+04

                                CHAMBER ENTHALPY =  -.19619+08 (10)
                                                                                                  Group 4
THERE ARE  6 PARTICLE SPECIES PRESENT IN THE GAS-PARTICLE MIXTURE (11)
THE FOLLOWING GAS PROPERTIES IN ENGLISH UNITS ARE FOR SEP PROP PC=1000 (12)
                                REAL GAS PROPERTIES
                  H-TOTAL (13)
                  -.28631+06
S (14)    V (15)    R (16)    GAMMA (17)  T (18)    P (19)    PR (20)   VIS (21)  CP (22)
-.17515+04
          .00000    .19864+04 .12039+01   .48098+04 .18000+04 .57039+00 .17610-05 .12302+05
          .32399+04 .19836+04 .12134+01   .41603+04 .10111+04 .58520+00 .16373-05 .11552+05
          .51771+04 .19815+04 .12260+01   .36228+04 .36000+03 .60100+00 .14258-05 .10865+05
          .48117+04 .19812+04 .12316+01   .31844+04 .18000+03 .50332+00 .12734-05 .10554+05
          .66587+04 .19811+04 .12355+01   .27927+04 .90000+02 .60147+00 .11702-05 .10404+05
          .71778+04 .19811+04 .12376+01   .24457+04 .45000+02 .59727+00 .10569-05 .10327+05
          .77242+04 .19811+04 .12372+01   .20511+04 .18000+02 .58936+00 .92142-06 .10143+05
          .82231+04 .19811+04 .12352+01   .16175+04 .60000+01 .58769+00 .76936-06 .89[illegible]+04
                                                                                                  Group 5
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Sample Printout for Two-Phase Chemical Equilibrium Flow

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 1

PAGE 2

SPACE SHUTTLE SEP MOTOR NOZZLE

REAL GAS PROPERTIES

H-TOTAL

S	V	R	GAMMA	T	P	PR	VIS	CP
-.17515+04								
	.84091+04	.19811+04	.12942+01	.14422+04	.36000+01	.58760+00	.69560-06	.87208+04
	.86241+04	.19811+04	.13062+01	.12289+04	.18000+01	.58584+00	.60805-06	.84554+04
	.89932+04	.19811+04	.13317+01	.83245+03	.36000+00	.58277+00	.42702-06	.79585+04
	.91091+04	.19811+04	.13413+01	.69912+03	.18000+00	.58035+00	.36311-06	.77937+04
	.93072+04	.19811+04	.13600+01	.46019+03	.36000-01	.57207+00	.23588-06	.74839+04
.94545+04								
	.00000	.19995+04	.11754+01	.46839+04	.80000+02	.50737+00	.17256-05	.15844+05
	.31967+04	.19905+04	.11920+01	.43074+04	.45254+02	.53093+00	.16219-05	.13464+05
	.51556+04	.19831+04	.12182+01	.36197+04	.16000+02	.58140+00	.14247-05	.11313+05
	.59941+04	.19816+04	.12286+01	.31911+04	.80000+01	.59755+00	.12954-05	.10726+05
	.64845+04	.19812+04	.12347+01	.28012+04	.40000+01	.60024+00	.11729-05	.10443+05
	.71663+04	.19811+04	.12374+01	.24537+04	.20000+01	.59719+00	.10591-05	.10334+05
	.77152+04	.19811+04	.12372+01	.20579+04	.80000+00	.58942+00	.92375-06	.10382+05
	.82163+04	.19811+04	.12850+01	.16730+04	.26667+00	.59798+00	.76548-06	.89351+04
	.84031+04	.19811+04	.12940+01	.14872+04	.16000+00	.58792+00	.69760-06	.87236+04
	.86169+04	.19811+04	.13060+01	.12333+04	.80000-01	.58718+00	.60989-06	.84608+04
	.89394+04	.19811+04	.13316+01	.83555+03	.16000-01	.58320+00	.43049-06	.79616+04
	.91060+04	.19811+04	.13412+01	.70177+03	.80000-02	.58081+00	.36443-06	.77934+04
	.93050+04	.19811+04	.13599+01	.46199+03	.16000-02	.57264+00	.23686-06	.74911+04

REAL GAS PROPERTIES

H-TOTAL
-.24125+08

S	V	R	GAMMA	T	P	PR	VIS	CP
-.84769+03								
	.00000	.19923+04	.11919+01	.51581+04	.18000+04	.55000+00	.18540-05	.13825+05
	.31540+04	.19867+04	.12032+01	.47059+04	.10145+04	.56677+00	.17326-05	.12372+05
	.53837+04	.19823+04	.12201+01	.39342+04	.36000+03	.59339+00	.15166-05	.11133+05
	.62562+04	.19814+04	.12277+01	.34668+04	.18000+03	.60145+00	.13793-05	.10729+05
	.69335+04	.19812+04	.12330+01	.30450+04	.90000+02	.60279+00	.12501-05	.10497+05
	.74773+04	.19811+04	.12364+01	.26690+04	.45000+02	.60017+00	.11302-05	.10370+05
	.80896+04	.19811+04	.12378+01	.22387+04	.18000+02	.59362+00	.98632-06	.10319+05
	.85730+04	.19811+04	.12791+01	.17727+04	.60000+01	.59495+00	.82327-06	.90864+04
	.87667+04	.19811+04	.12860+01	.15835+04	.36000+01	.59551+00	.75144-06	.88648+04
	.89953+04	.19811+04	.13004+01	.13527+04	.18000+01	.59562+00	.65929-06	.85828+04
	.91957+04	.19811+04	.13269+01	.92084+03	.36000+00	.59368+00	.47031-06	.80459+04
	.92947+04	.19811+04	.13363+01	.77973+03	.18000+00	.59212+00	.40013-06	.78660+04

Group 5 (Cont'd)

Sample Printout for Two-Phase Chemical Equilibrium Flow

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 1 PAGE 3

SPACE SHUTTLE SEP MOTOR NOZZLE

REAL GAS PROPERTIES

H-TOTAL
=.53902+04

S	V	R	GAMMA	T	P	PR	VIS	CP
	.00000	.20148+04	.11587+01	.49404+04	.80000+02	.48389+00	.17940-05	.14517+05
	.32826+04	.20006+04	.11725+01	.45937+04	.45564+02	.49992+00	.17007-05	.16272+05
	.53419+04	.19862+04	.12045+01	.39195+04	.16000+02	.55086+00	.15120-05	.12284+05
	.62212+04	.19824+04	.12205+01	.34762+04	.80000+01	.58410+00	.13820-05	.11195+05
	.69048+04	.19815+04	.12303+01	.30614+04	.40000+01	.59829+00	.12552-05	.10648+05
	.74538+04	.19812+04	.12357+01	.26055+04	.20000+01	.59940+00	.11355-05	.10402+05
	.80313+04	.19811+04	.12378+01	.22530+04	.80000+00	.59379+00	.99120-06	.10320+05
	.85592+04	.19811+04	.12386+01	.17844+04	.26667+00	.59542+00	.82766-06	.90980+04
	.87565+04	.19811+04	.12876+01	.15943+04	.16000+00	.59602+00	.75563-06	.88758+04
	.89549+04	.19811+04	.12999+01	.13621+04	.80000-01	.59619+00	.66313-06	.85926+04
	.93745+04	.19811+04	.13266+01	.92762+03	.18000-01	.59440+00	.47343-06	.80527+04
	.95025+04	.19811+04	.13366+01	.78054+03	.80000-02	.59291+00	.40294-06	.78718+04
	.97148+04	.19811+04	.13560+01	.51575+03	.16000-02	.58770+00	.26575-06	.75514+04

REAL GAS PROPERTIES

H-TOTAL
=.21872+04

S	V	R	GAMMA	T	P	PR	VIS	CP
=.41765+03								
	.00000	.19965+04	.11858+01	.53183+04	.18000+04	.54000+00	.18960-05	.19817+05
	.34056+04	.19892+04	.11973+01	.48497+04	.10166+04	.55602+00	.17769-05	.12936+05
	.54108+04	.19830+04	.12164+01	.40875+04	.36000+03	.58723+00	.15604-05	.11371+05
	.63721+04	.19816+04	.12253+01	.36078+04	.18000+03	.59908+00	.14214-05	.10752+05
	.70643+04	.19812+04	.12315+01	.31720+04	.90000+02	.60269+00	.12696-05	.10505+05
	.76704+04	.19812+04	.12355+01	.27319+04	.45000+02	.60123+00	.11667-05	.10403+05
	.82657+04	.19811+04	.12378+01	.23340+04	.18000+02	.59537+00	.10188-05	.10318+05
	.87414+04	.19811+04	.12760+01	.18517+04	.60000+01	.59771+00	.85239-06	.91745+04
	.89420+04	.19811+04	.12850+01	.16557+04	.36000+01	.59875+00	.77938-06	.85308+04
	.91745+04	.19811+04	.12974+01	.14161+04	.18000+01	.59925+00	.68599-06	.86591+04
	.93756+04	.19811+04	.13245+01	.96651+03	.36000+00	.59827+00	.49122-06	.80917+04
	.97022+04	.19811+04	.13342+01	.81389+03	.18000+00	.59714+00	.41696-06	.77608+04
	.99192+04	.19811+04	.13544+01	.53759+03	.36000-01	.59299+00	.29798-06	.72755+04
=.58511+04								
	.00000	.20241+04	.11523+01	.50500+04	.80000+02	.47482+00	.18225-05	.21634+05
	.32[illegible]0+04	.20076+04	.11637+01	.47181+04	.45709+02	.48755+00	.17343-05	.18018+05
	.55260+04	.19886+04	.11957+01	.40610+04	.16000+02	.53284+00	.15524-05	.13084+05
	.63753+04	.19830+04	.12149+01	.36169+04	.80000+01	.57163+00	.14238-05	.11537+05

Group 5 (Cont'd)

Sample Printout for Two-Phase Chemical Equilibrium Flow

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 1

ACE SHUTTLE SRB MOTOR NOZZLE

REAL GAS PROPERTIES

H-TOTAL
S .58411+04

V	R	GAMMA	T	P	PR	VIS	CP
.70757+04	.19818+04	.12271+01	.31928+04	.40000+01	.59459+00	.12959-05	.10816+05
.75987+04	.19813+04	.12342+01	.28041+04	.20000+01	.59963+00	.11738-05	.10467+05
.81810+04	.19811+04	.12377+01	.23536+04	.80000+00	.59558+00	.10254-05	.10324+05
.87227+04	.19811+04	.12754+01	.18680+04	.26667+00	.59820+00	.85829-06	.91805+04
.89255+04	.19811+04	.12844+01	.16706+04	.16000+00	.59936+00	.78508-06	.89841+04
.91605+04	.19811+04	.12968+01	.14292+04	.80000-01	.59994+00	.69025-06	.86628+04
.95660+04	.19811+04	.13240+01	.97594+03	.16000-01	.59915+00	.49550-06	.81612+04
.96939+04	.19811+04	.13343+01	.82199+03	.80000-02	.59810+00	.42283-06	.79129+04
.99133+04	.19811+04	.13541+01	.54415+03	.16000-02	.59420+00	.28081-06	.75812+04

REAL GAS PROPERTIES

H-TOTAL
-.19419+08
S .00000

V	R	GAMMA	T	P	PR	VIS	CP
.00000	.20017+04	.11798+01	.54686+04	.18000+04	.53040+00	.19396-05	.15475+05
.34537+04	.19925+04	.11911+01	.50261+04	.10187+04	.54593+00	.18188-05	.13715+05
.55738+04	.19840+04	.12121+01	.42383+04	.36000+03	.57942+00	.16030-05	.11671+05
.68835+04	.19820+04	.12224+01	.37483+04	.18000+03	.59535+00	.14627-05	.11008+05
.71907+04	.19813+04	.12297+01	.32994+04	.90000+02	.60190+00	.13287-05	.10643+05
.77591+04	.19812+04	.12344+01	.28956+04	.45000+02	.60196+00	.12030-05	.10444+05
.83575+04	.19811+04	.12376+01	.24304+04	.18000+02	.59704+00	.10513-05	.10327+05
.88057+04	.19811+04	.12731+01	.19319+04	.60000+01	.60000+00	.88132-06	.92428+04
.91111+04	.19811+04	.12819+01	.17290+04	.36000+01	.60158+00	.80732-06	.90137+04
.93825+04	.19811+04	.12944+01	.14807+04	.18000+01	.60246+00	.71089-06	.87172+04
.97516+04	.19811+04	.13220+01	.10132+04	.36000+00	.60236+00	.51232-06	.81391+04
.99918+04	.19811+04	.13325+01	.85401+03	.18000+00	.60163+00	.43803-06	.79447+04
.10115+05	.19811+04	.13527+01	.56614+03	.36000-01	.59865+00	.29237-06	.76037+04
.62828+04							
.00000	.20345+04	.11470+01	.51490+04	.80000+02	.46684+00	.18474-05	.23657+05
.33550+04	.20157+04	.11560+01	.48304+04	.45836+02	.47734+00	.17643-05	.20071+05
.55345+04	.19924+04	.11861+01	.41947+04	.16000+02	.51537+00	.15901-05	.14185+05
.61232+04	.19853+04	.12080+01	.37551+04	.80000+01	.55559+00	.14643-05	.12023+05
.71405+04	.19824+04	.12232+01	.33245+04	.40000+01	.58776+00	.13362-05	.11038+05
.77177+04	.19814+04	.12322+01	.29245+04	.20000+01	.59886+00	.12122-05	.10565+05
.83752+04	.19812+04	.12373+01	.24564+04	.80000+00	.59708+00	.10600-05	.10332+05
.88812+04	.19812+04	.12723+01	.19535+04	.26667+00	.60056+00	.88905-06	.92616+04
.93895+04	.19812+04	.12811+01	.17488+04	.16000+00	.60228+00	.81480-06	.90335+04

Group 5 (Cont'd)

Sample Printout for Two-Phase Chemical Equilibrium Flow

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SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                    GAS-PARTICLE FLOW SOLUTION
                    CASE NO.    1                                                    PAGE    5
SPACE SHUTTLE SEP MOTOR NOZZLE
                                   REAL GAS PROPERTIES
          H-TOTAL
     S          V          R        GAMMA        T          P         PR         VIS        CP
  .62928+04
            .93712+04  .19812+04  .12936+01  .14981+04  .80000-01  .60325+00  .71786-06  .87357+04
            .97489+04  .19812+04  .13213+01  .10259+04  .16000-01  .60338+00  .51901-06  .81521+04
            .98309+04  .19812+04  .13319+01  .86491+03  .80000-02  .60275+00  .44317-06  .79557+04
            .10108+05  .19812+04  .13522+01  .57364+03  .16000-02  .60006+00  .29629-06  .76113+04
                                   RUN CUTOFF INFORMATION
      (23)                                                                                    (28)
            UPPER BOUNDARY                    (25)                (26)        LOWER BOUNDARY
R=  .10000+04  X=  -.10000+04  THETA=  .00000   R=  .00000   X=  .10000+03  THETA=  .90000+02
      (29)   (30)   (24)   (31)                                                  (27)
                                   PARTICLE PHYSICAL DATA
     SPECIE   RADIUS      MASS DENSITY    EMISSIVITY (32)  ACCM. COEFF. (33)
       1     .11000+01    .25000+03       .00000           .00000
       2     .17000+01    .25000+03       .00000           .00000
       3     .25000+01    .25000+03       .00000           .00000
       4     .32000+01    .25000+03       .00000           .00000
       5     .45000+01    .25000+03       .00000           .00000
       6     .65000+01    .25000+03       .00000           .00000
                                (34)
     THE PARTICLES CONSTITUTE  3.81 PERCENT BY WEIGHT FLOW OF THE GAS-PARTICLE MIXTURE
                THE INDIVIDUAL PERCENTAGES ARE   .10  .20  .20  .20  .20  .10
     THE PARTICLE TEMPERATURE-ENTHALPY TABLE WILL BE READ IN WITH ENGLISH (36) UNITS (35)
                                   PARTICLE TEMPERATURE-ENTHALPY TABLE
                                (37)                (38)
     PHASE CHANGE DATA *** THELT=  .41885+04 HSOLID=  .34010+08 HLIQUID=  .46520+08 (39)
                                   CPMELT=   .85100+04 CPSOLID=  .81199+04
                                        (40)                (41)
```

Group 5 (Cont'd)

Group 6

Group 7

Sample Printout for Two-Phase Chemical Equilibrium Flow

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 1 PAGE 6

SPACE SHUTTLE SEP MOTOR NOZZLE

PARTICLE DRAG TABLE

I	RE (42)	DRAG COEF (43)
1	.00005	.10000+01
2	.12500+01	.10000+01
3	.12550+01	.10000+01
4	.12600+01	.10010+01
5	.12650+01	.10020+01
6	.15820+01	.10630+01
7	.19950+01	.11410+01
8	.25100+01	.12240+01
9	.31600+01	.13150+01
10	.39800+01	.14120+01
11	.50100+01	.15170+01
12	.63100+01	.16250+01
13	.79500+01	.17450+01
14	.10000+02	.18740+01
15	.12600+02	.20260+01
16	.15820+02	.21840+01
17	.19950+02	.23640+01
18	.25100+02	.25550+01
19	.31600+02	.27600+01
20	.39800+02	.30000+01
21	.50100+02	.32520+01
22	.63100+02	.32520+01
23	.79500+02	.38250+01
24	.10[illegible]+03	.41550+01
25	.31600+03	.79000+01
26	.10000+05	.20000+02
27	.10011+04	.20020+02
28	.10050+06	.20000+04

Group 7 (Cont'd)

Sample Printout for Two-Phase Chemical Equilibrium Flow

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 1

CE SHUTTLE SEP MOTOR NOZZLE

GASEOUS STARTING LINE INFO

44 R	45 X	46 M	THETA 47	S 48	MACH ANGLE 49	SHOCK ANGLE 50	H-TOTAL 51
.00000	.12847+00	.14166+01	.00000	.57051+02	.44904+02	.00000	-.19706+08
.58304-02	.12843+00	.14169+01	.45764+00	.57068+02	.44891+02	.00000	-.19707+08
.11661-01	.12833+00	.14178+01	.91650+00	.57120+02	.44853+02	.00000	-.19707+08
.17491-01	.12817+00	.14194+01	.13779+01	.57205+02	.44789+02	.00000	-.19707+08
.23321-01	.12794+00	.14217+01	.18428+01	.57325+02	.44700+02	.00000	-.19707+08
.29152-01	.12765+00	.14246+01	.23125+01	.57479+02	.44585+02	.00000	-.19707+08
.34982-01	.12729+00	.14281+01	.27893+01	.57670+02	.44445+02	.00000	-.19708+08
.40813-01	.12686+00	.14323+01	.32737+01	.57895+02	.44279+02	.00000	-.19708+08
.46643-01	.12637+00	.14373+01	.37678+01	.58157+02	.44087+02	.00000	-.19709+08
.52473-01	.12581+00	.14430+01	.42733+01	.58457+02	.43869+02	.00000	-.19709+08
.58304-01	.12519+00	.14494+01	.47920+01	.58795+02	.43624+02	.00000	-.19710+08
.64134-01	.12450+00	.14567+01	.53262+01	.59172+02	.43352+02	.00000	-.19711+08
.69964-01	.12375+00	.14648+01	.58781+01	.59591+02	.43053+02	.00000	-.19712+08
.75795-01	.12293+00	.14738+01	.64501+01	.60052+02	.42726+02	.00000	-.19712+08
.81625-01	.12204+00	.14839+01	.70449+01	.60558+02	.42369+02	.00000	-.19714+08
.87455-01	.12109+00	.14950+01	.76654+01	.61112+02	.41982+02	.00000	-.19715+08
.93286-01	.12008+00	.15073+01	.83145+01	.61715+02	.41564+02	.00000	-.19716+08
.10150+00	.11853+00	.15267+01	.92835+01	.62654+02	.40918+02	.00000	-.19718+08
.10495+00	.11785+00	.15358+01	.97115+01	.63082+02	.40626+02	.00000	-.19719+08
.10816+00	.11719+00	.15447+01	.10122+02	.63498+02	.40343+02	.00000	-.19720+08
.11497+00	.11572+00	.15654+01	.11038+02	.64441+02	.39703+02	.00000	-.19722+08
.12003+00	.11457+00	.15825+01	.11752+02	.65198+02	.39192+02	.00000	-.19724+08
.12232+00	.11284+00	.16100+01	.12849+02	.66371+02	.38398+02	.00000	-.19727+08
.13357+00	.11126+00	.16368+01	.13856+02	.67459+02	.37658+02	.00000	-.19730+08
.13993+00	.10952+00	.16675+01	.14943+02	.68637+02	.36848+02	.00000	-.19733+08
.14576+00	.10793+00	.16983+01	.16003+02	.69773+02	.34049+02	.00000	-.19737+08

Group 8

PARTICLE START LINE PROPERTIES

52 POINT	SPECIE 53	U 54	V 55	THETA 56	ENTHALPY 57	DENSITY 58
1	1	.43867+04	.00000	.00000	.50821+08	.41806-04
1	2	.41994+04	.00000	.00000	.51228+08	.94862-04
1	3	.39460+04	.00000	.00000	.51674+08	.11244-03
1	4	.37884+04	.00000	.00000	.52027+08	.12661-03
1	5	.35389+04	.00000	.00000	.52563+08	.15266-03
1	6	.32769+04	.00000	.00000	.53218+08	.93531-04
2	1	.43873+04	.27314+02	.36670+00	.50819+08	.41787-04
2	2	.42000+04	.22702+02	.30288+00	.51229+08	.94817-04
2	3	.39465+04	.16940+02	.23287+00	.51677+08	.11238-03
2	4	.37889+04	.12562+02	.18995+00	.52033+08	.12653-03
2	5	.35393+04	.74544+01	.12068+00	.52571+08	.15248-03
2	6	.32773+04	.25979+01	.44528-01	.53233+08	.93430-04

Group 9

Sample Print out for Two-Phase Chemical Equilibrium Flow

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 1

SHUTTLE SEP MOTOR NOZZLE

POINT	SPECIE	U	V	THETA	ENTHALPY	DENSITY
3	1	.43891+04	.54725+02	.71435+00	.50815+08	.41730-04
3	2	.42018+04	.44989+02	.60664+00	.51229+08	.94683-04
3	3	.39481+04	.32146+02	.46649+00	.51685+08	.11220-03
3	4	.37905+04	.25174+02	.38053+00	.52048+08	.12630-03
3	5	.35406+04	.14941+02	.24179+00	.52601+08	.15214-03
3	6	.32786+04	.51141+01	.89371-01	.53277+08	.93137-04
4	1	.43921+04	.82332+02	.10739+01	.50808+08	.41637-04
4	2	.42047+04	.66947+02	.91217+00	.51228+08	.94465-04
4	3	.39509+04	.48382+02	.70159+00	.51698+08	.11192-03
4	4	.37930+04	.37890+02	.57233+00	.52071+08	.12575-03
4	5	.35427+04	.22491+02	.36374+00	.52644+08	.15161-03
4	6	.32808+04	.77209+01	.13984+00	.53342+08	.92682-04
5	1	.43963+04	.11024+03	.14364+01	.50797+08	.41510-04
5	2	.42089+04	.89660+02	.12204+01	.51227+08	.94173-04
5	3	.39548+04	.64815+02	.93895+00	.51712+08	.11154-03
5	4	.37966+04	.50758+02	.76596+00	.52098+08	.12548-03
5	5	.35458+04	.30138+02	.48699+00	.52696+08	.15092-03
5	6	.32838+04	.10386+02	.18122+00	.53420+08	.92113-04
6	1	.44019+04	.13856+03	.18029+01	.50782+08	.41354-04
6	2	.42143+04	.11272+03	.15321+01	.51223+08	.93817-04
6	3	.39598+04	.81516+02	.11793+01	.51726+08	.11109-03
6	4	.38011+04	.63827+02	.96200+00	.52126+08	.12495-03
6	5	.35498+04	.37916+02	.61198+00	.52748+08	.15015-03
6	6	.32877+04	.13127+02	.22876+00	.53497+08	.91493-04
7	1	.44088+04	.16740+03	.21744+01	.50763+08	.41171-04
7	2	.42209+04	.13622+03	.18984+01	.51214+08	.93518-04
7	3	.39660+04	.98557+02	.14235+01	.51736+08	.11060-03
7	4	.38067+04	.77147+02	.11610+01	.52149+08	.12438-03
7	5	.35548+04	.45862+02	.73917+00	.52791+08	.14937-03
7	6	.32924+04	.15958+02	.27771+00	.53559+08	.90893-04
8	1	.44171+04	.19889+03	.25523+01	.50738+08	.40968-04
8	2	.42288+04	.16024+03	.21701+01	.51200+08	.92984-04
8	3	.39735+04	.11602+03	.16724+01	.51738+08	.11009-03
8	4	.38132+04	.90765+02	.13635+01	.52160+08	.12382-03
8	5	.35608+04	.54014+02	.86906+00	.52815+08	.14865-03
8	6	.32980+04	.18894+02	.32824+00	.53589+08	.90393-04
9	1	.44269+04	.22718+03	.29376+01	.50708+08	.40748-04
9	2	.42380+04	.18490+03	.24982+01	.51179+08	.92535-04
9	3	.39822+04	.13397+03	.19269+01	.51727+08	.10960-03
9	4	.38207+04	.10473+03	.15702+01	.52155+08	.12332-03
9	5	.35688+04	.62415+02	.10022+01	.52910+08	.14807-03
9	6	.33044+04	.21945+02	.38050+00	.53574+08	.90070-04
10	1	.44383+04	.25840+03	.33320+01	.50670+08	.40515-04
10	2	.42486+04	.21030+03	.28337+01	.51148+08	.92086-04
10	3	.39923+04	.15252+03	.21878+01	.51701+08	.10915-03
10	4	.38291+04	.11909+03	.17814+01	.52128+08	.12292-03
10	5	.35764+04	.71108+02	.11390+01	.52765+08	.14771-03
10	6	.33117+04	.25119+02	.43459+00	.53502+08	.89991-04

Group 9 (Cont'd)

Sample Printout for Two-Phase Chemical Equilibrium Flow

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 1

SPACE SHUTTLE SRB MOTOR NOZZLE

POINT	SPECIE	U	V	THETA	ENTHALPY	DENSITY
11	1	.44514+04	.29073+03	.37368+01	.50624+08	.40275-04
11	2	.42605+04	.23655+03	.31778+01	.51106+08	.91649-04
11	3	.40038+04	.17175+03	.24563+01	.51656+08	.10896-03
11	4	.38366+04	.13351+03	.19980+01	.52073+08	.12266-03
11	5	.35861+04	.80143+02	.12803+01	.52681+08	.14763-03
11	6	.33198+04	.28926+02	.49058+00	.53367+08	.90207-04
12	1	.44661+04	.32434+03	.41537+01	.50569+08	.40030-04
12	2	.42739+04	.26377+03	.35316+01	.51051+08	.91235-04
12	3	.40167+04	.19177+03	.27334+01	.51588+08	.10894-03
12	4	.38591+04	.14925+03	.22205+01	.51988+08	.12255-03
12	5	.35976+04	.89572+02	.14265+01	.52549+08	.14787-03
12	6	.33289+04	.31869+02	.54849+00	.53169+08	.90741-04
13	1	.44827+04	.35945+03	.45844+01	.50505+08	.39780-04
13	2	.42887+04	.29211+03	.38964+01	.50983+08	.90847-04
13	3	.40312+04	.21270+03	.30204+01	.51498+08	.10821-03
13	4	.38606+04	.16516+03	.24499+01	.51873+08	.12262-03
13	5	.36093+04	.99453+02	.15784+01	.52373+08	.14842-03
13	6	.33391+04	.35456+02	.60836+00	.52924+08	.91581-04
14	1	.45011+04	.39623+03	.50307+01	.50430+08	.39525-04
14	2	.43051+04	.32171+03	.42736+01	.50901+08	.90484-04
14	3	.40472+04	.23468+03	.33187+01	.51485+08	.10806-03
14	4	.38734+04	.18160+03	.26873+01	.51731+08	.12784-03
14	5	.36229+04	.10985+03	.17367+01	.52166+08	.14925-03
14	6	.33504+04	.39193+02	.67020+00	.52663+08	.92662-04
15	1	.45214+04	.43494+03	.54946+01	.50345+08	.39263-04
15	2	.43231+04	.35275+03	.46648+01	.50804+08	.90133-04
15	3	.40648+04	.25706+03	.36298+01	.51253+08	.10796-03
15	4	.38875+04	.19925+03	.29340+01	.51568+08	.12319-03
15	5	.36378+04	.12582+03	.19022+01	.51950+08	.15028-03
15	6	.33631+04	.43091+02	.73467+00	.52431+08	.93861-04
16	1	.45437+04	.47581+03	.59782+01	.50250+08	.38987-04
16	2	.43426+04	.38542+03	.50718+01	.50695+08	.89772-04
16	3	.40840+04	.28240+03	.39556+01	.51109+08	.10786-03
16	4	.39031+04	.21768+03	.31921+01	.51401+08	.12359-03
16	5	.36538+04	.13244+03	.20759+01	.51760+08	.15136-03
16	6	.33774+04	.47167+02	.80011+00	.52310+08	.94983-04
17	1	.45678+04	.51911+03	.65035+01	.50144+08	.38697-04
17	2	.43639+04	.41955+03	.54965+01	.50577+08	.89367-04
17	3	.41049+04	.30852+03	.42982+01	.50953+08	.10770-03
17	4	.39205+04	.23732+03	.34640+01	.51249+08	.12394-03
17	5	.36702+04	.14429+03	.22587+01	.51551+08	.15225-03
17	6	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]
18	1	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]
18	2	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]
18	3	.41372+04	[illegible]	[illegible]	[illegible]	[illegible]
18	4	.39486+04	.26763+03	.38775+01	.51126+08	.12905-03
18	5	.36963+04	.16357+03	.25337+01	.51782+08	.15259-03
18	6	.34201+04	.57919+02	.92013+00	.52730+08	.95448-04

Group 9 (Cont'd)

Sample Printout for Two-Phase Chemical Equilibrium Flow

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
CAS-PA TITLE FLOW SOLUTION
CASE NO. 1

SPACE SHUTTLE SEP ASTRO NOZZLE

POINT	SPECIE	U	V	THETA	ENTHALPY	DENSITY
19	1	.46217+04	.61505+03	.75681+01	.49906+08	.37957-04
19	2	.44116+04	.49564+03	.64108+01	.50332+08	.88214-04
19	3	.41517+04	.36642+03	.50437+01	.50739+08	.10679-03
19	4	.39620+04	.28153+03	.40646+01	.51132+08	.12365-03
19	5	.37073+04	.17179+03	.26561+01	.51998+08	.15217-03
20	1	.46378+04	.64234+03	.78859+01	.49936+08	.37709-04
20	2	.44260+04	.51539+03	.66802+01	.50270+08	.87757-04
20	3	.41657+04	.38393+03	.52556+01	.50716+08	.10628-03
20	4	.39753+04	.29525+03	.42476+01	.51185+08	.12345-03
20	5	.37175+04	.1[illegible]+03	.27741+01	.52322+08	.15135-03
21	1	.46733+04	[illegible]	.85290+01	.49685+08	.37064-04
21	2	.44694+04	[illegible]	.72813+01	[illegible]	.86472-04
21	3	.41969+04	.42372+03	.57651+01	.50769+08	.10463-03
21	4	.40070+04	.32728+03	.46694+01	.51507+08	.12174-03
22	1	.47009+04	.75631+03	.91398+01	.49574+08	.36507-04
22	2	.44841+04	.61097+03	.77589+01	.50110+08	.85149-04
22	3	.42214+04	.45401+03	.61655+01	.50938+08	.10272-03
23	1	.47417+04	.83396+03	.99750+01	.49425+08	.35456-04
23	2	.45235+04	.67601+03	.84997+01	.50120+08	.82500-04
24	1	.47773+04	.90564+03	.10734+02	.49320+08	.34786-04

Group 9 (Cont'd)

THE MESH CONSTRUCTION WILL BE CONTROLED BY THE FOLLOWING VARIABLES

INTERIOR= .300-01 DX AXIS= .200-01 DL LIM= .150+00 DL DELETE= .100-02 DEG P.M.= .600+01 F= .650+00

Group 10

59 60 61 62 63 64

Sample Printout for Two-Phase Chemical Equilibrium Flow

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SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                GAS-PARTICLE FLOW SOLUTION
                                CASE NO.   1                                                    PAGE   21
(65) SPACE SHUTTLE SRB MOTOR NOZZLE                                                                  (74)
(66)  (67)                  (68)          (69)          (70)          (71)          (72)          (73)
LINE PAGE  DSCRIP + REGIME        R          X             M          THETA       ENTROPY      VELOCITY    H-TOTAL   ITR
                          MACH ANGLE   PRESSURE      DENSITY    TEMPERATURE   GAS CONST    LOCAL GAMMA   SHOCK ANGLE (81)
PARTICLE DATA                (75)         (76)         (77)         (78)         (79)         (80)
 SPECIE POINT  DESCRIPTION        V (82)       THETA (83)       D M (84)      ENTHALPY (85)  DENSITY (86)   TEMPERATURE (87)
                                                                                                                                  Group 11
  1   24  INPUT  + CONTIN    .13357+00    .11124+00    .16368+01    .13856+02    .67437+02    .52419+04    .19930+00    0
                            .37658+02    .91139+03    .68525-02    .43588+04    .19851+04    .12093+01
PARTICLE DATA                (88)
      2% LIMIT STREAMLINE   .48242+04    .10738+02    .13284+00    .49320+08    .34284-04    .45174+04
  1   25  INPUT  + CONTIN    .13993+00    .10959+00    .16675+01    .14983+02    .68637+02    .53708+04    .19733+00    0
                            .36888+02    .39134+03    .65735-02    .43199+04    .19848+04    .12101+01
PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT
  1   26  INPUT  + CONTIN    .14576+00    .10798+00    .16993+01    .16083+02    .69773+02    .54515+04    .19337+00    0
                            .36099+02    .37152+03    .62942-02    .42831+04    .19845+04    .12107+01
PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT
GAS MASS FLOW RATE =    .85715+02   PARTICLE MASS FLOW RATE =    .37352+01   MIXTURE MASS FLOW RATE =    .88952+02
                          (89)                                                                              (91)
                                        PARTICLE PERCENT LOADINGS                                                          Group 12
                                                (90)
                                          RADIUS      LOADING
                                        .11000+01   .99998+01
                                        .17000+01   .20000+02
                                        .25000+01   .20000+02
                                        .32000+01   .20001+02
                                        .45000+01   .20001+02
                                        .65000+01   .99969+01
PARTICLE PERCENT LOADING RELATIVE TO THE GAS =   .37744+01   (92) PARTICLE PERCENT LOADING RELATIVE TO THE MIXTURE =   .34971+01
                                                                                                                        (93)
                                        MOMENTUM INTEGRATION RESULTS
                                                                                                                        (94)
                                     FORCEX      FORCEY      TORQZ       ISP
                                   -.18212+05    .00000      .00000    .20474+03
                                                                                                                        (95)
                                     DELFXG      DELFYG      TORQZG      DELFXP      DELFYP      TORQZP
                                   .33778+03    .00000      .00000    .90047+03    .00000      .00000
```

Group 13

NOTES: (1) Typical printout for the startline data surface.
(2) Some points have been omitted for demonstration purposes.

Sample Printout for Two-Phase Chemical Equilibrium Flow

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                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                          CASE NO.    1                                                    PAGE   27

    SPACE SHUTTLE SEP MOTOR NOZZLE

LINE POINT  DSCRIP - REGIME        R            X            M            THETA        ENTROPY      VELOCITY     H-TOTAL   ITR
                                 MACH ANGLE   PRESSURE     DENSITY     TEMPERATURE   GAS CONST.   LOCAL GAMMA  SHOCK ANGLE

PARTICLE DATA                                                                                                                 (96)
 SPECIF POINT  DESCRIPTION          V            THETA          D M          ENTHALPY       DENSITY        TEMPERATURE
  2     23   INTER  - CONTIN   .12851+00    .12060+00    .16501+01    .13627+02    .67676+02    .53263+04   -.19728+08   6
                                .37301+02    .40279+03    .67329-02    .93394+04    .19950+04    .12096+01
PARTICLE DATA
     1   23                    .991253+09   .10722+02    .12820+00    .49070+08    .33699-09    .99983+04
     2   23 LIMIT STREAMLINE   .966776+09   .92390+01    .20403+00    .49791+08    .78835-09    .95728+04
-----------------------------------------------------------------------------------------------------------------
  2     24   INTER  - CONTIN   .13512+00    .11912+00    .16794+01    .14769+02    .67880+02    .54015+04   -.19730+08   6
                                .36599+02    .38418+03    .64733-02    .93061+04    .19847+04    .12108+01
PARTICLE DATA
     1   24 LIMIT STREAMLINE   .996690+09    .11591+02    .13469+00    .48920+08    .32546-09    .99704+04
-----------------------------------------------------------------------------------------------------------------
  2     25   INTER  - CONTIN   .14289+00    .11722+00    .17128+01    .16001+02    .68837+02    .54854+04   -.19733+08   4
                                .35722+02    .36379+03    .61855-02    .92680+04    .19893+04    .12112+01
PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT
-----------------------------------------------------------------------------------------------------------------
  2     26   WALL   - CONTIN   .14799+00    .11545+00    .17947+01    .17199+02    .69773+02    .55852+04   -.19737+08   4
                                .34971+02    .34899+03    .59177-02    .92312+04    .19890+04    .12120+01
PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT
-----------------------------------------------------------------------------------------------------------------
                                          PRESSURE INTEGRATION RESULTS                                          (97)
                                 FORCEX       FORCEY       TORQZ       DELEX       DELEY        ISP
                               -.18318+05    .00000       .00000    -.10595+03    .00000    .20593+03
                                                                                                                  } Group 14

          PERCENT CHANGE IN MASS, MOMENTUM AND ENERGY NUMERICAL INTEGRATION FOR LINE  2 RELATIVE TO THE START LINE
          PERCENT CHANGE IN MASS FLOW, GAS =   -.14895-01 (98) PARTICLE =   -.36269-01 (99) MIXTURE (100) =  -.15672-01 (109)
   PERCENT CHANGE IN MOMENTUM, GAS=   .75299+04 (101) PARTICLE =   .87967+00 (102) MIXTURE =  -.12303+01  ISP =  -.12148+01 (104)
          PERCENT CHANGE IN ENERGY, GAS =  -.33491+00  PARTICLE =   .90037+00  MIXTURE =  -.62869-02                                  } Group 15
                                   (105)                          (106)                                (107)
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NOTES: (1) Typical printout for a data surface inside the nozzle.
(2) Some points have been omitted for demonstration purposes.

Sample Printout for Two-Phase Chemical Equilibrium Flow

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                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                          CASE NO.    1                                                    PAGE   80

     SPACE SHUTTLE SEP MOTOR NOZZLE

LINE POINT  DSCRIP - REGIME        R            X            M            THETA        ENTROPY      VELOCITY     H-TOTAL   ITR
                                 MACH ANGLE   PRESSURE     DENSITY     TEMPERATURE   GAS CONST.   LOCAL GAMMA   SHOCK ANGLE
 PARTICLE DATA
  SPECIE POINT  DESCRIPTION        V            THETA          D H          ENTHALPY      DENSITY      TEMPERATURE
 60      PRN-HR - CONTIN     .31517+00    .74059+00    .42582+01    .43440+07    .69773+02    .90487+04    -.19737+00   2
                             .13582+02    .39810+01    .16253-03    .17803+04    .19811+04    .12798+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

 65      PRN-HR - CONTIN     .31517+00    .74059+00    .46490+01    .49346+07    .69773+02    .92647+04    -.19737+00   2
                             .12835+02    .21759+01    .10161-03    .15545+04    .19811+04    .12907+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

 65      PRN-HR - CONTIN     .31517+00    .74059+00    .50997+01    .55253+07    .69773+02    .94877+04    -.19737+00   2
                             .11308+02    .11210+01    .81027-04    .13361+04    .19811+04    .13031+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

 66      PRN-HR - CONTIN     .31517+00    .74059+00    .56450+01    .61159+07    .69773+02    .96949+04    -.19737+00   2
                             .10204+02    .53735+00    .39801-04    .11223+04    .19811+04    .13157+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

 66      PRN-HR - CONTIN     .31517+00    .74059+00    .63139+01    .67046+07    .69773+02    .98259+04    -.19737+00   2
                             .91130+01    .23595+00    .18633-04    .92042+03    .19811+04    .13282+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

 66      PRN-HR - CONTIN     .31517+00    .74059+00    .71804+01    .72973+07    .69773+02    .99795+04    -.19737+00   2
                             .80055+01    .92585-01    .92566-05    .72700+03    .19811+04    .13412+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

 66      PRN-HR - CONTIN     .31517+00    .74059+00    .83201+01    .78879+07    .69773+02    .10115+05    -.19737+00   2
                             .69031+01    .31929-01    .51921-05    .55151+03    .19811+04    .13527+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT
```

NOTES: (1) Typical printout for a data surface containing a Prandtl-Meyer Expansion.
(2) Some points have been omitted for demonstration purposes.

Sample Printout for Two-Phase Chemical Equilibrium Flow

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                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                          CASE NO.    1                                                    PAGE  169

     SPACE SHUTTLE SEP MOTOR NOZZLE

LINE POINT  DSCRIP - REGIME        R            X            H            THETA        ENTROPY      VELOCITY     H-TOTAL   ITR
                              MACH ANGLE   PRESSURE     DENSITY    TEMPERATURE    GAS CONST.   LOCAL GAMMA   SHOCK ANGLE

PARTICLE DATA
 SPECIF POINT  DESCRIPTION        V            THETA        D H          ENTHALPY       DENSITY        TEMPERATURE

11A     1  WALL   - CONTIN    .00000       .16758+01    .32345+01    .00000       .66197+03    .81502+04    -.19[illegible]+08    3
                              .18069+02    .18060+02    .50643-03    .25920+04    .19812+04    .12365+01

PARTICLE DATA
        1    1                .794675+04   .00000       .80755-01    .22432+08    .21071-05    .27626+04
        2    1                .789160+04   .00000       .10288+00    .23066+08    .34966-05    .28407+04
        3    1                .776027+04   .00000       .15476+00    .25476+08    .43799-05    .31375+04
        4    1                .766955+04   .00000       .21457+00    .28232+08    .49694-05    .34769+04
        5    1                .727550+04   .00000       .34715+00    .33341+08    .64098-05    .41061+04
        6    1                .675315+04   .00000       .554944+00   .38867+08    .85327-05    .41885+04

118     22  FREEBD - CONTIN   .10128+01    .95075+00    .83199+01    .69088+07    -.69773+02   .10115+08    -.19737+08    2
                              .69037+01    .31449-01    .91992-05    .55160+03    .19811+04    .13527+01

PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

A NEW STREAMLINE HAS BEEN INSERTED ON LINE 117 BETWEEN POINTS  25 AND  26

119     1  WALL   - CONTIN    .00000       .16949+01    .32648+01    .00000       .66928+03    .81845+04    -.19653+08    3
                              .17834+02    .17079+02    .48396-03    .25651+04    .19812+04    .12367+01

PARTICLE DATA
        1    1                .796784+04   .00000       .84491-01    .22329+08    .20538-05    .27499+04
        2    1                .790313+04   .00000       .11225+00    .22983+08    .39363-05    .28305+04
        3    1                .777129+04   .00000       .16486+00    .25369+08    .43166-05    .31244+04
        4    1                .762089+04   .00000       .22484+00    .28107+08    .48977-05    .34619+04
        5    1                .728436+04   .00000       .35740+00    .33198+08    .63143-05    .40885+04
        6    1                .676694+04   .00000       .56598+00    .38744+08    .84699-05    .41885+04

119     23  FREEBD - CONTIN   .10267+01    .95406+00    .83194+01    .68960+07    -.69773+02   .10115+08    -.19737+08    2
                              .69037+01    .31449-01    .91992-05    .55160+03    .19811+04    .13527+01

PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

                                   POINT NO.  21 ON LINE 119 HAS BEEN DELETED

A NEW STREAMLINE HAS BEEN INSERTED ON LINE 118 BETWEEN POINTS  51 AND  52

A NEW STREAMLINE HAS BEEN INSERTED ON LINE 118 BETWEEN POINTS  53 AND  54
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NOTES: (1) Typical printout for a data surface in the exhaust plume.
(2) Some points have been omitted for demonstration purposes.

Sample Printout for Single-Phase Chemical Equilibrium Flow with Free Molecular Considerations

Sample Printout for Single-Phase Chemical Equilibrium Flow With Free Molecular Considerations

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 1

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

RUN CONTROL PARAMETERS

ICON(1)	ICON(2)	ICON(3)	ICON(4)	ICON(5)	ICON(6)	ICON(7)	ICON(8)
1	2	21	2	1	0	1	2
ICON(9)	**ICON(10)**	**ICON(11)**	**ICON(12)**	**ICON(13)**	**ICON(14)**	**ICON(15)**	**ICON(16)**
0	99	1	1	1	0	0	100

FLOW CALCULATIONS ARE IN ENGLISH UNITS WITH THE R,X COORDINATES IN FEET

THE FLOW FIELD DATA WILL NOT WRITTEN ON TAPE

UPPER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
2	1	.00000	.00000	.00000	.26795+00	.16969+00	.30909+01
3	0	.20000-02	.00000	.00000	.00000	.00000	.10000+04

LOWER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
2	0	.00000	.00000	.00000	.00000	.00000	.10000+04

THERE ARE 0 PARTICLE SPECIES PRESENT IN THE GAS-PARTICLE MIXTURE

THE FOLLOWING GAS PROPERTIES IN ENGLISH UNITS ARE FOR IDEAL GAS
REAL GAS PROPERTIES

O/F
.00000

S	V	R	GAMMA	T	P	PR	VIS	CP
.00000								
	.00000	.20016+04	.11793+01	.54684+04	.10000+04	.00000	.00000	[illegible]
	.34536+04	.19925+04	.11711+01	.50256+04	.10187+04	.00000	.00000	[illegible]
	.55746+04	.19840+04	.12121+01	.42390+04	.35999+03	.00000	.00000	[illegible]
	.64815+04	.19820+04	.12224+01	.37476+04	.18000+03	.00000	.00000	[illegible]
	.71902+04	.19813+04	.12297+01	.32994+04	.90000+02	.00000	.00000	[illegible]
	.77605+04	.19811+04	.12344+01	.28962+04	.45001+02	.00000	.00000	[illegible]
	.83577+04	.19811+04	.12376+01	.24300+04	.18000+02	.00000	.00000	[illegible]
	.89543+04	.19811+04	.12731+01	.19314+04	.60004+01	.00000	.00000	[illegible]
	.91468+04	.19811+04	.12817+01	.17296+04	.36005+01	.00000	.00000	[illegible]

Sample Printout for Single-Phase Chemical Equilibrium Flow With Free Molecular Considerations

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTsVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 2

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

REAL GAS PROPERTIES

H-TOTAL

S	V	R	GAMMA	T	P	PR	VIS	CP
.00000	.93361+04	.19811+04	.12944+01	.14814+04	.18003+01	.00000	.00000	.00000

STARTING LINE INFO

R	V	M	THETA	S	MACH ANGLE	SHOCK ANGLE	O/F
.00000	.32324+01	.42555+01	.00000	.00000	.13591+02	.00000	.00000
.51977-01	.32320+01	.42541+01	.82494+00	.00000	.13595+02	.00000	.00000
.10376+00	.32309+01	.42533+01	.16503+01	.00000	.13598+02	.00000	.00000
.15570+00	.32290+01	.42524+01	.24726+01	.00000	.13601+02	.00000	.00000
.20777+00	.32264+01	.42513+01	.32907+01	.00000	.13605+02	.00000	.00000
.25955+00	.32230+01	.42498+01	.41031+01	.00000	.13609+02	.00000	.00000
.31122+00	.32190+01	.42479+01	.49070+01	.00000	.13616+02	.00000	.00000
.36271+00	.32142+01	.42454+01	.56994+01	.00000	.13624+02	.00000	.00000
.41401+00	.32087+01	.42420+01	.64770+01	.00000	.13635+02	.00000	.00000
.46505+00	.32026+01	.42376+01	.72345+01	.00000	.13649+02	.00000	.00000
.51577+00	.31958+01	.42317+01	.79646+01	.00000	.13669+02	.00000	.00000
.56608+00	.31885+01	.42239+01	.86586+01	.00000	.13695+02	.00000	.00000
.61587+00	.31806+01	.42141+01	.93123+01	.00000	.13727+02	.00000	.00000
.66508+00	.31723+01	.42031+01	.99397+01	.00000	.13764+02	.00000	.00000
.71372+00	.31635+01	.41931+01	.10576+02	.00000	.13797+02	.00000	.00000
.76189+00	.31542+01	.41858+01	.11251+02	.00000	.13822+02	.00000	.00000
.80975+00	.31443+01	.41812+01	.11967+02	.00000	.13837+02	.00000	.00000
.85742+00	.31339+01	.41785+01	.12710+02	.00000	.13846+02	.00000	.00000
.90499+00	.31228+01	.41770+01	.13467+02	.00000	.13851+02	.00000	.00000
.95248+00	.31111+01	.41763+01	.14232+02	.00000	.13854+02	.00000	.00000
.10000+01	.30987+01	.41757+01	.15000+02	.00000	.13856+02	.00000	.00000

RUN CUTOFF INFORMATION

UPPER BOUNDARY				LOWER BOUNDARY	
R= .10000+03	X= -.10000+03	THETA= .00000	R= .00000	X= .20000+02	THETA= .90000+02

VIBNO	ROTNO	TRANNO	CHARL	GAMV	GAMR
.10000+03	.50000+02	.20000+02	.10000+01	.00000	.00000

Group 16*

THE MESH CONSTRUCTION WILL BE CONTROLED BY THE FOLLOWING VARIABLES

DL INTERIOR= .300+01 DX AXIS= .100+01 DL LIM= .100+01 DL DELETE= .500-02 DEG P.M.= .500+01 F= .500+00

*NOTE: Free molecular flow calculations can also be included in the gas-particle flow.

Sample Printout for Single-Phase Chemical **Equilibrium** Flow With Free Molecular Considerations

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 8

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

(74)

LINE	POINT	DSCRIP	- RIGIME	R MACH ANGLE	X PRESSURE	M DENSITY	THETA TEMPERATURE	ENTROPY GAS CONST.	VELOCITY LOCAL GAMMA	C/F SHOCK ANGLE	ITR
1	14	INPUT	- CONTIN	.66508+00 .13764+02	.31723+01 .46950+01	.42031+01 .18630-03	.99397+01 .18318+04	.00000 .19811+04	.90499+04 .12775+01	.00000	0
1	15	INPUT	- CONTIN	.71372+00 .13797+02	.31435+01 .47737+01	.41931+01 .18875-03	.10576+02 .18384+04	.00000 .19811+04	.90436+04 .12772+01	.00000	0
1	16	INPUT	- CONTIN	.76189+00 .13822+02	.31642+01 .48127+01	.41855+01 .19057-03	.11251+02 .18433+04	.00000 .19811+04	.90387+04 .12770+01	.00000	0
1	17	INPUT	- CONTIN	.80975+00 .13837+02	.31443+01 .48701+01	.41812+01 .19172-03	.11967+02 .18463+04	.00000 .19811+04	.90360+04 .12768+01	.00000	0
1	18	INPUT	- CONTIN	.85742+00 .13846+02	.31339+01 .48917+01	.41785+01 .19235-03	.12710+02 .18481+04	.00000 .19811+04	.90343+04 .12768+01	.00000	0
1	19	INPUT	- CONTIN	.90499+00 .13851+02	.31228+01 .49038+01	.41770+01 .19276-03	.13467+02 .18491+04	.00000 .19811+04	.90334+04 .12767+01	.00000	0
1	20	INPUT	- CONTIN	.95246+00 .13854+02	.31111+01 .49100+01	.41762+01 .19295-03	.14232+02 .18496+04	.00000 .19811+04	.90329+04 .12767+01	.00000	0
1	21	INPUT	- CONTIN	.10000+01 .13856+02	.30989+01 .49144+01	.41757+01 .19309-03	.15000+02 .18499+04	.00000 .19811+04	.90325+04 .12767+01	.00000	0
1	22	PRN-MR	- CONTIN	.10000+01 .12812+02	.30989+01 .28978+01	.45095+01 .12542-03	.19869+02 .18388+04	.00000 .19811+04	.92165+04 .12865+01	.00000	0
1	23	PRN-MR	- CONTIN	.10000+01 .11747+02	.30989+01 .15166+01	.49115+01 .77372-04	.24750+02 .18247+04	.00000 .19811+04	.93888+04 .12944+01	.00000	0
1	24	PRN-MR	- CONTIN	.10000+01 .10807+02	.30989+01 .85363+00	.53333+01 .49631-04	.29624+02 .18502+04	.00000 .19811+04	.95494+04 .12944+01	.00000	0
1	25	PRN-MR	- CONTIN	.10000+01 .99026+01	.30989+01 .45765+00	.58145+01 .30661-04	.34499+02 .18849+04	.00000 .19811+04	.96987+04 .12944+01	.00000	0
1	26	PRN-MR	- CONTIN	.10000+01 .90295+01	.30989+01 .23197+00	.63717+01 .18139-04	.39374+02 .92955+03	.00000 .19811+04	.98375+04 .12944+01	.00000	0

NOTES: (1) Typical printout for a startline data surface containing a Prandtl-Meyer Expansion.
(2) Some points have been omitted for demonstration purposes.

Sample Printout for Single-Phase Chemical Equilibrium Flow With Free Molecular Considerations

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 12

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

LINE	POINT	DSCRIP	REGIME	R MACH ANGLE	X PRESSURE	H DENSITY	THETA TEMPERATURE	ENTROPY GAS CONST.	VELOCITY LOCAL GAMMA	DEL SHOCK ANGLE
2	27	INTER	CONTIN	.10613+01 .80889+01	.31827+01 .10068+00	.71007+01 .95186-05	.44254+02 .76883+03	.00000 .19811+04	.79788+04 .12944+01	.00000
2	28	INTER	CONTIN	.10686+01 .72641+01	.31756+01 .43634-01	.79085+01 .49804-05	.49073+02 .63535+03	.00000 .19811+04	.10095+05 .12944+01	.00000
2	29	INTER	CONTIN	.10753+01 .64628+01	.31680+01 .17134-01	.88839+01 .24203-05	.53898+02 .51393+03	.00000 .19811+04	.10199+05 .12944+01	.00000
2	30	INTER	CONTIN	.10812+01 .54814+01	.31599+01 .60027-02	.10100+02 .10777-05	.58729+02 .40486+03	.00000 .19811+04	.10292+05 .12944+01	.00000
2	31	INTER	CONTIN	.10864+01 .49174+01	.31515+01 .18136-02	.11665+02 .42748-06	.63566+02 .30837+03	.00000 .19811+04	.10373+05 .12944+01	.00000
2	32	INTER	CONTIN	.10908+01 .41677+01	.31427+01 .45095-03	.13757+02 .14587-06	.68408+02 .22470+03	.00000 .19811+04	.10443+05 .12944+01	.00000
2	33	INTER	CONTIN	.10946+01 .34302+01	.31336+01 .85775-04	.16708+02 .40470-07	.73254+02 .15406+03	.00000 .19811+04	.10502+05 .12944+01	.00000
2	34	INTER	CONTIN	.10976+01 .27032+01	.31244+01 .11044-04	.21190+02 .83055-08	.78110+02 .96649+02	.00000 .19811+04	.10549+05 .12944+01	.00000
2	35	FREERD	CONTIN	.10987+01 .27780+01	.31201+01 .13907-04	.20603+02 .99245-08	.77877+02 .10185+03	.00000 .19811+04	.10545+05 .12944+01	.00000

POINT NO. 34 ON LINE 2 HAS BEEN DELETED

PERCENT CHANGE IN MASS, MOMENTUM AND ENERGY NUMERICAL INTEGRATION FOR LINE 2 RELATIVE TO THE START LINE

THE PERCENT CHANGE IN MASS FLOW IS = -.22084+00

PERCENT CHANGE IN MOMENTUM IS = .18840+04 ISP = -.19527+01

PERCENT CHANGE IN ENERGY IS = .00000

NOTES: (1) Typical printout for a data surface in the exhaust plume.
(2) Some points have been omitted for demonstration purposes.

Sample Printout for Single-Phase Chemical Equilibrium Flow With Free Molecular Considerations

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 23

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

LINE	POINT	DSCRIP	= REGIME	R MACH ANGLE	X PRESSURE	Y DENSITY	THETA TEMPERATURE	ENTROPY GAS CONST.	VELOCITY LOCAL GAMMA	[illegible] SHOCK ANGLE	ITR
6	29	INTER	= CONTIN	.11712+01 .57651+01	.32324+01 .67428-02	.99553+01 .11017-05	.57858+02 .41509+03	.00000 .19811+04	.10282+05 .12944+01	.00000	5
6	30	INTER	= CONTIN	.11808+01 .50786+01	.32158+01 .23711-02	.11797+02 .52584-06	.62206+02 .32776+03	.00000 .19811+04	.10357+05 .12944+01	.00000	5
6	31	INTER	= CONTIN	.11890+01 .43986+01	.31987+01 .71057-03	.13038+02 .20727-06	.66612+02 .24919+03	.00000 .19811+04	.10423+05 .12944+01	.00000	4
6	32	INTER	= FREE M	.11956+01 .45607+01	.31824+01 .21450-03	.12576+02 .76136-07	.69344+02 .20930+03	.00000 .19811+04	.10456+05 .16670+01	.00000	1
6	33	INTER	= FREE M	.12013+01 .38782+01	.31456+01 .43479-04	.14715+02 .20778-07	.73346+02 .15280+03	.00000 .19811+04	.10503+05 .16670+01	.00000	1
6	34	INTER	= FREE M	.12073+01 .31529+01	.31415+01 .72497-05	.13132+02 .51737-08	.78371+02 .10185+03	.00000 .19811+04	.10545+05 .16670+01	.00000	1

PERCENT CHANGE IN MASS, MOMENTUM AND ENERGY NUMERICAL INTEGRATION FOR LINE 6 RELATIVE TO THE START LINE

THE PERCENT CHANGE IN MASS FLOW IS = -.16398+01

PERCENT CHANGE IN MOMENTUM IS = .18485+04 ISP = -.23162+01

PERCENT CHANGE IN ENERGY IS = .00000

NOTES: (1) Typical printout for a data surface containing free molecular points.
(2) Some points have been omitted for demonstration purposes.

Sample Printout for Single-Phase
Finite Rate Chemistry Flow

Sample Printout for Single-Phase Finite Rate Chemistry Flow

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO.   21                                                                    PAGE    1

CASE 21 - SOOLRF 6/1 CONE, O/F=2.2 , FINITE RATE, INVISCID, VAR O/F

                                    RUN CONTROL PARAMETERS
          ICON(1)   ICON(2)   ICON(3)   ICON(4)   ICON(5)   ICON(6)   ICON(7)   ICON(8)
             3         2        21         2         1         0         1         3

          ICON(9)   ICON(10)  ICON(11)  ICON(12)  ICON(13)  ICON(14)  ICON(15)  ICON(16)
             0        50        21         1         0         0         0        301

FLOW CALCULATIONS ARE IN ENGLISH UNITS WITH THE R,Z COORDINATES IN FEET

THE FLOW FIELD DATA WILL BE WRITTEN ON TAPE

                                    UPPER BOUNDARY
   TYPE   ITRANS        A            B            C            D            E            MAX
    2       1        .00000       .00000       .00000      .26795+00    .36781-01    .20517+00
    3       0      .19407+02    .14000+01      .00000      .00000       .00000       .83333+01

                                    LOWER BOUNDARY
   TYPE   ITRANS        A            B            C            D            E            MAX
    2       0        .00000       .00000       .00000      .00000       .00000       .83333+01
```

Sample Printout for Single-Phase Finite Rate Chemistry Flow

```
SPECIE THERMODYNAMIC AND REACTION DATA
NT,NS,NR,NM,ICTAPE,KGUP,IDIOO=  24   16   23   3   0   8   1   (114)

PRANDTL NUMBER =   .70000000+00   (115)
BASE VISCOSITY =   .18651198-05   (116)
EXPONENT       =   .60000000+00   (117)
```

(118)	REACTIONS BEING CONSIDERED	KR=A*EXP(B/RT+.M)/T**N	(120) A	(121) N	(122) B	(123) M	(124) R-TYPE	(125) K-TYPE
1	H + OH + M1 = H2O + M1		2.219*22	2.0	.0	.0	2	2
2	O + H + M1 = OH + M1		7.260*15	.0	.0	.0	2	1
3	O + O + M1 = O2 + M1		1.379*18	1.0	-340.0	.0	2	4
4	H + H + M2 = H2 + M2		1.016*18	1.0	.0	.0	2	2
5	CO + O + M3 = CO2 + M3		7.26*14	.0	-4000.0	.0	2	3
6	OH + H = H2 + O		8.435*09	-1.0	-7000.0	.0	1	4
7	OH + O = H + O2		2.410*13	.0	.0	.0	1	1
8	OH + H2 = H2O + H		4.025*06	-2.0	-2900.0	.0	1	4
9	OH + CO = CO2 + H		6.627*04	-2.0	1600.0	.0	1	4
10	OH + OH = H2O + O		6.025*12	.0	-1100.0	.0	1	3
11	CH4 + OH = CH3 + H2O		2.837*13	.0	-5000.0	.0	1	3
12	CH4 + H = CH3 + H2		1.996*13	.0	-5000.0	.0	1	3
13	CH4 + O = CH3 + OH		2.109*13	.0	-9100.0	.0	1	3
14	CH3 + O = CH2O + H		6.627*13	.0	.0	.0	1	1
15	CH2O + OH = CHO + H2O		5.422*11	-.5	.0	.0	1	2
16	CH2O + H = CHO + H2		1.325*13	.0	-3800.0	.0	1	3
17	CH2O + O = CHO + OH		9.640*10	.0	.0	.0	1	1
18	CH2O + M1 = CO + H2 + M1		2.109*16	.0	-35000.0	.0	5	3
19	CHO + OH = CO + H2O		1.265*14	.0	.0	.0	1	1
20	CHO + H = CO + H2		5.001*13	.0	-10000.0	.0	1	3
21	CHO + O = CO + OH		1.265*14	.0	.0	.0	1	1
22	CHO + O2 = CO + H		5.001*13	.0	-1600.0	.0	7	3
23	CHO + M1 = CO + H + M1		7.230*13	.0	-15000.0	.0	5	3

CATALYTIC SPECIES BEING CONSIDERED (126)

```
M1  = 1.00 C    , 1.00 CH4  , 1.00 CO   , 1.00 H2   , 3.00 H2O  , 1.00 NH3  , 1.00 N2   ,
      2.00 CO2  , 1.00 H    , 1.00 NO   , 1.00 OH   , 1.00 O    , 1.00 O2   , 1.00 CH3  ,
      1.00 CH2O , 1.00 CHO  ,

M2  = 1.00 C    , 1.00 CH4  , 1.00 CO   , 1.00 H2   ,10.00 H2O  , 1.00 NH3  , 1.00 N2   ,
      3.00 CO2  , 1.00 H    , 1.00 NO   , 2.00 OH   , 1.00 O    , 1.00 O2   , 1.00 CH3  ,
      1.00 CH2O , 1.00 CHO  ,

M3  = 1.00 C    , 1.00 CH4  , 1.00 CO   , 1.00 H2   ,10.00 H2O  , 1.00 NH3  , 1.00 N2   ,
      3.00 CO2  , 1.00 H    , 1.00 NO   , 1.00 OH   , 1.00 O    ,20.00 O2   , 1.00 CH3  ,
      1.00 CH2O , 1.00 CHO  ,
```

Group 17

Sample Printout for Single-Phase Finite Rate Chemistry Flow

SPECIE MOLE FRACTIONS ON THE START LINE ARE READ FROM CARDS

POINT 127 128

POINT										
1	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.74780-01	.20780+00	.63820-03	.-3150+00	.85700-03	.12570-02	.28310+00	.56340-05	.00000	.00000
1	OH	O	O2	CH3	CH2O	CHO				
	.00000	.00000	.00000	.00000	.00000	.00000				
2	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.79100-01	.18990+00	.63360-02	.31840+00	.69990-02	.11890-02	.27820+00	.18310-03	.00000	.00000
2	OH	O	O2	CH3	CH2O	CHO				
	.00000	.00000	.00000	.00000	.00000	.00000				
3	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.57070-01	.12970+00	.62990-01	.47040+00	.16650-01	.88890-03	.26410+00	.16870-02	.00000	.00000
3	OH	O	O2	CH3	CH2O	CHO				
	.00000	.00000	.00000	.00000	.00000	.00000				
4	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.00000	.22630-01	.16690+00	.98510+00	.60060-01	.35010-03	.25730+00	.79110-02	.12170-03	.28850-06
4	OH	O	O2	CH3	CH2O	CHO				
	.77240-05	.00000	.00000	.00000	.00000	.00000				
5	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.00000	.32960-06	.15790+00	.31630+00	.21750+00	.28520-04	.28330+00	.21290-01	.29960-02	.12950-03
5	OH	O	O2	CH3	CH2O	CHO				
	.11510-02	.27660-04	.17390-04	.00000	.00000	.00000				
6	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.00000	.00000	.12350+00	.15270+00	.39160+00	.45390-05	.31050+00	.99860-01	.10100-01	.23370-02
6	OH	O	O2	CH3	CH2O	CHO				
	.11910-01	.10340-02	.18840-02	.00000	.00000	.00000				
7	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.00000	.00000	.84030-01	.65810-01	.38690+00	.00000	.32400+00	.71480-01	.12700-01	.81070-02
7	OH	O	O2	CH3	CH2O	CHO				
	.29160-01	.39190-02	.12170-01	.00000	.00000	.00000				
8	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.00000	.00000	.58790-01	.34920-01	.38990+00	.00000	.32850+00	.89300-01	.96100-02	.19290-01
8	OH	O	O2	CH3	CH2O	CHO				
	.39160-01	.47750-02	.33730-01	.00000	.00000	.00000				

Group 18

NOTE: Some points have been omitted for demonstration purposes.

Sample Printout for Single-Phase Finite Rate Chemistry Flow

```
20    OH          O           O2          CH3         CH2O        CHO
      .17030-02   .33800-04   .21280-04   .00000      .00000      .00000

21    C           CH4         CO          H2          H2O         NH3         N2          CO2         H           NO
      .00000      .74950-07   .14080+00   .21720+00   .30120+00   .82950-05   .30130+00   .33010-01   .45300-02   .17100-03

21    OH          O           O2          CH3         CH2O        CHO
      .17030-02   .33800-04   .21280-04   .00000      .00000      .00000

CHAMBER PRESSURE (ATM) =    .38014+02 CHAMBER TEMPERATURE (DEG-K) =    .37361+04

                THERE ARE  0 PARTICLE SPECIES PRESENT IN THE GAS-PARTICLE MIXTURE

                                    RUN CUTOFF INFORMATION
                    UPPER BOUNDARY                                          LOWER BOUNDARY
      R=    .25000+01   X=    .00000    THETA=    .00000    R=    .00000    X=    .60000+00   THETA=    .90000+02

                THE MESH CONSTRUCTION WILL BE CONTROLED BY THE FOLLOWING VARIABLES
  DL INTERIOR=   .150-01 DX AXIS=   .150-01 DL LIM=   .000   DL DELETE=   .100-04 DEG P.M.=   .400+01 F=   .375+00
```

Group 18 (Cont'd)

129

130

Sample Printout for Single-Phase Finite Rate Chemistry Flow

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                GAS-PARTICLE FLOW SOLUTION
                                CASE NO.   21                                                    PAGE    2

CASE 21 - SODLAF 6/1 CONE, O/F=2.2 , FINITE RATE, INVISCID, VAR O/F

LINE POINT  DSCRIP - REGIME        R              X              M            THETA        ENTROPY       VELOCITY      H-TOTAL   ITR
                                MACH ANGLE     PRESSURE       DENSITY     TEMPERATURE   GAS CONST.    LOCAL GAMMA   SHOCK ANGLE
                                   TO*            PO*            S*

  1     1   INPUT  - CONTIN     .00000         .84167-02      .10274+01    .00000        .00000        .31052+04     .13224+08    0
                                .76745+02      .27517+03      .54912-02    .18993+04     .37993+04     .12660+01
                                .21660+04      .51429+03      .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       7.4785-02   CH4     2.0781-01   CO      6.3824-04   H2      4.3153-01   H2O     8.5705-04   NH3     1.2571-03   N2      2.8312-01
CO2     5.6364-06   H       0.0000      NO      0.0000      OH      0.0000      O       0.0000      O2      0.0000      CH3     0.0000
CH2O    0.0000      CHO     0.0000
-----------------------------------------------------------------------------------------------------------------------------------

  1     2   INPUT  - CONTIN     .19561-02      .84167-02      .10291+01    .74624+00     .00000        .31483+04     .12984+08    0
                                .76336+02      .27440+03      .53672-02    .19242+04     .38260+04     .12712+01
                                .22006+04      .51479+03      .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       7.9104-02   CH4     1.8991-01   CO      6.3363-03   H2      4.3862-01   H2O     6.4443-03   NH3     1.1841-03   N2      2.7821-01
CO2     1.8311-04   H       0.0000      NO      0.0000      OH      0.0000      O       0.0000      O2      0.0000      CH3     0.0000
CH2O    0.0000      CHO     0.0000
-----------------------------------------------------------------------------------------------------------------------------------

  1     3   INPUT  - CONTIN     .39122-02      .84167-02      .10238+01    .15011+01     .00000        .32426+04     .11265+08    0
                                .77629+02      .27475+03      .50759-02    .20735+04     .37591+04     .12870+01
                                .23854+04      .51507+03      .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       5.7074-02   CH4     1.2471-01   CO      6.2444-02   H2      4.7043-01   H2O     1.4651-02   NH3     8.8846-04   N2      2.6612-01
CO2     1.4871-03   H       0.0000      NO      0.0000      OH      0.0000      O       0.0000      O2      0.0000      CH3     0.0000
CH2O    3.[illegible]       CHO     0.0000
-----------------------------------------------------------------------------------------------------------------------------------

  1     4   INPUT  - CONTIN     .58682-02      .84167-02      .10214+01    .22464+01     .00000        .35142+04     .69241+07    0
                                .78256+02      .27774+03      .43259-02    .26733+04     .33964+04     .13038+01
                                .30969+04      .51283+03      .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4     2.2433-02   CO      1.6692-01   H2      4.8516-01   H2O     6.0067-02   NH3     3.5014-04   N2      2.5733-01
CO2     7.4119-03   H       1.2171-04   NO      2.8453-07   OH      7.0268-06   O       0.0000      O2      0.0000      CH3     0.0000
CH2O    0.0000      CHO     0.0000
-----------------------------------------------------------------------------------------------------------------------------------
```

NOTES: (1) Typical printout for the startline data surface.
(2) Some points have been omitted for demonstration purposes.

Sample Printout for Single-Phase Finite Rate Chemistry Flow

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                GAS-PARTICLE FLOW SOLUTION
                                CASE NO.   21                                                    PAGE   45

CASE 21 - SOCLOF 6/1 CONE, O/F=7.2 , FINITE RATE, INVISCID, VAR O/F

LINE POINT  DSCRIP - REGIME        R            X            M            THETA        ENTROPY      VELOCITY     H-TOTAL    ITP
                                MACH ANGLE   PRESSURE     DENSITY     TEMPERATURE   GAS CONST.   LOCAL GAMMA  SHOCK ANGLE
                                   TO*          PO*          S*

 60     1  WALL    - CONTIN     .00000       .62272-01    .20063+01    .00000       .91272-05    .52447+04    .13199+09    3
                                .29896+02    .65120+02    .17854-02    .13825+04    .37993+04    .13011+01
                                .22201+04    .35364+03    .00000
CHEMICAL SPECIE MOLE FRACTIONS                (131)
C       7.4785-02   CH4     2.0781-01   CO      6.3824-04   H2      4.3153-01   H2O     8.5705-04   NH3     1.2571-03   N2      2.8312-01
CO2     5.6344-04   H       3.4528-19   NO      0.0000      OH      1.7397-25   O       3.9207-35   O2      0.0000      CH3     3.0251-18
CH2O    5.1725-10   CHO     1.1351-18   3
-----------------------------------------------------------------------------------------------------------------------------------

 63    21  WALL    - CONTIN     .51639-01    .55452-01    .19568+01    .15000+02    .77017+02    .67522+04    .36075+07    3
                                .30733+02    .70385+02    .10656-02    .37807+04    .25158+04    .12518+01
                                .56034+04    .35518+03    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4     4.9604-08   CO      1.4019-01   H2      2.1814-01   H2O     3.0192-01   NH3     8.3046-06   N2      3.0165-01
CO2     3.3906-02   H       3.4555-03   NO      1.7120-04   OH      6.3044-04   O       6.4868-06   O2      4.3406-06   CH3     1.9276-08
CH2O    9.5135-08   CHO     1.4114-05
-----------------------------------------------------------------------------------------------------------------------------------

                                                PRESSURE INTEGRATION RESULTS
                                FORCEX       FORCEY       TORQZ        DELFX        DELFY        ISP
                             -.47885+03    .00000       .00000      -.14807+01    .00000      .24229+03

 61     1  WALL    - CONTIN     .00000       .64003-01    .20242+01    .00000       .91334-05    .52747+04    .13195+09    3
                                .29606+02    .63188+02    .17445-02    .13728+04    .37993+04    .13019+01
                                .22720+04    .34887+03    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       7.4785-02   CH4     2.0781-01   CO      6.3824-04   H2      4.3153-01   H2O     8.5705-04   NH3     1.2571-03   N2      2.8312-01
CO2     5.6344-04   H       3.3760-19   NO      0.0000      OH      1.5902-25   O       2.5212-35   O2      0.0000      CH3     2.9587-18
CH2O    5.1736-10   CHO     1.2094-18
-----------------------------------------------------------------------------------------------------------------------------------

 61    21  WALL    - CONTIN     .52095-01    .57151-01    .19735+01    .15000+02    .78410+02    .67916+04    .34068+07    3
                                .30445+02    .68429+02    .10418-02    .37597+04    .25158+04    .12521+01
                                .54055+04    .35364+03    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4     4.9635-08   CO      1.4015-01   H2      2.1819-01   H2O     3.0190-01   NH3     8.3047-06   N2      3.0165-01
CO2     3.3845-02   H       3.4353-03   NO      1.7120-04   OH      6.1685-04   O       6.3040-06   O2      4.2352-06   CH3     1.9187-08
CH2O    9.2748-08   CHO     1.4215-05
-----------------------------------------------------------------------------------------------------------------------------------

                                                PRESSURE INTEGRATION RESULTS
                                FORCEX       FORCEY       TORQZ        DELFX        DELFY        ISP
                             -.48033+03    .0000        .00000      -.14831+01    .00000      .24304+03
```

NOTES: (1) Typical printout for a data surface inside the nozzle.
(2) Some points have been omitted for demonstration purposes.

Sample Printout for Single-Phase Finite Rate Chemistry Flow

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                GAS-PARTICLE FLOW SOLUTION
                                CASE NO.   21                                                    PAGE   89

CASE 21 - SOOLAF 6/1 CONE, O/F=2.2 , FINITE RATE, INVISCID, VAR O/F

LINE POINT  DSCRIP - REG 4E        R            X            M          THETA       ENTROPY      VELOCITY     H-TOTAL   ITR
                                MACH ANGLE   PRESSURE     DENSITY    TEMPERATURE   GAS CONST.   LOCAL GAMMA  SHOCK ANGLE
                                  TO*          PO*          S*

 114    25  PRN-HR - CONTIN     .91755-01    .20517+00    .35807+01    .29767+02    .12937+03    .93012+04    .36189+07    5
                                .16222+02    .39106+01    .10798-03    .20740+04    .25145+04    .12938+01
                                .66307+04    .63182+02    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4     5.0639-08   CO      1.3896-01   H2      2.1947-01   H2O     3.0133-01   NH3     8.3088-06   N2      3.0180-01
CO2     3.5089-02   H       2.9945-03   NO      1.7129-04   OH      1.1603-04   O       1.3375-06   O2      1.6412-06   CH3     1.7015-08
CH2O    2.2823-08   CHO     4.9038-05

 114    26  PRN-HR - CONTIN     .91755-01    .20517+00    .37735+01    .33459+02    .12937+03    .94722+04    .36189+07    5
                                .15372+02    .27979+01    .83120-04    .19277+04    .25145+04    .12999+01
                                .66307+04    .50267+02    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4     5.0639-08   CO      1.3896-01   H2      2.1947-01   H2O     3.0133-01   NH3     8.3088-06   N2      3.0180-01
CO2     3.5089-02   H       2.9945-03   NO      1.7129-04   OH      1.1603-04   O       1.3375-06   O2      1.6412-06   CH3     1.7015-08
CH2O    2.2823-08   CHO     4.9038-05

 114    27  PRN-HR - CONTIN     .91755-01    .20517+00    .39812+01    .37150+02    .12937+03    .96366+04    .36189+07    5
                                .14553+02    .19633+01    .63034-04    .17837+04    .25145+04    .13063+01
                                .66307+04    .39331+02    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4     5.0639-08   CO      1.3896-01   H2      2.1947-01   H2O     3.0133-01   NH3     8.3088-06   N2      3.0180-01
CO2     3.5089-02   H       2.9945-03   NO      1.7129-04   OH      1.1603-04   O       1.3375-06   O2      1.6412-06   CH3     1.7015-08
CH2O    2.2823-08   CHO     4.9038-05

 114    28  PRN-HR - CONTIN     .91755-01    .20517+00    .42109+01    .40842+02    .12937+03    .97993+04    .36189+07    5
                                .13743+02    .13481+01    .47135-04    .16380+04    .25145+04    .13135+01
                                .66307+04    .30288+02    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4     5.0639-08   CO      1.3896-01   H2      2.1947-01   H2O     3.0133-01   NH3     8.3088-06   N2      3.0180-01
CO2     3.5089-02   H       2.9945-03   NO      1.7129-04   OH      1.1603-04   O       1.3375-06   O2      1.6412-06   CH3     1.7015-08
CH2O    2.2823-08   CHO     4.9038-05
```

NOTES: (1) Typical printout for a data surface containing a Prandtl-Meyer Expansion.
(2) Some points have been omitted for demonstration purposes.

Sample Printout for Single-Phase Finite Rate Chemistry Flow

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                   GAS-PARTICLE FLOW SOLUTION
                                   CASE NO.   21                                          PAGE  115

CASE 21 - SOCLRF 6/1 CONE, O/F=2.2 , FINITE RATE, INVISCID, VAR O/F

LINE POINT  DSCRIP - REGIME        R            X            M            THETA        ENTROPY      VELOCITY     H-TOTAL    ITR
                                 MACH ANGLE   PRESSURE     DENSITY     TEMPERATURE   GAS CONST.   LOCAL GAMMA  SHOCK ANGLE
                                   T0*          P0*          S*

 129     1  WALL    - CONTIN     .00000       .22341+00    .29826+01    .00000       .91677-05    .64753+04    .13187+08    2
                                 .19590+02    .12303+02    .50779-03    .91833+03    .37993+04    .13509+01
                                 .23518+04    .14467+03    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       7.4785-02   CH4    2.0781-01   CO     6.3824-04   H2     4.3153-01   H2O    8.5705-04   NH3    1.2571-03   N2     2.8312-01
CO2     5.6364-06   H      1.2664-21   NO     0.0000      OH     5.3647-29   O      0.0000      O2     0.0000      CH3    1.4675-19
CH2O    5.1793-10   CHO    4.3574-18
-----------------------------------------------------------------------------------------------------------------------------------

 129    34  FREEBD - CONTIN      .95802-01    .70758+00    .58115+01    .60199+02    .13845+03    .10475+05    .36062+07    2
                                 .99084+01    .13472+00    .80696-05    .95627+03    .25140+04    .13514+01
                                 .66307+04    .58590+01    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4    5.0650-08   CO     1.3879-01   H2     2.1951-01   H2O    3.0140-01   NH3    8.3105-06   N2     3.0186-01
CO2     3.5096-02   H      2.7946-03   NO     1.7132-04   OH     1.1569-04   O      1.3377-06   O2     1.6416-06   CH3    1.7018-08
CH2O    2.2825-08   CHO    2.4958-04
-----------------------------------------------------------------------------------------------------------------------------------

                                   POINT NO.  32 ON LINE 129 HAS BEEN DELETED

 130     1  WALL    - CONTIN     .00000       .22400+00    .29853+01    .00000       .91677-05    .64778+04    .13186+08    2
                                 .19571+02    .12248+02    .50609-03    .91725+03    .37993+04    .13511+01
                                 .23522+04    .14428+03    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       7.4785-02   CH4    2.0781-01   CO     6.3824-04   H2     4.3153-01   H2O    8.5705-04   NH3    1.2571-03   N2     2.8312-01
CO2     5.6364-06   H      1.2417-21   NO     0.0000      OH     5.2150-29   O      0.0000      O2     0.0000      CH3    1.4575-19
CH2O    5.1793-10   CHO    4.3584-18
-----------------------------------------------------------------------------------------------------------------------------------

 130    33  FREEBD - CONTIN      .96187-01    .70776+00    .58109+01    .60318+02    .14056+03    .10475+05    .36064+07    2
                                 .99094+01    .13477+00    .80679-05    .95650+03    .25139+04    .13514+01
                                 .66308+04    .58578+01    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4    5.0652-08   CO     1.3876-01   H2     2.1957-01   H2O    3.0140-01   NH3    8.3107-06   N2     3.0187-01
CO2     3.5097-02   H      2.7646-03   NO     1.7132-04   OH     1.1562-04   O      1.3376-06   O2     1.6416-06   CH3    1.7018-08
CH2O    2.2825-08   CHO    2.7967-04
-----------------------------------------------------------------------------------------------------------------------------------
```

NOTES: (1) Typical printout for a data surface in the exhaust plume.
(2) Some points have been omitted for demonstration purposes.

3.3.2 Description of Unformatted Binary Output

The binary tape output on unit 13 is described in this section. Initial input data are written on the first part of the data tape and gaseous and particle data are written out for each data point in the flow field. This tape is formatted so that it may be used by other auxiliary routines (plot, plume impingement or radiation).

GROUP I — General Information

Number of Records = 1

Write ( ) (HEADER(I), I=1, 60), ISPECS, IMETRIC

- HEADER
  - run identification (2A4)
  - date (3A4)
  - description (55A4)
- ISPECS = number of particle species to be considered
- IMETRIC* = 0 English flowfield units
  = 1 Metric flowfield units

GROUP II — Gas Data

Number of Records = 1 + IOF*IS

Write ( ) (BETA(I), I=1, 6), IOF, IS

- BETA is gas identification name (6A4)
- IOF number of total enthalpy cuts through "Mollier chart" (max = 10)
- IS number of entropy cuts (max = 2)

DO M=1, IOF
DO I=1, IS

Write ( ) IV, IDATA, ((TEMP(J, K), K=1, IDATA), J=1, IV), IVT, ((CPM(J, K), K=1, 3), J=1. IVT), RSTAR, PINF, EMINF, GAMINF, FINF, EXINF, XSHIFT

*Determined from ICON(9).

- IV — number of velocity cuts through "Mollier chart" for this total enthalpy and entropy + 2 (max = 15)
- IDATA — number of gaseous species present for this total enthalpy and entropy (max = 98)
- GAMINF — freestream isentropic exponent
- IVT — = IV-2
- RSTAR — throat radius (ft or meters)
- PINF — ambient pressure (psf or Newtons/m^2)
- EMINF — freestream or external stream Mach number
- EXINF — limit to which equation applies
- FINF — linear static pressure gradient (slope) θ approach
- TEMP — contains the following information for each value of IOF, IS
- XSHIFT — nozzle length (ft or meters)

	1	2	3	4	5	6	7	8	9	. . . .	IDATA		
1	p_f						(A4			. . . .	(A4	( )	Species Name
2							A4)			. . . .	A4)		
3	Htg	P	T	S	ψ	γ	M_c	X_1		. . . .	X_F		
4	|			|		M^*	|			|		
5	|			|			|			|		
.	c			c				|			|		
.	o			o				|			|		
.	n			n				|		Mole	|		
.	s			s				|		Fractions	|		
.	t			t				|			|		
.	a			a				|			|		
.	n			n				|			|		
.	t			t				|			|		
.	|			|				|			|		
IV	Htg	P	T	S	ψ	γ	M	X_1			X_F		

- p_f — freeze pressure (atm)
- Htg — total enthalpy of the gas (cal/gm)
- P — pressure (atm)
- T — temperature (^oK)
- S — entropy (cal/gm-^oK)
- ψ — molecular weight (gm/gm-mole)

- γ isentropic exponent
- M_c chamber Mach number = 0
- M^* throat Mach number = 1
- M Mach number for this table entry
- CPM contains the following information

	1	2	3
1	Pr	μ	C_p
2			
3			
⋮			
IVT			

- Pr Prandtl number
- μ viscosity (poise)
- C_p specific heat at constant pressure (cal/gm-^oK)

GROUP III – Gas Partical Data

Number of Records = ISPECS+1

Write ( ) IDUM, ((PSP(I, J), I=1, 2), J=1, ISPECS)

- IDUM dummy word
- PSP(1, J) mass density of jth particle (slug/ft^3 or kg_m/m^3)
- PSP(2, J) radius (ft or m)

DO I=1, ISPECS

Write ( ) NTAB1, TMELT, HSOL, HLIQ, (HFIT(N, 1, I), HFIT(N, 2, I), N=1, NTAB)

- NTAB1 number of table entries for this species
- TMELT melt temperature (^oR or ^oK)
- HSOL enthalpy before phase change (ft^2/sec^2-^oR or m^2/sec^2-^oK)
- HLIQ enthalpy after phase change (ft^2/sec^2-^oR or m^2/sec^2-^oK)
- HFIT(N, 1, I) temperature (^oR or ^oK)
- HFIT(N, 2, I) enthalpy (ft^2/sec^2 or m^2/sec^2)
- NTAB number of table entries for this species

Note that if NTAB=1 species is ideal and HFIT(1, 1, I)=C_{PL} (specific heat of liquid) and HFIT(1, 2, I)=C_{PS} (specific heat of the solid).

GROUP IV — Flowfield Data

Number of Records = 1 + 2 * ILAST

Write ( ) (ILAST, I=1, 7), THRUST, AEXIT, IEXIT

- ILAST — number of data points on the following normal surface. If ILAST = 0 there is no information to follow
- THRUST — thrust (lb_f or Newtons)
- AEXIT — exit plane area (ft^2 or m^2)
- IEXIT — exit flag $\begin{cases} 0 \text{ if no exit} \\ 1 \text{ if exit} \end{cases}$

Write ( ) ((ITYPE, R, X, M, θ, S, μ, δ, Htg), I=1, ILAST), (V, I=1, ILAST), ($\dot{W}_g$, I=1, ILAST), ((ρ, P, T, γ, $\hat{R}$), I=1, ILAST)

- ITYPE — identifies type of point (wall, shock, interior, etc.)

0	input point
1	interior point
2	wall point
3	free boundary
4	upstream shock point
5	Prandtl-Meyer point
6	downstream shock point
7	slip line
8	shock intersection point
9	vibrational mode frozen
10	rotational mode frozen
11	translational mode frozen

- R — radial coordinate (ft or m)
- X — axial coordinate (ft or m)
- M — Mach number
- θ — flow angle (rad)
- S — entropy (ft^2/sec^2-^oR or m^2/sec^2-^oK)
- μ — Mach angle (rad)
- δ — shock angle (rad)
- Htg — gas total enthalpy (ft^2/sec^2 or m^2/sec^2)

- V — velocity (ft/sec or m/sec)
- $\dot{W}_g$ — mass flow between this streamline and axis (slug/sec or kg_m/sec)
- ρ — gas density (slug/ft^3 or kg_m/m^3)
- P — pressure (lb_f-ft^2 or N/m^2)
- T — temperature (^oR or ^oK)
- γ — isentropic exponent
- R — universal gas constant divided by molecular weight (ft^2/sec^2-^oR or m^2/sec^2-^oK)

DO I = 1, ILAST

Write ( ) ISP, ((U, V, T, H, ρ), J=1, ISP), ILIMIT

- ISP — number of particle sizes at this point
- U — axial velocity component (ft/sec or m/sec)
- V — radial velocity component (ft/sec or m/sec)
- T — temperature (^oR or ^oK)
- H — enthalpy (ft^2/sec^2 or m^2/sec^2)
- ρ — particle density (slug/ft^3 or kg_m/m^3)
- ILIMIT — 0 not a limiting streamline; 1 is a limiting streamline

NOTE: The flowfield data are repetitively stored on tape as indicated above — normal surface after normal surface. When ILAST = 0 the end of the data has been reached.

3.4 PROGRAM UTILIZATION COMMENTS

The primary purpose of this section is to provide the prospective user of Lockheed's RAMP program backup information for inputting and trouble-shooting the code. This section also presents the authors' experience on what to look for and what to do if certain problems are encountered while using the program. Included in the discussion are:

1. A description of each mesh control parameter and some suggested values
2. An explanation of "error" messages and other diagnostics, and
3. Problems commonly encountered and suggestions to correct them.

It is envisioned that this section will aid the user in becoming familiar with the use of the code. However, only experience in utilizing the code will provide knowledge for applying the code.

3.4.1 Mesh Control Variables

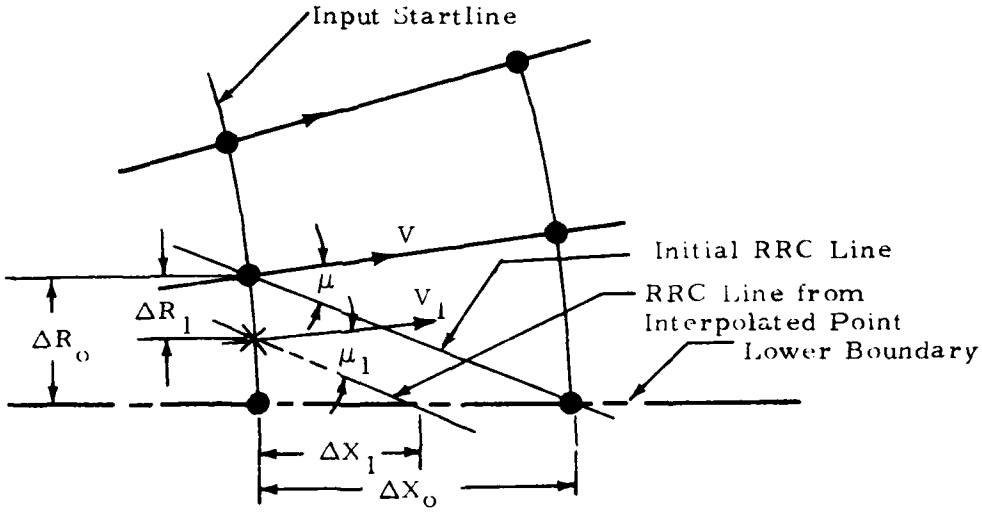
This subsection discusses each of the mesh control parameters which the program utilizes. The function of each of these parameters is discussed in relation to potential mesh control problems in construction of a typical flow solution.

Control of the insertion of interior points and the deletion of points on a known data surface is the function of subroutine CHECK. CHECK is normally called from subroutine PHASE1 after a line has been completed unless a special circumstance is encountered where a point needs to be inserted or deleted due to streamline crossings. The axial step control is performed by PHASE1.

3.4.1.1 Lower Wall Interpolation Factor (STEP(8))

Characteristic theory governs the construction of the initial data point on a new surface. The maximum axial step at the lower boundary is determined by the intersection of the right-running characteristic (RRC) emanating

from the first interior point on the normal and the lower boundary. The RRC is inclined at the local characteristic angle ($\theta - \mu$) toward the lower boundary. The axial step downstream of the known data surface is determined by the intersection of the RRC line (which is located a factor of STEP(8) ($\leq$ 1.0) of the distance between the axis point and first interior point) with the lower boundary. Details of this construction are noted in the sketch below.



ΔX_1 = Initial Axial Step

ΔR_o = Initial Radial Point Spacing

ΔX_o = Maximum Initial Axial Step

μ = Local Characteristic Angle

V = Local Velocity

The ΔRRC Step ΔX_1 is given by:

$$\Delta R_1 = \Delta R_o[1 - STEP(8)]$$

$$\Delta X_1 \cong \Delta R_o * STEP(8) * \tan(\pi/2 - \mu_1)$$

Consequently, STEP(8) is the primary parameter which controls the mesh construction and also has a significant impact on program run time. The radial point spacing on the start or previous line also helps to determine the initial axial step. The closer the point spacing the smaller the axial step.

Step size also affects the conservation of mass flow, momentum and energy. Most cases will maintain good mass flow conservation. However, there can be cases where poor mass flow conservation is observed. In these instances, normally there is an error in some of the input data. If no error is detected it may be necessary to take smaller step sizes to maintain the particle mass flow conservation. Gaseous cases with larger gradients across the flow field may also require smaller steps and more mesh points in order to conserve mass flow.

3.4.1.2 Axis Point Insertion Criteria (STEP(6))

The axis point insertion control parameter, STEP(6), limits the maximum axial step between data surfaces. If the data surface location between axis points for any reason exceeds STEP(6), the interpolation factor for the lower wall solution (STEP(8)) will be multiplied by 0.8. This results in a smaller axial step. The new axis point will be recomputed until it is less than a distance of STEP(6) away from the known axis point.

Typical values for STEP(6) are: 0.1 throat radii for two-phase nozzle flow problems, 0.1 exit radii for two-phase plume flow problems and 0.2 throat/radius for gas only nozzle solution and 0.2 exit radius for gas only plume flows.

3.4.1.3 Interior Point Insertion Criteri (STEP(3))

The purpose of the point insertion capability is to provide control of the streamline spacing in a rapidly expanding flow. Insertion of a streamline is accomplished in the following manner. The distance along a normal line between two grid points is computed in subroutine CHECK. If this distance exceeds STEP(3) a new streamline will be inserted midway between the two existing points. The new streamline point will be retained as the solution progresses.

3.4.1.4 Particle Limiting Streamline Insertion Criteria (STEP(9))

This parameter provides for control of streamline spacing on a data surface based on the entropy difference between two streamlines. This option is only used for two-phase flow cases and then only between a particle limiting streamline and the adjoint gas streamline. STEP(9) is the maximum allowable percentage change in entropy near a particle limiting streamline. The procedure is to first calculate the entropy difference (ΔS) between the particle limiting streamline and the adjacent streamline, above or below the particle limiting streamline. If ΔS is greater than STEP(9) times the entropy level of the limiting streamline then a new streamline point will be inserted midway between the two points. The procedure is identical to the interior point insertion scheme once the program has determined that a point should be added.

This mesh control parameter is utilized to avoid large entropy gradients near limiting streamlines. There will naturally be an entropy gradient across a limiting streamline, from a region where particles are present to a gas-only region. However, use of the STEP(9) control can minimize the chance of encountering numerical difficulties near limiting streamlines in two-phase flow problems.

3.4.1.5 Prandtl-Meyer Integration, (STEP(1))

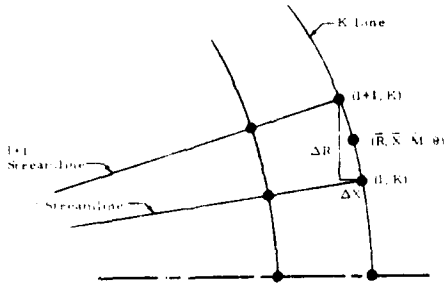
This parameter controls the number of mesh points which are distributed through the Prandtl-Meyer expansion. STEP(1) is the size of the integration step in degrees that is used to numerically integrate the Prandtl-Meyer function. STEP(1) then becomes the number of degrees between mesh points in the expansion fan.

3.4.1.6 Point Deletion Criteria (STEP(7))

The purpose of this mesh control parameter is to limit the spacing of adjacent streamline points on a normal to a minimum value. When streamlines begin to converge the solution can encounter numerical difficulty when computing locations of intersections of characteristic lines with normals to streamlines.

The procedure is to determine the radial and axial spacing, the Mach number difference and flow angle differences between two consecutive points on a normal ($\Delta R, \Delta X, \Delta M, \Delta\theta$). The average R, X, Mach number and flow angle for the two points are calculated ($\bar{R}, \bar{X}, \bar{M}, \bar{\theta}$). $\bar{R}$ and $\bar{X}$ are multiplied by STEP(7) and $\bar{M}$ and $\bar{\theta}$ are multiplied by built in values. If ΔR and ΔX are less than the average locations ($\bar{R}$ and $\bar{X}$) times STEP(7) and ΔM and $\Delta\theta$ are less than the average values ($\bar{M}$ and $\bar{\theta}$) times the built-in values then one of the two points will be deleted. This procedure is shown in the sketch on the following page.

The program will not delete the following types of points: upper or lower boundary, free boundary, Prandtl-Meyer, shock, slipline or limiting streamlines. Normally, the I point is deleted.



$\Delta M = (M(I,K) - M(I+1,K))$

$\Delta\theta = (\theta(I,K) - \theta(I+1,K))$

$\Delta R = (R(I,K) - R(I+1,K))$

$\Delta X = (X(I,K) - X(I+1,K))$

$\theta = (1/2)[\theta(I,K) + \theta(I+1,K)]$

$\bar{X} = (1/2)[X(I,K) + X(I+1,K)]$

$\bar{R} = (1/2)[R(I,K) + R(I+1,K)]$

$\bar{M} = (1/2)[M(I,K) + M(I+1,K)]$

$\bar{X} = \bar{X} * STEP(7)$

$\bar{R} = \bar{R} * STEP(7)$

$\bar{M} = \bar{M} * 2$

$\bar{\theta} = \bar{\theta} * 1$

IF $\Delta R < 1.1 * \bar{R}$ AND $\Delta X < 1.1 * \bar{X}$ AND $\Delta M < 1.7 * \bar{M}$ AND $\Delta\theta < 1.1 * \bar{\theta}$

Then the point I+1, K will be deleted

where M is the local Mach number and θ is the local flow angle

3.4.1.7 Finite Rate Chemistry Mesh Controls

The mesh control parameters for a finite rate chemistry case are the same as in the previous sections with the following exception.

The lower wall interpolation factor, STEP(8), is overriden by the "CFL" condition which requires that the Mach lines from any new point must intersect the base line between the base point and either of its neighboring points. This condition is assured by the equation

$$CFL = \Delta_N \sqrt{M^2 - 1}$$

where Δ_N is the normal distance between any 2 adjacent points on the base line and M is the Mach number. CFL is the maximum distance along the streamline through the base point the new point may extend and still ensure that the Mach lines intersect the adjacent points. This distance is calculated for each point on the base line and the minimum distance is used for the entire new line.

3.4.1.8 Recommended Mesh Control Variables

Table 3-8 presents a set of recommended values for the mesh control variables. This set of mesh control values has been found by the authors to be general for most of the cases which have been run. However, there probably will be cases where the run time or conservation of mass flow, energy and momentum will be unsatisfactory and adjustments to the mesh will be required. As the user becomes familiar with the code and runs more cases, changes in the mesh control variables and the resulting effect on the flow solution will become apparent.

3.4.1.9 Mesh Spacing Effect on Run Time and Conservation Equations

Run time is significantly affected by the point density for two reasons: (1) the computer run time is a direct function of the number of points on the

Table 3-8

RECOMMENDED MESH CONTROL VALUES

	Nozzle-Gas	Nozzle-Two-Phase	Plume – Low Altitude Two-Phase	Plume – Low Altitude Gas Only	Plume – High Altitude Two-Phase	Plume – High Altitude Gas Only
STEP(1), Prandtl-Meyer Control	4.0	4.0	4.0	4.0	6.0	6.0
STEP(3), Interior Insertion	0.1 R_T	0.1 R_T	0.1 R_E	0.2 R_E	0.3 R_E	0.5 R_E
STEP(6), Axis Insertion	0.2 R_T	0.1 R_T	0.1 R_E	0.2 R_E	0.2 R_E	0.3 R_E
STEP(7), Delete Criteria	0.001	0.001	0.005	0.005	0.005	0.005
STEP(8), Axis Point Interpolation	0.9	0.7	0.5	0.7	0.7	0.8
STEP(9), Limiting Streamline	1000.0	0.2	0.2	1000.0	0.2	1000.0

R_T = Throat Radius

R_E = Exit Radius

NOTE: If no limiting streamline, axis insertion, or interior insertion control is desired input a large number (~ 1000). If no deletion is desired use an extremely small number (1.E-5).

normals, i.e., for the same number of normal surfaces and twice the number of points on each normal there will be a factor of two difference in run time, (2) the more points on a given normal, the smaller will be the step size which will result in more execution time, i.e., twice as many points on a surface will result in the maximum axial step having one-half the length. This coupled with twice the points on the normal will result in four times as much computer time.

Coupled with conserving run time is the necessity that the solution be numerically valid, i.e., conserve mass, momentum and energy. The conservation functions for numerical solutions of the type employed by the RAMP program are somewhat controlled by the mesh spacing. For flows which contain large gradients in flow properties it is desirable to have more mesh points to avoid any large errors in mass flow, system energy and momentum. Thus there is some happy median between run time and system conservation.

3.4.1.10 Point Spacing

The type of solution which the RAMP code employs lends itself to uniformly spaced points on each data surface. However, particular flow solutions which have large radial gradients require close point spacing in the region of the large gradients. For these cases, smaller axial steps are necessary.

3.4.2 Explanation of Error Messages and Other Messages

1. Previously noted errors have propagated to lower boundary or problem limits have been reached. Case terminated.

   The program has terminated properly, the problem limits set by the user have been reached or another error which has been identified via a message has been encountered.

2. Lower boundary solution will not converge.

   The program is unable to obtain a solution at the lower boundary within the user specified number of iterations. The code will back up the line a maximum of 10 times in order to try to obtain a solution. If no solution is reached then the execution will terminate.

3. Interior solution will not converge.

The program is unable to obtain a solution for an interior point within the user specified number of iterations. The code will backup and take a smaller step. If the point still will not converge after backing up ten times then the solution will be terminated.

Possible causes of this problem are:

- Input error in boundary equations
- Numerical difficulties due to large point spacing in regions of steep gradients. Use more points or take smaller steps.
- If this occurs early in the solution, the startline may not be physically or numerically suited to the problem. Check the startline.
- Check for obvious errors in thermodynamic data.

4. Upper boundary solution will not converge

The program is unable to obtain a solution at the upper boundary. Causes and fixes are same as item 3.

5. Shock solution will not converge. Line terminated.

The code is unable to obtain a solution for a shock point within the user specified number of iterations. If this occurs early in solution it could be due to an inconsistency of the startline and boundary equations. May be taking too large a step — decrease step size.

6. ITSUB will not converge in RGMOFP

Real gas solution of Mach number as a function of pressure will not converge within preset number of iterations. Check the thermodynamic tables for errors and also the plume boundary conditions.

7. ITSUB will not converge in RGVOFM

Real gas solution of velocity as a function of Mach number will not converge within preset number of iterations. Check the thermodynamic tables for errors. For two-phase, real gas cases with a startline input from cards, be sure all the input Mach numbers fall within the thermodynamic table entries.

8. ITSUB WNC in THETPM

Unable to balance the last Prandtl-Meyer point pressure with the back pressure at the free boundary or flow angle

at a solid boundary, within the preset number of iterations. This can be caused by poor thermodynamic table construction or incompatible plume boundary conditions.

9. ITSUB WNC in AOASTR

Unable to balance the mass flow at input A/A^* with mass flow at throat within the preset number of iterations. Check thermodynamic tables.

10. ITSUB WNC in TURN

Unable to turn the flow through a specified turning angle within the preset number of iterations. Usually caused by flow going subsonic.

11. ITSUB WNC in OVEREX

Unable to turn the flow through a specified turning angle to match the plume boundary pressure within the preset number of iterations. Usually caused by the flow going subsonic.

12. The following case cannot be found on the master tape.

The program is unable to find the desired gas case among the cases present on the master tape. This is usually caused by the gas header card not matching any of the header cards which appear on the tape or the wrong tape was mounted.

13. ITSUB WNC in HYPER

Program is unable to find a velocity which will give the ambient boundary conditions within the number of preset iterations. Can be caused by trying to expand the flow too far or bad thermodynamic tables.

14. Subsonic Mach number encountered in TOFV

The characteristic theory utilizes Mach number in the definition of Mach angle ($\sqrt{M^2 - 1}$) and is limited to supersonic flow. Possible causes for this message are:

- Flow went subsonic
- Error in boundary equations
- Error in other input data
- A situation is encountered which the code is unable to handle.

15. Negative velocity encountered in TOFV

Something has happened during the solution which has resulted in a negative velocity being calculated. Probable causes are:

- Error in boundary equations
- Error in gas thermodynamic data
- Mesh problem caused by too large a step in a region of steep gradients. Try taking smaller steps.
- Program limitation.

16. ITSUB does not converge in PHYSOL

    Subroutine PHYSOL is unable to determine the characteristic intersection with the known data surface within the preset number of iterations. This is usually caused by too small a mesh size or a data surface that has been input, which is not a true normal.

17. Two straight lines in INRSCT are parallel

    Subroutine INRSCT's function is to determine the intersection of two straight lines. If two lines are found to be parallel this message is printed out. Usually caused by some inconsistency in the input data.

18. Slipline computation does not converge in SLPLIN

    The program is unable to converge on the slipline points (i.e., match flow angle and pressure) within the preset number of iterations. Usually caused by taking too large a step.

19. Characteristic lines diverge, last P-M point set free molecular

    Subroutine MOCSOL is unable to intersect right and left running lines while constructing the normal around a Prandtl-Meyer expansion. This is usually caused by trying to take too large a step past an expansion corner.

20. MOCSOL would not converge

    MOCSOL is unable to find the intersection of two characteristic lines within the preset number of iterations.

21. A problem with a RRC intersection with line X has been encountered. The line will be recalculated.

    This is the result of either an interior solution taking too many iterations or a situation where the program is unable to intersect the right running characteristic from the new point to the known data surface. The program will back up and take a smaller step for a maximum of ten iterations. If the same problem is still encountered the case will be terminated. This is usually caused by an error in a boundary equation, a startline which is not a normal, a poor point spacing.

22. Particle limiting streamline intersection with the boundary

This message occurs whenever a particle limiting streamline intersects a boundary (solid or free). The solution proceeds while assuming all mass which intersects the boundary passes on through.

23. Point number X on line Y has been deleted

This message is printed whenever a point is thrown out because it did not satisfy the mesh control criteria or whenever a gas and particle streamline cross.

24. A new streamline has been inserted on line Y between points X and Z.

This message will appear each time a point is added on a line due to mesh control criteria being exceeded between two points.

25. Due to gas-particle streamline crossing the point X has been replaced

This message occurs for two-phase cases whenever a gas and particle limiting streamline cross. The gas streamline is thrown out.

26. Your are trying to throw out point X, the point is a wall, limiting streamline or free boundary point. You probably have an error in your input.

This error message is usually due to an error in the startline or an error in the boundary equations. Check your input data.

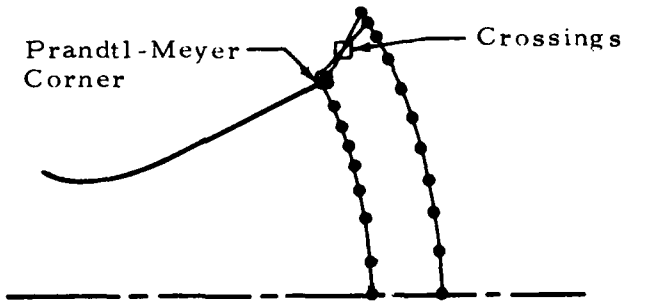
3.4.3 Problems Commonly Encountered and Suggested Fixes

This section is intended to aid the user in utilizing the program and avoiding some common problems. Also included are some general comments on inputting the code.

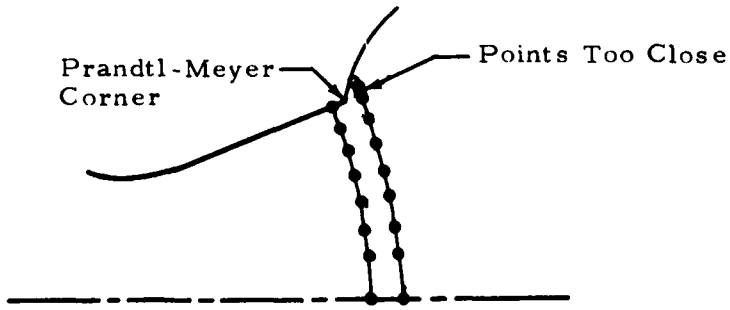
The following is a list of hints to the user:

- The numerical scheme which the program utilizes lends itself to evenly spaced points. Therefore, when setting up a startline try to insure that the points are as evenly spaced as possible. The only exception to this rule is in the vicinity of large gradients in flow properties, (e.g., Prandtl-Meyer corners). The points in this region should be closer together and smaller axial steps should be taken.

- In the region immediately downstream of a Prandtl-Meyer expansion it is necessary for the program to patch together a characteristic mesh with the streamline normal mesh (Section 6.9, Vol. I). This mesh construction can result in two unique problems. First, if the first normal beyond the corner is too far downstream of expansion, it is possible for the code to be unable to intersect characteristic lines. This normally will only occur for high altitude cases. To fix this take a small step. If too large a step is taken at lower altitudes, streamlines may cross which can result in a subsonic Mach number or negative velocity message. To correct, take smaller steps. On the other hand, if the first normal downstream of the corner is too close to the lip the points in the fan may be too close together. This may cause problems with characteristic line intersections with previous data surfaces and result in excessive iterations or no convergence of points in this region. It may also result in the necessity to take too small a step in order to proceed with the solution. To correct this problem, a slightly larger step must be taken so that the first normal is further downstream of the corner. Below are sketches of normals which are too close and too far from expansion corners.

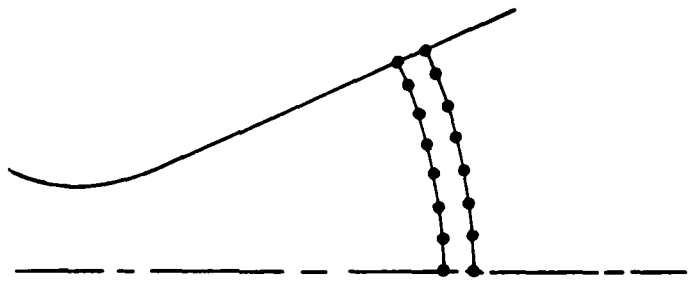


Normal Too Far Downstream of Expansion Corner



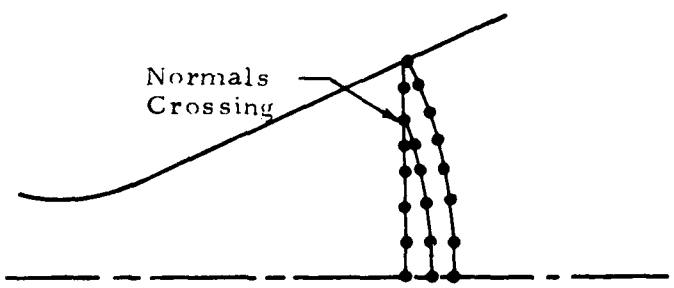
Normal Too Close to Expansion Corner

- The transonic solution requires the location of the intersection of the startline with the axis (ZAX) and the nozzle wall (THIW). There is an option in the code to let the program calculate a ZAX based on the input THIW. This is accomplished by not inputting a value on the transonic namelist. The value of ZAX which the code computes will result in a near normal startline. It should also be noted that the startline must be supersonic so if a subsonic Mach number is encountered from the transonic solution the startline must be moved further downstream (Card 36).
- Since the program uses streamlines and normals to streamlines to construct the mesh it is always assumed that each data surface is a true normal. If a startline is input which is not a normal, it is possible to encounter difficulties in getting the solution started. Below are three sketches of candidate initial data surfaces. Sketch A



Sketch A – True Normal

Sketch B – Normal Inclined Too Much



Sketch C – Normal Not Inclined Enough

is a true normal, Sketch B is inclined too much and Sketch C is not inclined enough. In the case of the data surface which is inclined too much the code will probably have trouble finding the characteristic line intersections with this surface during the next line's solution. When the code is unable to obtain an intersection, the new data surface is backed up until a solution is reached or if no solution is reached after backing up ten times the case is terminated. A normal which is not inclined enough will result in normal lines crossing as shown in Sketch C. The solution will usually have no trouble in obtaining a solution for the new data surface although several lines may overlap. To fix both of these cases, regenerate the startline so the normal line is a true normal.

- A large percentage of problems encountered are due to errors in the boundary equations. These errors can result in messages being printed out such as; subsonic Mach number, negative velocity or possible systems error messages due to bad interpolation factors. If any anomalies are encountered while the code is solving an upper boundary point, the following are some of the errors to look for:

    a. A discontinuity in boundary equations where they are supposed to match

    b. The boundary equations are not in the same units as the startline

    c. The startline does not fall on the first boundary equation

    d. For two-phase cases the input throat radius is not consistent with the throat equation

    e. There is an error in the equation itself.

- Care should be taken in selecting the particle size distribution for any particular case. If the particle sizes are too large for the motor being analyzed then the lags are too great, thereby compromising the results. If the sizes are too small then the particles may try to thermally and translationally equilibrate with the gas which may result in numerical problems. A discussion on how the authors determine mean sizes and distributions is contained in Appendix C of this volume.

- If the user is only interested in such things as nozzle wall pressure and initial plume expansion angle then a single particle size having the mean size for the motor is sufficient for good results. However, if the user is interested in two-phase impingement, then a good distribution is necessary in order to get satisfactory impingement results. Appendix C contains a discussion of particle distribution.

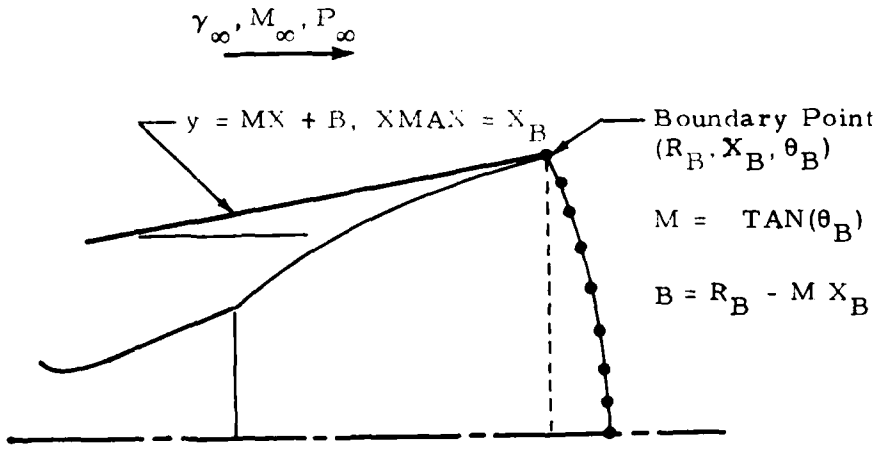
- There are some specific dos and don'ts associated with inputting a startline with cards. The following hints are what to be careful of when setting up a case where the startline is read from cards.

a. Make sure that the number of gaseous startline points corresponds to the value input on Card 4 (ICON(3)).

b. The gaseous startline points should be input starting from the nozzle centerline and proceeding to the upper boundary. The particle properties should be input starting with the first point nearest the upper boundary which has particles present and inputting the particle data down to the nozzle centerline. For each point the particles should be input from the smallest size (particle 1) up to the largest size (particle 6). The same particle number must always be used for each specific size.

c. A common mistake users make is to forget to input the number of gas points (NSETS, Card 23) which have particles present. This only applies to two-phase cases.

d. Whenever a restart is used it is necessary that the last point on the startline (upper boundary point) be a point on the first boundary equation. The first boundary equation must also be a type 1 or 2 boundary (conic or polynomial). Therefore, all boundary equations prior to the one which applies at the boundary startline point, must be removed and ICON(4) adjusted accordingly. Cases which are trying to be restarted in the plume require a fictitious boundary for the first equation. This equation consists of a straight line which passes through the boundary point and has the same slope. The next boundary equation should be the original free boundary equation. A sketch describing this requirement is shown below.



Fictitious Boundary for Plume Restart

e. The code presently has a limit of 50 startline points. If a line has been punched which has more than 50 points, omit enough points to obtain 50 maximum.

f. The Mach number which is input on the startline cards must be within the thermodynamic table entries for two-phase cases which utilize equilibrium tables with multiple enthalpy and entropy tables. This is normally a problem only for high altitude plume restarts. If this is ever encountered contact the authors for a temporary change to the program so that gas velocity may be read in instead of Mach number.

- If gas thermodynamic data is coming from tape be sure to set ICON(1) = 2 (Card 4) and also use exactly the same gas header card (Card 8) as was used by the TRAN72 program to generate the tape.

- For gas data coming from cards be sure that the units of the gas properties are consistent with the units identifier on the gas header card (Card 9).

- The entropy and total enthalpy levels of any startlines input into the program must be consistent with the gas thermodynamic tables. This is generally only important in two-phase cases. If the startline was punched by the program on a previous run and the same gas thermodynamic tables are used then the gas entropy and total enthalpy levels are consistent. However, if the startline is generated by some other code, care should be taken to enter the entropy and total enthalpy to obtain the correct static gas properties (P, ρ, T). For ideal gas two-phase cases the total enthalpy is calculated as follows:

$$H_T = C_p T_{OL}$$

where C_p is the ideal gas C_p defined as $C_p = \gamma R/(\gamma-1)$ and T_{OL} is the local total temperature including any two-phase losses. T_O and P_o are the combustion chamber total temperature and pressure. The static pressure is calculated via the following relationship:

$$P = \frac{P_o (T_{OL}/T_O)^{\gamma/\gamma-1}}{e^{S/R} \left(1 + \frac{(\gamma-1)}{2} M^2\right)^{\gamma/\gamma-1}}$$

The local static temperature is calculated using the local total temperature.

For equilibrium chemistry two-phase cases, the head loss due to the difference in total temperature between local and chamber conditions is accounted for by the change in entropy level between the total enthalpy tables. It is therefore necessary to use 2 entropy tables and more than one total enthalpy table for two-phase equilibrium cases. The user must also be sure that the gas total enthalpy at any point in the plume will never exceed that of the highest total enthalpy table ($\Delta H = 0$) or be less than the lowest total enthalpy table ($\Delta H_T = - \Delta H$ max). A ΔH_T of -300 cal/gm is probably the largest heat loss that need be used in the modified TRAN72 program for two-phase cases.

- For finite rate chemistry cases the following precautions should be taken

  1. Be sure that the order in which the chemical species names appear are the same for the thermodynamic data tables, the startline mole fractions and the catalytic species.
  2. Be sure that the temperatures in the data tables are the same for each species and that the number of temperatures are the same.
  3. Be sure that the enthalpies and entropies are referenced to the same temperature for each species.
  4. The program is set up to "freeze" the chemistry on the startline and will keep the chemistry frozen until a complete normal has been computed. It is recommended that the startline should be as near to a normal as possible.
  5. The run time for a finite rate chemistry case is much longer than for an equilibrium case.

3.5 BRIEF DESCRIPTION OF ROUTINES IN FUNCTIONAL GROUPINGS

The following subsection contains a brief description of the individual routines which comprise the RAMP program. The basic flow of the program is presented in Table 3-8. The routines are grouped and presented as indicated below:

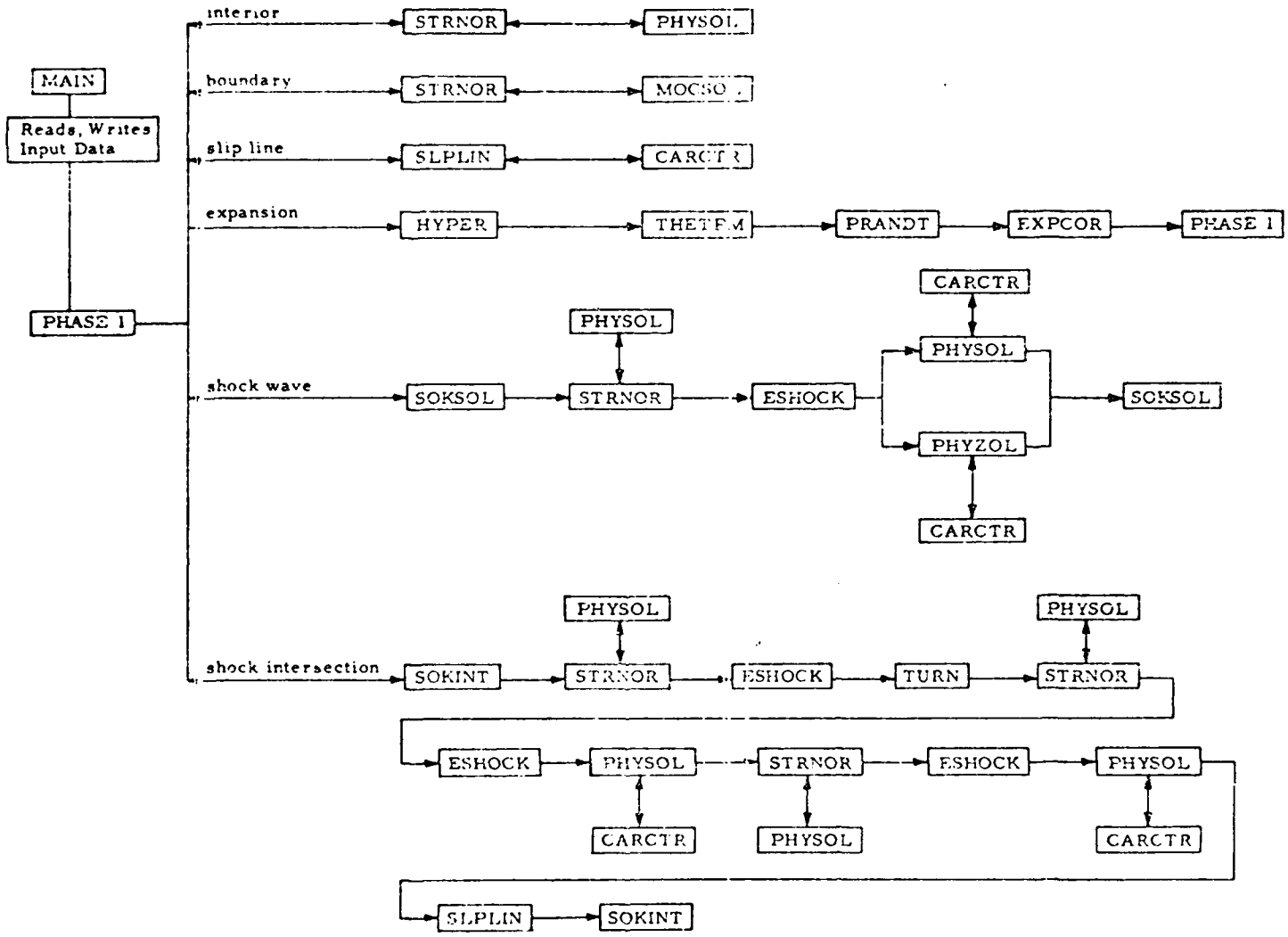
- General flow properties routines
- Shock calculation routines
- Input routines
- Logic control routines
- Free molecular routines
- Output routines
- Transonic routines
- Startline routines
- Boundary and problem limits routines
- Interpolation and iteration routines
- Property retrieval routines
- Chemistry routines
- Compatibility equation coefficient routines
- Corner point routines
- Initialization routines
- Performance calculation routines
- Characteristic routines
- Miscellaneous routines

3.5.1 General Flow Properties Routines

Routine	Description
EMOFP	This function computes the local Mach number as a function of local pressure (static) and local entropy.
EMOFV	This function computes the Mach number as a function of local velocity.
[illegible]	This subroutine interpolates for the gas and particle properties between two known data points.

Table 3-8

SCHEMATIC OF BASIC SOLUTION FOR VARIOUS TYPES OF POINTS



Routine	Description
POFEM	This function computes static pressure as a function of Mach number and entropy and total temperature (ideal gas two-phase only).
POFH	This routine utilizes the tabulated data of enthalpy and specific heat as functions of temperature for each species of a finite rate chemistry case to calculate pressure, as a function of enthalpy for a real gas, in a Prandtl-Meyer expansion.
PPATPT	This routine calculates and stores gas and particle dependent variables as a function of the independent flow properties.
RGMOFP	This subroutine finds Mach number as a function of pressure, O/F ratio (or total enthalpy) and entropy. The difference between this routine and EMOFP is that in this case the gas properties are not known prior to entry.
RGVOFM	This function computes velocity as a function of Mach number, entropy and O/F ratio (or total enthalpy). The difference between this routine and VOFEM is that the gas properties are not known prior to entry.
RHOFEM	This function computes the local density as a function of Mach number and entropy.
TOFEM	This function computes the local static temperature as a function of Mach number. TOFEM and TOFV are quite similar; the difference being if Mach number or velocity is the known quantity.
TOFENH	This function calculates the temperature as a function of enthalpy for a finite-rate chemistry case.
TOFH	This function calculates the temperature as a function of enthalpy for a finite-rate chemistry case during a Prandtl-Meyer expansion.
TOFV	This function computes the local static temperature as a function of velocity. TOFV and TOFEM are quite similar; the difference being if Mach number or velocity is the known variable.
UOFEM	This function computes the local Mach angle as a function of local Mach number. Prior to the calculation, a test is made to ensure that the Mach number is greater than one.
UOFV	This function computes the local Mach angle as a function of local velocity.
VOFEM	This function computes velocity as a function of Mach number.

3.5.2 Shock Calculation Routines

Routine	Description
DELTAF	This function computes the turning angle through an oblique shock wave knowing the shock angle and the upstream Mach number.
ENTROP	This function utilizes the oblique shock relations to find the entropy rise across a shock as a function of the shock angle and the upstream Mach number.
ESHOCK	This subroutine employs an iterative solution to perform the equilibrium shock calculations for a real or ideal gas. The real and ideal gas calculations are similar, the difference being that an ideal gas case converges on the first iteration.
NORSCK	This routine uses local flow properties to calculate properties downstream of a normal shock to obtain pitot pressure. This routine is used only for finite-rate chemistry, real gas cases.
SLPLIN	This subroutine handles the calculation of the points on the slipline. Two points are assigned to every slipline.
SOKINT	This subroutine computes the flow properties at the intersection of shock waves of the opposite family.
SOKSOL	This subroutine provides control for a shock point solution.
TURN	This subroutine solves for a shock wave which has a known turning angle (δ). A condition of known turning angle exists when the flow is turned through a compression corner on a solid boundary. Real gas effects are considered in calculating conditions downstream of the shock.
WEAK	This subroutine determines the independent variables, entropy and velocity, SD, VD, downstream of a weak oblique shock. The gas properties upstream of the shock are known prior to entry.

3.5.3 Input Routines

Routine	Description
GASRD	This subroutine reads in the gas properties. These properties may be real or ideal and read in via cards or tape. The routine also converts input gas properties from MKS units to English (ENG) units if necessary.

Routine	Description
GASTAP	This subroutine reads the real gas properties from the thermochemical data tape generated by the modified TRAN72 computer program and writes this same data on a flowfield tape for communication with other programs.
IMPUT	This routine reads the input cards or tape for the chemistry package. The reaction rate equations, rate constants, and startline species concentrations are read in and the appropriate conversions, if any, are performed. Tables of enthalpy, entropy and specific heats for each species are also input.
PARTIN	This subroutine reads in gas and particle property startline data. Data is read in from cards or tape.
PARTPH	This subroutine reads and sets up the data table of particle temperature versus enthalpy. This routine also prints out the particle drag tables as well as the temperature versus enthalpy tables.
PLUMIN	This subroutine reads in the input data (input via cards) necessary to perform the streamline-normal solution. This routine provides control for all input functions by selectively calling pertinent input routines and/or the transonic solution.

3.5.4 Logic Control Routines

Routine	Description
DRIVER	This subroutine provides the highest order control for program execution. The initialization and logic subroutines are called from here. Most of the common storage needed in the remainder of the program is specified in DRIVER.
MAIN	This subroutine drives the program.
MOCSOL	This subroutine solves the characteristic equations for gas only flow in the region around and downstream of an expansion corner.
PHASE1	This subroutine performs the overall control for the entire flowfield solution, selectively calling those calculations which are pertinent to the particular mesh construction as well as the highest level logic routine combining point or limited region solutions into an entire field solution.

Routine	Description
PLUMIN	This subroutine reads in the input data (input via cards) necessary to perform the streamline/normal solution. This routine provides control for all input functions by selectively calling pertinent input routines and/or the transonic solution.
STRNOR	This subroutine provides the regional control for the streamline/normal solution. It has a lower level of logical control than PHASE1 being interested only in determining the location and flow properties of a single new mesh point.
TRANS	This subroutine provides overall control for initializing the data and reading the namelist data for the Kliegel two-phase transonic solution of a supersonic gas particle startline.

3.5.5 Free Molecular Routines

Routine	Description
AVERAG	This subroutine determines the appropriate flow regime based on Knudsen number for non-continuum flow and sets the appropriate gas total conditions.
FREEMC	This subroutine computes flowfield properties in the free molecular regime.
STGMOD	This subroutine computes the gas thermodynamic properties in the transition flow regime.
WTFLOF	This function computes the area normal to the flow which is bounded by two streamline points.

3.5.6 Output Routines

Routine	Description
ERRORS	This subroutine contains print messages for various errors which may occur. This is an open ended routine in that it can easily be extended to handle more print messages.
IDTAPE	This subroutine writes the gas properties which were input via cards on the flowfield program tape. The format used to write them on tape is compatible with that used for a real gas.

Routine	Description
OUT	This subroutine writes the calculated data for data points along with the corresponding title and headings.
OUTBIN	This subroutine writes the calculated normal data on the binary output tape. This is done for any number of data points.
PAGE	This subroutine page ejects and writes the header comments and page number on each page of the printout.
PLMOUT	This subroutine prints the data read by PLUMIN.
RITE	This subroutine tells the program user (in no uncertain terms) that he has made a "fatal" error. The next executable statement is a STOP.

3.5.7 Transonic Routines

Routine	Description
ABCALC	
CCALC	
DCALC	
FCALC	
FIND11	
JAMES	
LEGS	
NEWT	A complete description of each of these routines is contained in Ref. 7.
ONED	
PARTIL	
PCALC	
PROP	
STRMLN	
TRACE	
TRANS	
WDGI	

3.5.8 Startline Routines

Routine	Description
AOASTR	This function finds the Mach number corresponding to a given area ratio by one-dimensional theory. Real gas effects are considered in this calculation.
LIPIN	This subroutine calculates information for the starting line points when the simplified straight start line option is used (i.e., when ICON(2)$\neq$2).

Routine	Description
MASCON	This subroutine calculates the Mach number distribution at an area downstream of the throat such that total mass flow is conserved. Mass flow, calculated at the throat, is used as the constant for comparison.
SETHTG	This subroutine computes the gas total enthalpy for a case when finite-rate chemistry is being used and the startline is to be generated by the program for gaseous flows only.
WOFA	This subroutine computes the weight flow per unit area as a function of Mach number. This calculation is only used in function AOASTR.

3.5.9 Boundary and Problem Limit Routines

Routine	Description
BOUND	This subroutine finds the radial coordinate and flow angle (radians) for a given axial coordinate on an upper or lower solid boundary.
FNEWTN	This function solves for the Newtonian impact pressure along the plume boundary. The calculation is applicable for all free stream velocities including quiescent conditions (i.e., $M_\infty = 0$).
ITERM	This function tests each normal lower wall point to determine if it is within the predefined problem limits. If the point falls outside the limits, the case is terminated.
LAGRNG	This subroutine determines the radial location and flow angle for solid boundaries which are input as tables of R, X and flow angle.
LIMITS	This subroutine tests the new boundary point to determine if it is within the limits of the current boundary equation.
PRFRBD	This subroutine calculates the flow properties at the intersection of a particle limiting streamline and a plume boundary.

3.5.10 Interpolation and Iteration Routines

Routine	Description
ALGINT	This routine does a log interpolation between two values of a variable.
DRAGCP	This routine determines the drag coefficient F $(C_D/C_{D_{Stokes}})$ as a function of Reynolds number.
DRAGMR	This subroutine determines the local drag coefficient $(C_D/C_{D_{Stokes}})$ as a function of particle Reynolds number and particle Mach number.
GAPPBI	This subroutine interpolates for the gas and particle properties between two known data points.
ITSUB	This subroutine controls the iterative solution of any set of equations which can ultimately be expressed as a function of one variable; it can also be used to control an integration loop.
SITER	This subroutine computes entropy as a function of pressure, total enthalpy and velocity.
TEMTAB	This subroutine will perform a table lookup for particle temperature as a function of enthalpy or for particle enthalpy as a function of temperature.
TKEY	This routine determines the proper index to be used in the enthalpy and specific heat tables and calculates interpolation factors.

3.5.11 Property Retrieval Routines

Routine	Description
IDMPFP	This function computes the particle storage location within the PFPARY array.
IDMTAB	This function computes the gas property storage location within the TABB array.
IDMXSI	This function computes the gas interpolation parameter storage location within the XSIDIM array.

Routine	Description
PFP	This function computes the particle property data storage location and retrieves data from the PFPARY array.
RWU	This routine is a MSFC Univac 1108 system routine used to read and write from FASTRAN files.
SPCTX	This routine controls the input and output from a FASTRAN file of the chemical species in a finite-rate chemistry case.
TAB	This function computes the thermodynamic data storage location and retrieves data from the TABB array.
XSI	This function computes the storage location for the nonlinear interpolation weighting functions required for thermodynamic property look-up and retrieves data from XSIDIM.

3.5.12 Chemistry Routines

Routine	Description
CHEM	This routine evaluates the chemical reaction-rate equations to determine the new chemical species concentrations.
FABLE	This subroutine utilizes real or ideal gas information obtained from a master tape or input cards to calculate properties locally in the flow. The maximum size of the array used by FABLE is limited to eight gas properties ($V, R, \gamma, T_o, P_o, \mu, Pr, C_p$) at 13 velocity "cuts" for each of two entropy cuts and 10 O/F or total enthalpy cuts.
THERMO	This subroutine utilizes real or ideal gas information obtained from the flowfield tape (or tables) and a local O/F ratio (or total enthalpy) to call subroutine FABLE to calculate thermodynamic gas properties locally in the flow.
THERM1	This routine determines the gas thermodynamic properties for a finite-rate chemistry case.

3.5.13 Compatibility Equation Coefficient Routines

Routine	Description
COEFEQ	This subroutine calculates the coefficients CI and C1J for use in the gas-particle system compatibility equation along the gas Mach lines. CI is the gas total enthalpy term and C1J is the particle contribution to the equation.
COEFF3	This subroutine calculates the new particle properties at the point under consideration, and the intersection of the particle streamlines through this point with the J-line.
NEWENT	This subroutine calculates the change in entropy and gas total enthalpy along a gas streamline for gas particle flows.
ROTERM	This function computes the geometrical factor, F_I, F_{II}, used in the axisymmetric term of the compatibility equation and as an interpolation parameter.

3.5.14 Corner Point Solution Routines

Routine	Description
EXPCOR	This subroutine calculates the flow properties of those field points near an expansion corner.
HYPER	This subroutine calculates the balanced pressure at a corner point (i.e., at the intersection of a solid boundary and the pressure boundary). The pressure balance is determined for either the overexpanded or underexpanded case with impact or ambient free-stream pressure.
OVEREX	This subroutine solves for the shock angle at the nozzle lip when the flow is over expanded. Provisions are made to calculate the shock angle for an upper or lower lip point. Real gas effects are considered in calculating flow properties downstream of the shock.
PRANDT	This subroutine computes the Prandtl-Meyer expansion angle for a given boundary angle and divides this angle into a series of expansion "rays" (unless the number of rays has been specified in the input). The flow properties at each angular increment are set and stored in the PHO array.

Routine	Description
THETPM	This subroutine performs a numerical integration to calculate properties through a Prandtl-Meyer expansion. Either the case of known final velocity or known final expansion angle may be handled.

3.5.15 Initialization Routines

Routine	Description
BLKDAT	This routine initializes the Kliegel (Ref.7) and Crowe (Ref. 11) gas-particle drag coefficients which are used by the code.
INITP	This subroutine initializes the values of various control parameters, thereby providing for proper operation of the program. These initial values include: 1. The counter for the upper and lower boundary equations, 2. The counter for the first characteristic line. 3. The initial number of degrees per Prandtl-Meyer ray, 4. Convergence criteria, and 5. Maximum number of iterations.
SETHTG	This subroutine computes the gas total enthalpy for a case when finite-rate chemistry is being used and the startline is to be generated by the program for gaseous flows only.

3.5.16 Performance Calculation Routines

Routine	Description
INTEGR	This subroutine calculates the incremental force and energy between two adjacent points in the flow field.
MASSCK	This subroutine keeps a running check on the mass flow. Mass flow at the starting line is calculated and compared with that crossing each normal line downstream.

Routine	Description
THRUST	This subroutine computes the vacuum thrust produced by a two-dimensional or axisymmetric nozzle. Addition of the thrust at the throat and the integrated pressure along the nozzle wall yields the final thrust.

3.5.17 Characteristic Routines

Routine	Description
BOUNDA	This subroutine finds the radial and axial coordinates as well as flow angle at the intersection of a straight line with a solid boundary.
CARCTR	This subroutine calculates velocity along either a I or II characteristic line with a known or assumed flow angle.
MOCSOL	This subroutine solves the characteristic equations for gas only flow in the region around and downstream of an expansion corner.
PHYSOL	This subroutine computes the intersection of physical characteristics with a "normal" data line.

3.5.18 Miscellaneous Routines

Routine	Description
CHECK	This subroutine determines whether or not to add or delete streamline points based on user input mesh controls.
DOTPRD	This function calculates the dot product of two vectors and returns the result to the calling routine.
INRSCT	This subroutine finds the intersection of two straight lines.
KIKOFF	This subroutine terminates the use if an error in the calculation is encountered.
MAXTIM	This subroutine is a Univac 1108 machine language routine that checks a user input time (seconds) against the remaining CPU time before run termination and returns to a specified label in the calling routine.

Routine	Description
SLDP	This subroutine finds the solutions to a set of N simultaneous linear equations.
VEMAG	This function determines the magnitude of a vector.

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3.6 DETAILED DISCUSSION OF THE INDIVIDUAL ROUTINES

This subsection contains a detailed description of each routine used in the program.

Described are:

- Function (if applicable) of each routine
- Calling sequence
- Common blocks and other routines used, and
- The method used in performing the routine functions

For your convenience, the routines are organized alphabetically.

NOTE: The following routines are not included in this section as they comprise the two-phase transonic solution of Kliegel which is incorporated in the RAMP code. A complete description of each of these routines is contained in Ref. 7.

ABCALC	JAMES	PARTIL
CCALC	LEGS	PCALC
FCALC	NEWT	PROP
FIND11	ONED	TRACE
		WDGI

FUNCTION NAME: ALGINT

DESCRIPTION

This routine does a log interpolation between two values of a variable.

CALLING SEQUENCE

= ALGINT (H, R1, R2)

where H is the interpolation factor and R1 and R2 are the values of the variables between which the interpolation is being made.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON - None

UTILITY - None

METHOD OF SOLUTION

$$A = \ln(R1) + H * (\ln(R2) - \ln R1)$$

$$ALGINT = e^{A}$$

FUNCTION NAME: AOASTR

DESCRIPTION

This function finds the Mach number corresponding to a given area ratio by one-dimensional theory. Real gas effects are considered in this calculation.

CALLING SEQUENCE

EM = AOASTR (OF, S, AOA, K1W1, K2W2)

where EM is the Mach number which exists, one-dimensionally, at an area ratio of AOA, an entropy S, and at an O/F ratio or total enthalpy, OF.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON-None
ERRORS
ITSUB
RGVOFM
THERMO
WOFA

METHOD OF SOLUTION

The weight flow per unit area at Mach one is evaluated. An initial guess for the desired Mach number is made and ITSUB is initialized. An iterative solution of the equation FOFEM = AOA - WOFA1/WOFA(EM), driving FOFEM to zero, is performed with the aid of ITSUB.

SUBROUTINE NAME: AVERAG

DESCRIPTION

This subroutine determines the appropriate flow regime based on Knudsen number for non-continuum flow and sets the appropriate gas total conditions.

CALLING SEQUENCE

CALL AVERAG(IS, J, N, K, ITYPE)

where IS is the base point streamline number on the J data surface, N is the streamline point on the K line for which the flow regime is to be determined and ITYPE is a flag which is returned to the calling routine to indicate the flow regime.

ITYPE	Flow Regime
1	Continuum
2	Vibrationally frozen
3	Rotationally frozen
4	Translationally frozen

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/TOTAL/	TOFV
COMMON/GSV/	RHOFEM
COMMON/GAPPA/	STGMOD
COMMON/GASCON/	
COMMON/CONTRL/	
COMMON/FREE/	
COMMON/FSTAG/	
COMMON/DATAR/	
COMMON/MOL/	
COMMON/TEMPER/	
THERMO	
EMOFV	

METHOD OF SOLUTION

The average Knudsen number between the old streamline base point is calculated via the following equation:

$$Kn = .788539\,\bar{\gamma}\,(\bar{M}^2/\bar{R}_E)\,|\ln T_1 - \ln T_2|/dS$$

where the (–) properties are averaged between the old (1) and new (2) streamline points. The flow regime is determined by checking the calculated Knudsen number against the input Knudsen number criteria for vibrational, rotational or translational freezing. Once the flow regime has been determined the appropriate specific heat ratio (gamma) and total conditions are calculated.

SUBROUTINE NAME: BLKDAT

DESCRIPTION

This routine initializes the Kliegel (Ref. 7) and Crowe (Ref. 11) gas-particle drag coefficients which are used by the code.

CALLING SEQUENCE

None

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/DRAGCF/

COMMON/DRUG/

UTILITY – None

METHOD OF SOLUTION

Not applicable

SUBROUTINE NAME: BOUND

DESCRIPTION

This subroutine finds the radial coordinate and flow angle (radians) for a given axial coordinate on an upper or lower solid boundary.

CALLING SEQUENCE

CALL BOUND (R, X, THETA, ITYPE, K1W1, K1W2)

where R is the radial coordinate, X is the known axial coordinate, THETA is the wall angle and ITYPE indicates whether upper or lower boundary equations are to be used.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/DATAR/
COMMON/WAFT/
LAGRNG

METHOD OF SOLUTION

The common block region DATAR contains boundary equations or wall coordinates necessary to evaluate R and THETA. The two types of equations used are:

$$r = a\left[\sqrt{b + cx + dx^2} + e\right] \qquad \text{Conic Type 1}$$

$$r = ax^4 + bx^3 + cx^2 + dx + e \qquad \text{Polynomial Type 2}$$

When the upper or lower boundary is described by discrete points (R, X, THETA) subroutine LAGRNG is called to interpolate for the R and THETA of the point. The input fixed point variable ITYPE has a one or a two in the units position which selects the upper (2) or lower (1) coefficients or points and control information. IEQNOW contains the number of the equation to be used.

SUBROUTINE NAME: BOUNDA

DESCRIPTION

This subroutine finds the radial and axial coordinates as well as flow angle at the intersection of a straight line with a solid boundary.

CALLING SEQUENCE

CALL BOUNDA (PL, PM, RB, XB, AB, ITYPE, K1W1, K1W2)

where

PL(8) is the storage array for the known boundary point

PM(8) is the storage array for the known field point where the straight line passes through

RB and XB are the radial and axial coordinates of the point of intersection

AB is the angle of the solid boundary at the point of intersection

ITYPE denotes the type of combination being considered

ITYPE	Type of Straight Line	Boundary
51	normal	lower
52	normal	upper
61	II-characteristic	lower
62	I-characteristic	upper
121	right-running shock wave	lower
122	left-running shock wave	upper

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/

COMMON/DATAR/

COMMON/TEMPO1/

BOUND

ERRORS

INRSCT

KIKOFF

CONTRL

TEMPO1

METHOD OF SOLUTION

Intersection of the straight line from PM and the tangent from PL is found first with the aid of subroutine INRSCT. The radial coordinate and the flow angle on the boundary at this given axial coordinate of the intersection just found can be calculated from the solid boundary equation by using subroutine BOUND. Then, if the boundary is not a straight line, the newly found point on the boundary is used to repeat the same process until the exact intersection is found.

SUBROUTINE NAME: CARCTR

DESCRIPTION

This subroutine calculates velocity along either a I or II characteristic line with a known or assumed flow angle.

CALLING SEQUENCE

CALL CARCTR (LOORUP, P3I, K1W1, K1W2)

where

LOORUP = 1 for a I characteristic
= 2 for a II characteristic
P3I(8) is the storage array for the point under consideration

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTROL/
COMMON/CRITER/
COMMON/DATAR/
COMMON/GASCON/
COMMON/SLIPPT/
COMMON/PARTP2/
COMMON/GAPPA/
ROTERM
UOFV
PPATPT
THERMO
COEFEQ

METHOD OF SOLUTION

For the first pass of the solution the flow properties, except the flow angle, at the point under consideration are assumed to be identical to those of the upstream point on the same streamline. Equation (3.3) is then used to calculate the "updated" velocity. Other properties are calculated according to the new velocity. This routine is used in the iteration for a shock point solution.

SUBROUTINE NAME: CHECK

DESCRIPTION

This subroutine determines whether or not to add or delete streamline points based on user input mesh controls.

CALLING SEQUENCE

CALL CHECK (I, K, IS, J, IGO, ITOTK, ITOTJ)

where (I, K) and (IS, J) are the two points the program is checking the mesh control constraints against. IGO = -1 for checking deletion and greater than zero for inserting points. ITOTK and ITOTJ are the total number of points on the J and K normals.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/POINTC/	COMMON/CHEMXX/
COMMON/DATAR/	SPCTX
COMMON/GLOBAL/	PFP
COMMON/PARTP1/	IDMPFP
COMMON/PARTP2/	GAPPBI
COMMON/STEPC/	
COMMON/CONTRL/	
COMMON/GAPPA/	
COMMON/FSTAG/	
COMMON/DROP/	
COMMON/CHEMCN/	

METHOD OF SOLUTION

See Section 3.5.1 for a description of mesh control parameters.

SUBROUTINE NAME: CHEM

DESCRIPTION

This routine evaluates the chemical reaction-rate equations to determine the new chemical species concentrations.

CALLING SEQUENCE

CALL CHEM (DXX, RHO, U, T)

where DXX is the distance along the gas streamline from the base point to the new point

RHO = gas density
U = gas velocity
T = gas temperature

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CRITER/
COMMON/RUE/
COMMON/CONTRL/
COMMON/CHEMCN/
COMMON/GASDAT/
COMMON/CHEMXX/
COMMON/CHEMYY/
TKEY
RWU
SLDP

METHOD OF SOLUTION

The reaction rate equations for the various chemical reactions are solved simultaneously using an implicit finite differencing scheme.

SUBROUTINE NAME: COEFEQ

DESCRIPTION

This subroutine calculates the coefficients CI and C1J for use in the gas-particle system compatibility equation along the gas Mach lines. CI is the gas total enthalpy term and C1J is the particle contribution to the equation.

CALLING SEQUENCE

CALL COEFEQ (M, IPA, IPB, IPC)

where M is equal to 1 for limiting streamlines, IPA is the base point number for the RRC, IPB is the base point number of the LRC and IPC is the new point number.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/SLIPPT/
COMMON/DATAR/
COMMON/GAPPA/
COMMON/ONTSPT/
COMMON/AVPROP/
COMMON/CONTRL/
COMMON/CHEMXX/
COMMON/CHEMCN/
UTILITY – None

METHOD OF SOLUTION

The following finite difference relations are used to solve for the coefficients:

$$CI_{1,2} = \frac{\cos\bar{\alpha}_{1,2}}{\sin\bar{\alpha}_{1,2}\,\bar{q}^2_{1,2}}$$

and

$$CIJ_{1,2} = \left\{ \sum_{j=1}^{NP} \bar{\rho}^{j}_{1,2} \bar{A}^{j}_{1,2} \left[\pm (\bar{v}_{1,2} - \bar{v}^{j}_{1,2}) \cos\bar{\beta}_{1,2} \mp (\bar{u}_{1,2} - \bar{u}^{j}_{1,2}) \sin\bar{\beta}_{1,2} + \frac{\bar{B}^{j}_{1,2}}{\bar{q}_{1,2} \sin\bar{\alpha}_{1,2}} \right] \right\} \frac{\Delta x_{1,2}}{\bar{\rho}_{1,2} \bar{q}^{2}_{1,2} \cos\bar{\beta}_{1,2}}$$

For a detailed description of the calculation procedure, see Volume I, Section 3.3.

SUBROUTINE NAME: COEFF3

DESCRIPTION

This subroutine calculates the new particle properties at the point under consideration, and the intersection of the particle streamlines through this point with the J-line.

CALLING SEQUENCE

```
CALL COEFF3 (KP, M, VERT, IH, KH, I8, K8, I9, K9,
    I7, K7, ITYPE, IPA, IPB, IPC, P3, PG)
```

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/	COMMON/PSEC/
COMMON/DATAR/	COMMON/PSLD/
COMMON/TOTAL/	COMMON/XXSH/
COMMON/PARTP1/	COMMON/GASCON/
COMMON/GAPPA/	COMMON/CPMUK/
COMMON/ONTSPT/	COMMON/SLIPPT/
COMMON/POINTC/	IDMPFP
COMMON/PARSTU/	PFP
COMMON/CRITER/	INRSCT
	PPATPT
	GAPPBI

METHOD OF SOLUTION

For a detailed description of the calculation procedure, see Volume I, Section 6.1.

FUNCTION NAME: DELTAF

DESCRIPTION

This function computes the turning angle through an oblique shock wave knowing the shock angle and the upstream Mach number.

CALLING SEQUENCE

DELTA = DELTAF (EPS, EM, K1W1, K1W2)

where DELTA, the turning angle is found from the shock angle, EPS, and the upstream Mach number, EM. NOTE: The appropriate values of gas properties must be stored in common upon entry to this routine.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/

UTILITY – None

METHOD OF SOLUTION

The oblique shock relationships are used to determine the turning angle through an oblique shock wave.

$$\delta = \epsilon - \tan^{-1}\left\{\tan\epsilon\left(\frac{1}{M^2 \sin^2\epsilon} + \frac{\gamma - 1}{2}\right)\left(\frac{2}{\gamma + 1}\right)\right\}$$

FUNCTION NAME: DOTPRD

DESCRIPTION

This function calculates the dot product of two vectors and returns the result to the calling routine.

CALLING SEQUENCE

= DOTPRD(V1, V2)

where V1 and V2 are any two vectors.

UTILITY ROUTINES AND COMMON REFERENCES

None

METHOD OF SOLUTION

Vector V1 is dotted into vector V2, The resultant is a scalar returned as DOTPRD.

FUNCTION NAME: DRAGCP

DESCRIPTION

This routine determines the drag coefficient F ($C_D/C_{D_{Stokes}}$) as a function of Reynolds number.

CALLING SEQUENCE

= DRAGCP (RE)

where

RE is the particle Reynolds number.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/DRAGCF/

UTILITY – None

METHOD OF SOLUTION

$C_D/C_{D_{Stokes}}$ is tabulated as a function of particle Reynolds number and a linear interpolation is performed based on Reynolds number to obtain CD/CD_{Stokes}. This tabulation is that of Kliegel (Ref. 7).

FUNCTION NAME: DRAGMR

DESCRIPTION

This subroutine determines the local drag coefficient ($C_D/C_{D_{Stokes}}$) as a function of particle Reynolds number and particle Mach number.

CALLING SEQUENCE

= DRAGMR (EM, RE)

where

EM is the particle Mach number

RE is the particle Reynolds number.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/DRUG/

ALGINT

METHOD OF SOLUTION

$C_D/C_{D_{Stokes}}$ as presented by Crowe (Ref. 11) is tabulated as a function of particle Reynolds number and Mach number. A logarithmic interpolation is performed based on RE and EM to obtain the appropriate value of $C_D/C_{D_{Stokes}}$.

SUBROUTINE NAME: DRIVER

DESCRIPTION

DRIVER provides the highest order control for program execution. The initialization and logic subroutines are called from here. Most of the common storage needed in the remainder of the program is specified here.

CALLING SEQUENCE

CALL DRIVER (K, K1W1, K1W2)

where K is a control constant indicating whether or not errors exist in the execution of the program. (K = 1 for a detected error, K = 0 for no errors.) K1W1 and K1W2 are flags which have various uses in the code.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/AUX/	COMMON/TPEH/
COMMON/CONTRL/	COMMON/WAFT/
COMMON/CRITER/	COMMON/NSF/
COMMON/DRAGCF/	COMMON/XSICOM/
COMMON/CUTFO/	COMMON/GAPPA/
COMMON/DATAR/	COMMON/DISCOM/
COMMON/XXSH/	COMMON/GRINT/
COMMON/FREE/	COMMON/TFLAG/
COMMON/FORCE/	COMMON/TEMPER/
COMMON/GASCON/	COMMON/ONTSPT/
COMMON/HEAD/	COMMON/WRITPT/
COMMON/SIGNAL/	COMMON/PSLD/
COMMON/INPUT/	COMMON/CPMUK/
COMMON/MASSC/	COMMON/MOL/
COMMON/STEPC/	COMMON/FAB/
COMMON/TAPRIT/	COMMON/WT/
COMMON/PARTP1/	INITP
COMMON/PARTP2/	PLUMIN
COMMON/GASDAT/	PHASE 1

METHOD OF SOLUTION: Not applicable.

FUNCTION NAME: EMOFP

DESCRIPTION

This routine computes the local Mach number as a function of local pressure (static) and local entropy.

CALLING SEQUENCE

EM = EMOFP (P, S, K1W1, K1W2)

where EM is the resultant Mach number found from the pressure, P, and entropy, S. NOTE: The appropriate values of the gas properties must be stored in common upon entry to this routine.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/TEMPER/
COMMON/GASCON/
UTILITY – None

METHOD OF SOLUTION

Thermally perfect gas relationships are used to find the Mach number.

$$M = \sqrt{\left[\left(\frac{P_o e^{-S/R} (T_o/T_c)^{\gamma/\gamma-1}}{P}\right)^{\gamma-1/\gamma} - 1\right]\frac{2}{\gamma-1}}$$

FUNCTION NAME: EMOFV

DESCRIPTION

This routine finds Mach number as a function of local velocity.

CALLING SEQUENCE

EM = EMOFV (V, K1W1, K1W2)

where EM is the local Mach number found as a function of the local velocity, V. NOTE: The appropropriate values of the gas properties must be stored in common upon entry to this routine.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/

TOFV

METHOD OF SOLUTION

Thermally perfect gas relationships are used to find the Mach number.

$$M = \sqrt{\left(\frac{T_o}{T} - 1\right)\left(\frac{2}{\gamma - 1}\right)}$$

FUNCTION NAME: ENTROP

DESCRIPTION

This routine utilizes the oblique shock relations to find the entropy rise across a shock as a function of the shock angle and the upstream Mach number.

CALLING SEQUENCE

SD = ENTROP (EPS, EMU, K1W1, K1W2)

where SD is the entropy rise across the shock and is a function of the shock angle, EPS, and the upstream Mach number, EMU. NOTE: The appropriate values of the gas properties must be stored in common upon entry to this routine.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/

UTILITY – None

METHOD OF SOLUTION

The oblique shock relations are employed to find the entropy rise across the shock.

$$ds = \frac{R}{\gamma - 1}\left\{ \ln\left[\frac{(2\gamma M^2 \sin^2\epsilon - (\gamma - 1))}{\gamma + 1}\right] + \gamma \ln\left[\frac{\tan(\epsilon - \delta)}{\tan\epsilon}\right]\right\}$$

SUBROUTINE NAME: *ERRORS*

DESCRIPTION

ERRORS contains print messages for various errors which may occur. This is an open ended routine in that it can easily be extended to handle more print messages.

CALLING SEQUENCE

CALL ERRORS (I, K1W1, K1W2)

where I selects the message to be printed.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/

UTILITY – None

METHOD OF SOLUTION

Not applicable.

SUBROUTINE NAME: ESHOCK

DESCRIPTION

This subroutine employs an iterative solution to perform the equilibrium shock calculations for a real or ideal gas. The real and ideal gas calculations are similar, the difference being that an ideal gas case converges on the first iteration.

CALLING SEQUENCE

CALL ESHOCK (OF, S1, V1, EP, DELTA, S2, V2, K2W, K1W)

where the input properties are, OF, the upstream O/F ratio or total enthalpy, S1, V1, the upstream entropy and velocity and, EP, the shock angle. The subroutine returns with DELTA, the turning angle and S2, V2, the downstream entropy and velocity.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/
COMMON/GASCON/
EMOFV
THERMO
POFEM
DELTAF
ENTROP
RHOFEM
WEAK

METHOD OF SOLUTION

The continuity equation coupled with the equations for conservation of normal and tangential momentum are solved in an iterative manner utilizing thermochemical property data to satisfy the conservation of energy equation. This set of four equations is expressed in terms of the four unknown quantities:

ϵ = shock angle
δ = turning angle
S_2 = entropy downstream of shock
V_2 = velocity downstream of shock

SUBROUTINE NAME: EXPCOR

DESCRIPTION

EXPCOR calculates the flow properties of those field points near an expansion corner.

CALLING SEQUENCE

CALL EXPCOR (NPM, J, K, ITOTJ, ITOTK, IPNT, K2W, K1W)

where

NPM	=	number of Prandtl-Meyer expansion rays emanating from the expansion corner
J	=	known normal line upstream of the expansion corner
K	=	the normal line under consideration downstream of the expansion corner
ITOTJ	=	adjusted total number of points on the J-line, not including the Prandtl-Meyer expansion points NPM
ITOTK	=	number of points on K-line before the Prandtl-Meyer expansion points are added; returns to the calling routine with the total number of points on K-line including Prandtl-Meyer expansion points
IPNT		indicates if an upper (=2) or lower (=1) boundary is being considered.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CHEMXX/	COMMON/FSTAG/
COMMON/GLOBAL/	COMMON/GAPPA/
COMMON/CONTRL/	INRSCT
COMMON/DATAR/	MOCSOL
COMMON/INPUT/	OUT
COMMON/STEPC/	SPCTX
COMMON/AUX/	PPATPT

METHOD OF SOLUTION

Flow properties at the expansion corner points are known (from PRANDT). Calculation starts from one of the corner points which have zero turning angle and proceeds toward the point with an increasing turning angle. Subroutine MOCSOL is used to solve for the flow properties of the intersection of the characteristic lines from two known points. The properties of the intersection of the normal from the known point on the new line (K-line, normal to the streamlines), with the characteristic of the corresponding point at the corner, are then interpolated. This point is then used along with another point at the expansion corner to find another new point, and so forth. The last of the expansion corner points is used twice in the calculation to find two points on the new normal — one on the characteristic line, the other on the streamline.

A weak shock is then initialized at the point on this last characteristic line and a mesh point is inserted between this point and the point on the last expansion ray which is a streamline rather than a characteristic line.

For a detailed description of the calculation procedure, see Volume I, Section 6.9.

SUBROUTINE NAME: FABLE

DESCRIPTION

This subroutine utilizes real or ideal gas information obtained from a master tape or input cards to calculate properties locally in the flow. The maximum size of the array used by FABLE is limited to eight gas properties ($V, R, \gamma, T_o, P_o, \mu, Pr, C_p$) at 13 velocity "cuts" for each of two entropy cuts and 10 O/F or total enthalpy cuts.

CALLING SEQUENCE

CALL TABLE (SS, VV, IF)

where SS is the local entropy, IF is the O/F or enthalpy table of interest and VV is the local velocity at the point of interest.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/XSICOM/	COMMON/GASDAT/
COMMON/CONTRL/	COMMON/MOL/
COMMON/GASCON/	COMMON/FILIT/
COMMON/FAB/	TOFV
COMMON/GRINT/	POFEM
COMMON/TEMPER/	EMOFV
COMMON/CPMUK/	XSI
COMMON/PARTFP/	TAB

METHOD OF SOLUTION

The routine is entered with an O/F or enthalpy table, IF, the local entropy, SS, and velocity, VV. A test is then made to determine if the gas is real or ideal. If the test indicates an ideal gas, the local properties are set to those stored in the TABB common array. If the test indicates real gas, a double interpolation scheme is utilized to locate gas properties between tabulated values of velocity and entropy. In the case of an entry beyond the range of the tables, an ideal gas extrapolation from the last table value is made to determine the gas properties.

FUNCTION NAME: FNEWTN

DESCRIPTION

This function solves for the Newtonian impact pressure along the plume boundary. The calculation is applicable for all free stream velocities including quiescent conditions (i.e., $M_\infty = 0$).

CALLING SEQUENCE

$$P_{IM} = \text{FNEWTN (THETA3, X, ITYPE1, K1W1, K1W2)}$$

where P_{IM} is the hypersonic Newtonian impact pressure at the plume boundary, THETA3 is the local flow angle at the boundary, X is the axial coordinate of the boundary point, and ITYPE indicates if an upper (=2) or lower (=1) boundary is being considered.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/DATAR/

UTILITY – None

METHOD OF SOLUTION

The common block region WALLCO contains the necessary information to evaluate the freestream gas properties at the plume boundary point. The impact pressure is then calculated using the following equation

$$P = P_\infty (1 + eX) \left[1 + \gamma_\infty M_\infty^2 \sin^2(\theta_B - \theta_\infty)\right]$$

SUBROUTINE NAME: FREEMC

DESCRIPTION

This subroutine computes flowfield properties in the free molecular regime.

CALLING SEQUENCE

CALL FREEMC (I1, J1, K1, ITOT, IOO, IOUT, IMOD)

where I1 is the point number for the first free molecular point on a normal, J1 is the old data surface, K1 is the new data surface, ITOT is the total number of points on the line, IOO is the line number for which a complete line is to be printed, IOUT is the total number of lines to skip between complete printout and IMOD is the number of points to shift on the old data surface to locate each base point streamline.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/	COMMON/GLOBAL/
COMMON/DATAR/	BOUND
COMMON/PARTP1/	ITERM
COMMON/PARTP2/	INRSCT
COMMON/FREE/	WTFLOF
COMMON/GASCON/	IDMPFP
COMMON/FSTAG/	PFP
COMMON/CUTFO/	OUT
COMMON/STEPC/	OUTBIN
COMMON/CRITER/	

METHOD OF SOLUTION

Once it has been determined that a point is free molecular all successive calculations of the particular streamline point are made via FREEMC. The point properties are determined assuming that temperature, gas velocity, flow angle, gas constant and specific heat ratio (γ) are constant along a streamline. The gas density is determined from a source flow calculation (i.e., conservation of mass between streamlines).

$$\rho_2 = \frac{\rho_1 u_1 A_1}{u_2 A_2}$$

where subscript 1 is the old data surface properties and subscript 2 is the new data surface properties. The pressure at the new point is then determined from the equation of state.

SUBROUTINE NAME: GAPPBI

DESCRIPTION

This subroutine interpolates for the gas and particle properties between two known data points.

CALLING SEQUENCE

CALL GAPPBI (I8, JU, I9, KU, JB, M, ISKIPG, PG, FACTOR, M1)

where I8 is the base point number, JU is the base point line number, I9 is the second point number, KU is the second point line number, JP is the temporary location in the IPFP array to store the interpolated data, M is the number of particles present, ISKIPG is a flag used to determine what arrays to use to do the interpolation, PG is the array in which the interpolated point properties are stored, FACTOR is the interpolation factor, and M1 = 0 gas only, M1 = 1 particles present.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/TFLAG/	COMMON/DRAGCF/
COMMON/DATAR/	COMMON/PCTC/
COMMON/PARTP1/	COMMON/VISEX/
COMMON/PARTP2/	ALGINT
COMMON/GAPPA/	PFP
COMMON/GASCON/	THERMO
COMMON/POINTC/	UOFV
COMMON/CPMUK/	TOFV
COMMON/CONTRL/	EMOFV
COMMON/FSTAG/	POFEM
COMMON/TEMPER/	TEMTAB
COMMON/CRITER/	DRAGMR
COMMON/PSLD/	DRAGCP
COMMON/XXSH/	

METHOD OF SOLUTION

The routine performs a linear interpolation between the properties of two known points and stores the results in temporary arrays which are used in other parts of the program during the calculation. ISKIPG is a flag which tells GAPPBI which arrays to use for the interpolation and whether or not to interpolate on particle properties.

SUBROUTINE NAME: GASRD

DESCRIPTION

This subroutine reads in the gas properties. These properties may be real or ideal and read in via cards or tape. The routine also converts input gas properties from MKS units to English (ENG) units if necessary.

CALLING SEQUENCE

CALL GASRD (IPAR)

where IPAR is a 1 for two-phase flow and a zero for gas-only flow.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/XSICOM/
COMMON/CONTRL/
COMMON/INTCR/
COMMON/GASCON/
COMMON/GASDAT/
COMMON/MOL/
COMMON/FSTAG/
XSI
GASTAP
IDMXSI
IDTAPE
IDMTAB
TAB

METHOD OF SOLUTION

The gas name, ALPHA(I), type units, number of O/F tables and number of entropy cuts are read in from an input card. If the gas properties are on cards, this subroutine reads the cards. If the gas properties are on tape, control of the reading of properties is given to GASTAP. In either case, the properties are converted from MKS to English (ENG) units by this subroutine if necessary.

SUBROUTINE NAME: GASTAP

DESCRIPTION

GASTAP reads the real gas properties from the thermochemical data tape generated by the modified TRAN72 computer program and writes this same data on a flowfield tape for communication with other programs.

CALLING SEQUENCE

CALL GASTAP

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASDAT/	COMMON/XXSH/
COMMON/CONTRL/	COMMON/BPRESW/
COMMON/DATAR/	COMMON/TAPRIT/
COMMON/HEAD/	COMMON/SIGMB/
COMMON/PARTP2/	IDMTAB
COMMON/CHEMCN/	ERRORS
COMMON/PCTC/	IMPUT

METHOD OF SOLUTION

The gas name, ALPHA(I), specified on the input data is compared with available cases on the TRAN72 thermochemical data tape until a match is found. This particular case is then read, stored in core, arranged in a form such that automatic transmission of data to other programs is possible, and then written on the RAMP flowfield tape.

SUBROUTINE NAME: HYPER

DESCRIPTION

This subroutine calculates the balanced pressure at a corner point (i.e., at the intersection of a solid boundary and the pressure boundary). The pressure balance is determined for either the overexpanded or underexpanded case with impact or ambient freestream pressure.

CALLING SEQUENCE

CALL HYPER (PB, I, K, ITYPE1, K1W1, K1W2)

where PB is the boundary pressure, I, K locates the boundary point, and ITYPE1 indicates if an upper (=2) or lower (=1) boundary is being considered.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/	FNEWTN
COMMON/DATAR/	OVEREX
COMMON/PCTC/	ITSUB
COMMON/FSTAG/	THETPM
THERMO	TOFH
POFEM	ERRORS
EMOFV	

METHOD OF SOLUTION

The boundary pressure (may be impact or ambient) is compared to the static pressure at the corner point. Depending on whether the comparison indicates the flow is overexpanded or underexpanded, a branch is made to OVEREX or THETPM. In either of these routines an iterative process balances the boundary pressure with the flowfield pressure at the boundary.

FUNCTION NAME: IDMPFP

DESCRIPTION

This function computes the particle storage location within the PFPARY array.

CALLING SEQUENCE

= IDMPFP (I, J, K, L)

where I, J, K, L are indices used to determine the storage location.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/PARTP1/
COMMON/PARTP2/
COMMON/PARTP3/
RWU

METHOD OF SOLUTION

The particle storage location is computed using the following relation

IDMPFP = I + 5 * (J-1 + 10 * (K-1 + 100 * (L-1)))

FUNCTION NAME: IDMTAB

DESCRIPTION

This function computes the gas property storage location within the TABB array.

CALLING SEQUENCE

= IDMTAB (I, J, K, L)

where I, J, K, L are indices used to determine the storage location.

UTILITY ROUTINES AND COMMON REFERENCES

None

METHOD OF SOLUTION

The gas property storage location, is computed using the following relation

IDMTAB = I + 10 * (J-1 + 2 * (K-1 + 13 * (L-1)))

FUNCTION NAME: IDMXSI

DESCRIPTION

This function computes the gas interpolation parameter storage location within the XSIDIM array.

CALLING SEQUENCE

= IDMXSI (I, J, K, L)

where I, J, K, L are indices used to determine the storage location.

UTILITY ROUTINES AND COMMON REFERENCES

None

METHOD OF SOLUTION

The gas interpolation parameter storage location is computed using the following relation

IDMXSI = I + 10 * (J-1 + 2 * (K-1 + 13 * (L-1)))

SUBROUTINE NAME: IDTAPE

DESCRIPTION

This subroutine writes the gas properties which were input via cards on the flowfield program tape. The format used to write them on tape is compatible with that used for a real gas.

CALLING SEQUENCE

CALL IDTAPE (UNITS, K1W1, K1W2)

where UNITS indicates whether the gas properties are being read in with English (ENG) or MKS units.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/XXSH/	COMMON/BPRESW/
COMMON/TAPRIT/	COMMON/PARTP2/
COMMON/CONTRL/	COMMON/GASDAT/
COMMON/HEAD/	TAB

METHOD OF SOLUTION

Gas property data are read in from cards. If not already in MKS units, the data are converted. These converted data are then written on the flowfield tape.

SUBROUTINE NAME: IMPUT

DESCRIPTION

This routine reads the input cards or tape for the chemistry package. The reaction rate equations, rate constants, and startline species concentrations are read in and the appropriate conversions, if any, are performed. Tables of enthalpy, entropy, and specific heats for each species are also input.

CALLING SEQUENCE

CALL IMPUT (IDATA)

where IDATA specifies the proper index of the array being input from a CEC data tape from which species concentrations are being extracted.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/
COMMON/CHEMCN/
COMMON/DATAR/
COMMON/GASDAT/
COMMON/CHEMXX/
COMMON/CPMUK/
COMMON/VISEX/
COMMON/PCTC/
COMMON/GASCON/
COMMON/VARSL/
SPCTX

METHOD OF SOLUTION

The routine reads species thermodynamic data and constructs a Gibbs free energy array to replace the entropy array. The reaction rate constant data, reactions, and third body data are input and stored. Finally the startline species concentrations are input via cards or tape and converted to mole/mass ratios.

SUBROUTINE NAME: INITP

DESCRIPTION

This subroutine initializes the values of various control parameters, thereby providing for proper operation of the program. These initial values include:

1. The counter for the upper and lower boundary equations,
2. The counter for the first characteristic line,
3. The initial number of degrees per Prandtl-Meyer ray,
4. Convergence criteria, and
5. Maximum number of iterations.

CALLING SEQUENCE

CALL INITP (K1W1, K1W2)

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/
COMMON/CRITER/
COMMON/DATAR/
COMMON/DISCOM/
COMMON/HEAD/
COMMON/STEPC/
UTILITY – None

METHOD OF SOLUTION

Not applicable.

SUBROUTINE NAME: INRSCT

DESCRIPTION

INRSCT finds the intersection of two straight lines.

CALLING SEQUENCE

CALL INRSCT (T1, T2, T3, T4, T5, T6, R3, X3, K1W1, K1W2)

where T1, T2, T3 and T4, T5, T6 define the equations of the two straight lines which intersect at R3, X3.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON – None

ERRORS

METHOD OF SOLUTION

The equations of the straight lines are written

$$r = \tan T3\,(x - T2) + T1$$

and

$$x = \cot T6\,(r - T4) + T5$$

These equations are solved for x, but a test on the slopes is made to prevent indeterminate forms. If an indeterminate form is possible, the points are mapped one onto another, thus precluding the possibility of indeterminancy except when the lines are parallel.

SUBROUTINE NAME: INTEGR

DESCRIPTION

This subroutine calculates the incremental force and energy between two adjacent points in the flow field.

CALLING SEQUENCE

```
CALL INTEGR (DELX, DELY, THTBR, R, DA, V,
RHO, P, X, I, K, FXP, FYP, TRP, FXG, FYG, TRG,
AXO2D, ENU, EG, EP, EM, DW)
```

where

DELX = difference in axial position between the two points

DELY = difference in radial position between the two points

THTBR = average flow angle of the two points

R = average radial position of the two points

DA = absolute distance between the two points

V = average gas velocity of the two points

RHO = average gas density of the two points

P = average gas pressure of the two points

X = average axial position of the two points

I = point number of the base point

K = line number of the base point

FXP = incremental force in axial direction due to the particle momentum

FYP = incremental force in radial direction due to the particle momentum

TRP = incremental torque due to particle momentum

FXG = incremental force in axial direction due to gas

FYG = incremental force in radial direction due to gas

TRG = incremental torque due to gas axial and radial forces

AXO2D = geometric term for axisymmetric or 2-D flow

ENU = angle the line connecting the two points has referenced to horizontal

EG = incremental gas energy

EP = incremental particle energy

EM = sum of incremental particle and gas energy (i.e., mixture)

DW = incremental gas mass flow between the two points.

UTILITY ROUTINES AND COMMON REFERENCE

COMMON/CONTRL/

COMMON/PARTP1/

COMMON/PARTP2/

COMMON/DATAR/

COMMON/FSTAG/

COMMON/INTCR/

PFP

VEMAG

METHOD OF SOLUTION

This subroutine calculates the mass flow, energy, momentum and thrust produced by the particles and gas contained in each streamtube bounded by two streamline points on a normal. The resulting values are integrated along each normal and compared to the initial data surface to determine how well the solution is conserving the conservation equations.

FUNCTION NAME: ITERM

DESCRIPTION

ITERM tests each normal lower wall point to determine if it is within the predefined problem limits. If the point falls outside the limits, the case is terminated.

CALLING SEQUENCE

FUNCTION = ITERM (IP, K, K1W1, K1W2)

where IP identifies the characteristic point on the new K line.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CUTFO/
COMMON/DATAR/
UTILITY – None

METHOD OF SOLUTION

The angular orientation of a line drawn from the upper or lower cutoff coordinates to the characteristic point is determined. Comparing this angle to the angle of the upper or lower cutoff line determines if the point is inside or outside the problem limits.

SUBROUTINE NAME: ITSUB

DESCRIPTION

This subroutine controls the iterative solution of any set of equations which can ultimately be expressed as a function of one variable; it can also be used to control an integration loop.

CALLING SEQUENCE

CALL ITSUB (FOFY, Y, SAVE, CONV, NTIMES, K1W1, K1W2)

where

FOFY is the function of Y which is driven to zero

Y is the variable which is iteratively solved for

SAVE is the program control array, i.e., SAVE(1) is a control counter, SAVE(2) is the Y increment

CONV is the convergence criteria for FOFY

NTIMES = maximum number of iterations to be performed

UTILITY ROUTINES AND COMMON REFERENCES

None

METHOD OF SOLUTION

ITSUB modifies Y in the proper direction by the increment value SAVE(2) until the root has been bracketed. The method of false position is then used to modify Y until the solution is reached. Immediately after entering ITSUB each time, the function is inspected for convergence. If the function has converged, a program control is set, and computer control is transferred to the calling routine.

SUBROUTINE NAME: KIKOFF

DESCRIPTION

This subroutine terminates the use if an error in the calculation is encountered.

CALLING SEQUENCE

CALL KIKOFF (K1W1, K2W2)

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/

UTILITY – None

METHOD OF SOLUTION

Not applicable.

SUBROUTINE NAME: LAGRNG

DESCRIPTION

This subroutine determines the radial location and flow angle for solid boundaries which are input as tables of R, X and flow angle.

CALLING SEQUENCE

CALL LAGRNG (IER, ID, ARG, R, THETA, ITYPE)

where

IER is an error flag, ID is a table location,

ARG is the axial value for which the radial coordinate, R, of the wall and flow angle, THETA, at the wall are desired,

ITYPE indicates if an upper (= 2) or lower (= 1) boundary is being considered.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/DATAR/

COMMON/CONTRL/

COMMON/WAFT/

UTILITY – None

METHOD OF SOLUTION

The routine uses the Lagrange interpolation formula to solve for R and flow angle as a function of axial position, X, from a set of tabular points describing a solid boundary. The routine uses the three closest points to the desired X to solve the interpolation formula. In the vicinity of large nonlinear variations in R and flow angle the points should be placed close together.

SUBROUTINE NAME: LIMITS

DESCRIPTION

This subroutine tests the new boundary point to determine if it is within the limits of the current boundary equation. Depending on the test, the options are:

1. use the current boundary equation,
2. advance to the next boundary equation, or
3. the current equation is the last one specified.

CALLING SEQUENCE

CALL LIMITS (I, K, ITYPE, IOK, K1W1, K1W2)

where I, K represents the location of the boundary point in the PHO array, ITYPE indicates if an upper or lower boundary is being considered, and IOK is a control indicating if option 1, 2 or 3 is to be used.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/
COMMON/DATAR/
BOUND

METHOD OF SOLUTION

The radius, RMAX, and boundary angle, THETAMAX, at the limiting axial value XMAX is calculated in BOUND. RMAX or XMAX is compared to R or X for the point in question. The results of the comparison determine which of options 1, 2 or 3 is to be used.

SUBROUTINE NAME: LIPIN

DESCRIPTION

LIPIN calculates information for the starting line points when the simplified straight start line option is used (i.e., when ICON(2)≠2).

CALLING SEQUENCE

CALL LIPIN (COOR, S, INTOT, DELM, K1W1, K1W2)

where COOR is the starting line information array, S is the entropy level of the start line, INTOT is the total number of input points specified (50 Max), DELM is Mach number gradient along the startline, and K1W1 is a flag which determines the type of startline point distribution.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/INPUT/
COMMON/CONTRL/
COMMON/PCTC/
COMMON/FSTAG/
COMMON/GASCON/
RGVOFM
UOFV
THERMO

METHOD OF SOLUTION

The startline input data are divided into the specified number of increments. Radial gradients in Mach number, X and θ, are calculated.

K1W1 = 0	The startline points are concentrated near the upper boundary
K1W1 = 1	The startline points are evenly spaced
K1W1 = 2	The startline points are evenly spaced on a source line

SUBROUTINE NAME: MASCON

DESCRIPTION

MASCON calculates the Mach number distribution at an area downstream of the throat such that total mass flow is conserved. Mass flow, calculated at the throat, is used as the constant for comparison.

CALLING SEQUENCE

CALL MASCON (E, SE, DELM, KIW1, KIW2)

where E is the input line array CORLIP, SE is the input line entropy level, and DELM is the Mach number gradient along the startline.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/
RGVOFM
ERRORS
EMOFV
ITSUB
RHOFEM

METHOD OF SOLUTION

The mass flow rate at the throat, $\dot{m}^*$, is calculated. This $\dot{m}^*$ is compared to that at the input line location for an initial Mach number distribution. The Mach number distribution is then perturbed until mass flow is conserved.

SUBROUTINE NAME: MASSCK

DESCRIPTION

This subroutine keeps a running check on the mass flow. Mass flow at the starting line is calculated and compared with that crossing each normal line downstream.

CALLING SEQUENCE

CALL MASSCK (ILAST, ISTART, K, K1W1, K1W2)

where ILAST is the last point on the normal line, ISTART is a number of the first point on the normal and K represents the normal line under consideration.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/DATAR/	COMMON/FORCE/
COMMON/MASSC/	COMMON/WT/
COMMON/INPUT/	COMMON/PARTP1/
COMMON/PSLD/	COMMON/PARTP2/
COMMON/CONTRL/	COMMON/INTCR/
COMMON/NSF/	COMMON/FSTAG/
COMMON/STEPC/	INTEGR
COMMON/SIGNAL/	PFP

METHOD OF SOLUTION

The mass flow through the startline is calculated and stored. Mass flow through lines downstream is calculated and these values compared with the initial value. A percent change in mass flow is printed for each normal line. The total mass flow passing under each point on a characteristic line is stored so the mass flow can be written on the output tape to permit streamline tracing.

SUBROUTINE NAME: MAXTIM

DESCRIPTION

This subroutine is a Univac 1108 machine language routine that checks a user input time (seconds) against the remaining CPU time before run termination and returns to a specified label in the calling routine.

CALLING SEQUENCE

CALL MAXTIM ($LABEL, TIME)

where

LABEL = the statement number in the calling routine where execution is sent if TIME is greater than the remaining CPU time for the run.

TIME = time in seconds before CPU maximum time when the run is to be terminated normally.

UTILITY ROUTINES AND COMMON BLOCKS

None

METHOD OF SOLUTION

TIME is checked against the remaining CPU time for the particular run. If the remaining CPU time is less than TIME then control of program execution is returned to statement LABEL in the calling routine.

SUBROUTINE NAME: MOCSOL

DESCRIPTION

This subroutine solves the characteristic equations for gas only flow in the region around and downstream of an expansion corner.

CALLING SEQUENCE

CALL MOCSOL (IN, KN, IN1, KN1, IN2, KN2, IFLAG, ITYPE, K1W1, K1W2

where IN, KN identifies the storage location for the new point to be computed, IN1, KN1 identifies the right running known point, and IN2, KN2 identifies the left running known point. IFLAG is an error indicator and ITYPE selects the type calculation.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/PARTP1/	COEFF3
COMMON/PARTP2/	INRSCT
COMMON/GAPPA/	POFEM
COMMON/ONTSPT/	COEFEQ
COMMON/AVPROP/	PPATPT
COMMON/SLIPPT/	PFP
COMMON/GLOBAL/	IDMPFP
COMMON/FSTAG/	BOUND
COMMON/FREE/	ROTERM
COMMON/STEPC/	VOFEM
COMMON/CPMUK/	RGMOFP
COMMON/PCTC/	FNEWTN
COMMON/CONTRL/	TOFH
COMMON/CRITER/	UOFV
COMMON/DATAR/	NEWENT
COMMON/GASCON/	ERRORS
	SPCTX

METHOD OF SOLUTION

The four characteristic equations are written as a function of five variables, R, X, θ, V and S. An additional relationship is obtained by assuming the entropy, S, varies linearly between known data points. Using these characteristic equations in finite difference form, the routine solves for a new mesh point, knowing two mesh points of an opposite family.

The solution is begun by setting the average values of properties over the step length equal to the known values at the base points. Subsequent passes in the iterative solution result in "updated" average values. The iterative solution is continued until the desired convergence on velocity or flow angle is reached or until the maximum number of iterations is exceeded.

MOSCOL is utilized by subroutine EXPCOR to solve the normal line immediately downstream of any expansion corner.

SUBROUTINE NAME: NEWENT

DESCRIPTION

This subroutine calculates the change in entropy and gas total enthalpy along a gas streamline for gas particle flows.

CALLING SEQUENCE

CALL NEWENT (NP, IT1, IT2, S3, H3, K, PB)

where

NP	=	number of particles present on streamline
IT1	=	1 for interior point
		2 for wall point
IT2	=	1 for interior or lower wall point
	=	2 for upper wall point
S3	=	entropy at new point
H3	=	total enthalpy at new point
K	=	5 gas only streamline
		7 gas and particles present on streamline
PB	=	array containing streamline base point properties (upstream)

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/	COMMON/CHEMXX/
COMMON/CHEMXY/	COMMON/CHEMCN/
COMMON/AVPROP/	COMMON/VISEX/
COMMON/GAPPA/	CHEM
COMMON/SLIPPT/	

METHOD OF SOLUTION

The compatibility relations for gas total enthalpy and entropy (Eqs. (3.2), and (3.1) of Table 3-1) are solved at the new streamline point knowing the gas and particle properties at the new and base streamline points. For gas only flows (and streamlines not crossing a shock) the gas total enthalpy and entropy are held constant along a given streamline.

SUBROUTINE NAME: NORSCK

DESCRIPTION

This routine uses local flow properties to calculate properties downstream of a normal shock to obtain pitot pressure. This routine is used only for finite rate chemistry, real gas cases.

CALLING SEQUENCE

CALL NORSCK (VI, PI, EMI, TI, GMI, RI, HI, POSTR)

where

VI, PI, . . . , HI are the local values of velocity, pressure, Mach number, temperature, gamma, gas constant and enthalpy

POSTR is the pitot pressure.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/

COMMON/PCTC/

TOFENH

ITSUB

METHOD OF SOLUTION

The downstream conditions are first estimated using ideal gas relations. The routine then performs an iteration as follows:

1. Calculate downstream static enthalpy from energy equation.
2. Iterate in subroutine TOFENH for temperature, gamma and gas constant.
3. Calculate downstream pressure from continuity and equation of state.
4. Check to see if resultant pressure satisfies the Rayleigh line equation. If not, increment the downstream velocity and repeat steps 1 through 4.
5. When the iteration is complete, the pitot pressure is determined from the downstream conditions.

SUBROUTINE NAME: OUT

DESCRIPTION

OUT writes the calculated data for data points along with the corresponding title and headings.

CALLING SEQUENCE

CALL OUT (I1, I2, K, K1W1, K1W2)

where I1, I2 refer to the point numbers of the points to be output (any number of points may be output at one time. K represents the current normal line (takes on the value 1 or 2).

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/	COMMON/CHEMCN/
COMMON/DATAR/	COMMON/CHEMXX/
COMMON/GASCON/	COMMON/GASDAT/
COMMON/HEAD/	POFEM
COMMON/PARTP1/	PAGE
COMMON/PARTP2/	PFP
COMMON/GAPPA/	THERMO
COMMON/WRITPT/	PPATPT
COMMON/TEMPER/	NORSCK
COMMON/FSTAG/	VEMAG
COMMON/CRITER/	SPCTX
COMMON/TOTAL/	ESHOCK

METHOD OF SOLUTION

Not applicable.

SUBROUTINE NAME: OUTBIN

DESCRIPTION

This subroutine writes the calculated normal data on the binary output tape. This is done for any number of data points.

CALLING SEQUENCE

CALL OUTBIN (I1, I2, JK, K1W1, K1W2)

where I1, I2 identifies the range of points to be written on tape (I1 is first point, I2 is last). JK represents the current characteristic line (1 or 2).

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/TAPRIT/
COMMON/DATAR/
COMMON/FORCE/
COMMON/GAPPA/
COMMON/PARTP1/
COMMON/PARTP2/
COMMON/CONTRL/
COMMON/GLOBAL/
COMMON/AUX/
MAXTIM
PFP
TEMTAB

METHOD OF SOLUTION

Not applicable.

SUBROUTINE NAME: OVEREX

DESCRIPTION

OVEREX solves for the shock angle at the nozzle lip when the flow is over expanded. Provisions are made to calculate the shock angle for an upper or lower lip point. Real gas effects are considered in calculating flow properties downstream of the shock.

CALLING SEQUENCE

CALL OVEREX (PB, I, K, ITYPE1, K1W1, K1W2)

where PB is the freestream pressure at the boundary; I, K defines the location of the lip point in the characteristic data (PHO) array and ITYPE1 indicates whether an upper (=2) or lower (=1) boundary is to be considered.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/DATAR/
COMMON/PARTP1/
COMMON/PARTP2/
EMOFV
ESHOCK
THERMO
POFEM
ITSUB
PFP
UOFV
IDMPFP
ERRORS

METHOD OF SOLUTION

For the first pass through the solution, an initial shock angle is assumed. This shock angle is perturbed in ITSUB and the result used to calculate flow properties including static pressure downstream of the shock. The calculated static pressure is compared with the boundary pressure to determine if the desired convergence has been obtained. If the solution has not converged ITSUB is called again and the above procedure is repeated.

SUBROUTINE NAME: PAGE

DESCRIPTION

This subroutine page ejects and writes the header comments and page number on each page of printout.

CALLING SEQUENCE

CALL PAGE (LCNT, K1W1, K1W2)

where LCNT is a counter which monitors the number of lines of printed output per page. LCNT is reinitialized in PAGE.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/HEAD/
COMMON/CONTRL/
UTILITY – None

METHOD OF SOLUTION

When the maximum number of lines per page (55) have been output, PAGE is called to page eject. It then prints the identifying information and the page number, increments the page number and reinitializes the line counter.

SUBROUTINE NAME: PARTIN

DESCRIPTION

This subroutine reads in gas and particle property startline data. Data is read in from cards or tape.

CALLING SEQUENCE

CALL PARTIN (NSETS, NTAPE)

where

NSETS is the number of startline points where particles are present

NTAPE is the FORTRAN unit to read the startline data from (=7 for cards)

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/PARTP1/	COMMON/PCTC/
COMMON/PARTP2/	COMMON/GASDAT/
COMMON/INPUT/	COMMON/VISEX/
COMMON/CONTRL/	COMMON/FSTAG/
COMMON/MASSC/	RGVOFM
COMMON/WT/	UOFEM
COMMON/PSLD/	TOFEM
COMMON/ONTSPT/	POFEM
COMMON/GASCON/	SPCTX
COMMON/TEMPER/	THERMO
COMMON/NSF/	IDMPFP
COMMON/LIPCOM/	PFP

METHOD OF SOLUTION

The gas startline points are read starting with the axis point and input up to the boundary, while the particle startline data is input starting with the last limiting streamline or last gas startline point and input down to the axis.

SUBROUTINE NAME: PARTPH

DESCRIPTION

This subroutine reads and sets up the data table of particle temperature versus enthalpy. This routine also prints out the particle drag tables as well as the temperature versus enthalpy tables.

CALLING SEQUENCE

CALL PARTPH (IPFTOC, LCT, NGS)

where

IPFTOC = zero for two phase case
= 10000 for gas only case
LCT = line counter for printout purposes
NGS is a dummy variable

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASTPE/
COMMON/CONTRL/
COMMON/TPEH/
COMMON/GASDAT/
COMMON/DRAGCF/
COMMON/PARTP2/
COMMON/DATAR/
COMMON/TFLAG/
PAGE

METHOD OF SOLUTION

Not applicable.

FUNCTION NAME: PFP

DESCRIPTION

This function computes the particle property data storage location and retrieves data from the PFPARY array.

CALLING SEQUENCE

= PFP(I, J, K, L)

where

I, J, K, L are indices used to determine the storage location.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/PARTP1/
COMMON/PARTP2/
COMMON/PARTP3/
RWU

METHOD OF SOLUTION

The particle property data storage location is computed using the following relation

IX = I + 5 * (J-1 + 10 * (K-1 + 100 * (L-1)))

and retrieved using the relation

PFP = PFPARY(IX).

SUBROUTINE NAME: PHASE1

DESCRIPTION

This subroutine provides the necessary controlling logic for the complete flowfield calculation. Proper subroutines are called to handle different kinds of calculation.

CALLING SEQUENCE

Call PHASE1 (IFINIS, K2W1, K2W2)

where IFINIS is set to zero.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/	OUTBIN
COMMON/DROP/	SPCTX
COMMON/GASCON/	PPATPT
COMMON/NSF/	LIMITS
COMMON/DATAR/	BOUND
COMMON/GAPPA/	BOUNDA
COMMON/INPUT/	PRANDT
COMMON/GLOBAL/	UOFV
COMMON/STEPC/	ITERM
COMMON/PARTP1/	TURN
COMMON/TEMPO1/	HYPER
COMMON/TEMPO2/	POFEM
COMMON/TOTAL/	EMOFV
COMMON/OVERLA/	RGMOFP
COMMON/CRITER/	VOFEM
COMMON/INTEU/	THETPM
COMMON/PSEC/	TOFEM
COMMON/TEMPO3/	SOKSOL
COMMON/FREE/	STRNOR
COMMON/XXSH/	ERRORS
COMMON/BPRESW/	MAXTIM
COMMON/PCTC/	MASSCK
COMMON/CHEMXX/	CHECK
COMMON/VISEX/	PFP
COMMON/EXPER/	IDMPFP
COMMON/GASDAT/	INRSCT
COMMON/FSTAG/	SOKINT
OUT	FREEMC
THRUST	THERMO
	PRFRBD
	EXPCOR

METHOD OF SOLUTION

This subroutine makes most of the tests to determine what kind of calculation should be carried out for the point under consideration. The point may be a regular field point, solid or free boundary point, left- or right-running shock points, incident shock points or reflected shock points on the solid boundary, attached shock points on the solid boundary, shock wave intersection points (opposite family), slipline points, incident shock points and expansion corner points at the free boundary, expansion corner points at solid boundary, etc.

SUBROUTINE NAME: PHYSOL

DESCRIPTION

This subroutine finds the reference properties on the characteristic line so that the compatibility equations can be used to calculate the flow velocity and angle of a point downstream of the known reference normal line (or surface).

CALLING SEQUENCE

CALL PHYSOL (PRET, IS, JS, IN, KN, IDIR, IFLAG, K1W1, K1W2, PIS, PIN, PM, PM1, IPM, IPM1, KPM, JAG, P, ARGN, ISLIP, KSLIP, IFIX, I141, IQUAD, H, SAVE, DP)

where

PRET(8)	is the storage array of reference properties found
(IS, JS)	is the point on the reference normal line (J-line), normally on the same streamline as the one under consideration
(IN, KN)	is a known point just below the point under consideration on the new normal line (K-line)
IDIR	indicates if a I-characteristic (=+1) or a II-characteristic (=-1) is being considered
IFLAG	is a control indicator to return the proper message to the calling subroutine in order that a proper measure can be taken
PIS(8)	array containing the flow properties of the streamline base point
PIN(8)	array containing the new flow properties of the streamline point
PM(8)	array containing the flow properties of point IPM which brackets the characteristic intersection
PM1(8)	array containing the flow properties of point IPM1 which brackets the characteristic intersection
IPM, IPM1	the point numbers of the two adjacent points on the old data surface which brackets the characteristic intersection

KPM	if the characteristic line intersects a boundary, shock or slipline KPM is the point number on the new data surface which bounds the intersection
JAG	the point immediately above or below the streamline base point. This point is used to detect the presence of a slipline.
P(8)	array in which the characteristic intersection flow properties are stored
ARGN	the angle of the normal
ISLIP	flag which indicates if not enough data is known to obtain the characteristic intersection
KSLIP	if KSLIP is a 1 the characteristic has intersected a slipline
IFIX	index used within PHYSOL which indicates if the two points which bracket the characteristic intersection have been found
I141	flag which indicates if the characteristic intersection is below the first point or above the last point on the old data surface
IQUAD	1 - interpolation is being made on R 2 - interpolation is being made on X
H	interpolation factor between point IPM and IPM1 necessary to obtain the characteristic intersection
SAVE(8)	array which is used to retain data from previous intersections
DP(8)	array which contains the flow property differences between points IPM and IPM1.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/POINTC/
COMMON/GASCON/
COMMON/TEMPER/
COMMON/FSTAG/
COMMON/CHEMXX/
COMMON/CONTRL/
COMMON/DATAR/
COMMON/SLIPPT/
COMMON/TEMPO2/
COMMON/PARTP1/
COMMON/PARTP2/
COMMON/GAPPA/
COMMON/DROP/
COMMON/CRITER/
BOUND
THERMO
INRSCT
ITSUB
PFP
UOFV
GAPPBI
PPATPT

METHOD OF SOLUTION

The characteristic line is drawn from the point under consideration to intersect the known upstream reference normal line. The reference properties of this intersection are interpolated from the two known points on the reference normal line. Subroutine ITSUB and the average quantities are used to obtain a better approximation of the reference properties.

If the reference properties are not readily available, IFLAG is set to 2, and the reference properties are then assumed to enable the calculation to be continued. Normally, the calculation of this point is repeated afterward to obtain the correct reference properties for the calculation of the new point under consideration.

SUBROUTINE NAME: PHYZOL

DESCRIPTION

This subroutine handles the downstream shock points and wall point near the corner of a reflected or an attached shock wave.

CALLING SEQUENCE

CALL PHYZOL (P5I, P6I, P4I, KANT, IS, JS, IN, KN, ANGLE, IFLAG, ITYPE, K1W1, K1W2)

where

P5I(8)	is the storage array of the shock downstream point near the corner where the shock reflected or attached
P6I(8)	is the storage array of the shock downstream point at the point where shock reflected or attached
P4I(8)	is the storage array of the intersection of the wall with the average normal drawn from point P5I
KANT	1. first time calculation 2. iterative calculation
(IS, JS)	denotes the storage location of point P6I
(IN, KN)	denotes the storage location of the shock upstream point opposite of point P5I
ANGLE	is the angle between the shock wave and the axial coordinate
IFLAG	is a control indicator for sending in and out the proper information in order that corresponding measures can be taken
ITYPE	indicates if a strong or weak shock is being considered and where the shock is reflected or attached strong shock 51 (lower wall) 52 (upper wall) weak shock 151 (lower wall) 152 (upper wall)

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/DATAR/	BOUNDA
COMMON/PHISOL/	CARCTR
COMMON/SLIPPT/	ERRORS
COMMON/TEMPO1/	INRSCT
COMMON/CONTRL/	THERMO
	UOFV

METHOD OF SOLUTION

The shock points at the wall (where the shock reflected or attached) are known. The shock upstream point slightly downstream of the shock attachment point is also calculated, though the results may not be the final ones. The oblique shock relations are used to calculate the downstream point P5I. Through this point an average normal line is drawn to intersect the wall (BOUNDA). The flow properties of this point P4I are initially assumed to be the same as those of point P6I. Point P4I is treated as a wall point. The velocity of point P5I is then recalculated with the shock downstream properties; this newly calculated velocity is then compared with the velocity calculated with the oblique shock relations. Shock strength is adjusted until the velocity of point P5I calculated by both methods converge to the same value. The final results of the shock points, as well as the wall point downstream of the attached or reflected shock, are then returned to the calling subroutine. See Volume I, Section 6.8 for the details of calculation.

SUBROUTINE NAME: PLMOUT

DESCRIPTION

PLMOUT prints the data read by PLUMIN.

CALLING SEQUENCE

CALL PLMOUT (KP, LCNT, K1W1, K1W2)

where KP is a control parameter set in PLUMIN, and LCNT is the printed line counter.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/	COMMON/WT/
COMMON/CUTFO/	COMMON/STEPC/
COMMON/GASDAT/	COMMON/WAFT/
COMMON/DATAR/	COMMON/FREE/
COMMON/GASCON/	COMMON/MOL/
COMMON/HEAD/	COMMON/TAPRIT/
COMMON/INPUT/	COMMON/FSTAG/
COMMON/GAPPA/	PAGE
COMMON/PARTP1/	TAB
COMMON/PARTP2/	IDMTAB
COMMON/MASSC/	EMOFV
COMMON/PARTTP/	THERMO
COMMON/PSLD/	PFP
COMMON/DRAGCF/	

METHOD OF SOLUTION

Not applicable.

SUBROUTINE NAME: PLUMIN

DESCRIPTION

PLUMIN reads in the input data (input via cards) necessary to perform the streamline-normal solution. This routine provides control for all input functions by selectively calling pertinent input routines and/or the transonic solution.

CALLING SEQUENCE

CALL PLUMIN (K1W1, K1W2, NTAPE, NSETS, RRT, XSHSV, ITRS)

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/	COMMON/LIPCOM/
COMMON/CUTFO/	COMMON/DRAGCF/
COMMON/DATAR/	COMMON/PSLD/
COMMON/GASCON/	COMMON/CRITER/
COMMON/HEAD/	COMMON/WAFT/
COMMON/INPUT/	COMMON/XXSH/
COMMON/STEPC/	COMMON/FREE/
COMMON/TFLAG/	COMMON/MOL/
COMMON/SIGMB/	COMMON/TAPRIT/
COMMON/VISEX/	COMMON/CHEMCN/
COMMON/VARSL/	GASRD
COMMON/PARTTP/	BOUND
COMMON/PARTP1/	LIPIN
COMMON/PARTP2/	AOASTR
COMMON/GAPPA/	MASCON
COMMON/WRITPT/	SETHTG
COMMON/MASSC/	PARTIN
COMMON/BPRESW/	PARTPH
COMMON/SIGNAL/	PLMOUT

METHOD OF SOLUTION

Not applicable.

FUNCTION NAME: POFEM

DESCRIPTION

This function computes the local static pressure as a function of Mach number, entropy and total temperature (ideal gas, two phase only).

CALLING SEQUENCE

P = POFEM (EM, S, K1W1, K1W2)

where P is the resultant static pressure found from the Mach number, EM, and entropy, S. NOTE: The appropriate values of the gas properties must be stored in common upon entry to this routine.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/
COMMON/TEMPER/
UTILITY – None

METHOD OF SOLUTION

Thermally perfect gas relationships are used to find the pressure.

$$p = p_o e^{-S/R} \left(1 + \frac{\gamma - 1}{2} M^2\right)^{-\gamma/\gamma - 1} \left(\frac{T_o}{T_c}\right)^{-\gamma/\gamma - 1}$$

SUBROUTINE NAME: POFH

DESCRIPTION

This routine utilizes the tabulated data of enthalpy and specific heat as functions of temperature for each species of a finite rate chemistry case to calculate pressure, as a function of enthalpy for a real gas, in a Prandtl-Meyer expansion.

CALLING SEQUENCE

CALL POFH (VF, HT, DELTA)

where

VF is the final velocity
HT is the total enthalpy
DELTA is the flow deflection angle.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/
COMMON/PCTC/
COMMON/EXPER/
COMMON/CPMUK/
ITSUB

METHOD OF SOLUTION

The routine solves for pressure by incrementally changing the flow angle until the final flow angle is obtained. At each increment the routine determines new gas properties from the tables on enthalpy and specific heat as functions of temperature, then uses these properties for the next increment. The result is an integration of the flow properties through the angular change, DELTA.

SUBROUTINE NAME: PPATPT

DESCRIPTION

This subroutine calculates and stores gas and particle dependent variables as a function of the independent flow properties.

CALLING SEQUENCE

CALL PPATPT (M, IC, KC, VG, THETA, SG, K2W1, K2W2, KP, ISKIP, PG)

where

M	is the number of particle sizes present at the point
IC	is the point number for which particle and gas flow properties are to be calculated
KC	is the line identification flag
VG	is the gas velocity at the point
THETA	is the gas flow angle at the point
SG	is the gas entropy at the point
K2W1	is a dummy variable
K2W2	is a dummy variable
KP	is the temporary array storage location for the particle and gas flow properties
ISKIP	= 0 calculate particle properties only
	= 20 calculate gas and particle properties
	= 40 calculate gas properties only
PG	array containing the point independent flow properties

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/TFLAG/	COMMON/VISEX/
COMMON/PARTP1/	COMMON/TEMPER/
COMMON/PARTP2/	COMMON/FSTAG/
COMMON/GAPPA/	COMMON/DATAR/
COMMON/ONTSPT/	COMMON/FREE/
COMMON/GASCON/	COMMON/CRITER/
COMMON/CONTRL/	COMMON/PSLD/
COMMON/CPMUK/	COMMON/XXSH/

COMMON/DRAGCF/	POFEM
COMMON/PCTC/	PFP
THERMO	TEMTAB
TOFV	DRAGMR
EMOFV	DRAGCP

METHOD OF SOLUTION

The routine is entered knowing the gas independent variables (V, S, OF or H_T) and particle independent variables (u, v, ρ, h). The gas dependent variables (T, P, ρ, μ, C_p, Pr) and particle dependent variables (R_E, drag and heat transfer terms) are calculated and stored for use in other parts of the code.

SUBROUTINE NAME: PRANDT

DESCRIPTION

This subroutine computes the Prandtl-Meyer expansion angle for a given boundary angle and divides this angle into a series of expansion "rays" (unless the number of rays has been specified in the input). The flow properties at each angular increment are set and stored in the PHO array.

CALLING SEQUENCE

CALL PRANDT (I, J, THETAB, NPM, IFLAG, ITYPE, K1W1, K1W2)

where

I represents the corner point

J indicates a characteristic line

THETAB is the boundary angle

NPM = number of Prandtl-Meyer increments (calculated in PRANDT)

IFLAG is an error flag

ITYPE indicates if upper (2) or lower (1) boundary is being considered

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CRITER/	THERMO
COMMON/DATAR/	THETPM
COMMON/GASCON/	UOFV
COMMON/STEPC/	EMOFV
COMMON/CONTRL/	TOFV
COMMON/PCTC/	POFEM
COMMON/CPMUK/	TOFH
COMMON/PARTP1/	SPCTX
COMMON/PARTP2/	PFP
COMMON/FSTAG/	IDMPFP
COMMON/CHEMXX/	

METHOD OF SOLUTION

The routine is entered with known flow properties at the point of discontinuity along with the known corner and boundary flow angles. From the known angles and the preset number of degrees per ray, the number of increments is calculated. The distribution of P-M rays is then adjusted by a weighting function. Subroutine THETPM is entered with known initial conditions and the number of degrees per ray and returns with a velocity. These new conditions are then set into the PHO array. See Volume I, Sections 5 and 6.9, for the details of calculation.

SUBROUTINE NAME: PRFRBD

DESCRIPTION

This subroutine calculates the flow properties at the intersection of a particle limiting streamline and a plume boundary.

CALLING SEQUENCE

CALL PRFRBD (IS, JS, IN, KN, I, K)

where

IS = point number of the old (J) data surface plume boundary
JS = line indicator of the old data surface
IN = point number of the old (J) data surface limiting streamline
KN = line indicator of the old data surface
I = point number of the new (K) data surface limiting streamline
K = line indicator of the new data surface.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/DATAR/	COMMON/CONTRL/
COMMON/PARTP1/	COMMON/FSTAG/
COMMON/PARTP2/	PFP
COMMON/GAPPA/	INRSCT
COMMON/SLIPPT/	IDMPFP
COMMON/ONTSPT/	PPATPT

METHOD OF SOLUTION

Once the new data surface has been completed and it has been determined that a particle limiting streamline has crossed the plume boundary, the location of the intersection is determined by the intersection of a line passing through the old and new limiting streamline points. This establishes two interpolation factors. One along the limiting streamline and one along the plume boundary. Gas properties at the intersection point are interpolated for between the two plume boundary points and particle properties are interpolated for between the two limiting streamline points. The interpolated point and properties are then used as the plume boundary point for the new line and the calculation for the next line is then initiated.

FUNCTION NAME: RGMOFP

DESCRIPTION

This subroutine finds Mach number as a function of pressure, O/F ratio (or total enthalpy) and entropy. The difference between this routine and EMOFP is that in this case the gas properties are not known prior to entry.

CALLING SEQUENCE

EM = RGMOFP (OF, S, P, K2W1, K1W1)

where EM is the resultant Mach number, P is the local static pressure, S is the local entropy, and OF is the local O/F ratio (or total enthalpy).

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/
COMMON/GASCON/
COMMON/ISEA/
COMMON/GASDAT/
POFEM
EMOFV
ITSUB
VOFEM
EMOFP
ERRORS
TAB
THERMO

METHOD OF SOLUTION

The real gas tables have, as independent variables, OF ratio (total enthalpy), entropy and velocity. If the velocity is not known, an iterative solution must be employed to find Mach number from pressure, entropy, and OF ratio (or total enthalpy).

FUNCTION NAME: RGVOFM

DESCRIPTION

This subroutine finds velocity as a function of Mach number, entropy and O/F ratio (or total enthalpy). The difference between this routine and VOFEM is that the gas properties are not known prior to entry.

CALLING SEQUENCE

V = RGVOFM (OF, S, EM, K2W, K1W)

where V is the resultant velocity computed from O/F ratio or total enthalpy, OF, entropy, S, and Mach number, EM.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/
COMMON/CHEMCN/
COMMON/GASDAT/
COMMON/GASCON/
THERMO
TAB
VOFEM
EMOFV
ITSUB
ERRORS

METHOD OF SOLUTION

The real gas tables have, as independent variables, OF ratio (or total enthalpy), entropy and velocity. If the velocity is not known, an iterative solution must be employed to find the velocity from Mach number, OF ratio (or total enthalpy) and entropy.

FUNCTION NAME: RHOFEM

DESCRIPTION

RHOFEM computes the local density as a function of Mach number and entropy.

CALLING SEQUENCE

RHO = RHOFEM (EM, S, K1W1, K1W2)

where RHO is the resultant density found from local Mach number and local entropy. NOTE: The appropriate values of the gas properties must be stored in common upon entry to this routine.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/

POFEM

METHOD OF SOLUTION

Thermally perfect gas relationships are used to find the density.

$$\rho = \rho_o \left(1 + \frac{\gamma - 1}{2} M^2\right)^{-(1/\gamma - 1)}$$

SUBROUTINE NAME: RITE

DESCRIPTION

This subroutine tells the program user (in no uncertain terms) that he has made a fatal error. The next executable statement is a STOP.

CALLING SEQUENCE

```
CALL RITE(I)
```

UTILITY ROUTINES AND COMMON REFERENCES

None

METHOD OF SOLUTION

Not applicable.

FUNCTION NAME: ROTERM

DESCRIPTION

ROTERM computes the geometrical factor, F_I, F_{II}, used in the axisymmetric term of the compatibility equation and as an interpolation parameter.

CALLING SEQUENCE

F = ROTERM (THETA, DELTA, EMU, R3, RI, K2W1, K2W2)

where

THETA is the flow angles of the known points ($\bar{\theta}_I$ or $\bar{\theta}_{II}$)
DELTA defines the quadrant being considered
EMU is the Mach angles of the known points ($\bar{\mu}_I$ or $\bar{\mu}_{II}$)
R3 is the coordinates of the new point ($\bar{r}_{III}$ or $\bar{x}_{III}$)
RI is the coordinates of the known point (r_I or x_I)

UTILITY ROUTINES AND COMMON REFERENCES

None

METHOD OF SOLUTION

The method-of-characteristics solution uses this routine to determine a coefficient needed in its solution. This term (see Eq. (6.29), Section 6 of Ref. 4) can be written as:

$$F = \frac{\left|\sin\mu\right| (d_{III} - d)}{\sin(\pi/4 + \delta(\bar{\theta} + \bar{\mu} - \pi/4))}$$

By the proper choice of d(r or x), δ and the sign of μ, indeterminant forms are eliminated in the evaluation.

SUBROUTINE NAME: RWU

DESCRIPTION

This routine is a MSFC Univac 1108 system routine used to read and write from FASTRAN files.

CALLING SEQUENCE

CALL RWU (KSUNIT, A(I, J), NS, KSEC, IFCN, ISTAT, NWT)

where

KSUNIT is the unit number of the FASTRAN file
A(I, J) is the array being read or written
NS is the number of entries in the array
KSEC is the location in the file of the required data
IFCN indicates to read data (=16) or write data (=8)
ISTAT is a status indicator
NWT is an output indicator

UTILITY ROUTINES

None

METHOD OF SOLUTION

Not applicable.

SUBROUTINE NAME: SETHTG

DESCRIPTION

This routine computes the gas total enthalpy for a case when finite rate chemistry is being used and the startline is to be generated by the program for gaseous flows only.

CALLING SEQUENCE

CALL SETHTG

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/VISEX/
COMMON/PCTC/
COMMON/GASCON/
COMMON/CHEMCN/
COMMON/CHEMXX/
COMMON/LIPCOM/
COMMON/SIGMB/
COMMON/GASDAT/
TKEY
THERMO

METHOD OF SOLUTION

The routine interpolates for the flow properties at the specified start-line Mach number using the equilibrium thermodynamic data tables. The resultant temperature and velocity are then used to obtain the flow properties from the species enthalpy and specific heat tables. The total enthalpy is calculated from the static enthalpy and velocity. This procedure is used to ensure property compatibility when transferring from the equilibrium tables to the species finite rate tables.

SUBROUTINE NAME: SITER

DESCRIPTION

This routine determines the entropy of the gas knowing the velocity, static pressure and total enthalpy or O/F ratio.

CALLING SEQUENCE

CALL SITER(HG, S, EM, V, PC, PL)

where

HG is the known total enthalpy or O/F ratio
S is the gas entropy
EM is the gas Mach number
V is the known gas velocity
PC is the gas total pressure
PL is the known gas static pressure

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/
EMOFV
ITSUB
POFEM
THERMO

METHOD OF SOLUTION

This subroutine iterates on the gas entropy until the guessed entropy, known velocity and enthalpy results in a static pressure which is within the convergence criteria of the known static pressure.

SUBROUTINE NAME: SLDP

DESCRIPTION

This subroutine finds the solutions to a set of N simultaneous linear equations.

CALLING SEQUENCE

CALL SLDP(X, A, N)

where

X is the solution matrix

A is the coefficient matrix

N is the order of the coefficient matrix

UTILITY ROUTINES AND COMMON REFERENCES

None

METHOD OF SOLUTION

The set of N simultaneous equations are solved using a Gauss-Jordan reduction scheme with the diagonal pivot strategy.

SUBROUTINE NAME: SLPLIN

DESCRIPTION

This subroutine handles the calculation of the points on the slip line. Two points are assigned to every slip line.

CALLING SEQUENCE

CALL SLPLIN (IS, JS, IN, KN, IFLAG, ICAUNT, K1W2, K2W2)

where

IS, JS is the storage array of the known point on the lower side of the slip line of the reference normal line (J-line)

IN, KN is the storage array of the known point below the slip line on the current normal (K-line)

IFLAG is a control indicator for sending in and out necessary messages

ICAUNT indicates the status of the iterative solution
- 0 - first time calculation of a particular slip line
- 1 - calculated results converged
- 2 - calculation completed but not final

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/	EMOFV
COMMON/CRITER/	ERRORS
COMMON/DATAR/	INRSCT
COMMON/DROP/	ITSUB
COMMON/GASCON/	PHYSOL
COMMON/SLIPPT	POFEM
CARCTR	

METHOD OF SOLUTION

The slipline points location is found by the usual manner as one of the interior points, and their flow properties are assumed initially to be identical to those of the corresponding points on the reference normal line. The velocity of the lower side point of the slipline is calculated with the aid of subroutines PHYSOL and CARCTR by using the II-characteristic. Pressure is then calculated with subroutine POFEM.

Letting the upper side point of the slipline have the same flow angle as the lower side point; the velocity of the upper side point can be calculated with the I-characteristic. Pressure is then calculated.

The pressure calculated for the slipline points is compared. The flow angle is adjusted, if necessary, until identical pressure is attained on both sides of the slipline.

See Volume I, Section 6.10 for the details of the calculation.

SUBROUTINE NAME: SOKFLX

DESCRIPTION

This subroutine solves for the flow properties downstream of a reflected shock knowing the turning angle and the reflected shock upstream flow properties. Real gas effects are considered in the calculations.

CALLING SEQUENCE

CALL SOKFLX (PD, PU, J, K, ITYPE, K1W1, K2W2)

where

PD is the array containing the downstream flow properties
PU is the array containing the upstream flow properties
J is the line identifier for the upstream flow properties
K is a dummy variable
K1W1 is a dummy variable
K2W2 is a dummy variable

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CRITER/
COMMON/GASCON/
COMMON/DATAR/
COMMON/CONTRL/
ESHOCK
ITSUB
ERRORS
THERMO
UOFV

METHOD OF SOLUTION

The routine is entered with the flow properties, PU, downstream of the incident shock and a known flow angle downstream of the reflected shock. An initial shock angle is assumed and a flow angle is calculated. The calculated flow angle is compared to the known flow angle and successive iterations on shock angle are performed until the flow angle difference is sufficiently close to zero.

SUBROUTINE NAME: SOKSOL

DESCRIPTION

This subroutine handles the calculation of different types of shock wave points. The following cases are considered:

1. Right-running shock (ITYPE = 111)
2. Left-running shock (ITYPE = 112)
3. Right-running shock incident on a lower boundary (ITYPE = 121)
4. Left-running shock incident on an upper boundary (ITYPE = 122)
5. Right-running shock attached at upper compression corner (ITYPE = 131)
6. Left-running shock attached at lower compression corner (ITYPE = 132)
7. Right-running shock reflected from the upper boundary (ITYPE = 141)
8. Left-running shock reflected from the lower boundary (ITYPE = 142)
9. Right-running weak shock at the upper wall (ITYPE = 151)
10. Left-running weak shock at the lower wall (ITYPE = 152)

CALLING SEQUENCE

```
CALL SOKSOL (IN, KN, IS, J, ITOTK, IFLAG, ITYPE, K2W1, K2W2)
```

where

(IN, KN):	storage location in PHO array for the shock upstream point on the new normal (KN-line)
(IS, J):	storage location in PHO array for a reference point on the known normal (J-line)
ITOTK:	total number of the KN-line; this is corrected according to the type of shock point
IFLAG:	for sending in and out necessary messages
ITYPE:	denotes type of shock points to be calculated

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CRITER/	BOUNDA
COMMON/GASCON/	CARCTR
COMMON/DATAR/	ERRORS
COMMON/CONTRL/	ESHOCK
COMMON/SLIPPT/	INRSCT
COMMON/PHISOL/	ITSUB
COMMON/TEMPO1/	PHYSOL
COMMON/TEMPO2/	PHYZOL
COMMON/DROP/	PPATPT
COMMON/GLOBAL/	STRNOR
COMMON/GAPPA/	THERMO
COMMON/FSTAG/	STRNOR
COMMON/PARTFP/	

METHOD OF SOLUTION

The general technique for handling shock wave points is: (1) find the location of the shock points and the flow properties of the shock upstream point, (2) calculate the flow properties of the shock downstream point with the oblique shock relation by using the shock upstream properties, (3) calculate the flow velocity of the shock downstream point with one characteristic line by using the shock downstream properties, (4) compare the velocity calculated from Steps 2 and 3, and (5) if the velocity is not the same, adjust the shock strength and repeat the process from Step 1.

For each individual case, see Vol.I of this report for detail.

SUBROUTINE NAME: SPCTX

DESCRIPTION

This routine controls the input and output from a FASTRAN file of the chemical species in a finite rate chemistry case.

CALLING SEQUENCE

CALL SPCTX (IFCN, IPT, ILINE, JLINE)

where

IFCN	indicates to write (=1) on drum or to read (=2) from drum
IPT	is the flowfield point number
ILINE	is the flowfield line number (one or two)
JLINE	specifies to store the data in SPCT(I, 1) or SPCT(I, 2)

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CHEMXX/

COMMON/CHEMCN/

COMMON/CONTRL/

RWU

METHOD OF SOLUTION

The routine calculates the location in the FASTRAN file where the desired data are read from or stored in. Subroutine RWU is then called to perform the indicated operation.

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4 OF 5
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SUBROUTINE NAME: STGMOD

DESCRIPTION

This subroutine computes the gas thermodynamic properties in the transition flow regime.

CALLING SEQUENCE

CALL STGMOD(I, K)

where

I = the point number

K = the line number

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/

COMMON/FREE/

COMMON/GSV/

COMMON/FSTAG/

COMMON/DATAR/

UTILITY – None

METHOD OF SOLUTION

The routine is entered knowing the flow regime, Knudsen number and flow properties (M_w, T, P, V, γ, S, H, ρ) of the (I, K) point. The specific heat ratio is then determined based on the flow regime.

Continuum – γ is same as entered

Vibrational mode frozen – γ is set to 1.4

Rotational mode frozen – γ is set based on a curve fit of gamma from 1.4 (vibrationally frozen) to 1.667 (free molecular) based on Knudsen number

Translationally frozen (free molecular) – γ = 1.667

Once the local gamma is determined then the local static properties, T, P and V, are used to determine the local total conditions (T_o, P_o) and Mach number.

SUBROUTINE NAME: STRNOR

DESCRIPTION

This subroutine handles the calculation of the flow properties of the point in question. The following cases are considered:

1. Interior point, uses I- and II-characteristic (ITYPE = 11)
2. Lower solid boundary point, uses I-characteristic (ITYPE = 21)
3. Upper solid boundary point, uses II-characteristic (ITYPE = 22)
4. Lower free boundary point, uses I-characteristic (ITYPE = 31)
5. Upper free boundary point, uses II-characteristic (ITYPE = 32)

Except those ITYPE numbers shown above, sometimes, one of the following numbers (500, 600, 700, 800, 900) is added to the original number to transmit more information to this subroutine.

CALLING SEQUENCE

CALL STRNOR (I1, K1, IS1, JS1, IN1, KN1, IFLAG, ITYPE, K1W1, K1W2)

where

I1, K1	is the storage location in the PHO array for the point in question on the new normal (K-line)
IS1, JS1	is the storage location in the PHO array for the known reference point on the old normal (J-line); normally this point is on the same streamline as the point I1, K1
IN1, KN1	is the storage location in the PHO array for the known point I1, K1 on the new normal (K-line)
IFLAG	is a control indicator for sending in and out necessary messages
ITYPE	denotes the type of point to be calculated

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/FREE/	COMMON/CPMUK/
COMMON/ISEA/	COMMON/RUE/
COMMON/CHEMCN/	COMMON/CHEMXX/
COMMON/CHEMXY/	COMMON/TUIPA/

COMMON/CONTRL/	COMMON/PARSTU/
COMMON/CRITER/	COMMON/FSTAG/
COMMON/DATAR/	BOUND
COMMON/DROP/	IDMPFP
COMMON/GASCON/	PPATPT
COMMON/PHISOL/	FNEWTN
COMMON/SLIPPT/	INRSCT
COMMON/TEMPO2/	GAPPBI
COMMON/TOTAL/	PHYSOL
COMMON/CROSS/	SPCTX
COMMON/STEPC/	PFP
COMMON/AVPROP/	RGMOFP
COMMON/PARTP1/	COEFF3
COMMON/PARTP2/	ROTERM
COMMON/GAPPA/	SLPLIN
COMMON/ONTSPT/	NEWENT
COMMON/POINTC/	UOFV
COMMON/NSF/	VOFEM
COMMON/OVERLA/	COEFEQ
COMMON/GLOBAL/	AVERAG
COMMON/PSEC/	CHECK
COMMON/INTEU/	

METHOD OF SOLUTION

Initially, the flow properties of the point in question are assumed to be the same as those of the known upstream point on the same streamline, and its location is found by intersecting the average streamline from the reference point (IS1, JS1) on the J-line and the average normal from the known point (IN1, KN1) on the K-line. Subroutine PHYSOL is used to find the reference properties for the characteristic lines and Eq. (3.3) is then used to calculate velocity and flow angle for the new point. Under normal conditions, the mass flow rate between two streamlines is conserved, but when the streamline meets a shock wave, no attempt is made to conserve the mass flow rate, because the streamline

is terminated at the shock upstream region and a new streamline is generated from the shock downstream point.

The iterative method is employed to find the velocity and the flow angle until they do not change appreciably between the successive iterations. During this iteration, the location of the new point is perturbed.

FUNCTION NAME: TAB

DESCRIPTION

This function computes the thermodynamic data storage location and retrieves data from the TABB array.

CALLING SEQUENCE

= TAB (I, J, K, L)

where

I, J, K, L are indices which are used to determine the storage location

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASDAT/

UTILITY – None

METHOD OF SOLUTION

The thermodynamic data storage location is computed using the following relation

IX = I + 10 * (J-1 + 2 * (K-1 + 13 * (L-1))),

and retrieved using the relation

TABB = TABB(IX)

SUBROUTINE NAME: TEMTAB

DESCRIPTION

This subroutine will perform a table lookup for particle temperature as a function of enthalpy or for particle enthalpy as a function of temperature.

CALLING SEQUENCE

CALL TEMTAB(X, Y, WHICH)

where

X is the unknown variable

Y is the known variable

WHICH is the lookup control variable indicating to lookup temperature (=1) or enthalpy (=2)

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/

COMMON/TPEH/

COMMON/TFLAG/

UTILITY – None

METHOD OF SOLUTION

The unknown variable (particle temperature or enthalpy) is calculated by either assuming constant heat capacities or by applying linear interpolation techniques to the tabulated data input on cards 32.

SUBROUTINE NAME: THERMO

DESCRIPTION

This subroutine utilizes real or ideal gas information obtained from the flowfield tape (or tables) and a local O/F ratio (or total enthalpy) to call subroutine FABLE to calculate thermodynamic gas properties locally in the flow.

CALLING SEQUENCE

CALL THERMO (OF, SS, VV)

where

OF = gas total enthalpy or O/F ratio
SS = gas entropy
VV = gas velocity

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/	COMMON/GASDAT/
COMMON/CPMUK/	COMMON/FAB/
COMMON/GRINT/	COMMON/CONTRL/
COMMON/PARTP1/	TAB
COMMON/PARTP2/	FABLE
COMMON/TEMPER/	THERM1

METHOD OF SOLUTION

The routine is entered with the local O/F ratio (or total enthalpy), OF, entropy, SS, and velocity, VV. The local ratio is used to determine which set of thermodynamic tables that subroutine FABLE should use to perform table lookup of the local thermodynamic gas properties. Subroutine THERMO then uses the local thermodynamic gas properties obtained from FABLE to perform an interpolation between the O/F (or total enthalpy) tables based on the local O/F ratio (or total enthalpy).

SUBROUTINE NAME: THERM1

DESCRIPTION

This routine determines the gas thermodynamic properties for a finite rate chemistry case.

CALLING SEQUENCE

CALL THERM1(HT, V)

where

HT is the gas total enthalpy

V is the gas velocity

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/TEMPER/
COMMON/GASCON/
COMMON/PCTC/
COMMON/CPMUK/
COMMON/CONTRL/
COMMON/VISEX/
COMMON/CHEMCN/
COMMON/CHEMXX/
COMMON/GASDAT/
TKEY
TOFH

METHOD OF SOLUTION

The routine looks up enthalpy and specific heats from tabulated data of enthalpy and specific heats as functions of temperature. The enthalpy, specific heats and molecular weights of each species are used, along with species concentrations, to calculate the mixture gas constant, gamma, enthalpy, specific heat, and total pressure and temperature. These properties, along with velocity are used to calculate total enthalpy and Mach number.

SUBROUTINE NAME: THETPM

DESCRIPTION

THETPM performs a numerical integration to calculate properties through a Prandtl-Meyer expansion. Either the case of known final velocity or known final expansion angle may be handled.

CALLING SEQUENCE

CALL THETPM (OF, S, DELTA, VF, VI, IT, ITYPE, K1W, K2W)

where

OF	is the local O/F ratio or total enthalpy
S	is the local entropy level
DELTA	is the total expansion angle
VF	is the final velocity downstream of the expansion
VI	is the initial velocity upstream of the expansion
IT	is a control parameter indicating if expansion to a solid wall or free boundary is taking place
ITYPE	indicates if an upper (2) or lower (1) boundary is being considered.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/
COMMON/STEPC/
COMMON/CONTRL/
THERMO
TOFH
ITSUB
TOFV
ERRORS

METHOD OF SOLUTION

The integral equation

$$\int_{V_1}^{V_F} \sqrt{M^2 - 1}\,\frac{dV}{V} - \Delta\theta = f(V_F) = 0$$

where $M^2 = V^2/\gamma RT$ is solved knowing either the final velocity, V_F, or the expansion angle ($\Delta\theta$). As can be seen, if the final velocity, V_F, is known, the integration progresses straightforwardly to a solution. However, if the expansion angle is known, an iterative procedure must be employed to pick the velocity which produces the desired expansion angle.

SUBROUTINE NAME: THRUST

DESCRIPTION

THRUST computes the vacuum thrust produced by a two-dimensional or axisymmetric nozzle. Addition of the thrust at the throat and the integrated pressure along the nozzle wall yields the final thrust.

CALLING SEQUENCE

CALL THRUST (L, K, I1, J1, ITYPE, ICALC, K1W1, K1W2)

where L, K designates the unknown characteristic point and I1, J1 is the known characteristic point. ITYPE specifies if the point is on the upper or lower boundary and ICALC is a counter with the values of 1, 2 or 3. (1 specifies integration at the throat, 2 - along the nozzle and 3 - at the exit.)

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/
COMMON/DATAR/
COMMON/FORCE/
COMMON/INPUT/
COMMON/PARTP1/
COMMON/PARTP2/
COMMON/FSTAG/
COMMON/WT/
COMMON/PSLD/
COMMON/INTCR/
PFP
VEMAG

METHOD OF SOLUTION

Thrust is found by first computing the momentum thrust in the sonic area or throat of the nozzle. The static pressure is then integrated along the nozzle wall and the total thrust found by summation of the pressure and momentum terms (both gas and particle). Inclusion of a factor in the incremental force term accounts for either two-dimensional or axisymmetric flow.

SUBROUTINE NAME: TKEY

DESCRIPTION

This routine determines the proper index to be used in the enthalpy and specific heat tables and calculates interpolation factors.

CALLING SEQUENCE

CALL TKEY (T, TTB, ITKEY, SDT, HDT, NT)

where

T = the temperature

TTB = the temperature tables used as independent variables

ITKEY = the resultant index

SDT and HDT = interpolation factors

NT = number of entries in the temperature table.

UTILITY ROUTINES AND COMMON REFERENCES

None

METHOD OF SOLUTION

The routine searches the temperature table until the input temperature is bounded. The index of the lower bound is stored in ITKEY and the interpolation factors are calculated by the equations

$$SDT = \frac{T - TTB\ (ITKEY)}{TTB\ (ITKEY + 1) - TTB\ (ITKEY)}$$

and

$$HDT = \frac{TTB\ (ITKEY + 1) - T}{TTB\ (ITKEY + 1) - TTB\ (ITKEY)}$$

FUNCTION NAME: TOFEM

DESCRIPTION

TOFEM computes the local static temperature as a function of Mach number. TOFEM and TOFV are quite similar; the difference being if Mach number or velocity is the known quantity.

CALLING SEQUENCE

T = TOFEM (EM, K1W1, K1W2)

where T is the one-dimensionally calculated local static temperature which exists at the Mach number, . NOTE: The appropriate values of the gas properties must be stored in common upon entry to this routine.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/

UTILITY – None

METHOD OF SOLUTION

The thermally perfect gas relationships are used to find the static temperature at the local Mach number.

$$T = \frac{T_o}{1 + \frac{\gamma - 1}{2} M^2}$$

FUNCTION NAME: TOFENH

DESCRIPTION

This routine calculates the temperature as a function of enthalpy for a finite-rate chemistry case.

CALLING SEQUENCE

= TOFENH(HU)

where HU is the static enthalpy

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/
COMMON/PCTC/
COMMON/CPMUK/
COMMON/VISEX/
COMMON/CHEMCN/
COMMON/CHEMXX/
COMMON/GASDAT/
TKEY
ITSUB

METHOD OF SOLUTION

The temperature is estimated initially and this temperature is used to calculate an enthalpy from the temperature-enthalpy tables. If the resultant enthalpy does not match HU, the temperature is incremented and the process repeated until the enthalpies converge.

FUNCTION NAME: TOFH

DESCRIPTION

This routine calculates the temperature as a function of enthalpy for a finite rate chemistry case during a Prandtl-Meyer expansion.

CALLING SEQUENCE

= TOFH (HU, V)

where

HU is the enthalpy

V is the velocity

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/TEMPER/
COMMON/GASCON/
COMMON/PCTC/
COMMON/CPMUK/
COMMON/VISEX/
COMMON/CHEMCN/
COMMON/CHEMXX/
COMMON/GASDAT/
TKEY
ITSUB
POFH

METHOD OF SOLUTION

The methodology is the same as for TOFENH except that the gas constant, molecular weight, gamma and Mach number are also computed.

FUNCTION NAME: TOFV

DESCRIPTION

This function computes the local static temperature as a function of velocity. TOFV and TOFEM are quite similar; the difference being if Mach number or velocity is the known variable.

CALLING SEQUENCE

T = TOFV (V,K1W1,K1W2)

where T is the local static temperature which exists at the velocity, V. NOTE: The appropriate values of the gas properties must be stored in common upon entry to this routine.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/
RITE
ERRORS
KIKOFF

METHOD OF SOLUTION

The thermally perfect gas relationships are used to find the static temperature at the local velocity.

$$T = T_o - \frac{V^2}{2R}\left(\frac{\gamma - 1}{\gamma}\right)$$

SUBROUTINE NAME: TRANS

DESCRIPTION

This subroutine provides overall control for initializing the data and reading the namelist data for the Kliegel two-phase transonic solution of a supersonic gas particle startline.

CALLING SEQUENCE

CALL TRANS (NTAPE, NSETS, RUT)

where

NTAPE	=	FORTRAN unit on which the startline is written
NSETS	=	number of startline points where particles are present
RUT	=	throat radius (ft)

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CONTRL/	COMMON/PARTP2/
COMMON/GASDAT/	COMMON/ERR/
COMMON/GASCON/	COMMON/NAMEA/
COMMON/CPMUK/	COMMON/NAME1/
COMMON/TPEH/	COMMON/NAMEW/
COMMON/MASSC/	TAB
COMMON/DRAGCF/	PARTIL
COMMON/TRANS1/	

METHOD OF SOLUTION

Not applicable.

SUBROUTINE NAME: TURN

DESCRIPTION

TURN solves for a shock wave which has a known turning angle (δ). A condition of known turning angle exists when the flow is turned through a compression corner on a solid boundary. Real gas effects are considered in calculating conditions downstream of the shock.

CALLING SEQUENCE

CALL TURN (PU, PD, DELTA, IFLAG, K1W1, K1W2)

where PU, PD represent flow conditions upstream and downstream of the shock, DELTA is the turning angle, and IFLAG indicates if the solution will or will not converge.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/CRITER/
COMMON/CONTRL/
THERMO
EMOFV
UOFEM
ESHOCK
ITSUB
ERRORS
UOFV

METHOD OF SOLUTION

An initial shock angle is assumed. This shock angle is used to calculate a turning angle. The calculated turning angle is compared to the known turning angle and successive iterations on shock angle are performed until the turning angle difference is sufficiently close to zero.

FUNCTION NAME: UOFEM

DESCRIPTION

This function computes the local Mach angle as a function of local Mach number. Prior to the calculation a test is made to ensure that the Mach number is greater than one.

CALLING SEQUENCE

EMU = UOFEM (EM, K1W1, K1W2)

where EMU is the Mach angle which exists at the local Mach number, EM.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON – None

ERRORS

KIKOFF

RITE

METHOD OF SOLUTION

The following equation is solved for the local Mach angle.

$$\mu = \tan^{-1}\left(\frac{1}{\sqrt{M^2 - 1}}\right)$$

FUNCTION NAME: UOFV

DESCRIPTION

This function computes the local Mach angle as a function of local velocity.

CALLING SEQUENCE

EMU = UOFV (V, K1W1, K1W2)

where EMU is the Mach angle which exists at the local velocity, V.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON – None

UOFEM

EMOFV

METHOD OF SOLUTION

The local velocity is converted into a Mach number using EMOFV. Function UOFEM is then entered with the calculated Mach number. The Mach angle is obtained from the following equation.

$$\mu = \tan^{-1}\left(\frac{1}{\sqrt{M^2 - 1}}\right)$$

FUNCTION NAME: VEMAG

DESCRIPTION

VEMAG determines the magnitude of a vector.

CALLING SEQUENCE

= VEMAG(V)

where V is any vector.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON – None

DOTPRD

METHOD OF SOLUTION

The following equation is solved for the magnitude of a vector

$$\text{VEMAG} = \sqrt{V(1)^2 + V(2)^2}$$

where

$$\vec{V} = V(1)\vec{i} + V(2)\vec{j}$$

FUNCTION NAME: VOFEM

DESCRIPTION

This function computes velocity as a function of Mach number.

CALLING SEQUENCE

V = VOFEM (EM, K1W1, K1W2)

where V is the local velocity which corresponds to the local Mach number, EM. NOTE: The appropriate values of the gas properties must be stored in common upon entry to this routine.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/

TOFEM

METHOD OF SOLUTION

The thermally perfect gas relationship

$$V = \sqrt{\frac{R\gamma(T_o - T)}{\left(\frac{\gamma - 1}{2}\right)}}$$

is solved for velocity. Local static temperature, T, is obtained from the input Mach number.

SUBROUTINE NAME: WEAK

DESCRIPTION

This subroutine determines the independent variables, entropy and velocity, SD, VD, downstream of a weak oblique shock. The gas properties upstream of the shock are known prior to entry.

CALLING SEQUENCE

CALL WEAK (OF, SU, VU, EPS, DELTA, SD, VD, K1W, K2W)

where OF is the upstream O/F ratio (or total enthalpy), SU, VU are the upstream entropy and velocity, EPS, DELTA are the shock angle and turning angle, and SD, VD are the downstream entropy and velocity.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/
THERMO
EMOFV
POFEM
RHOFEM
ENTROP
DELTAF

METHOD OF SOLUTION

From the known upstream entropy and velocity, the local gas properties, pressure, density, and upstream Mach number are calculated. The entropy rise across the shock is added to the upstream entropy to get total downstream entropy. Downstream velocity is calculated from the following relationship.

$$V_D = \frac{V_U \cos(\xi)}{\cos(\xi - \delta)}$$

FUNCTION NAME: WOFA

DESCRIPTION

WOFA computes the weight flow per unit area as a function of Mach number. This calculation is only used in function AOASTR.

CALLING SEQUENCE

Weight Flow = WOFA (EM, K1W1, K1W2)

where EM is the local Mach number. NOTE: The appropriate values of the gas properties must be stored in common upon entry to this routine.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/GASCON/

UTILITY – None

METHOD OF SOLUTION

Weight flow per unit area, $\dot{W}/A$, is calculated from the thermally perfect gas relation.

$$\frac{\dot{W}}{A} = \sqrt{\frac{\gamma}{RT_o}} \left\{ \frac{P_o M}{\left[1 + \frac{\gamma - 1}{2} M^2\right]^{\frac{\gamma+1}{2(\gamma-1)}}} \right\}$$

FUNCTION NAME: WTFLOF

DESCRIPTION

This function computes the area normal to the flow which is bounded by two streamline points.

CALLING SEQUENCE

= WTFLOF (M, N, K, A)

where

M = the point number of the lower streamline point

N = the point number of the upper streamline point

K = the line number

A = a 1 for axisymmetric flow and a 0 for two-dimensional flow.

UTILITY ROUTINES AND COMMON REFERENCES

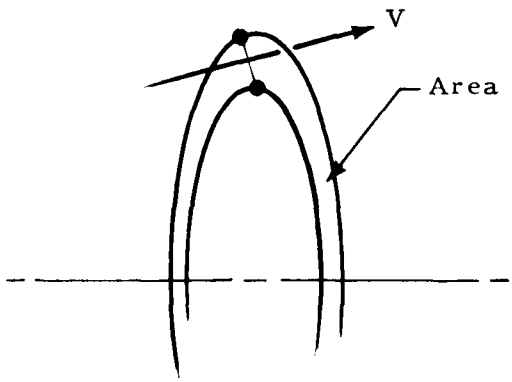
COMMON/DATAR/

COMMON/CONTRL/

UTILITY – None

METHOD OF SOLUTION

The area bounded by two points and normal to the average local flow vector is calculated via geometric relations



FUNCTION NAME: XSI

DESCRIPTION

This function computes the storage location for the nonlinear interpolation weighting functions required for thermodynamic property lookup and retrieves data from XSIDIM.

CALLING SEQUENCE

= XSI (I, J, K, L)

where

I, J, K, L are indices used to determine the storage location.

UTILITY ROUTINES AND COMMON REFERENCES

COMMON/XSICOM/

UTILITY – None

METHOD OF SOLUTION

The storage location is computed using the following relation

IX = I + 10 * (J-1 + 2 * (K-1 + 13 * (L-1)))

and retrieved using the relation

XSI = XSIDIM(IX)

3.7 EXAMPLE PROBLEMS

To familiarize the user with the operation of the RAMP computer program several sample cases are presented. Each sample case will consist of a description of the problem, a listing of the input data for the problem and a listing of the pertinent solution.

Example Problem 1

This problem analyzes a single phase chemical equilibrium flow field with the following stipulations:

1. Generate a startline at the nozzle exit plane for example problem 2,
2. The gas properties are to be read from cards, and
3. The startline at the nozzle throat is to be calculated internal to the program.

Figure 3-4 presents a schematic of a typical nozzle plume flow field. Table 3-7 presents first a flow chart and then a listing of the input data for the specified problem; some of these cards are indicated in Fig. 3-4. Table 3-8 presents a listing of the pertinent solution.

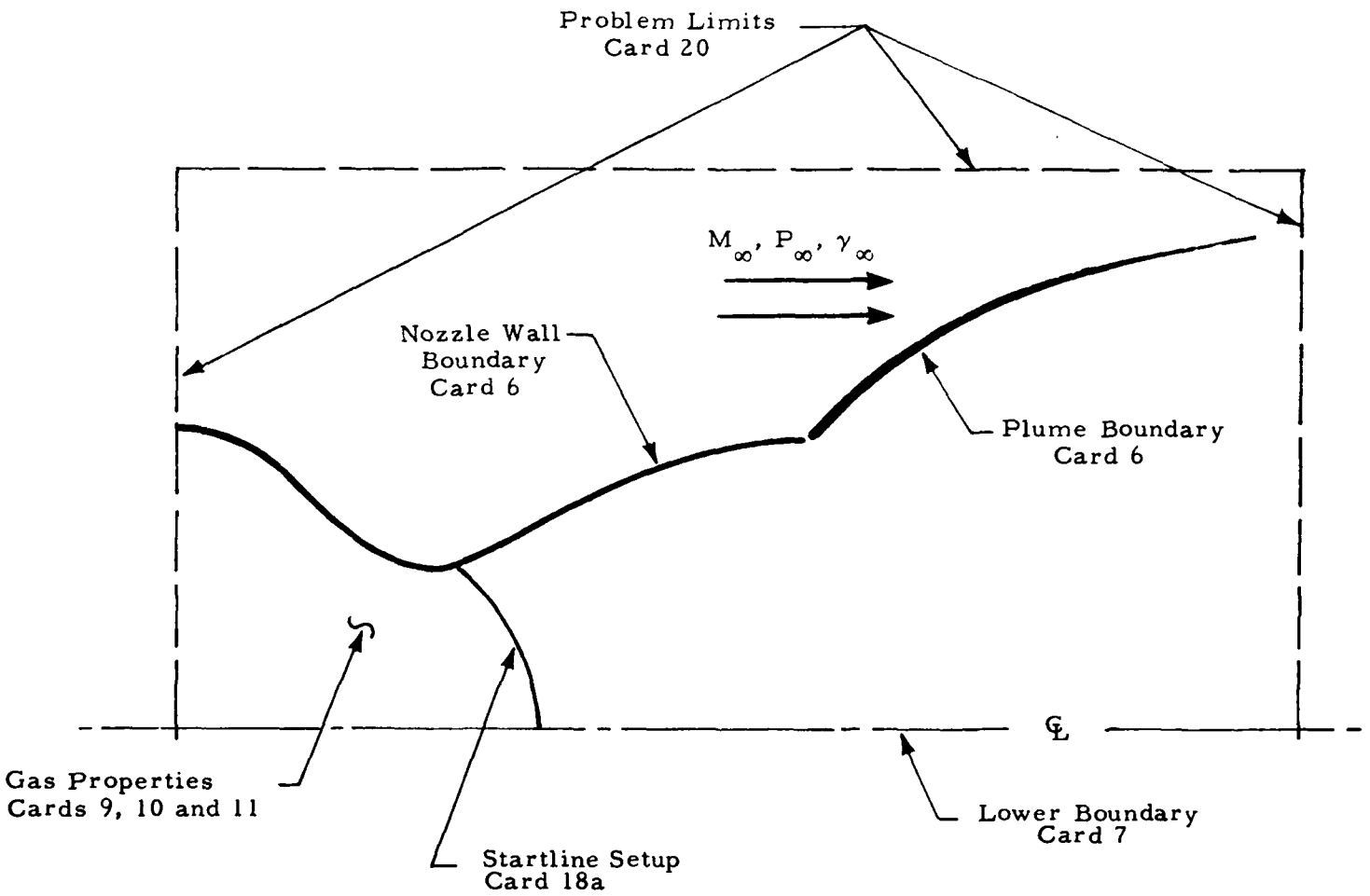
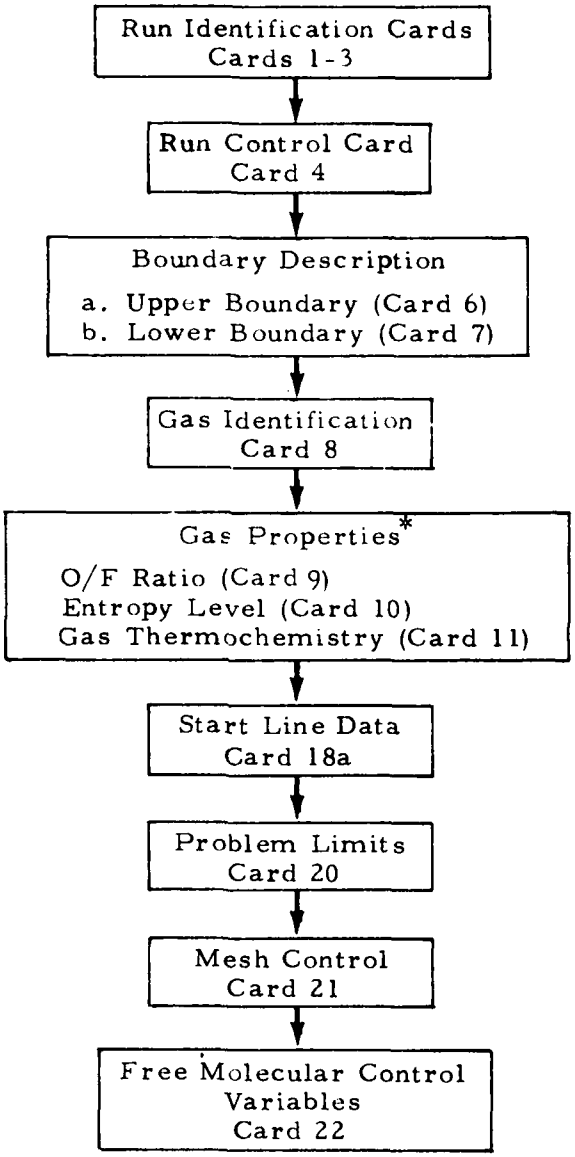


Fig. 3-4 - Schematic of a Typical Nozzle-Plume Flow Field with Control Cards Indicated

Table 3-7

REQUIRED INPUT FORMAT FOR EXAMPLE PROBLEM 1



*If gas properties are input on tape (ICON(1)=2) Cards 9, 10 and 11 are not required.

Table 3-7 (Concluded)

Cards 1-3	GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED								
Card 4	1	121	3	1	1	2	15	1	11	1	1200
Cards 6	1	-1.	.133333	0.0	-1.0	-.547722	.09450723				
	2 1				.26794919	.16969306	13.09674760				
	3	.0100					1000.				
Card 7	2						1000.				
Card 8	IDEAL GAS			ENG	1	1					
Card 9	.0										
Card 10	.0		13								
Cards 11	.0	24.834	1.1798	5468.4	122.48						
	1.0	24.948	1.1911	5025.6	69.321						
	1.746	25.055	1.2121	4239.0	24.496						
	2.151	25.080	1.2224	3747.6	12.248						
	2.538	25.089	1.2297	3299.4	6.1241						
	2.916	25.091	1.2344	2896.2	3.0621						
	3.424	25.091	1.2376	2430.0	1.2248						
	4.057	25.091	1.2731	1931.4	.4083						
	4.364	25.091	1.2819	1729.8	.2450						
	4.790	25.091	1.2944	1481.4	.1225						
	5.614	25.091	1.3220	1013.4	.0245						
	6.279	25.091	1.3325	853.2	.0122						
	7.680	25.091	1.3527	567.0	.0024						
Card 18a	.0	0.0	1.01								
Card 20	100.	-100.	0.0	0.0	5.0	90.					
Card 21	.50	.20	1.	.005	5.	.90					
Card 22	100.0	10.0	.10	1.0	1.0E-04	.60					

Table 3-8

EXAMPLE PROBLEM 1 PERTINENT SOLUTION

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 1

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

RUN CONTROL PARAMETERS

ICON(1)	ICON(2)	ICON(3)	ICON(4)	ICON(5)	ICON(6)	ICON(7)	ICON(8)
1	0	21	3	1	0	1	2

ICON(9)	ICON(10)	ICON(11)	ICON(12)	ICON(13)	ICON(14)	ICON(15)	ICON(16)
0	15	1	1	1	0	0	12000

FLOW CALCULATIONS ARE IN ENGLISH UNITS WITH THE R,X COORDINATES IN FEET

THE FLOW FIELD DATA WILL NOT WRITTEN ON TAPE

UPPER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
1	0	-.10000+01	.13333+00	.00000	-.10000+01	-.54772+00	.94507-01
2	1	.00000	.00000	.00000	.26795+00	.16969+00	.30987+01
3	0	.10000-01	.00000	.00000	.00000	.00000	.10000+04

LOWER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
2	0	.00000	.00000	.00000	.00000	.00000	.10000+04

THERE ARE 0 PARTICLE SPECIES PRESENT IN THE GAS-PARTICLE MIXTURE

THE FOLLOWING GAS PROPERTIES IN ENGLISH UNITS ARE FOR IDEAL GAS

REAL GAS PROPERTIES

O/F
.00000

S	V	R	GAMMA	T	P	PR	VIS	CP
.00000								
	.00000	.20016+04	.11798+01	.54684+04	.18000+04	.00000	.00000	.00000
	.34536+04	.19925+04	.11911+01	.60256+04	.10187+04	.00000	.00000	.00000
	.55746+04	.19840+04	.12121+01	.42390+04	.35999+03	.00000	.00000	.00000
	.64815+04	.19820+04	.12224+01	.37470+04	.18000+03	.00000	.00000	.00000
	.71902+04	.19813+04	.12297+01	.32994+04	.90000+02	.00000	.00000	.00000
	.77605+04	.19811+04	.12344+01	.28962+04	.45001+02	.00000	.00000	.00000
	.83577+04	.19811+04	.12376+01	.24300+04	.18000+02	.00000	.00000	.00000
	.89543+04	.19811+04	.12731+01	.19314+04	.60004+01	.00000	.00000	.00000

Table 3-8 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 2

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

REAL GAS PROPERTIES

H-TOTAL

S	V	R	GAMMA	T	P	PR	VIS	CP
.00000								
	.91468+04	.19811+04	.12819+01	.17298+04	.36005+01	.00000	.00000	.00000
	.93361+04	.19811+04	.12944+01	.14814+04	.18003+01	.00000	.00000	.00000
	.94719+04	.19811+04	.13220+01	.10134+04	.36005+00	.00000	.00000	.00000
	.94234+04	.19811+04	.13325+01	.85320+03	.17929+00	.00000	.00000	.00000
	.94670+04	.19811+04	.13527+01	.56700+03	.35270-01	.00000	.00000	.00000

STARTING LINE INFO

R	X	M	THETA	S	MACH ANGLE	SHOCK ANGLE	Q/F
.00000	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.91287-02	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.18257-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.27386-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.36515-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.45644-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.54772-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.63901-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.73030-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.82158-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.91287-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.10042+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.10954+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.11867+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.12780+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.13693+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.14606+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.15519+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.16432+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.17345+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.18257+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000

RUN CUTOFF INFORMATION

UPPER BOUNDARY						LOWER BOUNDARY					
R=	.10000+03	X=	-.10000+03	THETA=	.00000	R=	.00000	X=	.50000+01	THETA=	.90000+02

Table 3-8 (Continued)

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                   CASE NO.    1                                          PAGE    3
GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED
                    VIBNO        ROTNO        TRANNO        CHARL        GAMV        GAMR
                   .10000+03    .10000+02    .10000+00    .10000+01    .00000      .00000
                   THE MESH CONSTRUCTION WILL BE CONTROLED BY THE FOLLOWING VARIABLES
DL INTERIOR=  .500+00 DX AXIS=  .200+00 DL LIM=  .100+01 DL DELETE=  .500-02 DEG P.M.=  .500+01 F=  .900+00
```

Table 3-8 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 5

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

LINE	POINT	DSCRIP	- REGIME	R / MACH ANGLE	X / PRESSURE	M / DENSITY	THETA / TEMPERATURE	ENTROPY / GAS CONST.	VELOCITY / LOCAL GAMMA	O/F / SHOCK ANGLE	ITR
1	14	INPUT	- CONTIN	.11867+00	.00000	.10100+01	.00000	.00000	.34853+04	.00000	0
				.81931+02	.10076+04	.14517-01	.50166+04	.19924+04	.11914+01		
1	15	INPUT	- CONTIN	.12780+00	.00000	.10100+01	.00000	.00000	.34853+04	.00000	0
				.81931+02	.10076+04	.14517-01	.50166+04	.19924+04	.11914+01		
1	16	INPUT	- CONTIN	.13693+00	.00000	.10100+01	.00000	.00000	.34853+04	.00000	0
				.81931+02	.10076+04	.14517-01	.50166+04	.19924+04	.11914+01		
1	17	INPUT	- CONTIN	.14606+00	.00000	.10100+01	.00000	.00000	.34853+04	.00000	0
				.81931+02	.10076+04	.14517-01	.50166+04	.19924+04	.11914+01		
1	18	INPUT	- CONTIN	.15519+00	.00000	.10100+01	.00000	.00000	.34853+04	.00000	0
				.81931+02	.10076+04	.14517-01	.50166+04	.19924+04	.11914+01		
1	19	INPUT	- CONTIN	.16432+00	.00000	.10100+01	.00000	.00000	.34853+04	.00000	0
				.81931+02	.10076+04	.14517-01	.50166+04	.19924+04	.11914+01		
1	20	INPUT	- CONTIN	.17345+00	.00000	.10100+01	.00000	.00000	.34853+04	.00000	0
				.81931+02	.10076+04	.14517-01	.50166+04	.19924+04	.11914+01		
1	21	INPUT	- CONTIN	.18257+00	.00000	.10100+01	.00000	.00000	.34853+04	.00000	0
				.81931+02	.10076+04	.14517-01	.50166+04	.19924+04	.11914+01		

THE MASS FLOW RATE IS = .170473+03

MOMENTUM INTEGRATION RESULTS

FORCEX	FORCEY	TORQZ	ISP
-.33661+05	.00000	.00000	.19746+03

NOTES: (1) Typical printout for the nozzle throat startline data surface.
(2) Some points have been omitted for demonstration purposes.

Table 3-8 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 9

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

LINE	POINT	DSCRIP	- REGIME	R MACH ANGLE	X PRESSURE	M DENSITY	THETA TEMPERATURE	ENTROPY GAS CONST.	VELOCITY LOCAL GAMMA	O/F SHOCK ANGLE	I-R
10	21	WALL	- CONTIN	.18271+00 .64542+02	.99155-02 .90099+03	.11075+01 .13229-01	.15560+01 .49256+04	.00000 .19911+04	.37906+04 .11944+01	.00000	3
11	1	WALL	- CONTIN	.00000 .81931+02	.11647-01 .10076+04	.10100+01 .14517-01	.00000 .50166+04	.00000 .19924+04	.34853+04 .11914+01	.00000	1
11	21	WALL	- CONTIN	.18274+00 .63705+02	.10972-01 .89256+03	.11154+01 .13126-01	.17219+01 .49180+04	.00000 .19910+04	.38149+04 .11947+01	.00000	3
12	1	WALL	- CONTIN	.00000 .81931+02	.12812-01 .10076+04	.10100+01 .14517-01	.00000 .50166+04	.00000 .19924+04	.34853+04 .11914+01	.00000	1
12	21	WALL	- CONTIN	.18277+00 .62925+02	.12022-01 .88438+03	.11230+01 .13026-01	.18867+01 .49106+04	.00000 .19910+04	.38385+04 .11949+01	.00000	3
13	1	WALL	- CONTIN	.00000 .81931+02	.13977-01 .10076+04	.10100+01 .14517-01	.00000 .50166+04	.00000 .19924+04	.34853+04 .11914+01	.00000	1
13	21	WALL	- CONTIN	.18281+00 .62194+02	.13065-01 .87644+03	.11305+01 .12928-01	.20505+01 .49034+04	.00000 .19909+04	.38615+04 .11951+01	.00000	3
14	1	WALL	- CONTIN	.00000 .81931+02	.15141-01 .10076+04	.10100+01 .14517-01	.00000 .50166+04	.00000 .19924+04	.34853+04 .11914+01	.00000	1
14	21	WALL	- CONTIN	.18285+00 .61505+02	.14102-01 .86870+03	.11378+01 .12834-01	.22133+01 .48963+04	.00000 .19908+04	.38838+04 .11954+01	.00000	3
15	1	WALL	- CONTIN	.00000 .81931+02	.16306-01 .10076+04	.10100+01 .14517-01	.00000 .50166+04	.00000 .19924+04	.34853+04 .11914+01	.00000	1
15	21	WALL	- CONTIN	.18289+00 .60852+02	.15132-01 .86115+03	.11450+01 .12741-01	.23751+01 .48893+04	.00000 .19907+04	.39057+04 .11956+01	.00000	3
16	1	WALL	- CONTIN	.00000 .81931+02	.17471-01 .10076+04	.10100+01 .14517-01	.00000 .50166+04	.00000 .19924+04	.34853+04 .11914+01	.00000	1
16	21	WALL	- CONTIN	.18293+00 .60233+02	.16156-01 .85378+03	.11520+01 .12650-01	.25360+01 .48824+04	.00000 .19906+04	.39272+04 .11958+01	.00000	3

NOTES: (1) Typical printout for a data surface inside the nozzles.
(2) Some points have been omitted for demonstration purposes.

Table 3-8 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 33

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

LINE	POINT	DSCRIP	- REGIME	R MACH ANGLE	X PRESSURE	M DENSITY	THETA TEMPERATURE	ENTROPY GAS CONST.	VELOCITY LOCAL GAMMA	O/F SHOCK ANGLE	ITR
106	1	WALL	- CONTIN	.00000 .13752+02	.30900+01 .47962+01	.41903+01 .18944-03	.00000 .18402+04	.00000 .19811+04	.90418+04 .12771+01	.00000	5
106	2	INTER	- CONTIN	.49924-01 .13756+02	.30896+01 .48068+01	.41890+01 .18977-03	.82763+00 .18411+04	.00000 .19811+04	.90410+04 .12771+01	.00000	5
106	3	INTER	- CONTIN	.99857-01 .13759+02	.30885+01 .48124+01	.41883+01 .18994-03	.16556+01 .18416+04	.00000 .19811+04	.90405+04 .12770+01	.00000	5
106	4	INTER	- CONTIN	.14975+00 .13761+02	.30867+01 .48183+01	.41876+01 .19012-03	.24810+01 .18421+04	.00000 .19811+04	.90401+04 .12770+01	.00000	5
106	5	INTER	- CONTIN	.19958+00 .13765+02	.30842+01 .48255+01	.41867+01 .19035-03	.33027+01 .18427+04	.00000 .19811+04	.90395+04 .12770+01	.00000	5
106	6	INTER	- CONTIN	.24935+00 .13769+02	.30810+01 .48348+01	.41855+01 .19063-03	.41195+01 .18434+04	.00000 .19811+04	.90388+04 .12770+01	.00000	5
106	7	INTER	- CONTIN	.29901+00 .13774+02	.30770+01 .48470+01	.41840+01 .19101-03	.49296+01 .18444+04	.00000 .19811+04	.90378+04 .12769+01	.00000	5
106	8	INTER	- CONTIN	.34854+00 .13781+02	.30724+01 .48632+01	.41820+01 .19151-03	.57300+01 .18458+04	.00000 .19811+04	.90365+04 .12769+01	.00000	5
106	9	INTER	- CONTIN	.39790+00 .13790+02	.30671+01 .48847+01	.41794+01 .19217-03	.65178+01 .18475+04	.00000 .19811+04	.90349+04 .12768+01	.00000	5
106	10	INTER	- CONTIN	.44705+00 .13803+02	.30612+01 .49131+01	.41759+01 .19305-03	.72891+01 .18498+04	.00000 .19811+04	.90326+04 .12767+01	.00000	5
106	11	INTER	- CONTIN	.49595+00 .13819+02	.30546+01 .49509+01	.41713+01 .19422-03	.80382+01 .18529+04	.00000 .19811+04	.90297+04 .12765+01	.00000	5
106	12	INTER	- CONTIN	.54451+00 .13841+02	.30474+01 .50017+01	.41652+01 .19577-03	.87570+01 .18570+04	.00000 .19811+04	.90258+04 .12764+01	.00000	5
106	13	INTER	- CONTIN	.59266+00 .13870+02	.30397+01 .50696+01	.41571+01 .19786-03	.94370+01 .18624+04	.00000 .19811+04	.90206+04 .12761+01	.00000	5

NOTES: (1) Typical printout for a data surface at the nozzle exit plane.
(2) Some points have been omitted for demonstration purposes.

Table 3-8 (Concluded)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 34

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

LINE	POINT	DSCRIP - NAME	M MACH ANGLE	X PRESSURE	M DENSITY	THETA TEMPERATURE	ENTROPY GAS CONST.	VELOCITY LOCAL GAMMA	O/F SHOCK ANGLE	ITR
106	22	PRN-MR - CONTIN	.10000+01 .12876+02	.30987+01 .29328+01	.44874+01 .12902-03	.19590+02 .16522+04	.00000 .19811+04	.92063+04 .12658+01	.00000	5
106	23	PRN-MR - CONTIN	.10000+01 .11567+02	.30987+01 .12887+01	.49873+01 .68419+04	.24160+02 .13591+04	.00000 .19811+04	.93669+04 .13011+01	.00000	5
106	24	PRN-MR - CONTIN	.10000+01 .97053+01	.30987+01 .31681+00	.59319+01 .23452-04	.28773+02 .96188+03	.00000 .19811+04	.95089+04 .13210+01	.00000	5
106	25	PRN-MR - CONTIN	.10000+01 .69772+01	.30987+01 .16273+00	.65165+01 .14163-04	.33360+02 .83512+03	.00000 .19811+04	.96339+04 .13210+01	.00000	5
106	26	PRN-MR - CONTIN	.10000+01 .77733+01	.30987+01 .78163-01	.72063+01 .81314-05	.37951+02 .69887+03	.00000 .19811+04	.97485+04 .13210+01	.00000	5
106	27	PRN-MR - CONTIN	.10000+01 .71938+01	.30987+01 .34692-01	.80412+01 .43957-05	.42541+02 .57365+03	.00000 .19811+04	.98527+04 .13210+01	.00000	5
106	28	PRN-MR - CONTIN	.10000+01 .63327+01	.30987+01 .13972-01	.90661+01 .22081-05	.47131+02 .45991+03	.00000 .19811+04	.99463+04 .13210+01	.00000	5
106	29	PRN-MR - CONTIN	.10000+01 .55383+01	.30987+01 .49846-02	.10361+02 .10120-05	.51721+02 .35802+03	.00000 .19811+04	.10030+05 .13210+01	.00000	5
106	30	PRN-MR - CONTIN	.10000+01 .47583+01	.30987+01 .15215-02	.12055+02 .41215-06	.56311+02 .26833+03	.00000 .19811+04	.10102+05 .13210+01	.00000	5
106	31	PRN-MR - CONTIN	.10000+01 .39904+01	.30987+01 .37697-03	.14370+02 .14332-06	.60901+02 .19117+03	.00000 .19811+04	.10164+05 .13210+01	.00000	5
106	32	PRN-MR - CONTIN	.10003+01 .32324+01	.30987+01 .69551-04	.17735+02 .39873-07	.65491+02 .12679+03	.00000 .19811+04	.10216+05 .13210+01	.00000	5

NOTES: (1) Typical printout for a data surface contining a Prandtl-Meyer Expansion.
(2) Some points have been omitted for demonstration purposes.

Example Problem 2

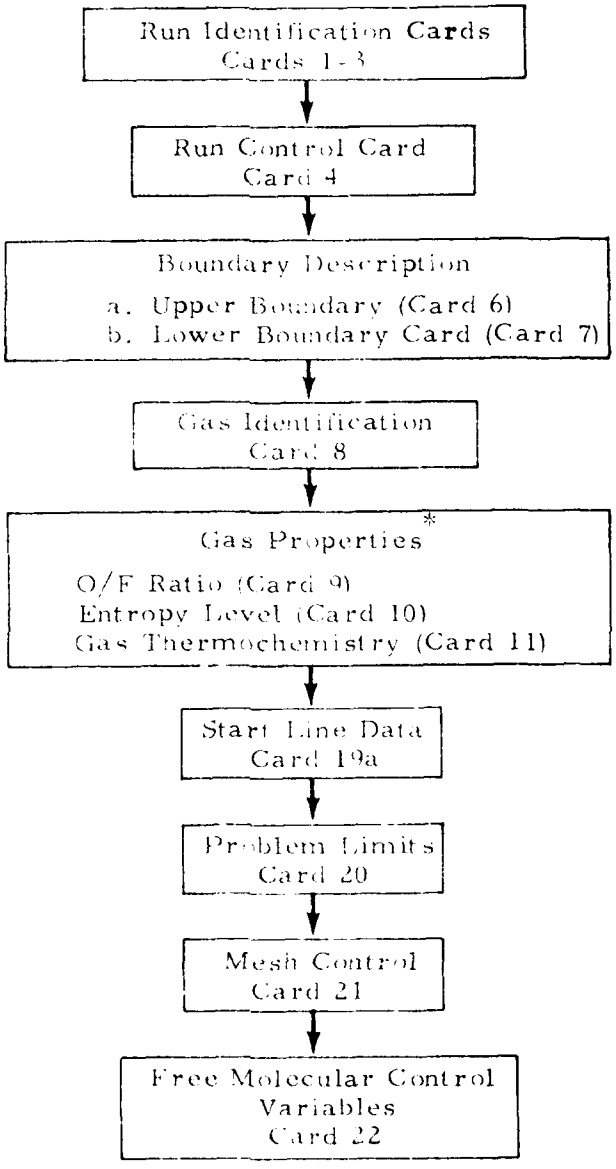
Example problem 2 is a continuation of the flowfield analysis begun in example problem 1 and is subject to the following stipulations:

1. The analysis is to begin at the nozzle exit plane and is to utilize the startline generated by example problem 1.
2. Free molecular calculations are to be considered, and
3. The gas properties are to be read from cards.

Table 3-9 presents first a flow chart and then a listing of the input data for the specified problem. Table 3-9a presents a listing of the pertinent solution.

Table 3-9

REQUIRED INPUT FORMAT FOR EXAMPLE PROBLEM 2



*If gas properties are input on tape (ICON(1)=2) Cards 9, 10 and 11 are not required.

Table 3-9 - (Concluded)

Cards 1-3	GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED											
Card 4	1	2	21	2	1	1	2	99	1	11	1	00100
Cards 6	2	1					•2679491	•1695936	015•99828			
	3		•0020							1000•		
Card 7	2									1000•		
Card 8	IDEAL GAS					ENG	1	1				
Card 9	•0											
Card 10	•0			10								
Cards 11	•0	24•334	1•1798	5466•4	122•46							
	1•0	24•940	1•1911	5025•0	69•321							
	1•746	25•055	1•2121	4239•0	24•496							
	2•151	25•080	1•2224	3747•6	12•248							
	2•536	25•089	1•2297	3299•4	6•1241							
	2•916	25•091	1•2344	2896•2	3•0621							
	3•424	25•091	1•2376	2430•0	1•2248							
	4•057	25•091	1•2731	1951•4	•4083							
	4•364	25•091	1•2819	1729•8	•2450							
	4•790	25•091	1•2944	1481•4	•1225							
Cards 19a	•0000000	•3242355+01	•4255566+01	•0000000	•0000000	•0000000						
	•5197684-01	•3231972+01	•4254140+01	•6249443+00	•0000000	•0000000						
	•1039527+00	•3230899+01	•4253355+01	•1650315+01	•0000000	•0000000						
	•1558485+00	•3229000+01	•4252466+01	•2472640+01	•0000000	•0000000						
	•2077969+00	•3226359+01	•4251346+01	•3290727+01	•0000000	•0000000						
	•2595539+00	•3223043+01	•4249891+01	•4103093+01	•0000000	•0000000						
	•3112162+00	•3219073+01	•4247967+01	•4907012+01	•0000000	•0000000						
	•3627149+00	•3214193+01	•4245415+01	•5699432+01	•0000000	•0000000						
	•4140085+00	•3208722+01	•4242050+01	•6476959+01	•0000000	•0000000						
	•4650489+00	•3202555+01	•4237622+01	•7234456+01	•0000000	•0000000						
	•5157675+00	•3195820+01	•4231737+01	•7964593+01	•0000000	•0000000						
	•5660755+00	•3188471+01	•4223951+01	•8656559+01	•0000000	•0000000						
	•6158719+00	•3180593+01	•4214127+01	•9312545+01	•0000000	•0000000						
	•6650321+00	•3172253+01	•4203152+01	•9939677+01	•0000000	•0000000						
	•7137183+00	•3163473+01	•4193167+01	•1057622+02	•0000000	•0000000						
	•7618934+00	•3154155+01	•4185607+01	•1125196+02	•0000000	•0000000						
	•8097543+00	•3144333+01	•4181166+01	•1196577+02	•0000000	•0000000						
	•8574128+00	•3133937+01	•4178534+01	•1270352+02	•0000000	•0000000						
	•9049370+00	•3123349+01	•4177059+01	•1346748+02	•0000000	•0000000						
	•9524523+00	•3111144+01	•4176303+01	•1423154+02	•0000000	•0000000						
	•1000000+01	•3098743+01	•4175701+01	•1500000+02	•0000000	•0000000						
Card 20	100•	-100•	0•0	0•0	20•	90•						
Card 21	•0	1•	1•	•005	1•	•1						
Card 22	1000•0	50•	20•	1•0	0•02-04•7							

Table 3-9a

EXAMPLE PROBLEM 2 PERTINENT SOLUTION

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 1

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

RUN CONTROL PARAMETERS

ICON(1)	ICON(2)	ICON(3)	ICON(4)	ICON(5)	ICON(6)	ICON(7)	ICON(8)
1	2	21	2	1	0	1	2

ICON(9)	ICON(10)	ICON(11)	ICON(12)	ICON(13)	ICON(14)	ICON(15)	ICON(16)
0	99	1	1	1	0	0	100

FLOW CALCULATIONS ARE IN ENGLISH UNITS WITH THE R,X COORDINATES IN FEET

THE FLOW FIELD DATA WILL NOT WRITTEN ON TAPE

UPPER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
2	1	.00000	.00000	.00000	.26795+00	.16969+00	.30969+01
3	0	.20000-02	.00000	.00000	.00000	.00000	.10000+04

LOWER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
2	0	.00000	.00000	.00000	.00000	.00000	.10000+04

THERE ARE 0 PARTICLE SPECIES PRESENT IN THE GAS-PARTICLE MIXTURE

THE FOLLOWING GAS PROPERTIES IN ENGLISH UNITS ARE FOR IDEAL GAS
REAL GAS PROPERTIES

O/F
.00000

S	V	R	GAMMA	T	P	PR	VIS	CP
.00000								
	.00000	.30016+04	.11798+01	.54684+04	.18000+04	.00000	.00000	.00000
	.34536+04	.19925+04	.11911+01	.50256+04	.10187+04	.00000	.00000	.00000
	.55746+04	.19840+04	.12121+01	.42390+04	.35999+03	.00000	.00000	.00000
	.64815+04	.19820+04	.12224+01	.37476+04	.18000+03	.00000	.00000	.00000
	.71902+04	.19813+04	.12297+01	.32994+04	.90000+02	.00000	.00000	.00000
	.77605+04	.19811+04	.12344+01	.28962+04	.45001+02	.00000	.00000	.00000
	.83577+04	.19811+04	.12376+01	.24300+04	.18000+02	.00000	.00000	.00000
	.89543+04	.19811+04	.12731+01	.19314+04	.60004+01	.00000	.00000	.00000
	.91468+04	.19811+04	.12819+01	.17290+04	.36005+01	.00000	.00000	.00000

Table 3-9a (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 2

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

REAL GAS PROPERTIES

H=TOTAL

S	V	R	GAMMA	T	P	PR	VIS	[illegible]
.00000	.93361+04	.19811+04	.12944+01	.14814+04	.18003+01	.00000	.00000	[illegible]

STARTING LINE INFO

R	V	M	THETA	S	MACH ANGLE	SHOCK ANGLE	O/F
.00000	.32324+01	.42555+01	.00000	.00000	.13591+02	.00000	.00000
.51977-01	.32320+01	.42541+01	.82494+00	.00000	.13595+02	.00000	.00000
.10396+00	.32309+01	.42533+01	.16503+01	.00000	.13598+02	.00000	.00000
.15590+00	.32290+01	.42524+01	.24726+01	.00000	.13601+02	.00000	.00000
.20777+00	.32264+01	.42513+01	.32907+01	.00000	.13605+02	.00000	.00000
.25955+00	.32230+01	.42498+01	.41031+01	.00000	.13609+02	.00000	.00000
.31122+00	.32190+01	.42479+01	.49070+01	.00000	.13616+02	.00000	.00000
.36271+00	.32142+01	.42454+01	.56994+01	.00000	.13624+02	.00000	.00000
.41401+00	.32087+01	.42420+01	.64770+01	.00000	.13635+02	.00000	.00000
.46505+00	.32026+01	.42376+01	.72345+01	.00000	.13649+02	.00000	.00000
.51577+00	.31958+01	.42317+01	.79646+01	.00000	.13649+02	.00000	.00000
.56608+00	.31885+01	.42239+01	.86586+01	.00000	.13695+02	.00000	.00000
.61587+00	.31806+01	.42141+01	.93123+01	.00000	.13727+02	.00000	.00000
.66508+00	.31723+01	.42031+01	.99397+01	.00000	.13764+02	.00000	.00000
.71372+00	.31635+01	.41931+01	.10576+02	.00000	.13797+02	.00000	.00000
.76189+00	.31542+01	.41858+01	.11251+02	.00000	.13822+02	.00000	.00000
.80975+00	.31443+01	.41812+01	.11967+02	.00000	.13837+02	.00000	.00000
.85742+00	.31339+01	.41785+01	.12710+02	.00000	.13846+02	.00000	.00000
.90499+00	.31228+01	.41770+01	.13467+02	.00000	.13851+02	.00000	.00000
.95246+00	.31111+01	.41763+01	.14232+02	.00000	.13854+02	.00000	.00000
.10000+01	.30987+01	.41757+01	.15000+02	.00000	.13853+02	.00000	.00000

RUN CUTOFF INFORMATION

UPPER BOUNDARY				LOWER BOUNDARY			
R= .10000+03	X= -.10000+03	THETA= .00000		R= .00000	X= .20000+02	THETA= .90000+02	

VIBNO	ROTNO	TRANNO	CHARL	GAMV	GAMR
.10000+03	.50000+02	.20000+02	.10000+01	.00000	.00000

THE MESH CONSTRUCTION WILL BE CONTROLED BY THE FOLLOWING VARIABLES

DL INTERIOR= .300+01 DX AXIS= .100+01 DL LIM= .100+01 DL DELETE= .500-02 DEG P.M.= .500+01 F= .500+00

Table 3-9a (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 8

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

LINE	POINT	DSCRIP	REGIME	R MACH ANGLE	X PRESSURE	M DENSITY	THETA TEMPERATURE	ENTROPY GAS CONST.	VELOCITY LOCAL GAMMA	SHOCK ANGLE	ITS
1	14	INPUT	CONTIN	.66508+00 .13764+02	.31723+01 .46950+01	.42031+01 .18630-03	.99397+01 .18318+04	.00000 .19811+04	.90499+04 .12775+01	.00000	0
1	15	INPUT	CONTIN	.71372+00 .13797+02	.31435+01 .47737+01	.41931+01 .18874-03	.10576+02 .18384+04	.00000 .19811+04	.90435+04 .12772+01	.00000	0
1	16	INPUT	CONTIN	.76189+00 .13822+02	.31642+01 .48327+01	.41658+01 .19057-03	.11251+02 .18433+04	.00000 .19811+04	.90387+04 .12770+01	.00000	0
1	17	INPUT	CONTIN	.80975+00 .13837+02	.31443+01 .48701+01	.41812+01 .19172-03	.11967+02 .18463+04	.00000 .19811+04	.90360+04 .12768+01	.00000	0
1	18	INPUT	CONTIN	.85742+00 .13846+02	.31339+01 .48917+01	.41785+01 .19239-03	.12710+02 .18481+04	.00000 .19811+04	.90343+04 .12768+01	.00000	0
1	19	INPUT	CONTIN	.90499+00 .13851+02	.31228+01 .49038+01	.41770+01 .19276-03	.13467+02 .18491+04	.00000 .19811+04	.90334+04 .12767+01	.00000	0
1	20	INPUT	CONTIN	.95246+00 .13854+02	.31111+01 .49100+01	.41763+01 .19295-03	.14232+02 .18496+04	.00000 .19811+04	.90329+04 .12767+01	.00000	0
1	21	INPUT	CONTIN	.10000+01 .13856+02	.30989+01 .49144+01	.41757+01 .19309-03	.15000+02 .18499+04	.00000 .19811+04	.90325+04 .12767+01	.00000	0
1	22	PRN-MR	CONTIN	.10000+01 .12812+02	.30989+01 .26978+01	.45096+01 .12542-03	.19869+02 .18388+04	.00000 .19811+04	.92165+04 .12865+01	.00000	0
1	23	PRN-MR	CONTIN	.10000+01 .11747+02	.30989+01 .15166+01	.49119+01 .77372-04	.24750+02 .18247+04	.00000 .19811+04	.93888+04 .12944+01	.00000	0
1	24	PRN-MR	CONTIN	.10000+01 .10807+02	.30989+01 .85363+00	.53333+01 .49631-04	.29624+02 .18502+04	.00000 .19811+04	.95494+04 .12944+01	.00000	0
1	25	PRN-MR	CONTIN	.10000+01 .99026+01	.30989+01 .45765+00	.58148+01 .30661-04	.34499+02 .18849+04	.00000 .19811+04	.96989+04 .12944+01	.00000	0
1	26	PRN-MR	CONTIN	.10000+01 .90295+01	.30989+01 .23197+00	.63717+01 .18139-04	.39374+02 .92955+03	.00000 .19811+04	.98375+04 .12944+01	.00000	0

NOTES: (1) Typical printout for a startline data surface containing a Prandtl-Meyer Expansion.
(2) Some points have been omitted for demonstration purposes.

Table 3-9a (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 12

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

LINE	POINT	DSCRIP	REGIME	R / MACH ANGLE	X / PRESSURE	M / DENSITY	THETA / TEMPERATURE	ENTROPY / GAS CONST.	VELOCITY / LOCAL GAMMA	SHOCK ANGLE	ITR
2	27	INTER	CONTIN	.10613+01	.31427+01	.71067+01	.44254+02	.00000	.19788+04	.00000	4
				.86889+01	.10068+00	.95186-05	.76883+03	.19811+04	.12944+01		
2	28	INTER	CONTIN	.10686+01	.31756+01	.79085+01	.49073+02	.00000	.10095+05	.00000	4
				.72641+01	.43639-01	.49804-05	.63535+03	.19811+04	.12944+01		
2	29	INTER	CONTIN	.10753+01	.31680+01	.88839+01	.53898+02	.00000	.10199+05	.00000	4
				.64628+01	.17134-01	.24233-05	.51393+03	.19811+04	.12944+01		
2	30	INTER	CONTIN	.10812+01	.31599+01	.10100+02	.58729+02	.00000	.10292+05	.00000	4
				.56815+01	.60027-02	.10777-05	.40486+03	.19811+04	.12944+01		
2	31	INTER	CONTIN	.10864+01	.31515+01	.11665+02	.63566+02	.00000	.10373+05	.00000	4
				.49174+01	.18136-02	.42748-06	.30837+03	.19811+04	.12944+01		
2	32	INTER	CONTIN	.10908+01	.31427+01	.13757+02	.68408+02	.00000	.10443+05	.00000	5
				.41677+01	.45095-03	.14587-06	.22470+03	.19811+04	.12944+01		
2	33	INTER	CONTIN	.10946+01	.31336+01	.16708+02	.73254+02	.00000	.10502+05	.00000	5
				.34302+01	.85775-04	.40470-07	.15406+03	.19811+04	.12944+01		
2	34	INTER	CONTIN	.10976+01	.31244+01	.21190+02	.78110+02	.00000	.10549+05	.00000	6
				.27032+01	.11044-04	.83055-08	.96649+02	.19811+04	.12944+01		
2	35	FREERD	CONTIN	.10987+01	.31201+01	.20633+02	.77877+02	.00000	.10545+05	.00000	4
				.27780+01	.13907-04	.99245-08	.10185+03	.19811+04	.12944+01		

POINT NO. 34 ON LINE 2 HAS BEEN DELETED

PERCENT CHANGE IN MASS, MOMENTUM AND ENERGY NUMERICAL INTEGRATION FOR LINE 2 RELATIVE TO THE START LINE

THE PERCENT CHANGE IN MASS FLOW IS = -.22084+00

PERCENT CHANGE IN MOMENTUM IS = .18840+04 ISP = -.19527+01

PERCENT CHANGE IN ENERGY IS = .00000

NOTES: (1) Typical printout for a data surface in the exhaust plume.
(2) Some points have been omitted for demonstration purposes.

Table 3-9a (Concluded)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 23

GASEOUS CHECK CASE WITH FREE MOLECULAR CALCULATIONS CONSIDERED

LINE	POINT	DSCRIP	REGIME	R MACH ANGLE	X PRESSURE	M DENSITY	THETA TEMPERATURE	ENTROPY GAS CONST.	VELOCITY LOCAL GAMMA	SHOCK ANGLE	ITR
6	29	INTER	CONTIN	.11712+01 .57651+01	.32324+01 .67428-02	.99553+01 .11817-05	.57858+02 .41599+03	.00000 .19811+04	.10282+05 .12944+01	.00000	5
6	30	INTER	CONTIN	.11908+01 .59786+01	.32158+01 .23711-02	.11297+02 .52584-06	.62206+02 .32776+03	.00000 .19811+04	.10357+05 .12944+01	.00000	5
6	31	INTER	CONTIN	.11890+01 .43983+01	.31987+01 .71057-03	.13038+02 .20727-06	.66612+02 .24919+03	.00000 .19811+04	.10523+05 .12944+01	.00000	4
6	32	INTER	FREE M	.11956+01 .45607+01	.31824+01 .21450-03	.12576+02 .75186-07	.69344+02 .20930+03	.00000 .19811+04	.10456+05 .16670+01	.00000	1
6	33	INTER	FREE M	.12013+01 .39782+01	.31456+01 .43479-04	.14785+02 .20778-07	.73346+02 .15280+03	.00000 .19811+04	.10503+05 .16670+01	.00000	1
6	34	INTER	FREE M	.12073+01 .31529+01	.31415+01 .72497-05	.18182+02 .51737-08	.78371+02 .10185+03	.00000 .19811+04	.10545+05 .16670+01	.00000	1

PERCENT CHANGE IN MASS, MOMENTUM AND ENERGY NUMERICAL INTEGRATION FOR LINE 6 RELATIVE TO THE START LINE

THE PERCENT CHANGE IN MASS FLOW IS = -.16398+01

PERCENT CHANGE IN MOMENTUM IS = .18485+04 ISP = -.23162+01

PERCENT CHANGE IN ENERGY IS = .00000

NOTES: (1) Typical data surface containing points in the free molecular regime.
(2) Some points have been omitted for demonstration purposes.

Example Problem 3

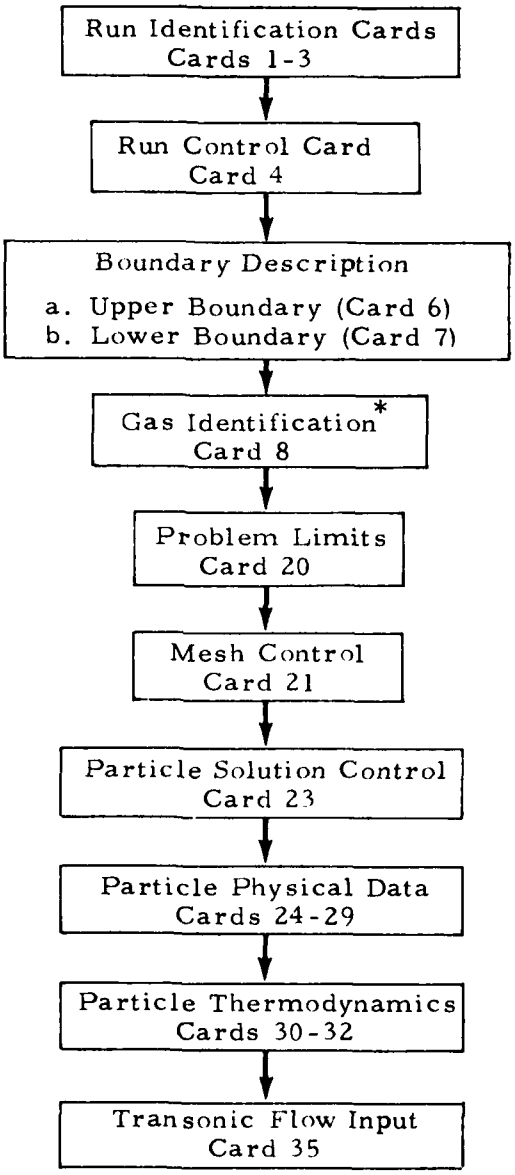
This problem analyzes a two-phase chemical equilibrium flow field with the following stipulations:

1. Free molecular flow calculations are not to be considered.
2. The gas properties are to be read directly from a data tape mounted on FORTRAN unit 10.
3. The start line is to be calculated internal to the program.

Table 3-10 presents first a flow chart and then a listing of the input data for the specified problem. Table 3-11 presents a listing of the pertinent solution. Table 3-12 presents a listing of the input data required for creation of the thermodynamic gaseous properties data tape using the modified TRAN72 computer program (see Section 2 for details).

Table 3-10

REQUIRED INPUT FORMAT FOR EXAMPLE PROBLEM 3



*The gas properties are input on tape. Therefore, Cards 9, 10 and 11 are not required.

Table 3-10 (Concluded)

```
Cards 1-3   SPACE SHUTTLE SEP MOTOR NOZZLE

Card 4        2        25     3    1          1     2    6    25    1    1                11510
Cards 6   1   0      -1.0      .15340277 0.0        -1.0       -.52224999.14672105
          1   1       1.0      5.1560945 2.1824232 -1.0       -2.1796085.74059416
          3   0      4.529                                                1000.      .13058333
Card 7    2   0                                                           1000.
Card 8    SEP PROP PC=1800              MKS        4    2
Card 20   1000.     -1000.     0.0       0.0       100.      90.
Card 21   .03       .02        .15       .001      6.        .65
Card 23                                 1
Card 24   .03805
Card 25   .1        .2         .2        .2        .2        .1
Card 26   1.1       1.7        2.5       3.2       4.5       6.5
Card 27   250.      250.       250.      250.      250.      250.
Card 28
Card 29
Card 30   AL203 EQ. OF STATE          1ENG
Card 31     1
Card 32   4188.5    1358.89    1658.72688.340016    .32443
Cards 35  $DATA THID=30.,THFD=7.,THJD=10.,THIW=16.,RRT=3.,CAPN=.75
          $END
```

Table 3-11

EXAMPLE PROBLEM 3 PERTINENT SOLUTION

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

GAS-PARTICLE FLOW SOLUTION

CASE NO. 1 PAGE 1

SPACE SHUTTLE SEP MOTOR NOZZLE

RUN CONTROL PARAMETERS

ICON(1)	ICON(2)	ICON(3)	ICON(4)	ICON(5)	ICON(6)	ICON(7)	ICON(8)
2	0	25	3	1	0	1	2

ICON(9)	ICON(10)	ICON(11)	ICON(12)	ICON(13)	ICON(14)	ICON(15)	ICON(16)
0	25	1	1	0	0	0	11510

FLOW CALCULATIONS ARE IN ENGLISH UNITS WITH THE R,X COORDINATES IN FEET

THE FLOW FIELD DATA WILL BE WRITTEN ON TAPE

UPPER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
1	0	-.10000+01	.15340+00	.00000	-.10000+01	-.52225+00	.14672+00
1	1	.10000+01	.51561+01	.21824+01	-.10000+01	-.21796+01	.74059+00
3	0	.46290+01	.00000	.00000	.00000	.00000	.10000+04

LOWER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
2	0	.00000	.00000	.00000	.00000	.00000	.10000+04

CHAMBER ENTHALPY = -.19619+08

THERE ARE 6 PARTICLE SPECIES PRESENT IN THE GAS-PARTICLE MIXTURE

THE FOLLOWING GAS PROPERTIES IN ENGLISH UNITS ARE FOR SEP PROP PC=1800

REAL GAS PROPERTIES

H-TOTAL
-.20631+06

S	V	R	GAMMA	T	P	PR	VIS	CP
-.17515+08								
	.00000	.19864+04	.12039+01	.40098+04	.18000+04	.57034+00	.17610-05	.12302+05
	.32374+04	.19835+04	.12134+01	.34603+04	.10111+04	.58520+00	.16373-05	.11552+05
	.51771+04	.19815+04	.12260+01	.36728+04	.36000+03	.60100+00	.14258-05	.10805+05
	.49117+04	.19812+04	.12316+01	.31604+04	.18000+03	.50332+00	.12734-05	.10554+05
	.66587+04	.19811+04	.12355+01	.27927+04	.90000+02	.60147+00	.11702-05	.10404+05
	.71778+04	.19811+04	.12374+01	.24957+04	.45000+02	.59727+00	.10564-05	.10327+05
	.77242+04	.19811+04	.12372+01	.20511+04	.18000+02	.58936+00	.92142-06	.10343+05
	.82731+04	.19811+04	.12352+01	.16175+04	.60000+01	.54769+00	.76436-06	.89326+04

Table 3-11 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 1

SPACE SHUTTLE SRB MOTOR NOZZLE

REAL GAS PROPERTIES

H-TOTAL

S	V	R	GAMMA	T	P	PR	VIS	CP
-.17515+04								
	.84091+04	.19811+04	.12942+01	.14823+04	.36000+01	.58760+00	.69560-06	.87203+04
	.86241+04	.19811+04	.13062+01	.12269+04	.18000+01	.58384+00	.60805-06	.80557+04
	.88932+04	.19811+04	.13317+01	.83245+03	.36000+00	.58277+00	.42702-06	.77535+04
	.91091+04	.19811+04	.13413+01	.69912+03	.18000+00	.58035+00	.36311-06	.77907+04
	.93072+04	.19811+04	.13600+01	.46019+03	.36000-01	.57207+00	.23580-06	.74839+04
.44545+04								
	.00000	.19995+04	.11754+01	.44839+04	.80000+02	.60737+00	.17256-05	.15844+05
	.31969+04	.19905+04	.11920+01	.43074+04	.45254+02	.53093+00	.16219-05	.13464+05
	.51556+04	.19931+04	.12182+01	.36197+04	.16000+02	.58140+00	.14247-05	.11313+05
	.59941+04	.19816+04	.12286+01	.31911+04	.80000+01	.59755+00	.12954-05	.10726+05
	.66845+04	.19812+04	.12342+01	.28012+04	.40000+01	.60024+00	.11729-05	.10443+05
	.71663+04	.19811+04	.12374+01	.24537+04	.20000+01	.59719+00	.10591-05	.10334+05
	.77152+04	.19811+04	.12372+01	.21579+04	.80000+00	.58942+00	.92375-06	.10382+05
	.82163+04	.19811+04	.12850+01	.16730+04	.26667+00	.58794+00	.76558-06	.87381+04
	.84031+04	.19811+04	.12940+01	.14472+04	.16000+00	.58792+00	.69760-06	.87236+04
	.86169+04	.19811+04	.13060+01	.12333+04	.80000-01	.58718+00	.60789-06	.84608+04
	.88396+04	.19811+04	.13316+01	.83555+03	.16000-01	.58320+00	.43049-06	.79616+04
	.91160+04	.19811+04	.13412+01	.70177+03	.80000-02	.58041+00	.36443-06	.77938+04
	.93050+04	.19811+04	.13599+01	.46197+03	.16000-02	.57264+00	.23686-06	.74911+04

REAL GAS PROPERTIES

H-TOTAL
-.24125+08

S	V	R	GAMMA	T	P	PR	VIS	CP
-.24769+03								
	.00000	.19923+04	.11919+01	.51581+04	.18000+04	.55000+00	.18540-05	.13625+05
	.33540+04	.19867+04	.12032+01	.47059+04	.10145+04	.56677+00	.17326-05	.12372+05
	.53837+04	.19823+04	.12201+01	.39342+04	.36000+03	.59339+00	.15166-05	.11133+05
	.62562+04	.19814+04	.12277+01	.34663+04	.18000+03	.60145+00	.13793-05	.10729+05
	.69335+04	.19812+04	.12330+01	.30450+04	.90000+02	.60279+00	.12501-05	.10499+05
	.74773+04	.19811+04	.12364+01	.26620+04	.45000+02	.60017+00	.11302-05	.10370+05
	.80296+04	.19811+04	.12378+01	.22387+04	.18000+02	.59362+00	.98632-06	.10319+05
	.85730+04	.19811+04	.12791+01	.17727+04	.60000+01	.59495+00	.82327-06	.90064+04
	.87667+04	.19811+04	.12980+01	.15035+04	.36000+01	.59551+00	.75144-06	.88648+04
	.89953+04	.19811+04	.13004+01	.13527+04	.18000+01	.59562+00	.65929-06	.85628+04
	.93357+04	.19811+04	.13769+01	.92886+03	.36000+00	.59360+00	.47031-06	.80459+04
	.95007+04	.19811+04	.13762+01	.77973+03	.18000+00	.59212+00	.40013-06	.78660+04

Table 3-11 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 1

SPACE SHUTTLE SEP MOTOR NOZZLE

REAL GAS PROPERTIES

H-TOTAL

S	V	R	GAMMA	T	P	PR	VIS	CP
.53902+04								
	.00000	.20140+04	.11587+01	.49404+04	.80000+02	.48389+00	.17940-05	.19517+05
	.32826+04	.20006+04	.11725+01	.45737+04	.45564+02	.49723+00	.17007-05	.16272+05
	.53412+04	.19862+04	.12045+01	.39195+04	.16000+02	.55086+00	.15120-05	.12284+05
	.62212+04	.19828+04	.12205+01	.34762+04	.80000+01	.58410+00	.13820-05	.11186+05
	.68048+04	.19815+04	.12303+01	.30619+04	.40000+01	.59828+00	.12552-05	.10648+05
	.76538+04	.19812+04	.12357+01	.26855+04	.20000+01	.59945+00	.11355-05	.10402+05
	.80311+04	.19811+04	.12378+01	.22530+04	.80000+00	.59379+00	.99120-06	.10320+05
	.85592+04	.19811+04	.12386+01	.17044+04	.28667+00	.57542+00	.82766-06	.90220+04
	.87565+04	.19811+04	.12876+01	.15943+04	.14000+00	.59602+00	.75563-06	.88758+04
	.89449+04	.19811+04	.12992+01	.13621+04	.80000-01	.59619+00	.66313-06	.85926+04
	.93745+04	.19811+04	.13266+01	.92762+03	.18000-01	.59440+00	.47343-06	.80527+04
	.96025+04	.19811+04	.13366+01	.70054+03	.80000-02	.59291+00	.40294-06	.78718+04
	.97148+04	.19811+04	.13560+01	.51575+03	.16000-02	.58770+00	.26576-06	.75514+04

REAL GAS PROPERTIES

H-TOTAL
-.21872+04

S	V	R	GAMMA	T	P	PR	VIS	CP
-.41765+03								
	.00000	.19965+04	.11858+01	.53183+04	.18000+04	.54000+00	.18960-05	.19407+05
	.34054+04	.19892+04	.11973+01	.48497+04	.10166+04	.55602+00	.17769-05	.12938+05
	.54608+04	.19830+04	.12164+01	.40875+04	.36000+03	.58723+00	.15604-05	.11371+05
	.63721+04	.19814+04	.12253+01	.36073+04	.18000+03	.59900+00	.14214-05	.10552+05
	.70643+04	.19812+04	.12315+01	.31120+04	.90000+02	.60269+00	.12596-05	.10569+05
	.76204+04	.19812+04	.12356+01	.27819+04	.45000+02	.60123+00	.11667-05	.10403+05
	.82652+04	.19811+04	.12378+01	.23041+04	.18000+02	.59537+00	.10188-05	.10318+05
	.87414+04	.19811+04	.12760+01	.18517+04	.60000+01	.59771+00	.85239-06	.91645+04
	.89120+04	.19811+04	.12850+01	.16557+04	.36000+01	.59875+00	.77938-06	.89389+04
	.91794+04	.19811+04	.12979+01	.14161+04	.18000+01	.59925+00	.68599-06	.86471+04
	.93754+04	.19811+04	.13245+01	.96651+03	.36000+00	.59827+00	.49172-06	.80917+04
	.95622+04	.19811+04	.13347+01	.81287+03	.18000+00	.59714+00	.41696-06	.79048+04
	.96192+04	.19811+04	.13544+01	.53757+03	.36000-01	.59299+00	.27283-06	.78755+04
.58411+04								
	.00000	.20241+04	.11523+01	.50503+04	.80000+02	.47482+00	.18225-05	.21634+05
	.33730+04	.20076+04	.11637+01	.47181+04	.45709+02	.48755+00	.17343-05	.18050+05
	.58268+04	.19981+04	.11957+01	.40413+04	.16000+02	.53284+00	.15524-05	.13086+05
	.63253+04	.19838+04	.12149+01	.36163+04	.80000+01	.57163+00	.14238-05	.11537+05

Table 3-11 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

GAS-PARTICLE FLOW SOLUTION

CASE NO. 1 PAGE 4

SPACE SHUTTLE SEP MOTOR NOZZLE

REAL GAS PROPERTIES

H-TOTAL

S	V	R	GAMMA	T	P	PR	VIS	CP
.58411+04								
	.70757+04	.19810+04	.12271+01	.31728+04	.40000+01	.59459+00	.12959-05	.10816+05
	.76887+04	.19813+04	.12342+01	.28941+04	.20000+01	.59963+00	.11738-05	.10967+05
	.81310+04	.19811+04	.12377+01	.23536+04	.80000+00	.59558+00	.10254-05	.10324+05
	.87227+04	.19811+04	.12754+01	.18580+04	.26667+00	.59820+00	.85829-06	.91805+04
	.89755+04	.19811+04	.12844+01	.16706+04	.16000+00	.59936+00	.78508-06	.89541+04
	.91405+04	.19811+04	.12968+01	.14792+04	.80000-01	.59994+00	.69025-06	.86628+04
	.95663+04	.19811+04	.13240+01	.97594+03	.16000-01	.59915+00	.49550-06	.81012+04
	.96939+04	.19811+04	.13343+01	.82199+03	.80000-02	.59810+00	.42243-06	.79129+04
	.99133+04	.19811+04	.13541+01	.54815+03	.16000-02	.59420+00	.28031-06	.75812+04

REAL GAS PROPERTIES

H-TOTAL
-.19619+03

S	V	R	GAMMA	T	P	PR	VIS	CP
.00000								
	.00000	.20017+04	.11798+01	.54986+04	.18000+04	.53040+00	.19346-05	.15475+05
	.34537+04	.19925+04	.11911+01	.50261+04	.10187+04	.54593+00	.18188-05	.13715+05
	.55738+04	.19840+04	.12121+01	.42383+04	.36000+03	.57942+00	.16030-05	.11671+05
	.68835+04	.19820+04	.12224+01	.37483+04	.18000+03	.59535+00	.14627-05	.11008+05
	.71907+04	.19813+04	.12297+01	.32794+04	.90000+02	.60190+00	.13287-05	.10643+05
	.77591+04	.19812+04	.12344+01	.28956+04	.45000+02	.60196+00	.12030-05	.10444+05
	.83575+04	.19811+04	.12376+01	.24304+04	.18000+02	.59704+00	.10513-05	.10327+05
	.89567+04	.19811+04	.12731+01	.19319+04	.60000+01	.60000+00	.88132-06	.92428+04
	.91111+04	.19811+04	.12819+01	.17290+04	.36000+01	.60159+00	.80732-06	.90137+04
	.93925+04	.19811+04	.12944+01	.14307+04	.18000+01	.60246+00	.71099-06	.87172+04
	.97516+04	.19811+04	.13220+01	.10132+04	.36000+00	.60235+00	.51232-06	.81391+04
	.99918+04	.19811+04	.13325+01	.85401+03	.18000+00	.60163+00	.43803-06	.79457+04
	.10115+05	.19811+04	.13527+01	.56614+03	.36000-01	.59865+00	.29237-06	.76037+04
.62828+04								
	.00000	.20345+04	.11470+01	.51490+04	.80000+02	.46664+00	.18478-05	.23857+05
	.33550+04	.20157+04	.11560+01	.48304+04	.45836+02	.47734+00	.17643-05	.20071+05
	.55345+04	.19924+04	.11861+01	.41947+04	.16000+02	.51537+00	.15901-05	.14185+05
	.61232+04	.19853+04	.12089+01	.37551+04	.80000+01	.55559+00	.14643-05	.12023+05
	.71805+04	.19824+04	.12232+01	.33745+04	.40000+01	.58776+00	.13362-05	.11038+05
	.77177+04	.19814+04	.12322+01	.29745+04	.20000+01	.59886+00	.12122-05	.10565+05
	.83752+04	.19812+04	.12373+01	.24564+04	.80000+00	.59708+00	.10600-05	.10337+05
	.90812+04	.19812+04	.12723+01	.19535+04	.26667+00	.60056+00	.88905-06	.92636+04
	.93895+04	.19812+04	.12811+01	.17589+04	.16000+00	.60278+00	.81480-06	.90332+04

Table 3-11 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

GAS-PARTICLE FLOW SOLUTION

CASE NO. 1 PAGE 5

SPACE SHUTTLE SRB MOTOR NOZZLE

REAL GAS PROPERTIES

H-TOTAL

S	V	R	GAMMA	T	P	PR	VIS	CP
.62920+04								
	.93312+04	.19812+04	.12936+01	.14901+04	.80000-01	.60325+00	.71786-06	.87357+04
	.97449+04	.19812+04	.13213+01	.10259+04	.16000-01	.50336+00	.51501-06	.81521+04
	.98039+04	.19812+04	.13319+01	.86491+03	.80000-02	.60275+00	.44317-06	.79557+04
	.10108+05	.19812+04	.13522+01	.57364+03	.16000-02	.60006+00	.29629-06	.74113+04

RUN CUTOFF INFORMATION

UPPER BOUNDARY						LOWER BOUNDARY			
R=	.10000+04	X=	-.10000+04	THETA=	.00000	R=	.00000	X=	.10000+03	THETA=	.90000+02

PARTICLE PHYSICAL DATA

SPECIE	RADIUS	MASS DENSITY	EMISSIVITY	ACCM. COEFF.
1	.11000+01	.25000+03	.00000	.00000
2	.17000+01	.25000+03	.00000	.00000
3	.25000+01	.25000+03	.00000	.00000
4	.32000+01	.25000+03	.00000	.00000
5	.45000+01	.25000+03	.00000	.00000
6	.65000+01	.25000+03	.00000	.00000

THE PARTICLES CONSTITUTE 3.91 PERCENT BY WEIGHT FLOW OF THE GAS-PARTICLE MIXTURE

THE INDIVIDUAL PERCENTAGES ARE .10 .20 .20 .20 .20 .10

THE PARTICLE TEMPERATURE-ENTHALPY TABLE WILL BE READ IN WITH ENGLISH UNITS

PARTICLE TEMPERATURE-ENTHALPY TABLE

PHASE CHANGE DATA ••• TMELT= .41885D+04 HSOLID= .34610D+08 HLIQUID= .46520D+08

CPMELT= .85100+04 CPSOLID= .81109+04

Table 3-11 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

GAS-PARTICLE FLOW SOLUTION

CASE NO. 1 PAGE 6

SPACE SHUTTLE SEP MOTOR NOZZLE

PARTICLE DRAG TABLE

I	RE	DRAG COEF
1	.00000	.10000+01
2	.12500+01	.10000+01
3	.12550+01	.10000+01
4	.12600+01	.10010+01
5	.12650+01	.10020+01
6	.15820+01	.10630+01
7	.19950+01	.11410+01
8	.25100+01	.12290+01
9	.31600+01	.13150+01
10	.39800+01	.14120+01
11	.50100+01	.15170+01
12	.63100+01	.16250+01
13	.79500+01	.17450+01
14	.10000+02	.18740+01
15	.12600+02	.20260+01
16	.15820+02	.21860+01
17	.19950+02	.23640+01
18	.25100+02	.25550+01
19	.31600+02	.27600+01
20	.39800+02	.30000+01
21	.50100+02	.32500+01
22	.63100+02	.32520+01
23	.79500+02	.33250+01
24	.10000+03	.41550+01
25	.31600+03	.79000+01
26	.10000+04	.20000+02
27	.10000+04	.25000+02
28	.10000+06	.20000+04

Table 3-11 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

GAS-PARTICLE FLOW SOLUTION

CASE NO. 1

SPACE SHUTTLE SEP MOTOR NOZZLE

GASEOUS STARTING LINE INFO

R	X	M	THETA	S	MACH ANGLE	SHOCK ANGLE	H-TOTAL
.00000	.12847+00	.14166+01	.00000	.57051+02	.44904+02	.00000	-.19706+08
.51304-02	.12843+00	.14169+01	.45764+00	.57068+02	.44891+02	.00000	-.19707+08
.11661-01	.12833+00	.14178+01	.91650+00	.57120+02	.44853+02	.00000	-.19707+08
.17491-01	.12817+00	.14194+01	.13779+01	.57205+02	.44789+02	.00000	-.19707+08
.23321-01	.12794+00	.14217+01	.18428+01	.57325+02	.44700+02	.00000	-.19707+08
.29152-01	.12765+00	.14246+01	.23128+01	.57479+02	.44585+02	.00000	-.19707+08
.35982-01	.12729+00	.14281+01	.27893+01	.57670+02	.44445+02	.00000	-.19708+08
.40813-01	.12686+00	.14323+01	.32737+01	.57895+02	.44279+02	.00000	-.19708+08
.47643-01	.12637+00	.14373+01	.37678+01	.58157+02	.44087+02	.00000	-.19709+08
.52473-01	.12581+00	.14430+01	.42733+01	.58457+02	.43869+02	.00000	-.19709+08
.57304-01	.12519+00	.14499+01	.47920+01	.58795+02	.43624+02	.00000	-.19710+08
.61134-01	.12450+00	.14567+01	.53262+01	.59172+02	.43352+02	.00000	-.19711+08
.65964-01	.12375+00	.14649+01	.58781+01	.59591+02	.43053+02	.00000	-.19712+08
.70795-01	.12293+00	.14738+01	.64501+01	.60052+02	.42726+02	.00000	-.19712+08
.81625-01	.12204+00	.14838+01	.70449+01	.60558+02	.42369+02	.00000	-.19714+08
.87455-01	.12109+00	.14950+01	.76654+01	.61112+02	.41982+02	.00000	-.19715+08
.97286-01	.12008+00	.15073+01	.83145+01	.61715+02	.41564+02	.00000	-.19716+08
.10150+00	.11853+00	.15267+01	.92934+01	.62654+02	.40918+02	.00000	-.19718+08
.10495+00	.11785+00	.15358+01	.97115+01	.63082+02	.40626+02	.00000	-.19719+08
.10816+00	.11719+00	.15447+01	.10127+02	.63498+02	.40343+02	.00000	-.19720+08
.11497+00	.11572+00	.15654+01	.11034+02	.64441+02	.39703+02	.00000	-.19722+08
.12003+00	.11457+00	.15825+01	.11752+02	.65198+02	.39193+02	.00000	-.19724+08
.12732+00	.11284+00	.16100+01	.12949+02	.66371+02	.38398+02	.00000	-.19727+08
.13357+00	.11124+00	.16368+01	.13856+02	.67459+02	.37658+02	.00000	-.19730+08
.13993+00	.10959+00	.16675+01	.14943+02	.68637+02	.36848+02	.00000	-.19733+08
.15576+00	.10798+00	.16993+01	.16003+02	.69773+02	.36048+02	.00000	-.19737+08

PARTICLE START LINE PROPERTIES

POINT	SPECIE	U	V	THETA	ENTHALPY	DENSITY
1	1	.43867+04	.00000	.00000	.50821+08	.41806-04
1	2	.41994+04	.00000	.00000	.51228+08	.94362-04
1	3	.39460+04	.00000	.00000	.51674+08	.11244-03
1	4	.37884+04	.00000	.00000	.52027+08	.12661-03
1	5	.35389+04	.00000	.00000	.52563+08	.15260-03
1	6	.32769+04	.00000	.00000	.53218+08	.93531-04
2	1	.43873+04	.27314+02	.35670+00	.50819+08	.41767-04
2	2	.42000+04	.22202+02	.30288+00	.51229+08	.94817-04
2	3	.39465+04	.16040+02	.23287+00	.51677+08	.11238-03
2	4	.37880+04	.12562+02	.18995+00	.52033+08	.12653-03
2	5	.35383+04	.74549+01	.12068+00	.52573+08	.15248-03
2	6	.32773+04	.25470+01	.44528-01	.53233+08	.93430-04

Table 3-11 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

GAS-PARTICLE FLOW SOLUTION

CASE NO. 1

SPACE SHUTTLE SRB MOTOR NOZZLE

POINT	SPECIE	U	V	THETA	ENTHALPY	DENSITY
3	1	.43891+04	.54725+02	.71435+00	.50815+08	.41730-04
3	2	.42018+04	.44089+02	.60664+00	.51229+08	.94683-04
3	3	.39481+04	.32146+02	.46649+00	.51685+08	.11220-03
3	4	.37905+04	.25174+02	.38053+00	.52048+08	.12630-03
3	5	.35406+04	.14941+02	.24179+00	.52601+08	.15214-03
3	6	.32786+04	.51141+01	.89371-01	.53277+08	.93137-04
4	1	.43921+04	.82332+02	.10739+01	.50908+08	.41637-04
4	2	.42047+04	.66947+02	.91217+00	.51228+08	.94465-04
4	3	.39509+04	.48382+02	.70159+00	.51698+08	.11192-03
4	4	.37930+04	.37890+02	.57233+00	.52071+08	.12575-03
4	5	.35427+04	.22491+02	.36374+00	.52644+08	.15161-03
4	6	.32808+04	.77209+01	.13984+00	.53342+08	.92682-04
5	1	.43963+04	.11024+03	.14364+01	.50797+08	.41510-04
5	2	.42089+04	.89660+02	.12204+01	.51227+08	.94173-04
5	3	.39548+04	.64815+02	.93895+00	.51712+08	.11154-03
5	4	.37966+04	.50758+02	.76596+00	.52098+08	.12548-03
5	5	.35450+04	.30138+02	.48699+00	.52696+08	.15092-03
5	6	.32838+04	.10386+02	.18122+00	.53420+08	.92113-04
6	1	.44019+04	.13854+03	.18029+01	.50782+08	.41354-04
6	2	.42143+04	.11272+03	.15321+01	.51223+08	.93817-04
6	3	.39598+04	.81516+02	.11793+01	.51726+08	.11109-03
6	4	.38011+04	.63827+02	.96200+00	.52126+08	.12495-03
6	5	.35498+04	.37916+02	.61198+00	.52748+08	.15015-03
6	6	.32877+04	.13127+02	.22876+00	.53497+08	.91993-04
7	1	.44088+04	.16740+03	.21744+01	.50763+08	.41171-04
7	2	.42209+04	.13622+03	.18984+01	.51214+08	.93518-04
7	3	.39660+04	.98557+02	.14235+01	.51736+08	.11060-03
7	4	.38067+04	.77147+02	.11610+01	.52149+08	.12439-03
7	5	.35548+04	.45862+02	.73917+00	.52791+08	.14937-03
7	6	.32924+04	.15934+02	.27771+00	.53559+08	.90893-04
8	1	.44171+04	.19862+03	.25523+01	.50738+08	.40968-04
8	2	.42280+04	.16029+03	.21701+01	.51200+08	.92784-04
8	3	.39735+04	.11602+03	.16724+01	.51738+08	.11009-03
8	4	.38132+04	.90765+02	.13635+01	.52160+08	.12382-03
8	5	.35608+04	.54014+02	.86706+00	.52815+08	.14865-03
8	6	.32980+04	.18894+02	.32824+00	.53589+08	.90393-04
9	1	.44269+04	.22718+03	.29376+01	.50708+08	.40748-04
9	2	.42390+04	.18490+03	.24982+01	.51179+08	.92535-04
9	3	.39823+04	.13397+03	.19269+01	.51727+08	.10960-03
9	4	.38207+04	.10473+03	.15702+01	.52155+08	.12332-03
9	5	.35680+04	.62415+02	.10022+01	.52810+08	.14807-03
9	6	.33044+04	.21545+02	.38050+00	.53579+08	.90070-04
10	1	.44283+04	.25740+03	.33320+01	.50670+08	.40515-04
10	2	.42406+04	.21023+03	.28337+01	.51148+08	.92056-04
10	3	.39923+04	.15252+03	.21878+01	.51701+08	.10915-03
10	4	.38291+04	.11709+03	.17819+01	.52128+08	.12292-03
10	5	.35743+04	.71108+02	.11370+01	.52768+08	.14771-03
10	6	.33117+04	.25119+02	.43959+00	.53502+08	.89391-04

Table 3-11 (Continued)

A SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

GAS-PARTICLE FLOW SOLUTION

CASE NO. 1

SPACE SHUTTLE SRB MOTOR NOZZLE

POINT	SPECIE	U	V	THETA	ENTHALPY	DENSITY
11	1	.44514+04	.29073+03	.37368+01	.50624+08	.40275-04
11	2	.42605+04	.23655+03	.31778+01	.51106+08	.91649-04
11	3	.40038+04	.17175+03	.24563+01	.51656+08	.10896-03
11	4	.33386+04	.13391+03	.19960+01	.52073+08	.12766-03
11	5	.35861+04	.50143+02	.12803+01	.52681+08	.14763-03
11	6	.33198+04	.28426+02	.49059+00	.53767+08	.90207+04
12	1	.44661+04	.32934+03	.41537+01	.50569+08	.40030-04
12	2	.42739+04	.26377+03	.35316+01	.51051+08	.91235-04
12	3	.40167+04	.19177+03	.27334+01	.51588+08	.10844-03
12	4	.38491+04	.14925+03	.22205+01	.51988+08	.12755-03
12	5	.35976+04	.89572+02	.14265+01	.52549+08	.14787-03
12	6	.33289+04	.31869+02	.54849+00	.53169+08	.90781-04
13	1	.44827+04	.35944+03	.45844+01	.50505+08	.39750-04
13	2	.42887+04	.29211+03	.38964+01	.50983+08	.90847-04
13	3	.40312+04	.21770+03	.30204+01	.51498+08	.10821-03
13	4	.38606+04	.16518+03	.24499+01	.51873+08	.12262-03
13	5	.36093+04	.99453+02	.15784+01	.52373+08	.14342-03
13	6	.33391+04	.35456+02	.60836+00	.52924+08	.91501-04
14	1	.45011+04	.39623+03	.50307+01	.50430+08	.39525-04
14	2	.43051+04	.32171+03	.42736+01	.50901+08	.90484-04
14	3	.40472+04	.23468+03	.33187+01	.51385+08	.10806-03
14	4	.38734+04	.18160+03	.26873+01	.51731+08	.12784-03
14	5	.36229+04	.10985+03	.17367+01	.52166+08	.14925-03
14	6	.33504+04	.39193+02	.67020+00	.52663+08	.92662-04
15	1	.45214+04	.43494+03	.54946+01	.50345+08	.39263-04
15	2	.43231+04	.35775+03	.46648+01	.50804+08	.90133-04
15	3	.40649+04	.25786+03	.36298+01	.51253+08	.10796-03
15	4	.38875+04	.19925+03	.29340+01	.51568+08	.12319-03
15	5	.36376+04	.12082+03	.19022+01	.51950+08	.15028-03
15	6	.33631+04	.43091+02	.73407+00	.52431+08	.93861-04
16	1	.45437+04	.47581+03	.59782+01	.50250+08	.38987-04
16	2	.43424+04	.38542+03	.50718+01	.50695+08	.89772-04
16	3	.40840+04	.28248+03	.39556+01	.51109+08	.10786-03
16	4	.39031+04	.21768+03	.31921+01	.51401+08	.12359-03
16	5	.36538+04	.13244+03	.20759+01	.51760+08	.15136-03
16	6	.33774+04	.47167+02	.80011+00	.52310+08	.94983-04
17	1	.45678+04	.51911+03	.64835+01	.50144+08	.38687-04
17	2	.43639+04	.41985+03	.54968+01	.50577+08	.89367-04
17	3	.41049+04	.30852+03	.42982+01	.50963+08	.10770-03
17	4	.39205+04	.23732+03	.34640+01	.51249+08	.12394-03
17	5	.36702+04	.14479+03	.22587+01	.51651+08	.15225-03
17	6	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]
18	1	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]
18	4	[illegible]	[illegible]	[illegible]	[illegible]	[illegible]
18	3	.41372+04	.34641+03	.48136+01	.50786+08	.10718-03
18	4	.39486+04	.26763+03	.38774+01	.51126+08	.12405-03
18	5	.36963+04	.16357+03	.25337+01	.51782+08	.15259-03
18	6	.34201+04	.57914+02	.97013+00	.53230+08	.95448-04

Table 3-11 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

GAS-PARTICLE FLOW SOLUTION

CASE NO. 1

SPACE SHUTTLE SEP MOTOR NOZZLE

POINT	SPECIE	U	V	THETA	ENTHALPY	DENSITY
19	1	.46217+04	.61405+03	.75681+01	.49906+08	.37957-04
19	2	.44116+04	.49568+03	.64108+01	.50332+08	.88214-04
19	3	.41517+04	.36642+03	.50437+01	.50739+08	.10679-03
19	4	.39620+04	.28153+03	.40646+01	.51132+08	.12385-03
19	5	.37073+04	.17199+03	.26561+01	.51998+08	.15217-03
20	1	.46378+04	.64238+03	.76859+01	.49836+08	.37709-04
20	2	.44260+04	.51839+03	.66802+01	.50270+08	.87757-04
20	3	.41657+04	.38393+03	.52658+01	.50716+08	.10628-03
20	4	.39753+04	.29525+03	.42476+01	.51185+08	.12345-03
20	5	.37175+04	.18013+03	.27741+01	.52322+08	.15135-03
21	1	.46733+04	.70585+03	.85690+01	.49685+08	.37084-04
21	2	.44584+04	.56765+03	.72813+01	.50160+08	.86472-04
21	3	.41969+04	.42372+03	.57651+01	.50769+08	.10463-03
21	4	.40070+04	.32720+03	.46694+01	.51507+08	.12174-03
22	1	.47009+04	.75631+03	.91398+01	.49574+08	.36507-04
22	2	.44841+04	.61097+03	.77589+01	.50110+08	.85149-04
22	3	.42214+04	.45601+03	.61655+01	.50938+08	.10272-03
23	1	.47417+04	.83396+03	.99750+01	.49425+08	.35956-04
23	2	.45235+04	.67601+03	.84997+01	.50120+08	.82500-04
24	1	.47773+04	.90564+03	.10734+02	.49320+08	.34286-04

THE MESH CONSTRUCTION WILL BE CONTROLED BY THE FOLLOWING VARIABLES

DL INTERIOR= .300-01 DX AXIS= .200-01 DL LIM= .150+00 DL DELETE= .100-02 DEG P.M.= .600+01 F= .650+00

Table 3-11 (Continued)

```
                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                          CASE NO.    1                                                    PAGE    21

     SPACE SHUTTLE SRB MOTOR NOZZLE

LINE POINT  DSCRIP - REGIME        R            X            M            THETA        ENTROPY      VELOCITY     M-TOTAL   ITR
                          MACH ANGLE     PRESSURE     DENSITY     TEMPERATURE   GAS CONST.   LOCAL GAMMA   SHOCK ANGLE

 PARTICLE DATA
  SPECIE POINT  DESCRIPTION        V            THETA            D M            ENTHALPY        DENSITY        TEMPERATURE

   1     24   INPUT  - CONTIN   .13357+00    .11124+00    .16368+01    .13856+02    .67459+02    .52919+04    .19730+08    0
                                .37658+02    .41134+03    .68525-02    .43544+04    .19851+04    .12093+01
 PARTICLE DATA
            24 LIMIT STREAMLINE  .86292+04    .10734+02    .13284+00    .49320+08    .34286-04    .45174+04

   1     25   INPUT  - CONTIN   .13993+00    .10959+00    .16676+01    .14943+02    .68637+02    .53709+04    .19733+08    0
                                .36848+02    .39136+03    .65735-02    .43194+04    .19848+04    .12101+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT

   1     26   INPUT  - CONTIN   .14576+00    .10798+00    .15993+01    .16003+02    .69773+02    .54515+04    .19737+08    0
                                .36049+02    .37152+03    .62942-02    .42831+04    .19845+04    .12109+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT

   GAS MASS FLOW RATE =     .85715+02    PARTICLE MASS FLOW RATE =     .32352+01    MIXTURE MASS FLOW RATE =     .86950+02

                                          PARTICLE PERCENT LOADINGS
                                            RADIUS      LOADING
                                          .11000+01   .99998+01

                                          .17000+01   .20000+02

                                          .25000+01   .20000+02

                                          .32000+01   .20001+02

                                          .45000+01   .20001+02

                                          .65000+01   .99989+01

 PARTICLE PERCENT LOADING RELATIVE TO THE GAS =   .37744+01   PARTICLE PERCENT LOADING RELATIVE TO THE MIXTURE =   .35371+01

                                          MOMENTUM INTEGRATION RESULTS
                                        FORCEX       FORCEY       TORQZ       ISP
                                     -.18212+05    .00000       .00000    .20474+03
                          DELFXG      DELFYG       TORQZG       DELFXP      DELFYP      TORQZP
                        .33778+03    .00000       .00000     .40047+03    .00000      .00000
```

NOTES: (1) Typical printout for the startline data surface.
(2) Some points have been omitted for demonstration purposes.

Table 3-11 (Continued)

```
                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                          CASE NO.    1                                                    PAGE   27

     SPACE SHUTTLE SEP MOTOR NOZZLE

LINE POINT  DSCRIP - REGIME        R              X              M              THETA          ENTROPY        VELOCITY       H-TOTAL    IT
                          MACH ANGLE     PRESSURE       DENSITY       TEMPERATURE    GAS CONST.     LOCAL GAMMA    SHOCK ANGLE

 PARTICLE DATA
  SPECIE POINT  DESCRIPTION        V              THETA          D M            ENTHALPY       DENSITY        TEMPERATURE
   2     23   INTER   - CONTIN   .12853+00     .12060+00     .16501+01     .13627+02     .67676+02     .53263+04     -.19728+08
                                 .37303+02     .40274+03     .67329-02     .43394+04     .19850+04     .12096+01
 PARTICLE DATA
       1    23                   .491253+04    .10722+02     .12820+00     .49070+08     .33699-04     .44480+04
       2    23 LIMIT STREAMLINE  .466776+04    .92340+01     .20403+00     .49791+08     .78835-04     .45723+04

   2     24   INTER   - CONTIN   .13512+00     .11912+00     .16794+01     .14769+02     .67880+02     .54014+04     -.19730+08
                                 .36544+02     .38418+03     .64733-02     .43061+04     .19847+04     .12104+01
 PARTICLE DATA
       1    24 LIMIT STREAMLINE  .496340+04    .11591+02     .13464+00     .48920+08     .32546-08     .44706+04

   2     25   INTER   - CONTIN   .14204+00     .11722+00     .17128+01     .16001+02     .68637+02     .54856+04     -.19732+08
                                 .35722+02     .36379+03     .61855-02     .42680+04     .19843+04     .12112+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

   2     26   WALL    - CONTIN   .14799+00     .11545+00     .17447+01     .17144+02     .69773+02     .55652+04     -.19737+08
                                 .34971+02     .34499+03     .59177-02     .42312+04     .19840+04     .12120+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

                                          PRESSURE INTEGRATION RESULTS
                                 FORCEX         FORCEY         TORQZ          DELFX          DELFY          ISP
                              -.18318+05      .00000         .00000        -.10595+05      .00000        .20593+03

          PERCENT CHANGE IN MASS, MOMENTUM AND ENERGY NUMERICAL INTEGRATION FOR LINE  2 RELATIVE TO THE START LINE
        PERCENT CHANGE IN MASS FLOW, GAS =    -.14895-01    PARTICLE =    -.36259-01    MIXTURE =    -.15672-01
     PERCENT CHANGE IN MOMENTUM, GAS=   .75294+04    PARTICLE =   .87987+00    MIXTURE =   -.12303+01 ISP =   -.12148+01
          PERCENT CHANGE IN ENERGY, GAS =   -.27641-02    PARTICLE =   .98037+00    MIXTURE =   -.62269-02
```

NOTES: (1) Typical printout for a data surface inside the nozzle.
(2) Some points have been omitted for demonstration purposes.

Table 3-11 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 1 PAGE 80

SPACE SHUTTLE SEP MOTOR NOZZLE

LINE	POINT	DSCRIP - REGIME	R / MACH ANGLE	X / PRESSURE	Y / DENSITY	THETA / TEMPERATURE	ENTROPY / GAS CONST.	VELOCITY / LOCAL GAMMA	H-TOTAL / SHOCK ANGLE	ITR
PARTICLE DATA SPECIE	POINT	DESCRIPTION	V	THETA	D M	ENTHALPY		DENSITY	TEMPERATURE	
60	43	PRN-MR - CONTIN	.31517+00	.74059+00	.92592+01	.93440+02	.69773+02	.90967+04	-.19737+00	
			.13592+02	.39810+01	.16253-03	.17803+04	.19811+04	.12798+01		
PARTICLE DATA										
NO PARTICLES ARE PRESENT AT THIS POINT										
60	44	PRN-MR - CONTIN	.31517+00	.74059+00	.96993+01	.99346+02	.69773+02	.92697+04	-.19737+00	2
			.12435+02	.21759+01	.10161-03	.15565+04	.19811+04	.12907+01		
PARTICLE DATA										
NO PARTICLES ARE PRESENT AT THIS POINT										
60	45	PRN-MR - CONTIN	.31517+00	.74059+00	.50997+01	.95253+02	.69773+02	.94877+04	-.19737+00	2
			.11308+02	.11710+01	.61027-04	.13351+04	.19811+04	.13031+01		
PARTICLE DATA										
NO PARTICLES ARE PRESENT AT THIS POINT										
60	46	PRN-MR - CONTIN	.31517+00	.74059+00	.56950+01	.61157+02	.69773+02	.96549+04	-.19737+00	2
			.10704+02	.53735+00	.34801-04	.11223+04	.19811+04	.13157+01		
PARTICLE DATA										
NO PARTICLES ARE PRESENT AT THIS POINT										
60	47	PRN-MR - CONTIN	.31517+00	.74059+00	.63139+01	.67066+02	.69773+02	.96259+04	-.19737+00	2
			.91130+01	.23595+00	.18633-04	.72042+03	.19811+04	.13282+01		
PARTICLE DATA										
NO PARTICLES ARE PRESENT AT THIS POINT										
60	48	PRN-MR - CONTIN	.31517+00	.74059+00	.71804+01	.72773+02	.69773+02	.97795+04	-.19737+00	2
			.80855+01	.92505-01	.92566-05	.72700+03	.19811+04	.13412+01		
PARTICLE DATA										
NO PARTICLES ARE PRESENT AT THIS POINT										
60	49	PRN-MR - CONTIN	.31517+00	.74059+00	.83201+01	.78879+02	.69773+02	.10115+05	-.19737+00	2
			.69031+01	.31929-01	.41921-05	.55151+03	.19811+04	.13527+01		
PARTICLE DATA										
NO PARTICLES ARE PRESENT AT THIS POINT										

NOTES: (1) Typical printout for a data surface containing a Prandtl-Meyer Expansion.
(2) Some points have been omitted for demonstration purposes.

Table 3-11 (Concluded)

```
                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                          CASE NO.    1                                                    PAGE  169

     SPACE SHUTTLE SEP MOTOR NOZZLE

LINE POINT  DSCRIP - REGIME        R            X            M            THETA        ENTROPY      VELOCITY     H-TOTAL    ITR
                              MACH ANGLE   PRESSURE     DENSITY    TEMPERATURE   GAS CONST.   LOCAL GAMMA  SHOCK ANGLE
 PARTICLE DATA
  SPECIE POINT  DESCRIPTION      V            THETA          D M          ENTHALPY       DENSITY        TEMPERATURE
 ---------------------------------------------------------------------------------------------------------------------
 118     1  WALL    - CONTIN   .00000      .16758+01    .32345+01    .00000       .66197+03    .81502+04    -.19654+08    3
                               .18069+02   .18060+02    .50643-03   .25920+04    .19812+04    .12365+01
 PARTICLE DATA
        1    1                .794475+04   .00000       .80755-01   .22432+08    .21071-05    .27626+04
        2    1                .789400+04   .00000       .10298+00   .23066+08    .39966-05    .28407+04
        3    1                .776027+04   .00000       .15476+00   .25476+08    .43749-05    .31375+04
        4    1                .768955+04   .00000       .21457+00   .28232+08    .49644-05    .34769+04
        5    1                .727550+04   .00000       .34715+00   .33341+08    .64048-05    .41061+04
        6    1                .675315+04   .00000       .55444+00   .38867+08    .45327-05    .41885+04
 ---------------------------------------------------------------------------------------------------------------------
 118    72  FREEBD  - CONTIN   .10128+01   .95075+00    .83194-01   .69088+02    .69773+02    .10115+05    -.19737+08    2
                               .69037+01   .31449-01    .41442-05   .55160+03    .19811+04    .13527+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT
 ---------------------------------------------------------------------------------------------------------------------

 A NEW STREAMLINE HAS BEEN INSERTED ON LINE 117 BETWEEN POINTS  25 AND  26

 119     1  WALL    - CONTIN   .00000      .16944+01    .32648+01    .00000       .66428+03    .81845+04    -.19653+08    3
                               .17834+02   .17079+02    .48396-03   .25651+04    .19812+04    .12367+01
 PARTICLE DATA
        1    1                .796704+04   .00000       .86491-01   .22329+08    .20538-05    .27499+04
        2    1                .790313+04   .00000       .11225+00   .22983+08    .39363-05    .28305+04
        3    1                .777124+04   .00000       .16486+00   .25369+08    .43166-05    .31294+04
        4    1                .762389+04   .00000       .22484+00   .28107+08    .48977-05    .34614+04
        5    1                .728934+04   .00000       .35760+00   .33198+08    .63193-05    .40885+04
        6    1                .676694+04   .00000       .56548+00   .38764+08    .44644-05    .41685+04
 ---------------------------------------------------------------------------------------------------------------------

 119    73  FREEBD  - CONTIN   .10267+01   .95606+00    .83194+01   .68960+02    .69773+02    .10115+08    -.19737+08    1
                               .69037+01   .31449-01    .41442-05   .55160+03    .19811+04    .13527+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT
 ---------------------------------------------------------------------------------------------------------------------

                                POINT NO.  21 ON LINE 117 HAS BEEN DELETED

 A NEW STREAMLINE HAS BEEN INSERTED ON LINE 118 BETWEEN POINTS  51 AND  52

 A NEW STREAMLINE HAS BEEN INSERTED ON LINE 118 BETWEEN POINTS  53 AND  54
```

NOTES: (1) Typical printout for a data surface in the exhaust plume.
(2) Some points have been omitted for demonstration purposes.

Table 3-12

INPUT DATA REQUIRED FOR CREATION OF THE THERMODYNAMIC GASEOUS PROPERTIES DATA TAPE

```
REACTANTS
H 3.40424N .85106 O 3.40424CL.85106                    .8375    -60200.   S 298.15 F
H 10.3357C 7.3165 O .10630                             .1091     1200.    S 298.15 F
H 11.3337C 5.9366 O 1.07940                            .0200    -65000.   S 298.15 F
H 8.09750C 5.3983 N .8997  O .8997                     .0109    -21000.   S 298.15 F
AL3.7064                                               .02        0.0     S 298.15 F
O 1.8787 FE1.2523                                      .0025    -123000.  S 298.15 F

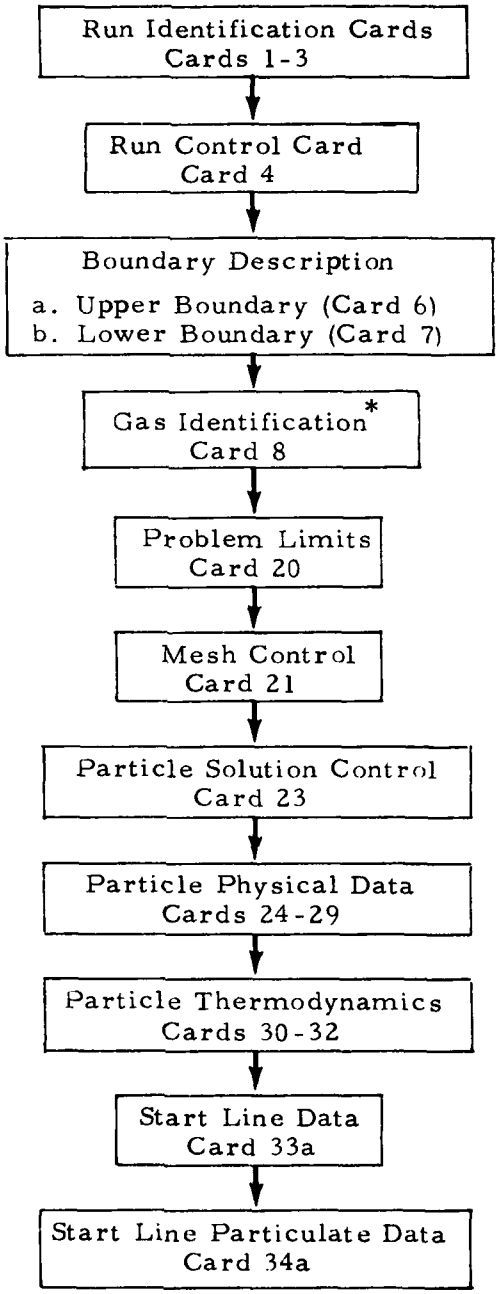
OMIT          AL(S)        AL(L)        ALCL3(S)      ALCL3(L)
OMIT          ALN(S)       ALN          AL2CL6        AL2O2
OMIT          CCL3         CCL4         CH            CH2
OMIT          CH3          CH4          COCL2         C2CL2
OMIT          C2H6         C3O2         C4            C5
OMIT          FE(S)        FE(L)        FECL2(S)      FECL2(L)
OMIT          H2O(S)       H2O(L)
NAMELISTS
 $INPT2
  RKT=T,PSIA=T,KASE=1,P=1800.,80.,MOC2P=T,MOCTF=T,PARTHT=T,
  QDOTP=-200.,-100.,-50.,0.0,NQI=4,NODATA=T
 $END
 $TAPGEN
      IREAD=1,IO=8,IN=10
 $END
SEP PROP PC=1800              MKS        4     2
 $RKTINP
  PCP=5.,10.,20.,40.,100.,300.,500.,1000.,5000.,10000.,50000.,NFZ=7
 $END
STOP
```

Example Problem 4

Example problem 4 is the same as example problem 3 except that the start line is input on cards. Table 3-13 presents a flow chart of the input data for the specified problem. Note that Card 35 has been replaced by Cards 33a and 34a. A listing of the pertinent solution is omitted as it is basically the same as for example problem 3.

Table 3-13

REQUIRED INPUT FORMAT FOR EXAMPLE PROBLEM 4



*The gas properties are input on tape. Therefore, Cards 9, 10 and 11 are not required.

Example Problem 5

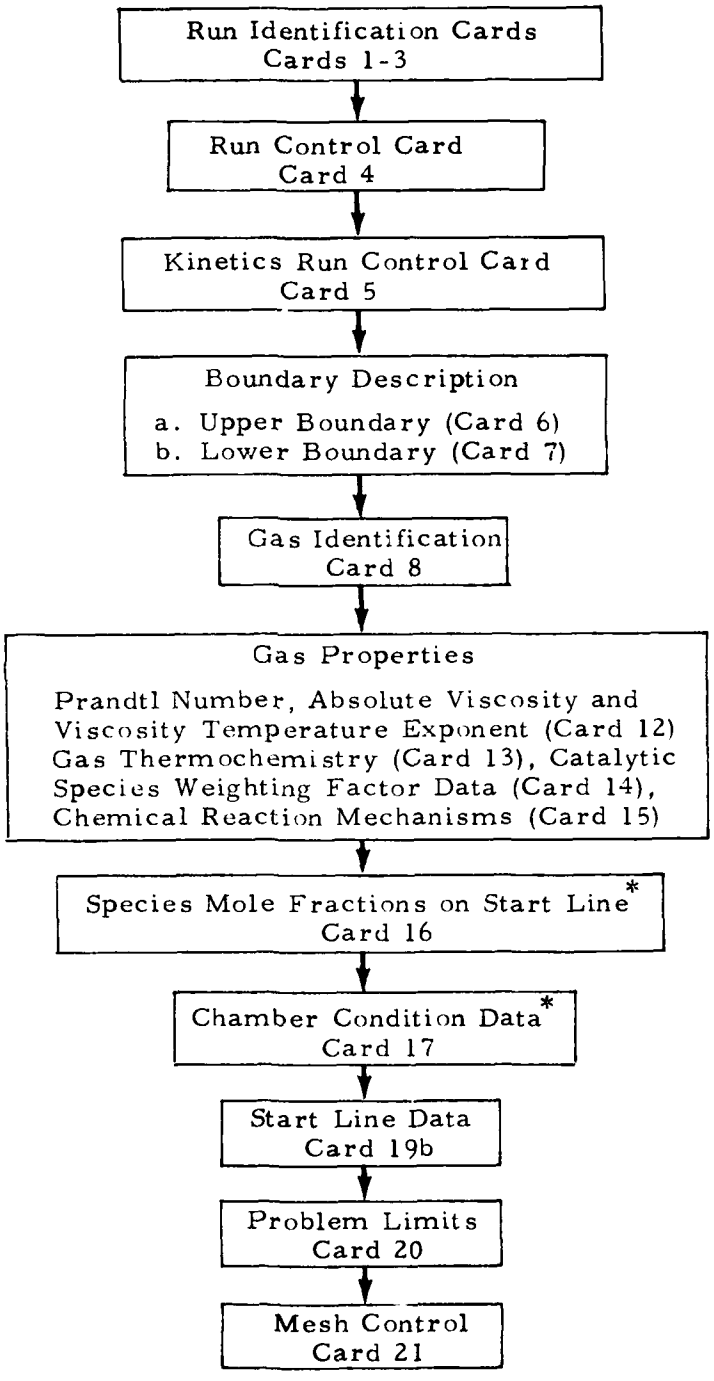
This problem analyzes a single phase finite rate chemistry flow field with the following stipulations:

1. Free molecular calculations are not to be considered,
2. Species mole fractions on the start line are to be read from cards, and
3. The start line is to be input on cards.

Table 3-14 presents first a flow chart and then a listing of the input data for the specified problem. Table 3-15 presents a listing of the pertinent solution.

Table 3-14

REQUIRED INPUT FORMAT FOR EXAMPLE PROBLEM 5



*If species mole fractions are input on tape (ICTAPE=1) Cards 16 and 17 are not required.

Table 3-14 (Continued)

```
Cards
 1-3   SA  21 - SOOLDF 671 CONL. O/F=2.2 . FINITE RATE. INVISCID. VAR O/F

Card 4     3    2   21    2    1    0    1   03        50   21   10    0    0    0.55010
Card 5    24   16    3   23    0    0    2    1
Cards 6   2    1                                  .2679492  .03078116  .20116667  .037375
          2          19.0        1.4                                   8.5333     .037372
Card 7    2                                                            8.5333
Card 8    FINITE RATE
Card 12   2        12.001     0.0
            .0       0.0        0.0       -.252      50.       .1975      .105      -.245
          100.       .395       .210      -.238     150.       .7965      .465      -.199
          200.      1.202       .720      -.160     250.      1.628      1.046      -.078
          300.      2.054      1.372       .004     400.      2.851      2.075       .250
          500.      3.496      2.784       .569     600.      4.038      3.471       .947
          700.      4.440      4.126      1.376     800.      4.740      4.739      1.831
         1000.      5.149      5.844      2.824    1200.      5.430      6.809      3.655
         1400.      5.605      7.661      4.988    1600.      5.721      8.417      6.112
         1800.      5.903      9.096      7.275    2000.      5.865      9.711      8.442
         2200.      5.936     10.536     10.212    2400.      5.992     11.267     12.208
         3000.      6.057     12.129     14.412    3200.      6.103     12.708     16.136
         4000.      6.150     13.241     18.074    4000.      6.213     13.895     20.140
        CH4     16.043    -17.895
            .0       0.0        0.0       -2.390     50.      3.9745     17.655     -1.9765
          100.      7.949     33.706     -1.601    150.      7.975     36.464     -1.200
          200.      8.001     41.227     -.621     250.      8.208     42.861     -.900
          300.      8.535     44.545      .010     400.      9.680     47.144      .915
          500.     11.076     49.453     1.990     600.     12.483     51.597      3.155
          700.     13.815     53.622     4.498     800.     15.041     55.548      5.697
         1000.     17.150     59.141     9.155    1200.     18.842     62.424     12.752
         1400.     20.150     65.431    16.037    1600.     21.161     68.191     20.772
         1800.     21.967     70.770    25.066    2000.     22.562     73.076     29.540
         2200.     23.256     74.279    35.418    2400.     23.758     79.162     43.474
         3000.     24.253     82.397    55.079    3200.     24.493     84.920     60.389
         4000.     24.695     87.060    67.768    4000.     24.901     89.673     77.690
        CO      28.010    -26.42
            .      6.956     39.613    -1.379     50.      6.956     39.613     -1.379
          100.      6.956     39.613    -1.379    150.      6.956     42.024     -1.031
          200.      6.957     44.435    -0.685    250.      6.961     45.846     -0.335
          300.      6.965     47.257     0.013    400.      7.013     49.265      0.711
          500.      7.121     50.641     1.417    600.      7.276     52.152      2.137
          700.      7.450     53.287     2.875    800.      7.624     54.293      3.627
         1000.      7.931     56.024     5.183    1200.     8.168     57.496      6.794
         1400.      8.346     58.779     8.446    1600.     8.480     59.893     10.130
         1800.      8.541     60.895    11.836    2000.     8.664     61.807     13.561
         2200.      8.706     63.024    16.175    2400.     8.825     64.102     18.813
         3000.      8.895     65.370    22.357    3200.     8.937     66.220     25.032
         3600.      8.973     66.999    27.719    4000.     9.014     67.946     31.316
        H2      2.016      0.
            .      5.393     20.649    -1.964     50.      5.393     20.649     -1.535
          100.      5.373     24.387    -1.265    150.      5.455     26.586     -0.994
          200.      5.516     28.520    -0.662    250.      5.706     29.995     -0.331
          300.      5.894     31.251     0.013    400.      6.975     33.247      0.707
          500.      6.993     34.806     1.466    600.      7.009     36.082      2.106
          700.      7.036     37.165     2.928    800.      7.037     38.107      3.514
         1000.      7.217     39.732     4.734    1200.     7.[illegible]     41.633      6.404
         1400.      7.600     42.187     7.905    1600.     7.[illegible]     43.117      9.446
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Cards 13

Table 3-14 (Continued)

Cards 13 (Cont'd)

1800.	8.016	44.150	11.030	2000.	8.195	45.004	12.651
2300.	8.432	46.160	15.157	2600.	8.639	47.213	17.700
3000.	8.659	48.465	21.210	3300.	9.0	49.6	23.000
3600.	9.3	50.8	25.00	4000.	9.4	53.0	28.000
H2O	18.016	-57.798					
.0	0.0	0.0	-2.367	50.	3.9603	18.198	-1.974
100.	7.961	36.396	-1.581	150.	7.965	39.156	-1.18
200.	7.969	41.916	- .784	250.	7.998	43.535	- .384
300.	8.027	45.155	.015	400.	8.186	47.483	.825
500.	8.415	49.334	1.654	600.	8.676	50.891	2.509
700.	8.954	52.249	3.390	800.	9.246	53.464	4.300
1000.	9.851	55.591	6.209	1200.	10.444	57.440	8.240
1400.	10.987	59.092	10.384	1600.	11.462	60.591	12.630
1800.	11.869	61.965	14.964	2000.	12.214	63.234	17.373
2300.	12.654	64.971	21.103	2600.	12.965	66.540	24.945
3000.	13.304	68.420	30.201	3300.	13.503	69.698	34.223
3600.	13.669	70.880	38.300	4000.	13.850	72.330	43.805
NH3	17.03061	-10.97					
.0	0.0	0.0	-2.404	50.	3.975	18.604	-2.006
100.	7.950	37.210	-1.609	150.	8.007	39.975	-1.21
200.	8.064	42.740	-0.811	250.	8.295	44.412	-.397[illegible]
300.	8.526	46.085	.016	400.	9.241	48.633	.9[illegible]
500.	10.036	50.780	1.867	600.	10.808	52.679	2.[illegible]
700.	11.538	54.400	4.027	800.	12.225	55.956	5.21[illegible]
1000.	13.467	58.651	7.787	1200.	14.550	61.404	10.59[illegible]
1400.	15.460	63.718	13.596	1600.	16.205	65.833	16.70[illegible]
1800.	16.762	67.776	20.066	2000.	17.220	69.566	23.46[illegible]
2300.	17.625	72.015	28.725	2600.	18.370	74.254	34.154
3000.	19.000	76.908	41.631	3300.	19.341	78.734	47.383
3600.	19.672	80.432	53.235	4000.	20.100	82.527	61.190
N2	28.0134	0.0					
.	6.956	38.170	-1.379	50.	6.956	38.170	-1.379
100.	6.956	38.170	-1.379	150.	6.956	40.586	-1.031
200.	6.957	42.992	-0.683	250.	6.959	44.402	-0.335
300.	6.961	45.613	0.013	400.	6.990	47.818	0.710
500.	7.069	49.385	1.413	600.	7.196	50.6[illegible]	2.125
700.	7.350	51.806	2.853	800.	7.512	52.798	3.596
1000.	7.815	54.507	5.129	1200.	8.061	55.955	6.716
1400.	8.252	57.212	8.350	1600.	8.395	58.324	10.015
1800.	8.512	59.320	11.707	2000.	8.601	60.222	13.41[illegible]
2300.	8.703	61.431	16.015	2600.	8.703	62.503	18.53[illegible]
3000.	8.855	63.765	22.165	3300.	8.855	64.611	24.82[illegible]
3600.	8.939	65.387	27.505	4000.	8.983	66.331	31.6[illegible]
CO2	44.0099	-94.054					
.	6.981	42.758	-1.543	50.	6.981	42.758	-1.54[illegible]
100.	6.981	42.758	-1.543	150.	7.407	45.263	-1.179
200.	7.734	47.769	-0.816	250.	8.315	49.443	-0.400
300.	8.896	51.127	0.016	400.	9.877	53.830	0.956
500.	10.666	56.122	1.987	600.	11.310	58.126	3.087
700.	11.846	59.910	4.245	800.	12.293	61.522	5.453
1000.	12.980	64.344	7.984	1200.	13.456	66.756	10.532
1400.	13.815	68.659	13.362	1600.	14.074	70.722	16.152
1800.	14.269	72.391	18.987	2000.	14.414	73.903	21.857
2300.	14.600	75.931	25.212	2600.	14.734	77.730	30.613
3000.	14.873	79.848	36.[illegible]	3300.	14.[illegible]	81.[illegible]	41.010
3600.	15.030	82.574	45.[illegible]	4000.	15.1[illegible]	84.1[illegible]	51.538
H	1.008	52.132					
.	4.068	14.[illegible]	-1.481	50.	4.408	15.382	-1.233

Table 3-14 (Continued)

Cards 13 (Cont'd)

100.	4.968	21.965	-0.984	150.	4.968	23.079	-0.[illegible]
200.	4.968	25.408	-0.488	250.	4.968	26.517	-0.[illegible]
300.	4.968	27.423	0.009	400.	4.968	28.852	0.[illegible]
500.	4.968	29.961	1.003	600.	4.968	30.867	1.[illegible]
700.	4.968	31.632	1.996	800.	4.968	32.[illegible]	[illegible]
1000.	4.968	33.404	3.487	1200.	4.968	34.310	4.[illegible]
1400.	4.968	35.075	5.474	1600.	4.968	35.739	6.468
1800.	4.968	36.325	7.461	2000.	4.968	36.946	8.455
2200.	4.968	37.538	9.946	2600.	4.968	38.152	11.436
3000.	4.968	38.862	13.423	3300.	4.968	39.394	14.923
3600.	4.968	39.926	16.423	4000.	4.968	40.636	18.410
NO 30.008 21.58							
.0	0.0	0.0	-2.197	50.0	3.8605	21.143	-1.824
100.	7.721	42.286	-1.451	150.	7.496	44.882	-1.078
200.	7.271	47.477	-0.705	250.	7.202	48.934	-.346
300.	7.132	50.392	.013	400.	7.157	52.444	.727
500.	7.287	54.053	1.448	600.	7.466	55.397	2.186
700.	7.655	56.562	2.942	800.	7.832	57.596	3.716
1000.	8.123	59.377	5.313	1200.	8.336	60.678	5.960
1400.	8.491	62.175	8.644	1600.	8.605	63.317	10.354
1800.	8.692	64.335	12.004	2000.	8.769	65.255	13.329
2200.	8.837	66.484	16.469	2600.	8.895	67.571	19.169
3000.	8.995	68.849	22.700	3300.	8.991	5[illegible].704	25.[illegible]
3600.	9.022	70.488	28.094	4000.	9.058	71.440	31.710
OH 17.008 9.33							
.0	0.0	0.0	-2.107	50.	3.7035	17.[illegible]	-1.[illegible]
100.	7.567	35.852	-1.451	150.	7.468	38.436	-1.[illegible]
200.	7.309	41.021	-.707	250.	7.2215	42.091	-.[illegible]
300.	7.134	43.952	.013	400.	7.077	46.[illegible]	.724
500.	7.049	47.582	1.430	600.	7.053	48.[illegible]	2.134
700.	7.037	49.956	2.841	800.	7.148	50.906	3.553
1000.	7.3[illegible]	52.520	5.0	1200.	7.548	53.875	6.487
1400.	7.764	55.055	8.018	1600.	7.953	56.105	9.591
1800.	8.136	57.053	11.202	2000.	8.285	57.918	12.496
2200.	8.470	59.089	15.358	2600.	8.621	60.157	17.923
3000.	8.778	61.382	21.404	3300.	8.873	62.223	24.352
3600.	8.995	62.999	26.726	4000.	9.046	63.947	30.327
5 16.0 59.559							
.0	0.0	0.0	-1.608	50.	2.833	16.233	-1.[illegible]
100.	5.666	32.466	-1.080	150.	5.600	34.4[illegible]	-.751
200.	5.434	36.340	-.523	250.	5.335	37.4[illegible]	-.2[illegible]7
300.	5.235	38.501	.010	400.	5.13[illegible]	39.[illegible]	.5[illegible]
500.	5.081	41.131	1.038	600.	5.047	42.[illegible]	1.[illegible]
700.	5.029	42.831	2.048	800.	5.015	43.[illegible]	2.[illegible]
1000.	4.999	44.619	3.552	1200.	4.990	45.[illegible]	4.[illegible]
1400.	4.984	46.298	5.548	1600.	4.981	46.[illegible]	6.[illegible]44
1800.	4.979	47.550	7.540	2000.	4.975	48.[illegible]	8.[illegible]
2200.	4.980	48.770	10.029	2600.	4.986	4[illegible]	11.[illegible]
3000.	5.004	50.096	13.522	3300.	5.005	50.[illegible]	1[illegible]
3600.	5.050	51.012	16.537	4000.	5.091	51.546	18.[illegible]
52 32.0 0.0							
.0	0.0	0.0	-2.075	50.	3.479	20.701	-1.72[illegible]
100.	6.958	41.402	-1.361	150.	6.9595	43.20[illegible]	-1.[illegible]
200.	6.961	46.225	-.685	250.	6.992	47.641	-.330
300.	7.023	49.054	.013	400.	7.196	51.097	.72[illegible]
500.	7.431	52.727	1.454	600.	7.670	54.103	2.21[illegible]
700.	7.983	55.302	2.987	800.	8.063	56.357	3.75[illegible]
1000.	8.336	56.197	[illegible]	1200.	8.527	57.733	7.114

Table 3-14 (Continued)

Cards 13 (Cont'd)

1400.	8.674	61.061	6.834	1600.	8.800	62.227	10.[illegible]
1800.	8.916	63.270	12.354	2000.	9.029	64.216	14.[illegible]
2300.	9.194	65.489	16.882	2600.	9.254	66.626	19.604
3000.	9.551	67.978	23.446	3300.	9.682	68.695	26.331
3600.	9.799	69.742	29.254	4000.	9.932	70.782	33.201
CH3	15.03506	34.820					
.	0.0	0.0	-2.487	50.	3.991	16.589	-2.0895
100.	7.982	37.178	-1.692	150.	8.25	40.012	-1.2815
200.	8.518	42.846	-.871	250.	8.89	44.642	-.427
300.	9.262	46.438	.017	400.	10.048	49.[illegible]	.953
500.	10.815	51.536	2.026	600.	11.541	53.572	3.144
700.	12.231	55.404	4.333	800.	12.888	57.35	[illegible]
1000.	14.09	60.088	8.29	1200.	15.109	6[illegible].75	11.[illegible]
1400.	15.939	65.144	14.321	1600.	16.602	67.317	17.576
1800.	17.129	69.304	20.953	2000.	17.348	71.131	[illegible]
2300.	18.028	73.618	29.762	2600.	18.38	75.651	[illegible]
3000.	18.716	78.506	42.649	3300.	18.901	80.297	[illegible]
3600.	19.045	81.95	53.966	4000.	19.194	83.763	[illegible]
CH20	30.027	-27.700					
.0	0.0	0.0	-2.395	50.	3.9745	21.7395	-1.997[illegible]
100.	7.949	43.479	-1.60	150.	7.978	46.2375	-1.202
200.	8.007	48.996	-.804	250.	8.241	50.6545	-.394
300.	8.475	52.313	.016	400.	9.385	54.869	.906
500.	10.46	57.077	1.898	600.	11.524	59.079	2.998
700.	12.505	60.931	4.20	800.	13.38	62.659	5.495
1000.	14.817	65.606	8.322	1200.	15.893	68.608	11.398
1400.	16.693	71.121	14.66	1600.	17.291	73.291	18.062
1800.	17.746	75.455	21.567	2000.	18.095	77.243	25.153
2300.	18.483	79.90	30.643	2600.	18.76	82.184	36.232
3000.	19.019	84.888	43.791	3300.	19.159	86.707	49.516
3600.	19.208	88.379	55.283	4000.	19.379	90.41[illegible]	63.014
CH3	29.019	-2.900					
.0	0.0	0.0	-2.387	50.	3.9745	22.4[illegible]	-1.[illegible]
100.	7.949	44.93	-1.593	150.	7.974	47.[illegible]	-1.1[illegible]
200.	7.999	50.447	-.796	250.	8.1[illegible]	[illegible]	-.[illegible]
300.	8.271	53.734	.015	400.	8.703	56.171	.[illegible]
500.	9.184	58.164	1.758	600.	9.66	59.[illegible]	2.[illegible]
700.	10.108	61.404	3.669	800.	10.[illegible]	6[illegible]	4.74
1000.	11.21[illegible]	65.206	6.696	1200.	11.756	[illegible]	[illegible]
1400.	12.172	69.146	11.591	1600.	12.457	7[illegible]	[illegible]
1800.	12.732	72.279	16.562	2000.	12.9[illegible]	7[illegible]	[illegible]
2300.	13.133	75.452	23.058	2600.	13.286	77.271	[illegible]
3000.	13.43	78.983	32.367	3300.	13.508	80.767	[illegible]
3600.	13.569	81.445	40.47	4000.	13.631	82.678	45.911

Cards 14

M1	1.0	1.0	1.0	1.0	3.0	1.0	1.0	2.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0
M2	1.0	1.0	1.0	1.0	10.0	1.0	1.0	3.0	1.0	1.0	2.0	1.0	1.0	1.0	1.0	1.0
M3	1.0	1.0	1.0	1.0	10.0	1.0	1.0	3.0	1.0	1.0	1.0	1.0	20.0	1.0	1.0	1.0

Cards 15

H	+OH	+M1	=H2O	+M1	22	6.10-26	2.0	0.0
O	+H	+M1	=OH	+M1	21	2.00-32	0.0	0.0
[illegible]	+O	+M1	=O2	+M1	24	3.60-30	1.0	-340.0
H	+H	+M2	=H2	+M2	22	2.50-30	1.0	0.0
[illegible]	+O	+M3	=O2	+M3	23	2.00-33	0.0	-4000.0
[illegible]	+H		=H2	+O	14	1.40-14	-1.0	-7000.0
[illegible]	+O		=H	+O2	11	4.00-11	0.0	[illegible]
[illegible]	+HO		=H2O	+H	[illegible]	[illegible]	[illegible]	[illegible]

Table 3-14 (Continued)

Cards 15 (Cont'd)

OH	+CO		=CO2	+H		14	1.10-19	-2.0	1600.0
OH	+OH		=H2O	+O		13	1.00-11	0.0	-1100.0
CH4	+OH		=CH3	+H2O		13	4.7 -11		-5000.0
CH4	+H		=CH3	+H2		13	2.4 -11		-5000.0
CH4	+O		=CH3	+OH		13	3.5 -11		-9100.0
CH3	+O		=CH2O	+H		11	1.1 -10		
CH2O	+OH		=CHO	+H2O		12	9.0 -13	-.5	
CH2O	+H		=CHO	+H2		13	2.2 -11		-3800.0
CH2O	+O		=CHO	+OH		11	1.6 -13		
CH2O	+M1		=CO	+H2	+M1	53	3.5 -08		-35000.0
CHO	+OH		=CO	+H2O		11	2.1 -10		
CHO	+H		=CO	+H2		13	8.3 -11		-10000.0
CHO	+O		=CO	+OH		11	2.1 -10		
CHO	+O2		=CO	+H	+O2	73	8.3 -11		-1600.0
CHO	+M1		=CO	+H	+M1	53	1.2 -10		-15000.0

Cards 16

.7478-01	.2078+00	.6382-03	.4315+00	.8570-03	.1257-02	.2831+00
.5636-05	.0000	.0000	.0000	.0000	.0000	
.7910-01	.1899+00	.6336-02	.4366+00	.6444-02	.1184-02	.2752+00
.1631-03	.0000	.0000	.0000	.0000	.0000	
.5707-01	.1247+00	.6244-01	.4704+00	.1665-01	.6584-03	.2661+00
.1087-02	.0000	.0000	.0000	.0000	.0000	
.0000	.2263-01	.1669+00	.4851+00	.6006-01	.3501-03	.2573+00
.7411-02	.1217-03	.2845-06	.7026-05	.0000	.0000	
.0000	.3246-06	.1574+00	.4163+00	.2175+00	.2852-04	.2833+00
.1124-01	.2946-02	.1245-03	.1151-02	.2766-04	.1739-04	
.0000	.0000	.1235+00	.1527+00	.3416+00	.4509-05	.3105+00
.9466-01	.1010-01	.2337-02	.1141-01	.1034-02	.1684-02	
.0000	.0000	.8603-01	.6581-01	.3864+00	.0000	.3240+00
.7168-01	.1270-01	.8107-02	.2910-01	.3919-02	.1217-01	
.0000	.0000	.5879-01	.3492-01	.3849+00	.0000	.3285+00
.6720-01	.9610-02	.1424-01	.3916-01	.6775-02	.3373-01	
.0000	.0000	.4197-01	.2165-01	.3756+00	.0000	.3305+00
.9968-01	.6842-02	.1814-01	.4154-01	.8028-02	.5676-01	
.0000	.0000	.3268-01	.1630-01	.3663+00	.0000	.3317+00
.1024+00	.5215-02	.1994-01	.4006-01	.7985-02	.7733-01	
.0000	.0000	.2739-01	.1315-01	.3612+00	.0000	.3325+00
.1046+00	.4280-02	.2088-01	.3914-01	.7928-02	.8879-01	
.0000	.0000	.2528-01	.1204-01	.3588+00	.0000	.3329+00
.1053+00	.3910-02	.2104-01	.3815-01	.7717-02	.9473-01	
.0000	.0000	.2462-01	.1171-01	.3585+00	.0000	.3332+00
.1057+00	.3786-02	.2095-01	.3766-01	.7592-02	.9616-01	
.0000	.0000	.2649-01	.1271-01	.3628+00	.0000	.3332+00
.1057+00	.4093-02	.2038-01	.3607-01	.7636-02	.8882-01	
.0000	.0000	.3062-01	.1526-01	.3633+00	.0000	.3330+00

Table 3-14 (Concluded)

	•1095+00	•4783-02	•1921-01	•3825-01	•7504-02	•7834-01	
Cards 16 (Cont'd)	•0000	•0000	•3678-01	•1890-01	•3770+00	•0000	•3326+00
	•1026+00	•5793-02	•1762-01	•3870-01	•7373-02	•6264-01	
	•0000	•0000	•4717-01	•2637-01	•3866+00	•0000	•3317+00
	•5795-01	•7365-02	•1492-01	•3742-01	•6656-02	•4378-01	
	•0000	•0000	•6587-01	•4215-01	•3967+00	•0000	•3297+00
	•6751-01	•9516-02	•1039-01	•3262-01	•4776-02	•2009-01	
	•0000	•0000	•1097+00	•1161+00	•3663+00	•1963-05	•3179+00
	•5632-01	•9686-02	•2830-02	•1360-01	•1227-02	•2347-02	
	•0000	•7495-07	•1408+00	•2172+00	•3012+00	•6295-05	•3013+00
	•3301-01	•4530-02	•1710-03	•1703-02	•3360-04	•2128-04	
	•0000	•7495-07	•1408+00	•2172+00	•3012+00	•6295-05	•3013+00
	•3301-01	•4530-02	•1710-03	•1703-02	•3360-04	•2128-04	

Card 17 34.014 3236.1

Cards 19b

•	•841666/E-02	•1027366E+010•		•1055177E+04	•1872436E+02
•1956063E-02	•841666/E-02	•1029127E+01	•7462402E+00	•1059910E+04	•1867169E+02
•3912167E-02	•841666/E-02	•1023770E+01	•1501096E+01	•1151956E+04	•1869575E+02
•5868250E-02	•841666/E-02	•1021379E+01	•2246439E+01	•1451161E+04	•1855997E+02
•7824333E-02	•841666/E-02	•1020366E+01	•2978366E+01	•2316396E+04	•1851260E+02
•9780417E-02	•841666/E-02	•1040766E+01	•3730434E+01	•2596[illegible]7E+04	•1[illegible]
•1173650E-01	•841666/E-02	•1059406E+01	•4493167E+01	•3109170E+04	•1[illegible]
•1369258E-01	•841666/E-02	•1066306E+01	•5240717E+01	•3113447E+04	•1[illegible]
•1564867E-01	•841666/E-02	•1079547E+01	•6004941E+01	•3074666E+04	•1799[illegible]
•1760475E-01	•841666/E-02	•1086776E+01	•6757037E+01	•3027[illegible]9E+04	•1[illegible]
•1956083E-01	•841666/E-02	•1100192E+01	•7509626E+01	•2998401E+04	•174[illegible]
•2151692E-01	•841666/E-02	•1115613E+01	•8264529E+01	•2978694E+04	•17147[illegible]
•2347300E-01	•841666/E-02	•1132729E+01	•9020210E+01	•2969294E+04	•16[illegible]
•2542908E-01	•841666/E-02	•1154970E+01	•9775045E+01	•2978566E+04	•16371[illegible]
•2738517E-01	•841666/E-02	•1179205E+01	•10533[illegible]1E+02	•2991671E+04	•1590245E+02
•2934125E-01	•841666/E-02	•1209937E+01	•11289[illegible]E+02	•3014766E+04	•1557251E+02
•3129734E-01	•841666/E-02	•1239830E+01	•12044065E+02	•3036111E+04	•1474476E+02
•3325342E-01	•841666/E-02	•1274133E+01	•12807985E+02	•3050450E+04	•141[illegible]
•3520950E-01	•841666/E-02	•1306148E+01	•13565061E+02	•2868920E+04	•1332472E+02
•3716[illegible]E-01	•841666/E-02	•1333497E+01	•14296084E+02	•2536821E+04	•1261320E+02
•[illegible]E-01	•841666/E-02	1.3345	15.0	2526.1	12.5926

Card 20 0.0 0.0 0.0 •6 90.0

Card 21 • 0.015 0.0 0.00001 4.0 •375

Table 3-15

EXAMPLE PROBLEM 5 PERTINENT SOLUTION

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                GAS-PARTICLE FLOW SOLUTION
                                CASE NO.   21                                          PAGE    1

CASE 21 - 500LBF 6/1 CONE, O/F=2.2 , FINITE RATE, INVISCID, VAR O/F

                                RUN CONTROL PARAMETERS
              ICON(1)   ICON(2)   ICON(3)   ICON(4)   ICON(5)   ICON(6)   ICON(7)   ICON(8)
                 3         2        21         2         1         0         1         3

              ICON(9)  ICON(10)  ICON(11)  ICON(12)  ICON(13)  ICON(14)  ICON(15)  ICON(16)
                 0        50        21         1         0         0         0       3010

FLOW CALCULATIONS ARE IN ENGLISH  UNITS WITH THE R,X COORDINATES IN FEET

THE FLOW FIELD DATA WILL BE WRITTEN ON TAPE
                                 1
                                UPPER BOUNDARY
      TYPE   ITRANS        A          B          C          D          E          MAX
       2       1       .00000     .00000     .00000     .26785+00  .36781-01  .20517+00
       3       0      .19400+02  .14000+01  .00000     .00000     .00000     .83333+01

                                LOWER BOUNDARY
      TYPE   ITRANS        A          B          C          D          E          MAX
       2       0       .00000     .00000     .00000     .00000     .00000     .83333+01
```

Table 3-15 (Continued)

```
SPECIF THERMODYNAMIC AND REACTION DATA
NT,NS,NR,NM,ICTAPE,KGUP,IDIDO=   24   16   23    3    0    2    1

PRANDTL NUMBER =   .70000000+00
BASE VISCOSITY =   .1865119A-05
EXPONENT       =   .60000000+00
```

	REACTIONS BEING CONSIDERED	KR=A*EXP(B/RT**N)/T**N	A	N	B	M	R-TYPE	K-TYPE
1	H + OH + M1 = H2O + M1		2.214+22	2.0	.0	.0	2	2
2	O + H + M1 = OH + M1		7.260+15	.0	.0	.0	2	1
3	O + O + M1 = O2 + M1		1.379+18	1.0	-340.0	.0	2	4
4	H + H + M2 = H2 + M2		1.016+18	1.0	.0	.0	2	2
5	CO + O + M3 = CO2 + M3		7.260+14	.0	-4000.0	.0	2	3
6	OH + H = H2 + O		8.435+09	-1.0	-7000.0	.0	1	4
7	OH + O = H + O2		2.410+13	.0	.0	.0	1	1
8	OH + H2 = H2O + H		6.025+06	-2.0	-2900.0	.0	1	4
9	OH + CO = CO2 + H		6.627+04	-2.0	1600.0	.0	1	4
10	OH + OH = H2O + O		6.025+12	.0	-1100.0	.0	1	3
11	CH4 + OH = CH3 + H2O		2.832+13	.0	-5000.0	.0	1	3
12	CH4 + H = CH3 + H2		1.448+13	.0	-5000.0	.0	1	3
13	CH4 + O = CH3 + OH		2.109+13	.0	-9100.0	.0	1	3
14	CH3 + O = CH2O + H		6.627+13	.0	.0	.0	1	1
15	CH2O + OH = CHO + H2O		5.422+11	-.5	.0	.0	1	2
16	CH2O + H = CHO + H2		1.325+13	.0	-3800.0	.0	1	3
17	CH2O + O = CHO + OH		9.640+10	.0	.0	.0	1	1
18	CH2O + M1 = CO + H2 + M1		2.109+16	.0	-35000.0	.0	5	3
19	CHO + OH = CO + H2O		1.265+14	.0	.0	.0	1	1
20	CHO + H = CO + H2		5.001+13	.0	-10000.0	.0	1	3
21	CHO + O = CO + OH		1.265+14	.0	.0	.0	1	1
22	CHO + O2 = CO + H		5.001+13	.0	-1600.0	.0	7	3
23	CHO + M1 = CO + H + M1		7.230+13	.0	-15000.0	.0	5	3

CATALYTIC SPECIES BEING CONSIDERED

```
M1   = 1.00 C    , 1.00 CH4  , 1.00 CO   , 1.00 H2   , 3.00 H2O  , 1.00 NH3  , 1.00 N2   ,
       2.00 CO2  , 1.00 H    , 1.00 NO   , 1.00 OH   , 1.00 O    , 1.00 O2   , 1.00 CH3  ,
       1.00 CH2O , 1.00 CHO  ,

M2   = 1.00 C    , 1.00 CH4  , 1.00 CO   , 1.00 H2   ,10.00 H2O  , 1.00 NH3  , 1.00 N2   ,
       3.00 CO2  , 1.00 H    , 1.00 NO   , 2.00 OH   , 1.00 O    , 1.00 O2   , 1.00 CH3  ,
       1.00 CH2O , 1.00 CHO  ,

M3   = 1.00 C    , 1.00 CH4  , 1.50 CO   , 1.00 H2   ,10.00 H2O  , 1.00 NH3  , 1.00 N2   ,
       3.00 CO2  , 1.00 H    , 1.00 NO   , 1.00 OH   , 1.00 O    ,20.00 O2   , 1.00 CH3  ,
       1.00 CH2O , 1.00 CHO  ,
```

Table 3-15 (Continued)

SPECIE MOLE FRACTIONS ON THE START LINE ARE READ FROM CARDS

POINT										
1	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.74780-01	.20780+00	.63820-03	.43150+00	.85700-03	.12570-02	.28310+00	.56360-05	.00000	.00000
1	OH	O	O2	CH3	CH2O	CHO				
	.00000	.00000	.00000	.00000	.00000	.00000				
2	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.79100-01	.18990+00	.63360-02	.43860+00	.64440-02	.11840-02	.27820+00	.18310-03	.00000	.00000
2	OH	O	O2	CH3	CH2O	CHO				
	.00000	.00000	.00000	.00000	.00000	.00000				
3	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.57070-01	.12470+00	.62440-01	.47040+00	.16650-01	.88840-03	.26610+00	.16870-02	.00000	.00000
3	OH	O	O2	CH3	CH2O	CHO				
	.00000	.00000	.00000	.00000	.00000	.00000				
4	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.00000	.22630-01	.16690+00	.48510+00	.60060-01	.35010-03	.25730+00	.74110-02	.12170-03	.28450-06
4	OH	O	O2	CH3	CH2O	CHO				
	.70260-05	.00000	.00000	.00000	.00000	.00000				
5	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.00000	.32460-06	.15740+00	.31630+00	.21750+00	.28520-04	.28330+00	.21240-01	.29460-02	.12450-03
5	OH	O	O2	CH3	CH2O	CHO				
	.11510-02	.27660-04	.17390-04	.00000	.00000	.00000				
6	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.00000	.00000	.12350+00	.15270+00	.34160+00	.45090-05	.31050+00	.44860-01	.10100-01	.23370-02
6	OH	O	O2	CH3	CH2O	CHO				
	.11410-01	.10340-02	.18840-02	.00000	.00000	.00000				
7	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.00000	.00000	.86030-01	.65610-01	.38640+00	.00000	.32400+00	.71680-01	.12700-01	.81070-02
7	OH	O	O2	CH3	CH2O	CHO				
	.29160-01	.39190-02	.12170-01	.00000	.00000	.00000				
8	C	CH4	CO	H2	H2O	NH3	N2	CO2	H	NO
	.00000	.00000	.58790-01	.34920-01	.38490+00	.00000	.32850+00	.89300-01	.96100-02	.14240-01
8	OH	O	O2	CH3	CH2O	CHO				
	.39160-01	.67750-02	.33730-01	.00000	.00000	.00000				

NOTE: Some points have been omitted for demonstration purposes.

Table 3-15 (Continued)

```
20      OH          O           O2          CH3         CH2O        CHO
        .17030-02   .33800-04   .21280-04   .00000      .00000      .00000

21      C           CH4         CO          H2          H2O         NH3         N2          CO2         H           NO
        .00000      .74950-07   .14080+00   .21720+00   .30120+00   .87950-05   .30130+00   .33010-01   .45300-02   .17100-03

21      OH          O           O2          CH3         CH2O        CHO
        .17030-02   .33800-04   .21280-04   .00000      .00000      .00000

CHAMBER PRESSURE (ATM) =    .34014+02 CHAMBER TEMPERATURE (DEG-K) =    .32361+04

                    THERE ARE  0 PARTICLE SPECIES PRESENT IN THE GAS-PARTICLE MIXTURE

                                        RUN CUTOFF INFORMATION
                    UPPER BOUNDARY                                  LOWER BOUNDARY
        R=    .25000+01   X=    .00000    THETA=    .00000    R=    .00000    X=    .60000+00    THETA=    .90000+02

                    THE MESH CONSTRUCTION WILL BE CONTROLED BY THE FOLLOWING VARIABLES
        DL INTERIOR=    .150-01 DX AXIS=    .150-01 DL LIM=    .000    DL DELETE=    .100-04 DEG P.M.=    .400+01 F=    .375+00
```

Table 3-15 (Continued)

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                GAS-PARTICLE FLOW SOLUTION
                                CASE NO.   21                                                    PAGE    2

CASE 21 - 500LBF 6/1 CONE, O/F=2.2 , FINITE RATE, INVISCID, VAR O/F

LINE POINT  DSCRIP - REGIME        R              X              M              THETA          ENTROPY        VELOCITY       M-TOTAL   ITR
                                 MACH ANGLE     PRESSURE       DENSITY      TEMPERATURE     GAS CONST.     LOCAL GAMMA    SHOCK ANGLE
                                   TO*            PO*            S*

   1     1  INPUT  - CONTIN      .00000         .84167-02      .10274+01      .00000         .00000         .31052+04      .13224+08    0
                                 .76745+02      .27517+03      .54912-02      .18993+04      .37993+04      .12660+01
                                 .21660+04      .51429+03      .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       7.4785-02   CH4    2.0781-01   CO     6.3824-04   H2     4.3153-01   H2O    8.5705-04   NH3    1.2571-03   N2     2.8312-01
CO2     5.6364-06   H      0.0000      NO     0.0000      OH     0.0000      O      0.0000      O2     0.0000      CH3    0.0000
CH2O    0.0000      CHO    0.0000

   1     2  INPUT  - CONTIN      .19561-02      .84167-02      .10291+01      .74624+00      .00000         .31483+04      .12984+08    0
                                 .76336+02      .27440+03      .53672-02      .19242+04      .38260+04      .12712+01
                                 .22006+04      .51479+03      .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       7.9104-02   CH4    1.8991-01   CO     6.3363-03   H2     4.3867-01   H2O    6.4443-03   NH3    1.1841-03   N2     2.7821-01
CO      1.8311-04   H      0.0000      NO     0.0000      OH     0.0000      O      0.0000      O2     0.0000      CH3    0.0000
CH2O    0.0000      CHO    0.0000

   1     3  INPUT  - CONTIN      .39122-02      .84167-02      .10238+01      .15011+01      .00000         .32426+04      .11265+08    0
                                 .77629+02      .27475+03      .50759-02      .20735+04      .37591+04      .12870+01
                                 .23854+04      .51502+03      .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       5.7074-02   CH4    1.2471-01   CO     6.2444-07   H2     4.7043-01   H2O    1.6651-02   NH3    8.8846-04   N2     2.6612-01
CO2     1.6871-03   H      0.0000      NO     0.0000      OH     0.0000      O      0.0000      O2     0.0000      CH3    0.0000
CH2O    0.0000      CHO    0.0000

   1     4  INPUT  - CONTIN      .58682-02      .84167-02      .10214+01      .22464+01      .00000         .35142+04      .69241+07    0
                                 .78256+02      .27276+03      .43259-02      .26733+04      .33964+04      .13038+01
                                 .30969+04      .51283+03      .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4    2.2633-02   CO     1.6692-01   H2     4.8516-01   H2O    6.0067-02   NH3    3.5014-04   N2     2.5733-0
CO2     7.4119-03   H      1.2171-04   NO     2.8453-07   OH     7.0768-06   O      0.0000      O2     0.0000      CH3    0.0000
CH2O    0.0000      CHO    0.0000
```

NOTES: (1) Typical printout for the startline data surface.
(2) Some points have been omitted for demonstration purposes.

Table 3-15 (Continued)

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                GAS-PARTICLE FLOW SOLUTION
                                CASE NO.   21                                                    PAGE   45

CASE 21 - 500LBF 6/1 CONE, O/F=2.2 , FINITE RATE, INVISCID, VAR O/F

LINE POINT  DSCRIP - REGIME        R            X            M            THETA        ENTROPY      VELOCITY     H-TOTAL    ITR
                                 MACH ANGLE   PRESSURE     DENSITY     TEMPERATURE   GAS CONST.   LOCAL GAMMA  SHOCK ANGLE
                                   TO*          PO*          S*

 60     1  WALL    - CONTIN      .00000       .62272-01    .20063+01    .00000       .91272-05    .52447+04    .13194+08   3
                                .29896+02     .65120+02    .17854-02    .13825+04    .37993+04    .13011+01
                                .22201+04     .35364+03    .00000

CHEMICAL SPECIE MOLE FRACTIONS
C       7.4785-02   CH4    2.0781-01   CO     6.3824-04   H2     4.3153-01   H2O    8.5705-04   NH3    1.2571-03   N2     2.8312-01
CO2     5.6364-06   H      3.4528-19   NO     0.0000      OH     1.7397-25   O      3.9207-35   O2     0.0000      CH3    3.0251-18
CH2O    5.1725-10   CHO    1.1351-18

 60    21  WALL    - CONTIN      .51639-01    .55452-01    .19568+01    .15000+02    .77017+02    .67522+04    .36075+07   3
                                .30733+02     .70385+02    .10656-02    .37807+04    .25158+04    .12518+01
                                .56034+04     .35518+03    .00000

CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4    4.9604-08   CO     1.4019-01   H2     2.1814-01   H2O    3.0192-01   NH3    8.3046-06   N2     3.0165-01
CO2     3.3906-02   H      3.4555-03   NO     1.7120-04   OH     6.3044-04   O      6.4868-06   O2     4.3406-06   CH3    1.9276-08
CH2O    9.5135-08   CHO    1.4114-05

                                                PRESSURE INTEGRATION RESULTS
                                FORCEX       FORCEY       TORQZ        DELFX        DELFY        ISP
                              -.47885+03     .00000       .00000      -.14007+01    .00000      .24227+03

 61     1  WALL    - CONTIN      .00000       .64003-01    .20242+01    .00000       .91334-05    .52747+04    .13195+08   3
                                .29606+02     .63188+02    .17445-02    .13728+04    .37993+04    .13019+01
                                .22220+04     .34887+03    .00000

CHEMICAL SPECIE MOLE FRACTIONS
C       7.4785-02   CH4    2.0781-01   CO     6.3824-04   H2     4.3153-01   H2O    8.5705-04   NH3    1.2571-03   N2     2.8312-01
CO2     5.6364-06   H      3.3760-19   NO     0.0000      OH     1.5902-25   O      2.5212-35   O2     0.0000      CH3    2.9582-18
CH2O    5.1736-10   CHO    1.2096-18

 61    21  WALL    - CONTIN      .52095-01    .57151-01    .19735+01    .15000+02    .78410+02    .67916+04    .36068+07   3
                                .30445+02     .68429+02    .10418-02    .37597+04    .25158+04    .12521+01
                                .56055+04     .35064+03    .00000

CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4    4.9635-08   CO     1.4015-01   H2     2.1819-01   H2O    3.0190-01   NH3    8.3047-06   N2     3.0165-01
CO2     3.3845-02   H      3.4353-03   NO     1.7120-04   OH     6.1685-04   O      6.3040-06   O2     4.2352-06   CH3    1.9187-08
CH2O    9.2748-08   CHO    1.4215-05

                                                PRESSURE INTEGRATION RESULTS
                                FORCEX       FORCEY       TORQZ        DELFX        DELFY        ISP
                              -.48033+03     .00000       .00000      -.14831+01    .00000      .24304+03
```

NOTES: (1) Typical printout for a data surface inside the nozzle.
(2) Some points have been omitted for demonstration purposes.

Table 3-15 (Continued)

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                   GAS-PARTICLE FLOW SOLUTION
                                   CASE NO.   21                                                    PAGE   89

CASE 21 - SOOLAF 6/1 CONE, O/F=2.2 , FINITE RATE, INVISCID, VAR O/F

LINE POINT  DSCRIP - REGIME        R            X            M            THETA        ENTROPY      VELOCITY     M-TOTAL    ITR
                                 MACH ANGLE   PRESSURE    DENSITY     TEMPERATURE   GAS CONST.   LOCAL GAMMA  SHOCK ANGLE
                                   TO*          PO*          S*

 114    25  PRN-MR - CONTIN      .91755-01    .20517+00    .35807+01    .29767+02    .12437+03    .93012+04    .36189+07    5
                                 .16222+02    .39106+01    .10778-03    .20740+04    .25145+04    .12938+01
                                 .66307+04    .63180+02    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4   5.0639-08   CO    1.3896-01   H2    2.1947-01   H2O   3.0133-01   NH3   8.3088-06   N2    3.0180-01
CO2     3.5089-02   H     2.9945-03   NO    1.7129-04   OH    1.1603-04   O     1.3375-06   O2    1.6412-06   CH3   1.7015-08
CH2O    2.2823-08   CHO   4.9038-05

 114    26  PRN-MR - CONTIN      .91755-01    .20517+00    .37735+01    .33459+02    .12437+03    .94722+04    .36189+07    5
                                 .15372+02    .27979+01    .83120-04    .19277+04    .25145+04    .12999+01
                                 .66307+04    .50267+02    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4   5.0639-08   CO    1.3896-01   H2    2.1947-01   H2O   3.0133-01   NH3   8.3088-06   N2    3.0180-01
CO2     3.5089-02   H     2.9945-03   NO    1.7129-04   OH    1.1603-04   O     1.3375-06   O2    1.6412-06   CH3   1.7015-08
CH2O    2.2823-08   CHO   4.9038-05

 114    27  PRN-MR - CONTIN      .91755-01    .20517+00    .39812+01    .37150+02    .12437+03    .96366+04    .36189+07    5
                                 .14553+02    .19633+01    .63034-04    .17837+04    .25145+04    .13063+01
                                 .66307+04    .39331+02    .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4   5.0639-08   CO    1.3896-01   H2    2.1947-01   H2O   3.0133-01   NH3   8.3088-06   N2    3.0180-01
CO2     3.5089-02   H     2.9945-03   NO    1.7129-04   OH    1.1603-04   O     1.3375-06   O2    1.6412-06   CH3   1.7015-08
CH2O    2.2823-08   CHO   4.9038-05

 114    28  PRN-MR - CONTIN      .91755-01    .20517+00    .42109+01    .40842+02    .12437+03    .97943+04    .36189+07    5
                                 .13743+02    .13481+01    .47135-04    .16380+04    .25145+04    .13135+01
                                 .66307+04    .30288+02    .00000
CHEMICAL SPECIF MOLE FRACTIONS
C       0.0000      CH4   5.0639-08   CO    1.3896-01   H2    2.1947-01   H2O   3.0133-01   NH3   8.3088-06   N2    3.0180-01
CO2     3.5089-02   H     2.9945-03   NO    1.7129-04   OH    1.1603-04   O     1.3375-06   O2    1.6412-06   CH3   1.7015-08
CH2O    2.2823-08   CHO   4.9038-05
```

NOTES: (1) Typical printout for a data surface containing a Prandtl-Meyer Expansion.
(2) Some points have been omitted for demonstration purposes.

Table 3-15 (Concluded)

```
                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                          CASE NO.   21                                                    PAGE  115

CASE 21 - SOOLAF 6/1 CONE, O/F=2.2 , FINITE RATE, INVISCID, VAR O/F

LINE POINT  DSCRIP - REGIME        R              X              M              THETA          ENTROPY        VELOCITY       M-TOTAL    ITR
                                MACH ANGLE     PRESSURE       DENSITY      TEMPERATURE     GAS CONST.     LOCAL GAMMA    SHOCK ANGLE
                                   TO.            PO.            S.

 129     1  WALL    - CONTIN    .00000         .22341+00      .29826+01      .00000         .91677-05      .64753+04      .13187+08     2
                                .19590+02      .12303+02      .50779-03      .91833+03      .37993+04      .13509+01
                                .23518+04      .14467+03      .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       7.4785-02   CH4    2.0781-01   CO     6.3824-04   H2     4.3153-01   H2O    8.5705-04   NH3    1.2571-03   N2     2.8312-01
CO2     5.6364-06   H      1.2664-21   NO     0.0000      OH     5.3647-29   O      0.0000      O2     0.0000      CH3    1.4675-19
CH2O    5.1793-10   CHO    4.3574-18

 129    34  FREEBD  - CONTIN    .95802-01      .20754+00      .58115+01      .60194+02      .13845+03      .10475+05      .36062+07     2
                                .99084+01      .13472+00      .80696-05      .95627+03      .25140+04      .13514+01
                                .66307+04      .58590+01      .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4    5.0650-08   CO     1.3879-01   H2     2.1951-01   H2O    3.0140-01   NH3    8.3105-06   N2     3.0166-01
CO2     3.5096-02   H      2.7946-03   NO     1.7132-04   OH     1.1569-04   O      1.3377-06   O2     1.6416-06   CH3    1.7018-08
CH2O    2.2825-08   CHO    2.4958-04

                                POINT NO.  32 ON LINE 129 HAS BEEN DELETED

 130     1  WALL    - CONTIN    .00000         .22400+00      .29853+01      .00000         .91677-05      .64778+04      .13186+08     2
                                .19571+02      .12248+02      .50609-03      .91725+03      .37993+04      .13511+01
                                .23522+04      .14428+03      .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       7.4785-02   CH4    2.0781-01   CO     6.3824-04   H2     4.3153-01   H2O    8.5705-04   NH3    1.2571-03   N2     2.8312-01
CO2     5.6364-06   H      1.2417-21   NO     0.0000      OH     5.2150-29   O      0.0000      O2     0.0000      CH3    1.4575-19
CH2O    5.1793-10   CHO    4.3584-18

 130    33  FREEBD  - CONTIN    .96187-01      .20776+00      .58109+01      .60318+02      .14056+03      .10475+05      .36064+07     2
                                .99094+01      .13472+00      .80679-05      .95650+03      .25139+04      .13514+01
                                .66308+04      .58578+01      .00000
CHEMICAL SPECIE MOLE FRACTIONS
C       0.0000      CH4    5.0652-08   CO     1.3876-01   H2     2.1952-01   H2O    3.0140-01   NH3    8.3107-06   N2     3.0187-01
CO2     3.5097-02   H      2.7646-03   NO     1.7132-04   OH     1.1562-04   O      1.3376-06   O2     1.6416-06   CH3    1.7018-08
CH2O    2.2825-08   CHO    2.7967-04
```

NOTES: (1) Typical printout for a data surface in the exhaust plume.
(2) Some points have been omitted for demonstration purposes.

Example Problem 6

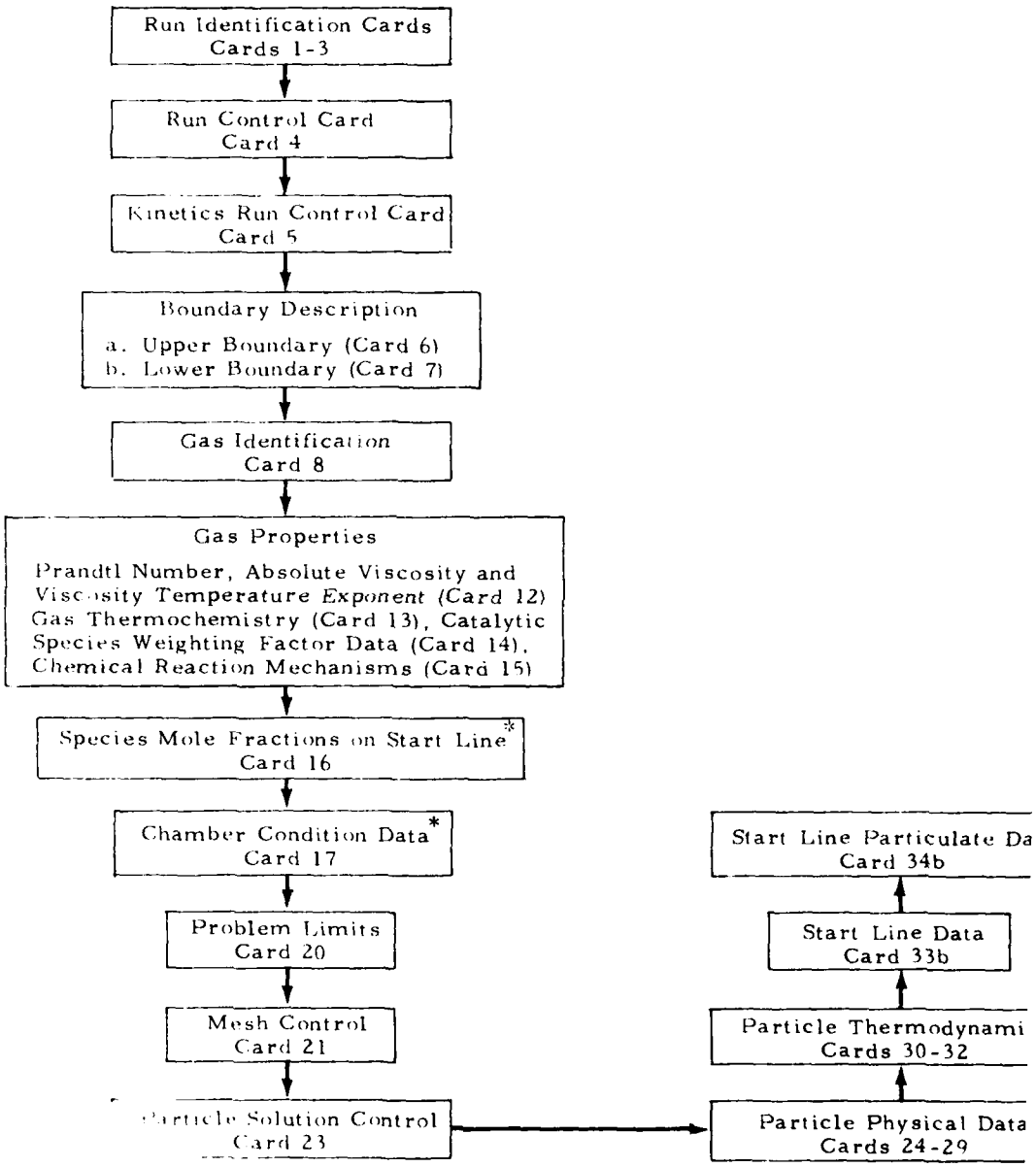
This problem analyzes a two phase finite rate chemistry flow field with the following stipulations:

1. Free molecular calculations are not to be considered.
2. Species mole fractions on the start line are to be read from cards, and
3. The start line is to be input on cards.

Table 3-16 presents first a flow chart and then a listing of the input data for the specified problem. Table 3-17 presents a listing of the pertinent solution.

Table 3-16

REQUIRED INPUT FORMAT FOR EXAMPLE PROBLEM 6



* Fractions are input on tape (ICTAPE=1) cards 16 and 17 are not re

Table 3-16 (Continued)

Cards 1-3

Card 4

Card 5

Cards 6

Card 7

Card 8

Card 12

Cards 13

Table 3-16 (Continued)

Cards 13
(Cont'd)

```
  [illegible]    6.516     26.520   -[illegible]   [illegible]    6.972      35.247      3.757
  [illegible]    7.107     36.002      2.106     [illegible]    7.067       3.127      3.514
     1000.0      7.217     37.702      4.914        1200.0      7.390      41.335      5.404
     1400.0      7.600     42.187      7.902        1600.0    [illegible] [illegible]  7.642
  [illegible]    8.125     45.004     12.651        2200.0      8.358   [illegible]  [illegible]
     2400.0      8.306     46.827   [illegible]     2600.0      8.639   [illegible]  [illegible]
     2700.0      8.701     47.540   [illegible]     2800.0      8.757   [illegible]  [illegible]
  [illegible] [illegible]  48.166   [illegible]     3000.0   [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible]  22.096    [illegible] [illegible] [illegible] [illegible]
[illegible]   [illegible]      -37.[illegible]
         .0  [illegible]   36.396   [illegible]      100.0   [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible]  -0.704        400.0      8.106   [illegible]  [illegible]
  [illegible] [illegible]  50.681      2.509         800.0   [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible]   1200.0   [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible]   1600.0   [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible]   2200.0   [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible] [illegible]   13.140   [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible]   3000.0   [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible]   3200.0   [illegible] [illegible] [illegible]
             [illegible].000      [illegible]
         .0  [illegible] [illegible]  -1.608         100.0   [illegible] [illegible] [illegible]
  [illegible] [illegible]  36.340   [illegible]      400.0   [illegible] [illegible] [illegible]
  [illegible] [illegible]  42.014   [illegible]   [illegible] [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible]   1200.0   [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible]
  [illegible]    4.773     45.074   [illegible]   [illegible] [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible]
  [illegible] [illegible]  55.260   [illegible]   [illegible]    5.017   [illegible] [illegible]
[illegible]      17.0074        9.[illegible]
         .0  [illegible]   35.720   [illegible]      100.0      7.798      35.720   [illegible]
  [illegible]    7.356   [illegible]  -0.711         400.0      7.087   [illegible]  [illegible]
      800.0      7.357     48.837      2.157         800.0      7.150   [illegible]  [illegible]
     1200.0   [illegible]  52.491      5.005        1200.0   [illegible] [illegible] [illegible]
     1400.0      7.706     55.027      6.025        1600.0      7.903      56.577   [illegible]
  [illegible] [illegible]  57.891     12.047        2200.0      8.415   [illegible]  [illegible]
     2400.0   [illegible]  59.424     16.214        2600.0      8.622      59.116   [illegible]
     2700.0   [illegible]  60.436     18.794        2800.0      8.706      60.752   [illegible]
  [illegible]    8.744     51.058     20.535        3000.0      8.720      61.355     21.411
  [illegible]    8.814     61.644     22.291        3200.0      8.846      61.924     23.174
            [illegible].000        0.0
         .0  [illegible]  [illegible] -2.075         100.0      6.958   [illegible]  [illegible]
  [illegible]    6.761     46.218     -0.665         400.0      7.196      51.091      3.724
  [illegible] [illegible]  54.096      2.210         800.0      8.063      56.361      3.786
  [illegible] [illegible]  58.192      5.427        1200.0      8.527   [illegible]     7.114
  [illegible] [illegible]  61.025   [illegible]     1600.0   [illegible] [illegible] [illegible]
  [illegible] [illegible]  64.210   [illegible]     2200.0      9.139   [illegible]     15.965
  [illegible] [illegible] [illegible]  17.504        2600.0      9.304      66.040   [illegible]
  [illegible] [illegible] [illegible] [illegible]   2800.0      9.455      67.317   [illegible]
  [illegible] [illegible] [illegible]  22.493        3000.0      9.551   [illegible]  [illegible]
  [illegible] [illegible] [illegible] [illegible] [illegible]   9.640   [illegible]  [illegible]
[illegible]   [illegible]      [illegible]
  [illegible] [illegible] [illegible] [illegible]    100.0   [illegible] [illegible]    -1.002
  [illegible] [illegible] [illegible] [illegible] [illegible]   5.370      41.013   [illegible]
  [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible]
  [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible] [illegible]
```

Table 3-16 (Continued)

Cards 13 (Cont'd)

```
  1400.0     5.197     47.735     1.000     1600.0     5.1[illegible]     48.420     [illegible]
  2000.0     5.101     49.570     [illegible]     2200.0     5.[illegible]     [illegible]     [illegible]
  2400.0     5.066     50.497     10.999     2600.0     5.053     [illegible]     [illegible]
  2700.0     5.046     51.092     12.516     2800.0     5.043     51.[illegible]     [illegible]
  2900.0     5.038     51.453     13.524     3000.0     5.034     51.[illegible]     [illegible]
  3100.0     5.031     51.788     14.551     3200.0     5.027     51.[illegible]     [illegible]
CL2     70.906        0.0
      .0     7.001     45.150     -2.194     100.0     7.001     [illegible]     -1.[illegible]
    200.0     7.576     50.156     -0.776     400.0     6.437     [illegible]     [illegible]
    600.0     8.741     59.212     2.507     800.0     6.078     61.[illegible]     [illegible]
   1000.0     9.956     63.727     6.115     1200.0     9.610     [illegible]     [illegible]
   1400.0     9.051     66.767     9.718     1600.0     9.066     67.[illegible]     [illegible]
   1800.0     9.149     70.013     13.179     2000.0     9.164     [illegible]     [illegible]
   2400.0     9.223     71.087     16.855     2600.0     9.[illegible]     [illegible]     [illegible]
   2700.0     9.295     72.777     21.069     2800.0     9.[illegible]     [illegible]     [illegible]
   2900.0     9.346     73.443     23.493     3000.0     9.[illegible]     [illegible]     [illegible]
   3100.0     9.403     74.060     25.[illegible]     3200.0     9.[illegible]     74.[illegible]     [illegible]
HCL     30.465        -22.063
      .0     6.959     37.041     -2.065     100.0     6.9[illegible]     37.041     -1.[illegible]
    200.0     6.761     41.065     -0.683     400.0     6.973     41.[illegible]     [illegible]
    600.0     7.067     47.534     [illegible]     800.0     7.1[illegible]     [illegible]     [illegible]
   1000.0     7.557     53.250     5.05[illegible]     1200.0     7.[illegible]     54.[illegible]     [illegible]
   1400.0     8.343     55.875     [illegible]     1600.0     8.[illegible]     [illegible]     [illegible]
   1800.0     8.509     58.030     [illegible]     2000.0     8.614     59.[illegible]     [illegible]
   2200.0     8.703     60.399     16.379     2400.0     8.778     61.[illegible]     [illegible]
   2600.0     8.814     61.431     19.707     2800.0     8.844     61.752     [illegible]
   2800.0     8.874     62.063     20.[illegible]     3000.0     8.902     62.[illegible]     [illegible]
   3000.0     8.928     62.550     22.750     3200.0     8.953     [illegible]     [illegible]
H2      [illegible]        0.0
      .0     6.955     38.170     -2.076     100.0     6.9[illegible]     38.170     -1.[illegible]
    200.0     6.727     42.992     -0.6[illegible]     400.0     6.9[illegible]     47.[illegible]     [illegible]
    600.0     7.146     50.[illegible]     [illegible]     800.0     7.[illegible]     [illegible]     [illegible]
   1000.0     7.51[illegible]     54.[illegible]     [illegible]     1200.0     8.[illegible]     [illegible]     [illegible]
   1400.0     [illegible]     57.212     [illegible]     1600.0     8.[illegible]     [illegible]     10.[illegible]
   1800.0     [illegible]     60.222     13.418     2000.0     8.072     61.[illegible]     [illegible]
   2200.0     8.721     61.[illegible]     16.[illegible]     2400.0     8.774     [illegible]     [illegible]
   2400.0     [illegible]     62.[illegible]     19.517     2600.0     8.8[illegible]     [illegible]     [illegible]
   2600.0     8.[illegible]     63.[illegible]     21.[illegible]     2800.0     8.855     [illegible]     [illegible]
   2800.0     8.[illegible]     64.[illegible]     23.[illegible]     3000.0     8.866     64.[illegible]     [illegible]
```

Cards 14

```
H1
  1.0   1.0   1.0   1.0   3.0   1.0   1.0   1.0   1.0   1.0   1.0   1.0   1.0

  [illegible]   [illegible]   [illegible]   1.0  10.0   1.0   1.0   1.0   1.0   1.0   1.0   1.0
H3
  1.0   [illegible]   1.0   1.0  10.0   1.0   1.0  20.0   1.0   1.0   1.0   1.0
```

Cards 15

```
H     [illegible]   +M1    =H2O   +M1                    22 6.10-[illegible]  [illegible]   0.0
[illegible]   +H    +M1    =OH    +M1                    21 [illegible]  0.0   0.0
[illegible]   +     +M1    =O2    +M1                    [illegible] [illegible]-[illegible]  1.0   -34[illegible].0
H     +H    +M2    =H2    +M2                    22 2.00-30  1.0   0.0
[illegible]   +     +M3    =CO2   +M3                    23 2.00-33  0.0   -90[illegible].0
H     +[illegible]   +M1    =HCO   +M1                    [illegible] 1.10-31  1.0   0.0
[illegible]   +H          =H2    +C                     14 1.40-14-1.0   -7000.0
[illegible]   +[illegible]          =H     +O2                    11 4.00-11  0.0   0.0
[illegible]   +H2         =H2O   +H                     14 1.00-17-2.0   -2[illegible]0.0
[illegible]   +[illegible]          =[illegible]   +H                     14 1.[illegible]-19-[illegible]   1600.0
CH    +[illegible]          =[illegible]   +[illegible]                    [illegible] 1.0  -11  [illegible].0   -11[illegible]0.0
CH    +[illegible]          =H2O   +C[illegible]                    1[illegible] 1.[illegible]-14-1.0   -100[illegible]
[illegible]   +[illegible]          =[illegible]   +[illegible]                    1[illegible] [illegible]00-12  [illegible]   -[illegible]
```

Table 3-16 (Concluded)

Cards 15 (Cont'd)

Cards 16

Card 17

Card 20

Card 21

Card 23

Card 24

Card 25

Card 26

Card 27

Card 28

Card 29

Card 30

Card 31

Card 32

Cards 33b

Cards 34b

Table 3-17

EXAMPLE PROBLEM 6 PERTINENT SOLUTION

TWO PHASE CHECK CASE USING NON-EQUILIBRIUM PROGRAM DATE 100475 PAGE 1

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

GAS-PARTICLE FLOW SOLUTION

CASE NO. 1 PAGE 1

1 PARTICLE(10MICRON)--SKM NOZZLE(RC/RT=2), NON-EQUILIBRIUM CHEMISTRY

RUN CONTROL PARAMETERS

ICON(1)	ICON(2)	ICON(3)	ICON(4)	ICON(5)	ICON(6)	ICON(7)	ICON(8)
3	2	20	15	1	0	1	2

ICON(9)	ICON(10)	ICON(11)	ICON(12)	ICON(13)	ICON(14)	ICON(15)	ICON(16)
0	5	1	1	0	0	0	11010

FLOW CALCULATIONS ARE IN ENGLISH UNITS WITH THE R,X COORDINATES IN FEET

THE FLOW FIELD DATA WILL NOT WRITTEN ON TAPE

UPPER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
1	0	-.10000+01	.20574+02	.00000	-.10000+01	-.68037+01	.15882+01
2	0	.00000	.00000	.00000	.45784+00	.18151+01	.23294+01
2	0	.00000	-.42870-02	.17936-01	.44407+00	.18041+01	.25876+01
2	0	.00000	-.18072-02	-.21431-02	.49816+00	.17556+01	.29192+01
2	0	.00000	.54416-03	-.24129-01	.56640+00	.16852+01	.35109+01
2	0	.00000	.57623-03	-.24493-01	.56779+00	.16835+01	.44396+01
2	0	.00000	.61760-03	-.25099-01	.57064+00	.16790+01	.55024+01
2	0	.00000	.48125-03	-.22721-01	.55694+00	.17053+01	.63770+01
2	0	.00000	.41850-03	-.21441-01	.54827+00	.17248+01	.76373+01
2	0	.00000	.32946-03	-.19316-01	.53131+00	.17697+01	.86488+01
2	0	.00000	.26175-03	-.18004-01	.51943+00	.18057+01	.10261+02
2	0	.00000	.22569-03	-.16245-01	.50105+00	.18696+01	.11216+02
2	0	.00000	.20578-03	-.15559-01	.49318+00	.18997+01	.12000+02
2	1	.00000	.00000	-.80133-02	.40098+00	.22751+01	.12667+02
3	0	.57900+03	.19000+01	.12500+01	.00000	.00000	.10000+04

LOWER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
2	0	.00000	.00000	.00000	.00000	.00000	.10000+04

Table 3-17 (Continued)

```
TWO PHASE CHECK CASE USING NON-EQUILIBRIUM PROGRAM                                   DATE 100475        PAGE    2

SPECIE THERMODYNAMIC AND REACTION DATA
NT,NS,NR,NM,ICTAPE,KGUP,IDIDO=   20   12   15    3    0    8    0

PRANDTL NUMBER =    .7000000E+00
BASE VISCOSITY =    .1865119E-05
EXPONENT       =    .6700000E+00

                    REACTIONS BEING CONSIDERED      KR=A*EXP(B/RT**M)/T**N      A          N        B        M     R-TYPE  K-TYPE
    1   H    + OH   + M1   = H2O   + M1                                      2.219+22   2.0       .0       .0      2       2
    2   O    + H    + M1   = OH    + M1                                      7.260+15    .0       .0       .0      2       1
    3   O    + O    + M1   = O2    + M1                                      1.379+18   1.0     -390.0     .0      2       4
    4   H    + H    + M2   = H2    + M2                                      1.016+18   1.0       .0       .0      2       2
    5   CO   + O    + M3   = CO2   + M3                                      7.260+14    .0     -4000.0    .0      2       3
    6   H    + CL   + M1   = HCL   + M1                                      3.993+16   1.0       .0       .0      2       2
    7   OH   + H            = H2    + O                                      8.435+09  -1.0     -7000.0    .0      1       4
    8   OH   + O            = H     + O2                                     2.410+13    .0       .0       .0      1       1
    9   OH   + H2           = H2O   + H                                      6.025+06  -2.0     -2900.0    .0      1       4
   10   OH   + CO           = CO2   + H                                      6.627+04  -2.0      1600.0    .0      1       4
   11   OH   + OH           = H2O   + O                                      6.025+12    .0     -1100.0    .0      1       3
   12   OH   + HCL          = H2O   + CL                                     6.025+09  -1.0     -1000.0    .0      1       4
   13   O    + HCL          = OH    + CL                                     1.205+12    .0     -4500.0    .0      1       3
   14   H    + CL2          = HCL   + CL                                     1.205+14    .0     -2400.0    .0      1       3
   15   CL   + H2           = HCL   + H                                      4.820+13    .0     -5260.0    .0      1       3

                    CATALYTIC SPECIES BEING CONSIDERED

                M1   = 1.00 CO    , 2.00 CO2   , 1.00 H     , 1.00 H2    , 3.00 H2O   , 1.00 O     , 1.00 OH    ,
                       1.00 O2    , 1.00 CL    , 1.00 CL2   , 1.00 HCL   , 1.00 N2    ,

                M2   = 1.00 CO    , 3.00 CO2   ,20.00 H     , 1.00 H2    ,10.00 H2O   , 1.00 O     , 1.00 OH    ,
                       1.00 O2    , 1.00 CL    , 1.00 CL2   , 1.00 HCL   , 1.00 N2    ,

                M3   = 1.50 CO    , 3.00 CO2   , 1.00 H     , 1.00 H2    ,10.00 H2O   , 1.00 O     , 1.00 OH    ,
                      20.00 O2    , 1.00 CL    , 1.00 CL2   , 1.00 HCL   , 1.00 N2    ,

SPECIE MOLE FRACTIONS ON THE START LINE ARE READ FROM CARDS

POINT
  1     CO          CO2         H           H2          H2O         O           OH          O2          CL          CL2
        .25335+00   .18930-01   .27600-01   .28554+00   .15906+00   .33000-03   .57000-02   .70000-04   .97500-02   .10000-04

  1     HCL         N2
        .14952+00   .92140-01

CHAMBER PRESSURE (ATM) =    .37697+02 CHAMBER TEMPERATURE (DEG-K) =    .33910+04

                    THERE ARE  1 PARTICLE SPECIES PRESENT IN THE GAS-PARTICLE MIXTURE

                                    RUN CUTOFF INFORMATION
                    UPPER BOUNDARY                                  LOWER BOUNDARY
        R=    .10000+03   X=   -.15000+03   THETA=    .00000    R=    .00000    X=    .50000+02   THETA=    .90000+02
```

Table 3-17 (Continued)

```
TWO PHASE CHECK CASE USING NON-EQUILIBRIUM PROGRAM                                   DATE 100475        PAGE    3

                                   PARTICLE PHYSICAL DATA
          SPECIE   RADIUS        MASS DENSITY      EMISSIVITY      ACCM. COEFF.
            1      .10000+02      .25000+03        .00000          .00000

        THE PARTICLES CONSTITUTE 40.28 PERCENT BY WEIGHT FLOW OF THE GAS-PARTICLE MIXTURE
                   THE INDIVIDUAL PERCENTAGES ARE  1.00
        THE PARTICLE TEMPERATURE-ENTHALPY TABLE WILL BE READ IN WITH ENGLISH      UNITS
```

Table 3-17 (Continued)

```
TWO PHASE CHECK CASE USING NON-EQUILIBRIUM PROGRAM                                    DATE 100475        PAGE    4

                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                          CASE NO.    1                                                    PAGE    2

( PARTICLE(10MICRON)--SRM NOZZLE(RC/RT=2), NON-EQUILIBRIUM CHEMISTRY

                                    PARTICLE TEMPERATURE-ENTHALPY TABLE

                PHASE CHANGE DATA *** TMELT=  .417000+04 HSOLID=  .278514+08 HLIQUID=  .403481+08
                                      CPMELT=   .84971+04 CPSOLID=   .66976+04
```

Table 3-17 (Continued)

TWO PHASE CHECK CASE USING NON-EQUILIBRIUM PROGRAM DATE 100475 PAGE 5

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

GAS-PARTICLE FLOW SOLUTION

CASE NO. 1 PAGE 3

; PARTICLE(10MICRON)--SRM NOZZLE(RC/RT=2), NON-EQUILIBRIUM CHEMISTRY

PARTICLE DRAG TABLE

I	RE	DRAG COEF
1	.00000	.10000+01
2	.12500+01	.10000+01
3	.12550+01	.10000+01
4	.12600+01	.10010+01
5	.12650+01	.10020+01
6	.15820+01	.10630+01
7	.19950+01	.11410+01
8	.25100+01	.12240+01
9	.31600+01	.13150+01
10	.39800+01	.14120+01
11	.50100+01	.15170+01
12	.63100+01	.16250+01
13	.79500+01	.17450+01
14	.10000+02	.18740+01
15	.12600+02	.20260+01
16	.15820+02	.21860+01
17	.19950+02	.23640+01
18	.25100+02	.25550+01
19	.31600+02	.27600+01
20	.39800+02	.30000+01
21	.50100+02	.32520+01
22	.63100+02	.32520+01
23	.79500+02	.38250+01
24	.10000+03	.41550+01
25	.31600+03	.79000+01
26	.10000+04	.20000+02
27	.10010+04	.20020+02
28	.10000+06	.20000+04

Table 3-17 (Continued)

```
TWO PHASE CHECK CASE USING NON-EQUILIBRIUM PROGRAM                                   DATE 100475        PAGE    6
                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                          CASE NO.    1                                                    PAGE    4
 1 PARTICLE(10MICRON)--SKN NOZZLE(RC/RT=2), NON-EQUILIBRIUM CHEMISTRY
                    THE MESH CONSTRUCTION WILL BE CONTROLED BY THE FOLLOWING VARIABLES
     DL INTERIOR=   .205+01 DX AXIS=   .200+00 DL LIM=   .300+00 DL DELETE=   .200-02 DEG P.H.=   .400+01 F=   .375+00
```

Table 3-17 (Continued)

```
TWO PHASE CHECK CASE USING NON-EQUILIBRIUM PROGRAM                                   DATE 100475        PAGE    7

                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                        CASE NO.    1                                                    PAGE    5

 1 PARTICLE(10MICRON)--SHM NOZZLE(RC/RT=2), NON-EQUILIBRIUM CHEMISTRY

LINE POINT  DSCRIP - REGIME        R            X            M          THETA       ENTROPY      VELOCITY     M-TOTAL   ITR
                              MACH ANGLE   PRESSURE     DENSITY     TEMPERATURE   GAS CONST.   LOCAL GAMMA   SHOCK ANGLE
 PARTICLE DATA
  SPECIL POINT  DESCRIPTION        V          THETA          D M          ENTHALPY       DENSITY        TEMPERATURE

   1     1   INPUT   - CONTIN   .00000     .47463+00    .11001+01    .22446-06    .00000       .45975+04    .20983+08    0
                                .65369+02    .23736+03    .24693-02    .55195+04    .25078+04    .12618+01
 PARTICLE DATA
      1    1                    .351177+04    .00000       .25980+00    .52657+08    .10284-02    .56186+04
CHEMICAL SPECIE MOLE FRACTIONS
CO      2.5335-01   CO2     1.8930-02   H       2.7600-02   H2      2.8554-01   H2O     1.5906-01   O       3.3000-04   OH      5.7000-03
O2      7.0000-05   CL      9.7500-03   CL2     1.0000-05   HCL     1.4952-01   N2      9.0140-02
-----------------------------------------------------------------------------------------------------------------------------------

   1     2   INPUT   - CONTIN   .12067+00    .47463+00    .11001+01    .31613+00    .00000       .45975+04    .20983+08    0
                                .65369+02    .23736+03    .24693-02    .55195+04    .25078+04    .12618+01
 PARTICLE DATA
      1    2                    .351177+04    -.16577+00   .25980+00    .52657+08    .10284-02    .56186+04
CHEMICAL SPECIE MOLE FRACTIONS
CO      2.5335-01   CO2     1.8930-02   H       2.7600-02   H2      2.8554-01   H2O     1.5906-01   O       3.3000-04   OH      5.7000-03
O2      7.0000-05   CL      9.7500-03   CL2     1.0000-05   HCL     1.4952-01   N2      9.0140-02
-----------------------------------------------------------------------------------------------------------------------------------

   1     3   INPUT   - CONTIN   .24135+00    .47463+00    .11001+01    .63225+00    .00000       .45975+04    .20983+08    0
                                .65369+02    .23736+03    .24693-02    .55195+04    .25078+04    .12618+01
 PARTICLE DATA
      1    3                    .351177+04    -.33155+00   .25980+00    .52657+08    .10284-02    .56186+04
CHEMICAL SPECIE MOLE FRACTIONS
CO      2.5335-01   CO2     1.8930-02   H       2.7600-02   H2      2.8554-01   H2O     1.5906-01   O       3.3000-04   OH      5.7000-03
O2      7.0000-05   CL      9.7500-03   CL2     1.0000-05   HCL     1.4952-01   N2      9.0140-02
-----------------------------------------------------------------------------------------------------------------------------------

   1     4   INPUT   - CONTIN   .36262+00    .47463+00    .11001+01    .94838+00    .00000       .45975+04    .20983+08    0
                                .65369+02    .23736+03    .24693-02    .55195+04    .25078+04    .12618+01
 PARTICLE DATA
      1    4                    .351177+04    -.49732+00   .25980+00    .52657+08    .10284-02    .56186+04
CHEMICAL SPECIE MOLE FRACTIONS
CO      2.5335-01   CO2     1.8930-02   H       2.7600-02   H2      2.8554-01   H2O     1.5906-01   O       3.3000-04   OH      5.7000-03
O2      7.0000-05   CL      9.7500-03   CL2     1.0000-05   HCL     1.4952-01   N2      9.0140-02
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NOTES: (1) Typical printout for the startline data surface.
(2) Some points have been omitted for demonstration purposes.

Table 3-17 (Continued)

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TWO PHASE CHECK CASE USING NON-EQUILIBRIUM PROGRAM                                   DATE 100475        PAGE    21

                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                          CASE NO.    1                                                  PAGE    17

 1 PARTICLE(10MICRON)--SRM NOZZLE(RC/RT=2), NON-EQUILIBRIUM CHEMISTRY

LINE POINT  DSCRIP - REGIME        R              X              M              THETA          ENTROPY        VELOCITY       H-TOTAL    ITR
                              MACH ANGLE     PRESSURE       DENSITY      TEMPERATURE      GAS CONST.     LOCAL GAMMA    SHOCK ANGLE
 PARTICLE DATA
  SPECIE POINT  DESCRIPTION        V              THETA            D M            ENTHALPY          DENSITY          TEMPERATURE

  12     1  WALL   - CONTIN    .00000         .75656+00      .10972+01      .00000         .35507+02      .45806+04      .20483+08    4
                              .65703+02      .23215+03      .24191-02      .55191+04      .25039+04      .12613+01
 PARTICLE DATA
       1    1                 .377147+04       .30000          .19381+00       .52442+08       .96507-03       .55934+04
CHEMICAL SPECIE MOLE FRACTIONS
CO      2.5347-01   CO2     1.9240-02   H       2.5783-02   H2      2.8655-01   H2O     1.5974-01   O       2.7828-04   OH      5.0653-03
O2      6.2410-05   CL      9.2317-03   CL2     1.1623-05   HCL     1.5029-01   N2      9.0283-02
-----------------------------------------------------------------------------------------------------------------------------------

  12     2  INTER  - CONTIN    .12214+00      .75626+00      .10971+01      .28146+00      .35481+02      .45804+04      .20483+08    5
                              .65710+02      .23217+03      .24193-02      .55192+04      .25039+04      .12613+01
 PARTICLE DATA
       1    2                 .377122+04      -.30002-01       .19382+00       .52443+08       .96504-03       .55934+04
CHEMICAL SPECIE MOLE FRACTIONS
CO      2.5347-01   CO2     1.9240-02   H       2.5786-02   H2      2.8655-01   H2O     1.5974-01   O       2.7836-04   OH      5.0661-03
O2      6.2428-05   CL      9.2328-03   CL2     1.1625-05   HCL     1.5029-01   N2      9.0283-02
-----------------------------------------------------------------------------------------------------------------------------------

  12     3  INTER  - CONTIN    .24427+00      .75536+00      .10970+01      .56369+00      .35423+02      .45801+04      .20484+08    5
                              .65720+02      .23221+03      .24196-02      .55193+04      .25039+04      .12613+01
 PARTICLE DATA
       1    3                 .377057+04      -.60341-01       .19390+00       .52443+08       .96511-03       .55935+04
CHEMICAL SPECIE MOLE FRACTIONS
CO      2.5347-01   CO2     1.9240-02   H       2.5789-02   H2      2.8655-01   H2O     1.5974-01   O       2.7844-04   OH      5.0670-03
O2      6.2447-05   CL      9.2338-03   CL2     1.1627-05   HCL     1.5028-01   N2      9.0282-02
-----------------------------------------------------------------------------------------------------------------------------------

  12     4  INTER  - CONTIN    .36639+00      .75386+00      .10969+01      .84617+00      .35322+02      .45796+04      .20486+08    5
                              .65738+02      .23227+03      .24202-02      .55195+04      .25039+04      .12613+01
 PARTICLE DATA
       1    4                 .376949+04      -.91734-01       .19403+00       .52445+08       .96531-03       .55936+04
CHEMICAL SPECIE MOLE FRACTIONS
CO      2.5347-01   CO2     1.9239-02   H       2.5795-02   H2      2.8654-01   H2O     1.5973-01   O       2.7859-04   OH      5.0687-03
O2      6.2480-05   CL      9.2357-03   CL2     1.1630-05   HCL     1.5028-01   N2      9.0282-02
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```

NOTES: (1) Typical printout for a data surface inside the nozzle.
(2) Some points have been omitted for demonstration purposes.

Table 3-17 (Continued)

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TWO PHASE CHECK CASE USING NON-EQUILIBRIUM PROGRAM                                   DATE 100475        PAGE    25
                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                                CASE NO.    1                                            PAGE   21
 1 PARTICLE(IOM(CHON)--AN NOZZLE(RC/RT=2), NON-EQUILIBRIUM CHEMISTRY
 ---------------------------------------------------------------------------------------------------------------------
 PNT POINT  DSCRIP - REGIME          P              X              M            THETA        ENTROPY      VELOCITY     H-TOTAL   ITR
                                  MACH ANGLE     PRESSURE       DENSITY     TEMPERATURE    GAS CONST.   LOCAL GAMMA   SHOCK ANGLE
 PARTICLE DATA
  SPECIE POINT  DESCRIPTION          V              THETA            D M            ENTHALPY        DENSITY          TEMPERATURE
 ---------------------------------------------------------------------------------------------------------------------
  14    16  INTER - CONTIN      .56191+01      .12693+02      .27992+01      .10488+02      .00000        .91296+04      .21706+08    4
                                 .20927+02      .14112+02      .24475-03      .33782+04      .24579+04     .12793+01
 PARTICLE DATA
  PARTICLES ARE PRESENT AT THIS POINT
 CHEMICAL SPECIE MOLE FRACTIONS
 0      2.9569-01   CO2    2.9186-02   H      2.8396-03   H2     3.0614-01   H2O    1.6858-01   O      8.1234-07   OH     1.1580-04
 2      1.8725-07   CL     1.1474-03   CL2    1.1289-07   HCL    1.6137-01   N2     9.1976-02
 ---------------------------------------------------------------------------------------------------------------------
 14    17  INTER - CONTIN      .58356+01      .12652+02      .27815+01      .10873+02      .00000        .90945+04      .21686+08    4
                                 .21976+02      .14580+02      .25115-03      .34611+04      .24578+04     .12786+01
 PARTICLE DATA
 PARTICLES ARE PRESENT AT THIS POINT
 CHEMICAL SPECIE MOLE FRACTIONS
 0      2.9600-01   CO2    2.9025-02   H      2.8188-03   H2     3.0596-01   H2O    1.6875-01   O      8.2101-07   OH     1.1629-04
 2      1.8973-07   CL     1.1375-03   CL2    1.2263-07   HCL    1.6139-01   N2     9.1978-02
 ---------------------------------------------------------------------------------------------------------------------
 14    18  WALL - CONTIN       .60465+01      .12667+02      .27670+01      .11198+02      .00000        .90661+04      .21595+08    4
                                 .21186+02      .14980+02      .25690-03      .34164+04      .24578+04     .12785+01
 PARTICLE DATA
 PARTICLES ARE PRESENT AT THIS POINT
 CHEMICAL SPECIE MOLE FRACTIONS
 0      2.9670-01   CO2    2.8927-02   H      2.7838-03   H2     3.0591-01   H2O    1.6865-01   O      8.1384-07   OH     1.1698-04
 2      1.8793-07   CL     1.1224-03   CL2    1.2940-07   HCL    1.6141-01   N2     9.1979-02
 ---------------------------------------------------------------------------------------------------------------------
 14    19  PRN-NR - CONTIN     .60465+01      .12667+02      .28952+01      .14518+02      .00000        .92668+04      .21595+08    4
                                 .20216+02      .11677+02      .21397-03      .32520+04      .24578+04     .12817+01
 PARTICLE DATA
 PARTICLES ARE PRESENT AT THIS POINT
 CHEMICAL SPECIE MOLE FRACTIONS
 0      2.9670-01   CO2    2.8927-02   H      2.7838-03   H2     3.0591-01   H2O    1.6885-01   O      8.1384-07   OH     1.1898-04
 2      1.8793-07   CL     1.1224-03   CL2    1.2940-07   HCL    1.6141-01   N2     9.1979-02
 ---------------------------------------------------------------------------------------------------------------------
```

NOTES: (1) Typical printout for a data surface containing a Prandtl-Meyer Expansion.
(2) Some points have been omitted for demonstration purposes.

AD-A094 633 LOCKHEED MISSILES AND SPACE CO INC HUNTSVILLE AL HUN--ETC F/G 21/8.2
SUPERSONIC FLOW OF CHEMICALLY REACTING GAS-PARTICLE MIXTURES. V--ETC(U)
JAN 76 M M PENNY, S D SMITH, P G ANDERSON NAS9-14517
UNCLASSIFIED LMSC-HREC-TR-D496555-2 NL

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Table 3-17 (Concluded)

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TWO PHASE CHECK CASE USING NON-EQUILIBRIUM PROGRAM                                   DATE 100475        PAGE    42

                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                          CASE NO.    1                                                  PAGE    38

1 PARTICLE(10MICRON)--SRM NOZZLE(RC/RT=2), NON-EQUILIBRIUM CHEMISTRY

I E POINT  DSCRIP - REGIME        Q            X            M            THETA        ENTROPY      VELOCITY     M-TOTAL    ITR
                                MACH ANGLE   PRESSURE    DENSITY    TEMPERATURE   GAS CONST.   LOCAL GAMMA   SHOCK ANGLE
PARTICLE DATA
 SPECIE POINT  DESCRIPTION      V            THETA          U M          ENTHALPY        DENSITY        TEMPERATURE
 27    1  WALL   - CONTIN    .00000       .13734+02    .25946+01    .00000       .11737+03    .85038+04    .17024+08    3
                             .22670+02    .66679+01    .11434-03    .34107+04    .24622+04    .12791+01
PARTICLE DATA
      1    1                .774589+04     .00000       .23124+00    .39259+08    .62302-04    .41700+04
CHEMICAL SPECIE MOLE FRACTIONS
0     2.4797-01   CO2    2.9378-02   H    5.2823-03   H2   3.0515-01   H2O  1.5793-01   O    2.8732-06   OH   2.1999-04
2     6.5941-07   CL     2.1216-03   CL2  1.1881-07   HCL  1.6012-01   N2   9.1819-02
-----------------------------------------------------------------------------------------------------------------------
 27   20  FREEBD - CONTIN    .62558+01    .13077+02    .33207+01    .24502+02    .61533+00    .98356+04    .21588+08    6
                             .17526+02    .55336+01    .11739+03    .27619+04    .24578+04    .12924+01
PARTICLE DATA
0 PARTICLES ARE PRESENT AT THIS POINT
CHEMICAL SPECIE MOLE FRACTIONS
0     2.4877-01   CO2    2.9037-02   H    2.7775-03   H2   3.0402-01   H2O  1.5881-01   O    3.5230-07   OH   4.5175-05
2     1.5190-07   CL     1.1952-03   CL2  7.0311-09   HCL  1.6134-01   N2   9.1980-02
-----------------------------------------------------------------------------------------------------------------------
 28    1  WALL   - CONTIN    .00000       .13770+02    .25947+01    .00000       .12106+03    .85039+04    .17022+08    3
                             .22668+02    .66557+01    .11414-03    .34105+04    .24622+04    .12791+01
PARTICLE DATA
      1    1                .774920+04     .00000       .23029+00    .39237+08    .62024-04    .41700+04
CHEMICAL SPECIE MOLE FRACTIONS
0     2.4796-01   CO2    2.9391-02   H    5.2800-03   H2   3.0517-01   H2O  1.5792-01   O    2.8694-06   OH   2.1980-04
2     6.5906-07   CL     2.1205-03   CL2  1.1876-07   HCL  1.6012-01   N2   9.1819-02
-----------------------------------------------------------------------------------------------------------------------
 28   20  FREEBD - CONTIN    .62735+01    .13110+02    .33214+01    .24445+02    .92792+00    .98364+04    .21588+08    6
                             .17522+02    .55270+01    .11728+03    .27612+04    .24578+04    .12924+01
PARTICLE DATA
0 PARTICLES ARE PRESENT AT THIS POINT
CHEMICAL SPECIE MOLE FRACTIONS
0     2.4878-01   CO2    2.9049-02   H    2.7769-03   H2   3.0403-01   H2O  1.5880-01   O    3.5164-07   OH   4.5097-05
2     1.4873-07   CL     1.1956-03   CL2  6.9973-09   HCL  1.6134-01   N2   9.1980-02
-----------------------------------------------------------------------------------------------------------------------
```

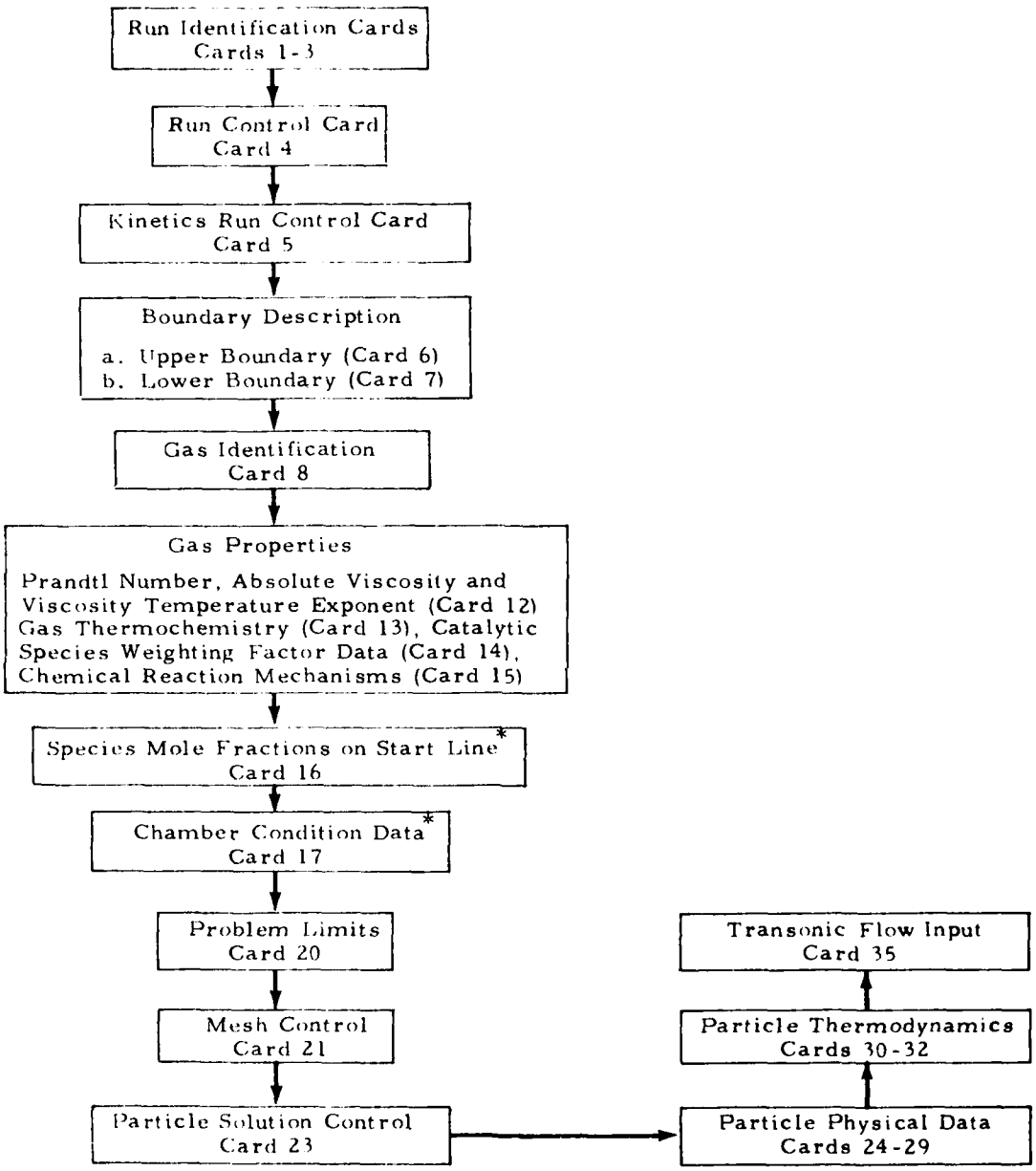
NOTES: (1) Typical printout for a data surface in the exhaust plume.
(2) Some points have been omitted for demonstration purposes.

Example Problem 7

Example problem 7 is the same as example problem 6 except that the start line is calculated internal to the program. Table 3-18 presents a flow chart of the input data for the specified problem. Note that Card 35 replaces Cards 33b and 34b of example problem 6. A listing of the pertinent solution is omitted as it is basically the same as for example problem 6.

Table 3-18

REQUIRED INPUT FORMAT FOR EXAMPLE PROBLEM 7



*If species mole fractions are input on tape (ICTAPE=1) cards 16 and 17 are not required.

Example Problem 8

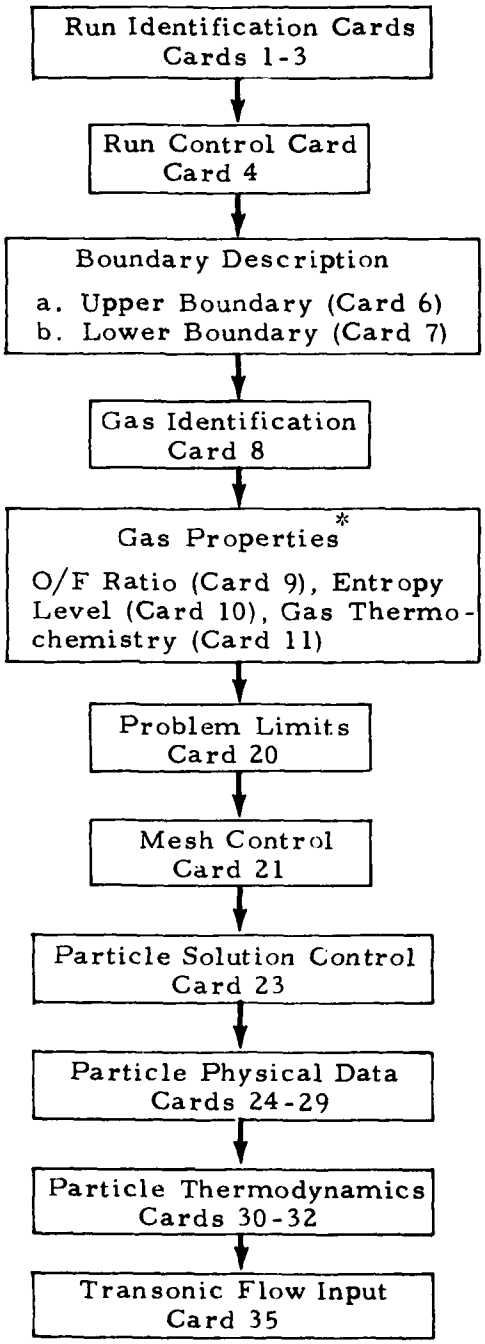
This problem analyzes a two-phase ideal gas flow field with the following stipulations:

1. Free molecular flow calculations are not to be considered.
2. The gas properties are to be read from cards, and
3. The start line is to be calculated internal to the program.

Table 3-19 presents first a flow chart and then a listing of the required input data for the specified problem. Table 3-20 presents a listing of the pertinent solution.

Table 3-19

REQUIRED INPUT FORMAT FOR EXAMPLE PROBLEM 8



*If gas properties are input on tape (ICON(1)=2) Cards 9, 10 and 11 are not required.

Table 3-19 (Concluded)

```
Cards      {TWO PHASE IDEAL GAS CHECK CASE
 1-3
Card 4          1     0   2540051     1     0     1     2     1    15   52     11                 02505
                     1.278071462.4517025 16.366          0      1.3261493 2.466111  17.
                     1.401649582.4899160818.             0      1.476722832.5150353 19.
                     1.551346332.5414608320.             0      1.6254973 2.5691848 21.
                     1.699153  2.5981983322.             0      1.7722913 2.6284933323.
                     1.844889582.66006   24.             0      1.8881803 2.6796065 24.6
                     1.904525  2.6855416724.6            0      2.0116    2.7345666724.6
                     2.1186666 72.7835833324.6           0      2.225733332.8326083324.6
                     2.332808332.861625  24.6            0      2.449708332.935     24.4824
                     2.590833332.9989583324.2765         0      2.749408333.07005   24.0146
                     2.922458333.1466    23.7123         0      3.108308333.2275833323.3785
                     3.305833333.3122416723.0204         0      3.514091673.399925  22.6438
Cards 6              3.732425  3.4901333322.2526         0      3.960241663.582425  21.8503
                     4.19715   3.6764583321.4390         0      4.44285   3.7718833321.0217
                     4.696775  3.8683916720.5999         0      4.9587    3.9657416720.1754
                     5.2283666 74.0636916719.7495        0      5.5096    4.1620666719.3
                     5.7900416 74.2606166718.8967        0      6.081658334.3592333318.4715
                     6.380191674.4577333318.0482         0      6.6854    4.55595   17.6279
                     6.997325  4.6538166717.2099         0      7.315733334.7511833316.7952
                     7.640516674.8479416716.3840         0      7.971566674.944     15.4766
                     8.308783335.0392583315.5732         0      9.001341675.2270916714.7792
                     9.356533335.3195    14.3888         0      9.717558335.410825  14.0020
                     10.08418335.5009666713.6222         0      10.45669175.58995   13.2456
                     10.834975 5.6776916712.8733         0      11.21874175.7641083312.5063
                     11.608175 5.8492    12.1434         0      12.0031   5.9326833311.7854
                     12.40336676.0151166711.4326         1      12.67025836.068552  11.2024
         3   0       10.                                                1000.      2.26791667
Card 7   2   0                                                          1000.
Card 8   SHUTTLE 700 PC                MKS        1     1
Card 9    .0
Card 10   .0                  1
Card 11   .0        20.245    1.25       3411.     47.632     .4810     .000934    .67
Card 20  100.       -100.     0.0        0.0       50.        90.
Card 21  2.0        .2        .2         .002       4.        .75
Card 23                                 1
Card 24  .40123
Card 25  1.0
Card 26  6.0
Card 27  250.
Card 28
Card 29
Card 30  AL203 EQ. OF STATE          IENG
Card 31    1
Card 32  4170.0     1112.8    1612.1     0.3395    0.2676
Cards 35 {$DATA THID=30.,THFD=7.,THJD=10.,THIW=16.366,RRT=2.,CAPN=.67,ZAX=.672
         {$END
```

Table 3-20

EXAMPLE PROBLEM 8 PERTINENT SOLUTION

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 52 PAGE 1

TWO PHASE IDEAL GAS CHECK CASE

RUN CONTROL PARAMETERS

ICON(1)	ICON(2)	ICON(3)	ICON(4)	ICON(5)	ICON(6)	ICON(7)	ICON(8)
1	0	25	40051	1	0	1	2

ICON(9)	ICON(10)	ICON(11)	ICON(12)	ICON(13)	ICON(14)	ICON(15)	ICON(16)
2	15	52	1	0	0	0	2505

FLOW CALCULATIONS ARE IN ENGLISH UNITS WITH THE R,X COORDINATES IN FEET

THE FLOW FIELD DATA WILL NOT WRITTEN ON TAPE

UPPER BOUNDARY POINTS

TYPE	ITRANS	X	R	THETA
2	0	.12781+01	.24517+01	.28564+00
2	0	.13261+01	.24661+01	.29671+00
2	0	.14016+01	.24899+01	.31416+00
2	0	.14767+01	.25150+01	.33161+00
2	0	.15513+01	.25415+01	.34907+00
2	0	.16255+01	.25692+01	.36652+00
2	0	.16992+01	.25982+01	.38397+00
2	0	.17723+01	.26285+01	.40143+00
2	0	.18449+01	.26601+01	.41888+00
2	0	.18162+01	.26796+01	.42935+00
2	0	.19645+01	.26855+01	.42935+00
2	0	.20116+01	.27346+01	.42935+00
2	0	.21187+01	.27836+01	.42935+00
2	0	.22257+01	.28326+01	.42935+00
2	0	.23326+01	.28816+01	.42935+00
2	0	.24497+01	.29353+01	.42935+00
2	0	.25928+01	.29992+01	.42935+00
2	0	.27499+01	.30701+01	.41913+00
2	0	.29925+01	.31466+01	.41386+00
2	0	.31183+01	.32276+01	.40623+00
2	0	.33258+01	.33122+01	.40178+00
2	0	.35141+01	.33999+01	.39521+00
2	0	.37324+01	.34901+01	.38838+00
2	0	.39612+01	.35824+01	.38136+00
2	0	.41971+01	.36765+01	.37416+00
2	0	.44428+01	.37719+01	.36672+00
2	0	.46968+01	.38684+01	.35954+00
2	0	.49587+01	.39657+01	.35213+00
2	0	.52284+01	.40637+01	.34469+00

Table 3-20 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 52

TWO PHASE IDEAL GAS CHECK CASE

UPPER BOUNDARY POINTS

TYPE	ITRANS	X	H	THETA			
2	0	.55056+01	.41621+01	.33085+00			
2	0	.57900+01	.42026+01	.32981+00			
2	0	.60817+01	.43592+01	.32239+00			
2	0	.63802+01	.44577+01	.31500+00			
2	0	.66859+01	.45559+01	.30766+00			
2	0	.69973+01	.46538+01	.30037+00			
2	0	.73157+01	.47512+01	.29313+00			
2	0	.76405+01	.48479+01	.28595+00			
2	0	.79716+01	.49440+01	.27884+00			
2	0	.83088+01	.50393+01	.27182+00			
2	0	.86513+01	.52271+01	.25795+00			
2	0	.90565+01	.53195+01	.25113+00			
2	0	.97176+01	.54108+01	.24440+00			
2	0	.10084+02	.55010+01	.23775+00			
2	0	.10457+02	.55900+01	.23118+00			
2	0	.10835+02	.56777+01	.22468+00			
2	0	.11219+02	.57641+01	.21828+00			
2	0	.11608+02	.58492+01	.21194+00			
2	0	.12003+02	.59329+01	.20569+00			
2	0	.12403+02	.60151+01	.19954+00			
2	1	.12672+02	.60666+01	.19552+00			
3	0	.10000+02	.00000	.00000	.00000	.00000	.10000+04

LOWER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
2	0	.00000	.00000	.00000	.00000	.00000	.10000+04

THERE ARE 1 PARTICLE SPECIES PRESENT IN THE GAS-PARTICLE MIXTURE

THE FOLLOWING GAS PROPERTIES IN ENGLISH UNITS ARE FOR SHUTTLE 700 PC

IDEAL GAS PROPERTIES

V	H	GAMMA	TO	PO	RK	VIS	EXP
.00000	.24594+04	.12500+01	.61398+04	.70000+03	.48100+00	.19508-05	.67000+00

Table 3-20 (Continued)

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                    GAS-PARTICLE FLOW SOLUTION                                          PAGE    3
                    CASE NO.   52

TWO PHASE IDEAL GAS CHECK CASE

                    RUN CUTOFF INFORMATION
                UPPER BOUNDARY                                  LOWER BOUNDARY
   R=   .10000+03   X=   -.10000+03   THETA=   .00000   R=   .00000   X=   .50000+02   THETA=   .90000+02

                    PARTICLE PHYSICAL DATA
   SPECIE   RADIUS        MASS DENSITY    EMISSIVITY    ACCM. COEFF.
     1      .00000+01     .25000+03       .00000        .00000

   THE PARTICLES CONSTITUTE 42.12 PERCENT BY WEIGHT FLOW OF THE GAS-PARTICLE MIXTURE
              THE INDIVIDUAL PERCENTAGES ARE   1.00
   THE PARTICLE TEMPERATURE-ENTHALPY TABLE WILL BE READ IN WITH ENGLISH      UNITS

                    PARTICLE TEMPERATURE-ENTHALPY TABLE

   PHASE CHANGE DATA *** TMELT=   .41700+04 HSOLID=   .27851+08 HLIQUID=   .40348+08
                         CPMELT=   .84971+04 CPSOLID=   .66976+04
```

Table 3-20 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 52

TWO PHASE IDEAL GAS CHECK CASE

PARTICLE DRAG TABLE

I	RE	DRAG COEF
1	.00000	.10000+01
2	.12500+01	.10000+01
3	.12550+01	.10000+01
4	.12600+01	.10010+01
5	.12650+01	.10020+01
6	.15820+01	.10630+01
7	.19950+01	.11410+01
8	.25100+01	.12240+01
9	.31620+01	.13150+01
10	.39800+01	.14120+01
11	.50120+01	.15170+01
12	.63100+01	.16250+01
13	.79500+01	.17450+01
14	.10000+02	.18740+01
15	.12500+02	.20200+01
16	.15820+02	.21860+01
17	.19950+02	.23640+01
18	.25100+02	.25550+01
19	.31620+02	.27600+01
20	.39800+02	.30000+01
21	.50120+02	.32520+01
22	.63100+02	.32520+01
23	.79500+02	.36250+01
24	.10000+03	.41550+01
25	.31620+03	.79000+01
26	.10000+04	.20000+02
27	.10010+04	.20020+02
28	.10000+06	.20000+04

Table 3-20 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 52

TWO PHASE IDEAL GAS CHECK CASE

GASEOUS STARTING LINE INFO

R	X	H	THETA	S	MACH ANGLE	SHOCK ANGLE	H-TOTAL
.00000	.15240+01	.10678+01	.00000	.49594+03	.66822+02	.00000	.74705+08
.98068-01	.15236+01	.10881+01	.34952+00	.49623+03	.66780+02	.00000	.74705+08
.19614+00	.15225+01	.10892+01	.70118+00	.49710+03	.66654+02	.00000	.74704+08
.29422+00	.15205+01	.10909+01	.10571+01	.49857+03	.66445+02	.00000	.74702+08
.39227+00	.15177+01	.10933+01	.14196+01	.50063+03	.66155+02	.00000	.74699+08
.49034+00	.15142+01	.10965+01	.17809+01	.50332+03	.65785+02	.00000	.74696+08
.58841+00	.15099+01	.11004+01	.21735+01	.50665+03	.65338+02	.00000	.74692+08
.68646+00	.15048+01	.11050+01	.25699+01	.51064+03	.64816+02	.00000	.74687+08
.78454+00	.14989+01	.11105+01	.29830+01	.51535+03	.64222+02	.00000	.74681+08
.88261+00	.14922+01	.11168+01	.34156+01	.52080+03	.63559+02	.00000	.74674+08
.98066+00	.14847+01	.11241+01	.38710+01	.52705+03	.62828+02	.00000	.74666+08
.10787+01	.14764+01	.11322+01	.43527+01	.53417+03	.62033+02	.00000	.74657+08
.11768+01	.14674+01	.11414+01	.48643+01	.54223+03	.61174+02	.00000	.74647+08
.12749+01	.14575+01	.11518+01	.54099+01	.55131+03	.60255+02	.00000	.74636+08
.13731+01	.14469+01	.11633+01	.59938+01	.56154+03	.59275+02	.00000	.74623+08
.14712+01	.14355+01	.11762+01	.66204+01	.57304+03	.58235+02	.00000	.74609+08
.15691+01	.14233+01	.11905+01	.72948+01	.58596+03	.57136+02	.00000	.74593+08
.16672+01	.14103+01	.12065+01	.80218+01	.60050+03	.55977+02	.00000	.74576+08
.17652+01	.13965+01	.12244+01	.88069+01	.61688+03	.54757+02	.00000	.74556+08
.18633+01	.13820+01	.12444+01	.96554+01	.63536+03	.53476+02	.00000	.74533+08
.19614+01	.13666+01	.12667+01	.10573+02	.65629+03	.52132+02	.00000	.74508+08
.20594+01	.13505+01	.12918+01	.11564+02	.68007+03	.50723+02	.00000	.74480+08
.22141+01	.13252+01	.13347+01	.13173+02	.72141+03	.48522+02	.00000	.74431+08
.22556+01	.13169+01	.13520+01	.13792+02	.73826+03	.47702+02	.00000	.74411+08
.23536+01	.12974+01	.13842+01	.15033+02	.77403+03	.46086+02	.00000	.74369+08
.24517+01	.12781+01	.14294+01	.16368+02	.81545+03	.44396+02	.00000	.74322+08

PARTICLE START LINE PROPERTIES

POINT	SPECIE	U	V	THETA	ENTHALPY	DENSITY
1	1	.39807+04	.00000	.00000	.50838+08	.15069-02
2	1	.39816+04	.14438+02	.20776+00	.50836+08	.15057-02
3	1	.39844+04	.28963+02	.41677+00	.50832+08	.15019-02
4	1	.39870+04	.43751+02	.62840+00	.50823+08	.14959-02
5	1	.39959+04	.58876+02	.84422+00	.50811+08	.14879-02
6	1	.40240+04	.74514+02	.10662+01	.50793+08	.14784-02
7	1	.40145+04	.92857+02	.12965+01	.50768+08	.14669-02
8	1	.40271+04	.10813+03	.15381+01	.50736+08	.14572-02
9	1	.40417+04	.12662+03	.17943+01	.50693+08	.14467-02
10	1	.40595+04	.14664+03	.20640+01	.50643+08	.14370-02
11	1	.40785+04	.16856+03	.23667+01	.50573+08	.14287-02
12	1	.41105+04	.19280+03	.26920+01	.50492+08	.14221-02

Table 3-20 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO. 52

PAGE 8

TWO PHASE IDEAL GAS CHECK CASE

POINT	SPECIE	U	V	THETA	ENTHALPY	DENSITY
13	1	.41250+04	.21981+03	.30502+01	.50395+08	.14175-02
14	1	.41522+04	.25604+03	.34461+01	.50281+08	.14149-02
15	1	.41821+04	.28393+03	.38840+01	.50150+08	.14140-02
16	1	.42147+04	.32166+03	.43670+01	.50002+08	.14142-02
17	1	.42500+04	.36403+03	.48957+01	.49837+08	.14145-02
18	1	.42874+04	.41039+03	.54670+01	.49659+08	.14133-02
19	1	.43283+04	.46245+03	.60723+01	.49472+08	.14090-02
20	1	.43715+04	.51307+03	.66948+01	.49283+08	.13969-02
21	1	.44156+04	.56613+03	.73071+01	.49102+08	.13802-02
22	1	.44610+04	.61609+03	.78616+01	.48942+08	.13495-02
23	1	.45319+04	.67176+03	.84327+01	.48795+08	.12736-02

THE MESH CONSTRUCTION WILL BE CONTROLLED BY THE FOLLOWING VARIABLES

DL INTERIOR= .200+01 DX AXIS= .200+00 DL LIM= .200+00 DL DELETE= .200-02 DEG P.M.= .400+01 F= .760+00

Table 3-20 (Continued)

```
                    SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                                          GAS-PARTICLE FLOW SOLUTION
                                          CASE NO.   52                                                    PAGE   12

TWO PHASE IDEAL GAS CHECK CASE

LINE POINT  DSCRIP - REGIME        R            X            M            THETA        ENTROPY      VELOCITY     M-TOTAL   ITR
                              MACH ANGLE   PRESSURE     DENSITY    TEMPERATURE    GAS CONST.   LOCAL GAMMA   SHOCK ANGLE
 PARTICLE DATA
  SPECIE POINT  DESCRIPTION        V            THETA          D M          ENTHALPY        DENSITY        TEMPERATURE

  1    26  INPUT - CONTIN     .23536+01    .12974+01    .13882+01    .15333+02    .77403+03    .53733+04    .74369+08    0
                              .46266+02    .16232+03    .19498-02    .48818+04    .24554+04    .12500+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

  1    28  INPUT - CONTIN     .24517+01    .12781+01    .14294+01    .16368+02    .81545+03    .64995+04    .74122+08    0
                              .44376+02    .15[illegible]9+03    .18254-02    .48223+04    .24554+04    .12500+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

   GAS MASS FLOW RATE =      .73752+04    PARTICLE MASS FLOW RATE =      .29617+04    MIXTURE MASS FLOW RATE =      .10337+05

                                          PARTICLE PERCENT LOADINGS
                                                RADIUS     LOADING
                                              .00000+01   .10000+03

   PARTICLE PERCENT LOADING RELATIVE TO THE GAS =   .40158+02   PARTICLE PERCENT LOADING RELATIVE TO THE MIXTURE =   .28652+02

                                          MOMENTUM INTEGRATION RESULTS
                                          FORCEX       FORCEY       TORQZ       ISP
                                        -.20786+07    .00000      .00000    .20111+03
                                 DELFXG       DELFYG       TORQZG       DELFXP       DELFYP       TORQZP
                              -.47147+05    .00000       .00000       .39146+06    .00000       .00000
```

NOTES: (1) Typical printout for the startline data surface.
(2) Some points have been omitted for demonstration purposes.

Table 3-20 (Continued)

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                    GAS-PARTICLE FLOW SOLUTION
                    CASE NO.   52                                                    PAGE   16

TWO PHASE IDEAL GAS CHECK CASE

LINE POINT  DESCRIP - REGION        M          X          M          THETA      ENTROPY    VELOCITY   H-TOTAL   IIR
                                  MACH ANGLE  PRESSURE   DENSITY    TEMPERATURE  GAS CONST.  LOCAL GAMMA  SHOCK ANGLE

 PARTICLE DATA
  PARTICLE POINT  DESCRIPTION        X          THETA        U M        ENTHALPY     DENSITY     TEMPERATURE

 2    1  WALL   - CONTIN        .23904+01  .13164+01  .14664+01  .15374+02  .77403+03  .54128+04  .74309+08   3
                               .46592+02  .13944+03  .19223-02  .46645+04  .24554+04  .12500+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT

 2    2  WALL   - CONTIN        .24544+01  .12095+01  .14344+01  .16639+02  .81545+03  .55143+04  .74322+08   3
                               .44221+02  .14923+03  .18153-02  .46154+04  .24554+04  .12500+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT

                                          PRESSURE INTEGRATION RESULTS
                                FORCEX     FORCEY     TORQZ      DELFX      DELFY      ISP
                              -.22799+07  .00000    .00000   -.10653+04  .00000   .20121+03

          PERCENT CHANGE IN MASS, MOMENTUM AND ENERGY NUMERICAL INTEGRATION FOR LINE  2 RELATIVE TO THE START LINE
          PERCENT CHANGE IN MASS FLOW, GAS =     -.19320-01    PARTICLE =     -.56777-01    MIXTURE =     -.30052-01
          PERCENT CHANGE IN MOMENTUM, GAS =     .62371+04    PARTICLE =     .12728+00    MIXTURE =    -.52166+00  ISP =    -.49115+00
          PERCENT CHANGE IN ENERGY, GAS =    -.34322-01    PARTICLE =     .31157+00    MIXTURE =    -.26113-01

 3    1  WALL   - CONTIN        .00000  .15889+01  .16987+01  .00000  .50956+03  .44254+04  .74686+08   5
                               .65924+02  .25956+03  .29551-02  .52860+04  .24554+04  .12500+01
 PARTICLE DATA
                               .41237+00  .00000  .99237-01  .50696+08  .14823+02  .53876+04
 NO PARTICLES ARE PRESENT AT THIS POINT

 3    2  WALL   - CONTIN        .24623+01  .13135+01  .14461+01  .16833+02  .81545+03  .55501+04  .74322+08   3
                               .43752+02  .14654+03  .17936-02  .47993+04  .24554+04  .12500+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT

 4    1  WALL   - CONTIN        .00000  .16232+01  .11355+01  .00000  .51664+03  .44490+04  .74679+08   5
                               .64752+02  .25593+03  .29557-02  .52767+04  .24554+04  .12500+01
 PARTICLE DATA
                               .12494+04  .00000  .99416-01  .50623+08  .14702+02  .53792+04
```

NOTES: (1) Typical printout for a data surface inside the nozzle.
(2) Some points have been omitted for demonstration purposes.

Table 3-20 (Continued)

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
                    GAS-PARTICLE FLOW SOLUTION
                    CASE NO.   52                                                    PAGE   60

TWO PHASE IDEAL GAS CHECK CASE

LINE POINT  DSCRIP - REGIME        M          X          M        THETA     ENTROPY    VELOCITY    M-TOTAL   ITR
                              MACH ANGLE  PRESSURE   DENSITY  TEMPERATURE  GAS CONST.  LOCAL GAMMA  SHOCK ANGLE
 PARTICLE DATA
  SPECIE POINT  DESCRIPTION      V        THETA        D M        ENTHALPY    DENSITY    TEMPERATURE
 -----------------------------------------------------------------------------------------------------------
 +3    +1  PRM-MN - CONTIN   .62666+01  .12673+02  .39426+01  .42170+02  .81545+03  .99063+04  .74322+08   3
                             .14693+02  .21198+01  .60438-04  .20573+04  .24554+04  .12500+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT
 -----------------------------------------------------------------------------------------------------------
 +3    +2  PRM-MN - CONTIN   .62666+01  .12673+02  .41549+01  .46937+02  .81545+03  .10078+05  .74322+08   3
                             .13927+02  .14902+01  .45590-04  .19170+04  .24554+04  .12500+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT
 -----------------------------------------------------------------------------------------------------------
 +3    +3  PRM-MN - CONTIN   .62666+01  .12673+02  .43828+01  .49911+02  .81545+03  .10244+05  .74322+08   3
                             .13187+02  .10263+01  .33888-04  .17799+04  .24554+04  .12500+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT
 -----------------------------------------------------------------------------------------------------------
 +3    +4  PRM-MN - CONTIN   .62666+01  .12673+02  .46274+01  .53782+02  .81545+03  .10403+05  .74322+08   3
                             .12479+02  .69613+00  .24798-04  .16463+04  .24554+04  .12500+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT
 -----------------------------------------------------------------------------------------------------------
 +3    +5  PRM-MN - CONTIN   .62666+01  .12673+02  .48922+01  .57648+02  .81545+03  .10555+05  .74322+08   3
                             .11795+02  .46179+00  .17858-04  .15166+04  .24554+04  .12500+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT
 -----------------------------------------------------------------------------------------------------------
 +3    +6  PRM-MN - CONTIN   .62666+01  .12673+02  .51858+01  .61524+02  .81545+03  .10701+05  .74322+08   3
                             .11131+02  .27938+00  .12615-04  .13964+04  .24554+04  .12500+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT
 -----------------------------------------------------------------------------------------------------------
 +3    +7  PRM-MN - CONTIN   .62666+01  .12673+02  .54936+01  .65346+02  .81545+03  .10846+05  .74322+08   3
                             .10468+02  .16927+00  .87439-05  .12685+04  .24554+04  .12500+01
 PARTICLE DATA
 NO PARTICLES ARE PRESENT AT THIS POINT
 -----------------------------------------------------------------------------------------------------------
```

NOTES: (1) Typical printout for a data surface containing a Prandtl-Meyer Expansion.
(2) Some points have been omitted for demonstration purposes.

Table 3-20 (Concluded)

```
SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM
GAS-PARTICLE FLOW SOLUTION
CASE NO.   52                                                                    PAGE   78

TWO PHASE IDEAL GAS CHECK CASE

LINE POINT  DESCRIP - REGIME        M            X            R            THETA        ENTROPY      VELOCITY     M-TOTAL    ITR
                                  MACH ANGLE   PRESSURE     DENSITY     TEMPERATURE    GAS CONST.   LOCAL GAMMA   SHOCK ANGLE
 PARTICLE DATA
  SPECIE POINT  DESCRIPTION         V            THETA          D R          ENTHALPY      DENSITY      TEMPERATURE

 111    44  FREEBD - CONTIN      .73951+01    .13299+02    .62166+01    .70594+02    .81545+03    .11097+05    .74322+08    2
                                 .72569+01    .67445-01    .39226-05    .10383+04    .24554+04    .12500+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

 112    1   WALL   - CONTIN      .00000       .15142+02    .24302+01    .00000       .42265+04    .80420+04    .76144+08    4
                                 .24321+02    .83717-01    .13758-03    .35687+04    .24554+04    .12500+01
 PARTICLE DATA
        1                        .784351+04   .00000       .59981-01    .25652+08    .64440-04    .38301+04
DUE TO GAS-PARTICLE STREAMLINE CROSSING THE POINT 29 HAS BEEN REPLACED

 112    44  FREEBD - CONTIN      .73922+01    .13153+02    .62166+01    .70845+02    .81545+03    .11097+05    .74322+08    2
                                 .72569+01    .67445-01    .39226-05    .10383+04    .24554+04    .12500+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

 113    1   WALL   - CONTIN      .00000       .15367+02    .24269+01    .00000       .42207+04    .80371+04    .76167+08    4
                                 .24339+02    .83792-01    .13752-03    .35734+04    .24554+04    .12500+01
 PARTICLE DATA
        1    1                   .785227+04   .00000       .55810-01    .25542+08    .63386-04    .38136+04

 113    44  FREEBD - CONTIN      .73956+01    .13215+02    .62166+01    .70649+02    .81545+03    .11097+05    .74322+08    2
                                 .72569+01    .67445-01    .39226-05    .10383+04    .24554+04    .12500+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT

 114    1   WALL   - CONTIN      .00000       .15581+02    .24236+01    .00000       .42335+04    .80317+04    .76184+08    4
                                 .24369+02    .83924-01    .13755-03    .35763+04    .24554+04    .12500+01
 PARTICLE DATA
        1                        .785145+04   .00000       .51694-01    .25441+08    .62401-04    .37986+04

DUE TO GAS-PARTICLE STREAMLINE CROSSING THE POINT 28 HAS BEEN REPLACED

 114    44  FREEBD - CONTIN      .73956+01    .13253+02    .62166+01    .70461+02    .81545+03    .11097+05    .74322+08    2
                                 .72569+01    .67445-01    .39226-05    .10383+04    .24554+04    .12500+01
 PARTICLE DATA
NO PARTICLES ARE PRESENT AT THIS POINT
```

NOTES: (1) Typical printout for a data surface in the exhaust plume.
(2) Some points have been omitted for demonstration purposes.

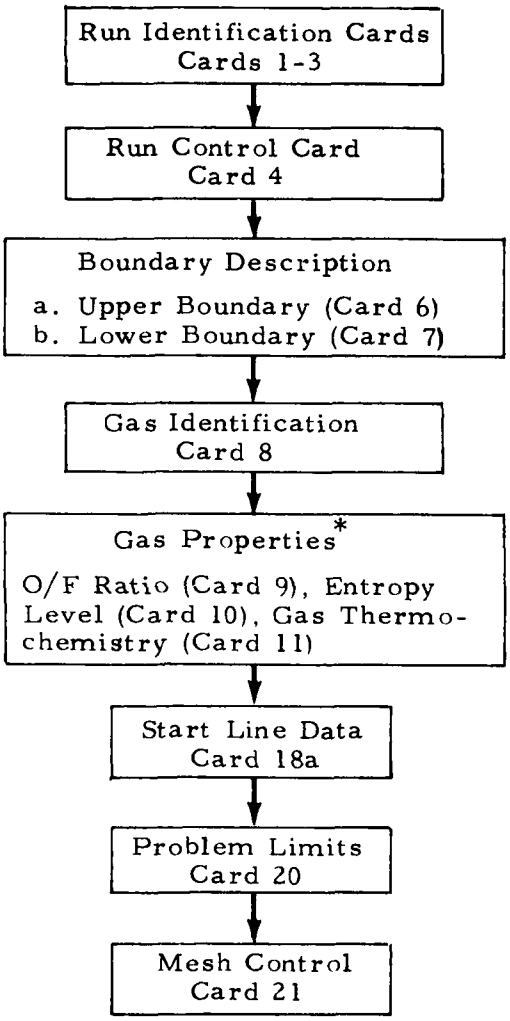
Example Problem 9

Example problem 9 is the same as example problem 8 except that a single phase ideal gas flow field will be analyzed.

Table 3-21 presents first a flow chart and then a listing of the input data for the specified problem. Table 3-22 presents a listing of the pertinent solution.

Table 3-21

REQUIRED INPUT FORMAT FOR EXAMPLE PROBLEM 9



*If gas properties are input on tape (ICON(1)=2) Cards 9, 10 and 11 are not required.

Table 3-21 (Concluded)

Cards 1-3	GASEOUS CHECK CASE						
Card 4	1	121	3	1	1	2 15	1 11 200
Cards 6	1	-1.	.50002	0.0	-1.0	-1.0607	.18659
	2 1				.27357	.32757	2.4560
	3	1400.					1000.
Card 7	2						1000.
Card 8	IDEAL GAS			ENG	1	1	
Card 9	.0						
Card 10	.0		1				
Card 11	.0	27.23473	1.1443	6049.8	40.827436		
Card 18a	.0	0.0	1.01				
Card 20	100.	-100.	0.0	0.0	4.0	90.	
Card 21	.2	.1	1.	.005	5.	.85	

Table 3-22

EXAMPLE PROBLEM 9 PERTINENT SOLUTION

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 1

GASEOUS CHECK CASE

RUN CONTROL PARAMETERS

ICON(1)	ICON(2)	ICON(3)	ICON(4)	ICON(5)	ICON(6)	ICON(7)	ICON(8)
1	0	21	3	1	0	1	2

ICON(9)	ICON(10)	ICON(11)	ICON(12)	ICON(13)	ICON(14)	ICON(15)	ICON(16)
0	15	1	1	0	0	0	2000

FLOW CALCULATIONS ARE IN ENGLISH UNITS WITH THE R,X COORDINATES IN FEET

THE FLOW FIELD DATA WILL NOT WRITTEN ON TAPE

UPPER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
1	0	-.10000+01	.50002+00	.00000	-.10000+01	-.10607+01	.18659+00
2	1	.00000	.00000	.00000	.27357+00	.32757+00	.24580+01
3	0	.14000+04	.00000	.00000	.00000	.00000	.10000+04

LOWER BOUNDARY

TYPE	ITRANS	A	B	C	D	E	MAX
2	0	.00000	.00000	.00000	.00000	.00000	.10000+04

THERE ARE 0 PARTICLE SPECIES PRESENT IN THE GAS-PARTICLE MIXTURE

THE FOLLOWING GAS PROPERTIES IN ENGLISH UNITS ARE FOR IDEAL GAS

IDEAL GAS PROPERTIES

V	R	GAMMA	TO	PO
.00000	.16252+04	.11443+01	.60498+04	.60000+03

STARTING LINE INFO

R	X	M	THETA	S	MACH ANGLE	SHOCK ANGLE	D/F
.00000	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.17677-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.35358-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.53037-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.70716-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.88395-01	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.10607+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.12375+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000

Table 3-22 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 2

GASEOUS CHECK CASE

STARTING LINE INFO

R	X	M	THETA	S	MACH ANGLE	SHOCK ANGLE	O/F
.14143+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.15911+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.17679+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.19447+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.21215+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.22983+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.24751+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.26518+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.28286+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.30054+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.31822+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.33590+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000
.35358+00	.00000	.10100+01	.00000	.00000	.81931+02	.00000	.00000

RUN CUTOFF INFORMATION

UPPER BOUNDARY

HB .10000+03 X= -.10000+03 THETA= .00000

LOWER BOUNDARY

R= .00000 X= .40000+01 THETA= .90000+02

THE MESH CONSTRUCTION WILL BE CONTROLED BY THE FOLLOWING VARIABLES

DL INTERIOR= .200+00 DX AXIS= .100+00 DL LIM= .100+01 DL DELETE= .500-02 DEG P.M.= .500+01 F= .850+00

Table 3-22 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 4

GASEOUS CHECK CASE

LINE	POINT	DSCRIP - REGIME	R / MACH ANGLE	X / PRESSURE	M / DENSITY	THETA / TEMPERATURE	ENTROPY / GAS CONST.	VELOCITY / LOCAL GAMMA	D/F / SHOCK ANGLE	ITM
1	14	INPUT - CONTIN	.22983+00	.00000	.10100+01	.00000	.00000	.34649+04	.00000	0
			.81931+02	.34164+03	.47833-02	.56351+04	.18252+04	.11443+01		
1	15	INPUT - CONTIN	.24751+00	.00000	.10100+01	.00000	.00000	.34649+04	.00000	0
			.81931+02	.34164+03	.47833-02	.56351+04	.18252+04	.11443+01		
1	16	INPUT - CONTIN	.26518+00	.00000	.10100+01	.00000	.00000	.34649+04	.00000	0
			.81931+02	.34164+03	.47833-02	.56351+04	.18252+04	.11443+01		
1	17	INPUT - CONTIN	.28206+00	.00000	.10100+01	.00000	.00000	.34649+04	.00000	0
			.81931+02	.34164+03	.47833-02	.56351+04	.18252+04	.11443+01		
1	18	INPUT - CONTIN	.30054+00	.00000	.10100+01	.00000	.00000	.34649+04	.00000	0
			.81931+02	.34164+03	.47833-02	.56351+04	.18252+04	.11443+01		
1	19	INPUT - CONTIN	.31822+00	.00000	.10100+01	.00000	.00000	.34649+04	.00000	0
			.81931+02	.34164+03	.47833-02	.56351+04	.18252+04	.11443+01		
1	20	INPUT - CONTIN	.33590+00	.00000	.10100+01	.00000	.00000	.34649+04	.00000	0
			.81931+02	.34164+03	.47833-02	.56351+04	.18252+04	.11443+01		
1	21	INPUT - CONTIN	.35358+00	.00000	.10100+01	.00000	.00000	.34649+04	.00000	0
			.81931+02	.34164+03	.47833-02	.56351+04	.18252+04	.11443+01		

THE MASS FLOW RATE IS = .209434+03

MOMENTUM INTEGRATION RESULTS

FORCEX	FORCEY	TORQZ	ISP
-.41877+05	.00000	.00000	.19995+03

NOTES: (1) Typical printout for the start line data surface.
(2) Some points have been omitted for demonstration purporses.

Table 3-22 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 23

GASEOUS CHECK CASE

LINE	POINT	DSCRIP	- REGIME	R MACH ANGLE	X PRESSURE	M DENSITY	THETA TEMPERATURE	ENTROPY GAS CONST.	VELOCITY LOCAL GAMMA	O/F SHOCK ANGLE	ITN
76	1	WALL	- CONTIN	.00000 .24455+02	.98905+00 .36990+02	.24156+01 .68547-03	.00000 .42574+04	.00000 .18252+04	.72031+04 .11443+01	.00000	3
76	21	WALL	- CONTIN	.57707+00 .26656+02	.91200+00 .52849+02	.22290+01 .93628-03	.15300+02 .44534+04	.00000 .18252+04	.67980+04 .11443+01	.00000	1
77	1	WALL	- CONTIN	.00000 .23928+02	.10512+01 .33552+02	.24655+01 .62945-03	.00000 .42054+04	.00000 .18252+04	.73070+04 .11443+01	.00000	3
77	21	WALL	- CONTIN	.59442+00 .26068+02	.97543+00 .48396+02	.22757+01 .86695-03	.15300+02 .44042+04	.00000 .18252+04	.69019+04 .11443+01	.00000	1
78	1	WALL	- CONTIN	.00000 .23526+02	.11168+01 .31031+02	.25052+01 .58792-03	.00000 .41642+04	.00000 .18252+04	.73882+04 .11443+01	.00000	3
78	21	WALL	- CONTIN	.61268+00 .25496+02	.10422+01 .44213+02	.23231+01 .80110-03	.15300+02 .43543+04	.00000 .18252+04	.70058+04 .11443+01	.00000	1
79	1	WALL	- CONTIN	.00000 .23277+02	.11849+01 .29517+02	.25305+01 .56277-03	.00000 .41380+04	.00000 .18252+04	.74393+04 .11443+01	.00000	3
79	21	WALL	- CONTIN	.63154+00 .24952+02	.11111+01 .40370+02	.23705+01 .73990-03	.15300+02 .43046+04	.00000 .18252+04	.71076+04 .11443+01	.00000	1
80	1	WALL	- CONTIN	.00000 .23202+02	.12544+01 .29068+02	.25383+01 .55528-03	.00000 .41300+04	.00000 .18252+04	.74548+04 .11443+01	.00000	2
80	21	WALL	- CONTIN	.45060+00 .24445+02	.11808+01 .36923+02	.24165+01 .68439-03	.15300+02 .42565+04	.00000 .18252+04	.72051+04 .11443+01	.00000	1
81	1	WALL	- CONTIN	.00000 .23282+02	.13240+01 .29547+02	.25300+01 .56328-03	.00000 .41385+04	.00000 .18252+04	.74382+04 .11443+01	.00000	2
81	21	WALL	- CONTIN	.66942+00 .23982+02	.12496+01 .33895+02	.24603+01 .63508-03	.15300+02 .42108+04	.00000 .18252+04	.72963+04 .11443+01	.00000	3
82	1	WALL	- CONTIN	.00000 .23417+02	.13927+01 .30365+02	.25162+01 .57689-03	.00000 .41528+04	.00000 .18252+04	.74104+04 .11443+01	.00000	2

NOTES: (1) Typical printout for a data surface inside the nozzle.
(2) Some points have been omitted for demonstration purposes.

Table 3-22 (Continued)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 30

GASEOUS CHECK CASE

LINE	POINT	DSCRIP	- REGIME	R / MACH ANGLE	X / PRESSURE	M / DENSITY	THETA / TEMPERATURE	ENTROPY / GAS CONST.	VELOCITY / LOCAL GAMMA	O/F / SHOCK ANGLE	ITR
97	14	INTER	- CONTIN	.63350+00	.25093+01	.29873+01	.98245+01	.00000	.82822+04	.00000	4
				.19557+02	.11649+02	.24973-03	.36802+04	.18752+04	.11443+01		
97	15	INTER	- CONTIN	.68433+00	.25002+01	.29967+01	.10463+02	.00000	.82980+04	.00000	4
				.19493+02	.11424+02	.24551-03	.36711+04	.18752+04	.11443+01		
97	16	INTER	- CONTIN	.73551+00	.24905+01	.30045+01	.11160+02	.00000	.83111+04	.00000	4
				.19441+02	.11240+02	.24205-03	.36636+04	.18752+04	.11443+01		
97	17	INTER	- CONTIN	.78696+00	.24800+01	.30104+01	.11920+02	.00000	.83209+04	.00000	4
				.19401+02	.11104+02	.23949-03	.36580+04	.18752+04	.11443+01		
97	18	INTER	- CONTIN	.83842+00	.24687+01	.30145+01	.12729+02	.00000	.83277+04	.00000	4
				.19374+02	.11009+02	.23770-03	.36541+04	.18752+04	.11443+01		
97	19	INTER	- CONTIN	.88997+00	.24567+01	.30172+01	.13572+02	.00000	.83322+04	.00000	4
				.19356+02	.10948+02	.23654-03	.36515+04	.18752+04	.11443+01		
97	20	INTER	- CONTIN	.94131+00	.24439+01	.30187+01	.14433+02	.00000	.83347+04	.00000	4
				.19346+02	.10914+02	.23590-03	.36500+04	.18752+04	.11443+01		
97	21	WALL	- CONTIN	.10000+01	.24580+01	.30237+01	.15300+02	.00000	.83514+04	.00000	4
				.19283+02	.10688+02	.23162-03	.36404+04	.18752+04	.11443+01		
97	22	PRNTHR	- CONTIN	.10000+01	.24580+01	.30741+01	.16769+02	.00000	.84260+04	.00000	4
				.18984+02	.97213+01	.21321-03	.35972+04	.18752+04	.11443+01		

NOTES: (1) Typical printout for a data surface containing a Prandtl-Meyer expansion.
(2) Some points have been omitted for demonstration purposes.

Table 3-22 (Concluded)

SUPERSONIC FLOW ANALYSIS USING THE LOCKHEED-HUNTSVILLE MULTIPLE SHOCK COMPUTER PROGRAM

CASE NO. 1 PAGE 35

GASEOUS CHECK CASE

LINE	POINT	DSCRIP	- REGIME	R MACH ANGLE	X PRESSURE	M DENSITY	THETA TEMPERATURE	ENTROPY GAS CONST.	VELOCITY LOCAL GAMMA	O/F SHOCK ANGLE	ITR
103	1	WALL	- CONTIN	.00000	.27461+01	.30081+01	.00000	.00000	.83171+04	.00000	2
				.19417+02	.11157+02	.24048-03	.36602+04	.18252+04	.11443+01		
103	22	FREEBD	- CONTIN	.10405+01	.26000+01	.30740+01	.15238+02	.00000	.84259+04	.00000	2
				.18984+02	.97222+01	.21323-03	.35972+04	.18252+04	.11443+01		
104	1	WALL	- CONTIN	.00000	.27883+01	.30227+01	.00000	.00000	.83415+04	.00000	2
				.19319+02	.10821+02	.23416-03	.36461+04	.18252+04	.11443+01		
104	22	FREEBD	- CONTIN	.10513+01	.26404+01	.30740+01	.14820+02	.00000	.84259+04	.00000	3
				.18984+02	.97222+01	.21323-03	.35972+04	.18252+04	.11443+01		
105	1	WALL	- CONTIN	.00000	.28313+01	.30375+01	.00000	.00000	.83659+04	.00000	2
				.19221+02	.10494+02	.22795-03	.36320+04	.18252+04	.11443+01		
105	22	FREEBD	- CONTIN	.10621+01	.26818+01	.30740+01	.14404+02	.00000	.84259+04	.00000	3
				.18984+02	.97222+01	.21323-03	.35972+04	.18252+04	.11443+01		
106	1	WALL	- CONTIN	.00000	.28751+01	.30523+01	.00000	.00000	.83904+04	.00000	2
				.19124+02	.10174+02	.22187-03	.36179+04	.18252+04	.11443+01		
106	22	FREEBD	- CONTIN	.10728+01	.27241+01	.30740+01	.13993+02	.00000	.84259+04	.00000	
				.18984+02	.97222+01	.21323-03	.35972+04	.18252+04	.11443+01		
107	1	WALL	- CONTIN	.00000	.29390+01	.30736+01	.00000	.00000	.84253+04	.00000	2
				.18987+02	.97301+01	.21338-03	.35976+04	.18252+04	.11443+01		
107	22	FREEBD	- CONTIN	.10879+01	.27862+01	.30740+01	.13412+02	.00000	.84259+04	.00000	2
				.18984+02	.97222+01	.21323-03	.35972+04	.18252+04	.11443+01		
108	1	WALL	- CONTIN	.00000	.30040+01	.30952+01	.00000	.00000	.84602+04	.00000	2
				.18849+02	.93015+01	.20514-03	.35772+04	.18252+04	.11443+01		
108	22	FREEBD	- CONTIN	.11029+01	.28503+01	.30740+01	.12837+02	.00000	.84259+04	.00000	2
				.18984+02	.97222+01	.21323-03	.35972+04	.18252+04	.11443+01		
109	1	WALL	- CONTIN	.00000	.30717+01	.31169+01	.00000	.00000	.84952+04	.00000	2
				.18713+02	.88881+01	.19715-03	.35568+04	.18252+04	.11443+01		

NOTES: (1) Typical printout for a data surface in the exhaust plume.
(2) Some points have been omitted for demonstration purposes.

Section 4
CONCLUSIONS

A versatile computer program has been described in the preceding sections. The code has numerous options which have necessitated a somewhat generalized set of input data. These options include:

- Gas-Particle Flows
- Chemistry
  - Equilibrium
  - Kinetics
  - Chemically Frozen
  - Constant Thermodynamics
- Single-Phase Solution
  - Non-Isoenergetic Flow
- Non-Continuum Flow
- Performance Calculations
- Shock Waves

In its present form, the code has the capability of producing data for the following applications:

- Gas/Gas-Particle Impingement (Heat Transfer Loads)
- Rocket Nozzle Performance (Thrust, I_{sp})
- IR Signatures (Radiating Species)
- RF Attenuation (Electron Densities)
- Plume Radiation (Radiative Heat Transfer Gas/Particles)
- Vehicle Base Pressure
- Base Heating (Convection-Recirculation)

A primary consequence of this work is the extension of gas-particle solutions to treat chemical kinetics for nozzle-exhaust plume flow fields. Since the code has the option of treating single-phase flow, chemical kinetics can also be included in liquid propellant motor analyses as well as solid propellant calculations. The method by which the kinetic equations are modeled also permits thermal nonequilibrium to be treated.

The RAMP code is an advance in the state of the art in the area of two-phase flowfield numerical solutions. Future development of the code may be done in the area of imbedded subsonic regions (Mach disks) and subsonic-supersonic mixing.

Section 5

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Appendix A

USER'S INPUT GUIDE FOR THE RAMP RADIAL LOOKUP PROGRAM

Appendix A

CARD 1 - Run control card

Format: 16I5

Column	Parameter	Value	Description
5	IORDR	0	Will not call data ordering routines but will execute lookup routines. Ordered flowfield tape must be input.
		1	Will order flowfield data and generate Radiance tape.
		2	Will order flowfield data but will not generate Radiance tape.
10	IWRITE	0	No intermediate printout in property lookup routines.
		1	Use a one only if problems are encountered with program and intermediate printout is necessary to determine problem.
14-15	ISP	0	Species and species concentrations will come from flowfield tapes or finite-rate chemistry case.
		N	Number of species and species concentrations to be read from cards (Assumes species and species concentrations constant throughout plume.) (25 max).
20	IDUM1	0	If two entropy tables are present on the RAMP tape both tables will be used to determine local flow properties and species concentrations.
		1	Only first entropy table will be used to determine flow properties.
			Ignore for finite rate chemistry case.

CARD 1 (Continued)

Column	Parameter	Value	Description
23-25	IXCUT	N	Number of axial cuts to be written on flowfield tape. The values of the cuts will be read from Card 10 (100 max)
26-30	KASE	N	Case number to be written on Radiance tape.
35	INUNIT	0	Output pressure and temperature in English units. Temperature, ^{o}R; pressure, lb/ft^2
		1	Output pressure and temperature in metric units. Temperature, ^{o}K; pressure, atm.
40	LSOLID	0	Do not perform 2-phase flow energy calculations for heating analysis.
		1	Perform 2-phase flow energy calculations.
45	LSOLGS	0	MOC input tape on Unit 8.
		1	RAMP input tape on Unit 8.
50	INRS	0	No radiation data on input tape.
		N	Number of radiating species on input tape.
54-55	NS	0	Equilibrium or frozen chemistry.
		N	Number of species on input tape for finite rate chemistry case (RAMP only) (25 max).
60	IPSTR	0	Pitot pressure data not on input tape.
		1	Pitot pressure data on input tape.
65	KUNIT	1	English units used internally.
		2	MKSunits used internally (Required only if NS>0).

CARD 2

Reference Card for Property Lookup. These data are used to non-dimensionalize the axial and radial coordinates which are to be looked up in the ordered flow field.

Format: 3E10.6

Column	Parameter	Description
1-10	XREFF	Axial coordinate to which each input axial station is referenced (ft or m).
11-20	ST	Reference length by which all input axial stations and radial coordinates are multiplied (ft or m).
21-30	RREFF	Radial coordinate to which each radial coordinate is referenced (ft or m).

NOTE: RREFF, XREFF and ST are used as follows (in main routine only):

X = X*ST–XREFF
R = R*ST–RREFF

CARD 3

This card contains the necessary information to limit the calculations to those areas of interest. Units are consistent with the ordered flow field.

Format: 8E10.6

Column	Parameter	Description
1-10	CUTDAT(1)	Radial coordinate defining upper cut off (ft or m).
11-20	CUTDAT(2)	Axial coordinate defining upper cut off (ft or m).
21-30	CUTDAT(3)	Angle cutoff line makes with horizontal (deg).

CARD 3 (Continued)

Column	Parameter	Description
31-40	CUTDAT(4)	Radial coordinate defining downstream cut off (ft or m).
41-50	CUTDAT(5)	Axial coordinate defining downstream cut off (ft or m).
51-60	CUTDAT(6)	Angle cut off line makes with horizontal (deg).

CARD 4

This card inputs radiation data only when INRS (Card 1) is greater than zero.

Format: 5(A6, 6X)

Column	Parameter	Description
1-6	AIDR(1)	Name of first initial radiating species.
13-18	AIDR(2)	Name of second initial radiating species.
.	.	.
.	.	.
.	.	.
	AIDR(K)	Name of last initial radiating species, where K=INRS.

CARD 5

This card inputs radiation data only when INRS (Card 1) is greater than zero.

Format: 5(A6, 6X)

Column	Parameter	Description
1-6	AIDRT(1)	Name of species that AIDR(1) transforms to during radiation process.
13-18	AIDRT(2)	Name of species that AIDR(2) transforms to during radiation process.
.	.	.
.	.	.
.	.	.
	AIDRT(K)	Name of species that AIDR(K) transforms to during radiation process.

CARD 6

Control card for the ordering section. Cards 6 and 7 are used only when IORDR (Card 1) is greater than zero.

Format: 16I5

Column	Parameter	Value	Description
5	ISTART		Ordering the flowfield data will begin with this characteristic line number.
10	ISIGN	-1	If the flow field was generated with a reflected shock from the nozzle axis, otherwise leave blank.
15	NUMBER		Number of flowfield data points desired per data record (max. of 300).
20	IDEL	>0	If any points are to be deleted from the flow field.

CARD 6 (Continued)

Column	Parameter	Value	Description
25	IPRINT	>0	If intermediate data are to be printed as the flow field is ordered by distance from the engine exit plane.
30	ITERM		Characteristic line number, where ordering of flowfield data is to be terminated. (This line is not used by program).
35	ISEND	1	If plume boundary is to be curve-fitted for use in the interpolation scheme.
		2	If only the cutoff limits read as input data are to be used to see if a point is within a prescribed boundary.
40	ISKIP		If ISEND = 1 every ISKIP line will be examined for a free boundary point.

CARD 7

Column	Parameter	Description
1-10	RREF*	Radial coordinate to which each flowfield data point will be referenced (ft or m).
11-20	XREF*	Axial coordinate to which each flowfield data point will be referenced (ft or m).
21-30	DELETE	One of two points with a distance between them less than DELETE will be deleted from the flowfield data. Will not delete shock point.
31-40	DIAM	Reference factor, units consistent with plume dimensions. Can be used to scale, etc., the local plume coordinates.

*The coordinates XREF and RREF are used to accomplish any desired coordinate system translation.

NOTE: RREF, XREF and DIAM are used as follows:

$$R = (R-RREF)/DIAM$$
$$X = (X-XREF)/DIAM$$

CARD 8

This card inputs particulate heat transfer data and is used only if LSOLID (Card 1) is greater than zero and when IORDR is greater than zero.

Format: 6E10.6

Column	Parameter	Description
1-10	ACOMCF	Accommodation coefficient.
11-20	TWALL	Wall temperature (^{o}R or ^{o}K).
21-30	CPS	Particulate phase heat capacity.

CARD 9

Species concentration cards (Input only if ISP >0 and NS = 0) these cards contain the species names and mole fractions if the species concentrations are constant throughout the plume. There are four species per card up to a maximum of 25 species. Overrides species on flowfield tape.

Format· 4(A6, 4X, E10.6)

Column	Parameter	Description
1-6	SONAME(I, 1)	Species name — left adjusted, consistent with RAMP species names.
11-20	AMO(I)	Mole fraction of species.

NOTE: Repeat SONAME and AMO, 4 pairs to a card until all ISP species are read in.

CARD 10

This card(s) reads in the axial stations and the radial increment to be used in constructing the radiance tape. There are 2 stations per card up to 100 stations.

Format: 6E10.6

Column	Parameter	Description
1-10	X(1)	First axial station at which radial distribution of flowfield properties are desired (ft or m).
11-20	DR(1)	Radial increment between data points along radial for station 1 (ft or m)
21-30	RMAX(1)	Maximum value of radial distance desired for station 1. If zero, program determines maximum (ft or m).
31-40	X(2)	Second axial station at which radial distribution of flowfield properties are desired.
41-50	DR(2)	Radial increment between data points along radial for station 2.
51-60	RMAX(2)	Maximum value of radial distance desired for station 2. If zero, program determines maximum.

Repeat until IXCUT (Card 1) number of stations have been input.

Table A-1

MAGNETIC TAPE ASSIGNMENTS FOR THE RAMP RADIAL LOOKUP PROGRAM

Where Required	Tape Units U-1108	Tape Unit Function
Section 1		
SORTCT	10	Flowfield tape generated by RAMP program-input.
Subroutine SORTCT is the controlling routine for this section which arranges the RAMP output in the form used by the data acquisition routines. This section is used once per flowfield calculation.	8	Flowfield data ordered for use in property lookup—output.
	2	Flowfield limits data—output.
	3	Scratch tape.
	4	Scratch tape for species concentrations & radiation data.
Section 2		
GENERATE RADIANCE TAPE	4	Radiance tape—output
This section performs the local property lookup and generates the radiance tape.	8	Ordered flowfield data generated by Section 1—input.
	2	Flowfield limits data generated by Section 1—input.

Appendix B

ON THE ACCURACY OF PREDICTED EXHAUST PLUME FLOWFIELD VARIABLES

Appendix B

ON THE ACCURACY OF PREDICTED EXHAUST PLUME FLOWFIELD VARIABLES*

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ABSTRACT

Various assumptions are used by many organizations to compute rocket motor plumes. In applying plume data, the question of accuracy invariably arises. Some guidelines are therefore needed to estimate the accuracy of the plume data based upon the assumptions that are employed. This paper is intended to serve as a guide for estimating plume accuracy and to alert the plume analyst to the magnitude of error which might be expected if certain assumptions are used. Much of the information contained in this paper, however, is based upon somewhat subjective data and/or certain cases from which some experience has been gained. The data presented should, therefore, be used judiciously, the problem at hand should be carefully considered, and the fact that the error bands have been somewhat grossly estimated should be kept in mind.

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INTRODUCTION

During the past several years sophisticated techniques for computing rocket motor exhaust plumes have been developed. The prediction methods can take into account such influencing parameters as combustion chamber losses, flow striations, reaction kinetics and non-continuum effects. When a plume flow field is to be computed, the degree of analytical sophistication that will be used should be based on an assessment of such factors as: (1) ultimate purpose of the data; (2) time available to accomplish the calculations; and (3) degree of accuracy required. In most cases, all effects that can be calculated should be included in the calculations. To include all effects may, of course, be time-consuming; this is not always practical if schedules are to be met. Plume data are therefore sometimes generated which circumvent the various effects that are felt to be small. Since much plume data are generated by using various assumptions, some guidelines are needed to estimate the accuracy of the resulting plumes based upon the assumptions that are employed.

Although an absolute accuracy cannot at this time be assigned to the final numbers generated for any given plume calculation, at least a reasonable estimate can be made of the anticipated accuracy, depending upon the various assumptions. Some of the assumptions influence specific regions of the flow field, and the accuracy of the calculations varies with position in the plume.

This document is intended to serve as a guide for estimating the accuracy of axisymmetric plume flowfield calculations. Much of the information, however, is based upon somewhat subjective data and/or certain cases (perhaps even unique cases) from which some experience has been gained. Also, only steady state rocket motor operation is considered. Ignition and shutdown transient influences are omitted.

DISCUSSION

The effects which are considered important in plume calculations are categorized and discussed in this section. Tables I and II summarize the important flowfield parameters and the estimated percentage of error that may be introduced by each item. The error that is discussed is the error which could exist if an accurate evaluation of the influence of the item is not included in the plume flowfield analysis. The error bands in Table I are considered to correspond to worst-on-worst or three-sigma cases for a 95 percent confidence interval. The error bands are rather large since they reflect the maximum values which have been observed. Most rocket motors will not encounter these effects to the extent shown in Table I. A set of data corresponding to an estimated one-sigma deviation for a 95 percent confidence interval is presented in Table II. The items which contribute to the accuracy bands shown in Tables I and II are discussed in the following paragraphs.

Motor Operating Conditions: Motor operating conditions refers to the fact that rocket motors are generally specified to operate at a nominal set of conditions (chamber pressure, mass flow rate, and oxidizer-to-fuel ratio (O/F)). Variations from nominal conditions frequently occur during actual operation. A band of ± 10 percent was arbitrarily assigned for chamber conditions (pressure, O/F ratio, mass flow). Influences of this ± 10 percent band on other motor and plume environmental conditions are shown in Table I and Table II.

Combustion Chamber Momentum Loss and Efficiency: Combustion chamber momentum loss and efficiency is included because combustion in a rocket motor does not take place at zero velocity as implied by an equilibrium, infinite area ratio calculation. The situation actually is analogous to heat addition in a finite area duct which results in a decrement in total pressure. The maximum momentum loss that can occur is a function of the propellant system and motor geometry and it can be as high as 20 percent of the actual pressure immediately downstream of the injector face. Most motors, however, fall in the range of 2 to 15 percent momentum loss (Ref. 1).

Coupled with the momentum loss is combustion efficiency; i.e., incomplete mixing and/or reaction of the incoming propellants. This anomally first appeared when experimental performance data were compared with computed data. Even when all known performance losses were included in the analytical prediction, some descrepancy still existed. This discrepancy has been termed combustion efficiency and several theories have been proffered as possible explanations. The JANNAF Performance Standardization Committee has recommended an arbitrary reduction in the initial propellant energy to account for this loss (Ref. 2). Recently, however, this committee has been working on a droplet varporization model which will be recommended as the explanation for combustion efficiency. Whatever its source, combustion efficiency must be properly estimated to increase the accuracy of the exhaust plume calculation. The most striking result of combustion efficiency is a temperature prediction considerably below that predicted by the usual adiabatic flame calculation. In this paper, the momentum loss and combustion efficiency problems are combined and assigned a maximum error, which corresponds to the deviations that have been observed between motor performance test data and theoretical results for no-momentum loss and for complete equilibrium chemistry combustion at a nominal motor operating value of O/F.

Flow Striations (O/F Ratio Gradient): The flow striation problem is a result of non-uniform distribution of propellant mixture ratio within the combustion chamber. Flow striations may be deliberately induced in the nozzle flow, as in the case of film cooling, or it may result from incomplete mixing and/or combustion in the combustion chamber. The effects that are introduced are variations of the thermochemical data due to combustion at a local O/F ratio which is different from the nominal O/F value (Ref. 3). Tables I and II show error bands relative to the nominal O/F value.

The flow striation effect may be closely related to the combustion efficiency problem; however, these effects are considered independently in this paper.

Reaction Kinetics: Reaction kinetics, as used here, involves the problem of appropriately defining the location in the flow field where the chemical reactions deviate from equilibrium enough that the flow can be considered chemically frozen. From this point on, the species concentrations are constant and the thermodynamic properties vary only with temperature. The problem thus is one of correctly assessing a representative freeze point. The error bands shown in the charts relate the error magnitudes resulting from comparison of results for a finite rate chemistry analysis (Ref. 4) and results obtained by an assumed freeze point based on an equilibrium/frozen chemistry analysis. The errors presented are the range of values which can be expected in the highly expanded plume. The errors in the field nearer the freeze point are not nearly as large. The major source of the errors is related to differences in the values of the thermodynamic properties used to calculate the flow field.

Non-Continuum Effects: The error caused by non-continuum effects is due to the lack of rigorous flow models which can consider the gradual deviation in thermodynamic properties which result as the rate of intermolecular collisions is reduced below a value corresponding to thermodynamic equilibrium. The error bands which are listed in Tables I and II for this item refer to variations which occur between a rigorous non-continuum solution (Refs. 5 and 6) and a sudden-freeze solution which uses continuum flow equations until a "free-molecular" condition is reached (Ref. 7). When this freeze point is reached, the flow calculation is handled as a free molecular calculation. In the transition flow region (Knudsen number greater than 0.1) the error increases until the sudden freeze condition is reached. The maximum error occurs near the freeze point and is the error shown in Tables I and II. Beyond the freeze point, the rigorous solution and the sudden freeze solution tend to converge toward common values (Knudsen number greater than 1.0). The sudden freeze solution yields results which show significant deviation in static temperature. Density and velocity calculations, however, are not greatly affected.

The error bands shown in Tables I and II are based upon the differences found between cases analyzed with: (1) a sudden freeze analysis; and (2) with a rigorous theoretical solution. An additional large error, not shown in the charts, would appear if the rigorous analysis were compared with an all continuum analysis. This would result from the fact that the temperature in a continuum analysis approaches a zero limit while the rigorous solution indicates that the temperature approaches a low but finite value.

Calculational Accuracy: This item is an arbitrary estimate of the maximum error conceivable for the numerical computational procedures used.

Viscous Effects (Boundary Layer): The viscous (boundary layer) effects of the nozzle flow have been shown to be of minor consequence on the inviscid flow in the nozzle. (That is, if the boundary layer is considered in terms of displacement thickness to alter the nozzle contour, the effect on the nozzle flow is generally negligible.) The effect considered here is that the boundary layer will influence the plume flow field to some degree and will cause the maximum expansion angle at the nozzle lip to be significantly different. Basically, the boundary layer will tend to: (1) permit the flow to expand well beyond the limiting inviscid expansion angle at the nozzle lip; and (2) alter the temperature, pressure and density in the portion of the theoretically inviscid plume which is influenced by the boundary layer.

The boundary layer affects the entire plume to some extent but the most pronounced effect is in the outer 40 percent of the mass flow within the plume (Refs. 8 and 9).

Condensation: For a rocket motor, the influence of gases condensing in low temperature flow fields has been numerically evaluated only to a limited extent. The condensation will usually occur at low temperatures, at low pressures, and at velocities near the limiting velocity of the gas (Ref. 10). The influences will occur in the highly expanded regions of a flow field corresponding to temperatures below the condensation temperature of the gas. (The flow upstream of the condensation point is not influenced.) Normally the condensation will occur at points in the flow field where the temperature is some 10 to 50°K below the equilibrium condensation point. After initial condensation takes place, the temperature/pressure relations of the flowing system will tend initially to be parallel to and then to converge toward the temperature/pressure variation of a static system in equilibrium. Condensation will cause local static pressures to be different than they would otherwise be by factors of 0 to -100 (condensation causes lower static pressures). Static temperatures will be influenced (with respect to the no-condensation case) by factors of zero to +5 (condensation increases static temperatures). The influence of condensation on some of the other parameters has not currently been defined to a sufficient degree but consequential effects can be expected.

Start Line: The influence of the starting flow conditions has been observed to have significant effects for regions close to the start line (Refs. 9, 11, 12, 13, 14) but these effects tend to weaken farther downstream (2 to 4 start line diameters downstream of the nozzle exit). Near the start line some parameters may be locally in error by almost a factor of 10 (between an estimated and an accurate start line). Downstream the errors will tend to be smaller (on the centerline, less than 25 percent; in the expansion region, as much as 50 to 100 percent). Plume calculations that are begun at the nozzle throat tend to be relatively free from start line effects. Plume calculations initiated at the nozzle exit tend to permit errors in local properties that correspond to a position error in the flow field of plus or minus one startline diameter.

Shock Waves: If shock waves in the nozzle and flow field are not considered, and a plume is computed as an isentropic flow, the errors in the plume flow field are similar in magnitude to those associated with start line effects (Item 9), (Refs. 8 and 9) except that in the immediate vicinity of the shock wave, variations in flow properties can be extremely different from the "no-shock" case. The greatest influence tends to occur along the centerline of the plume where the shock wave is strongest. In the highly expanded portion of a high-altitude (near vacuum) plume calculation the influence of the shock waves diminishes as the shock waves become weaker and weaker. Tables I and II present the maximum error band values anticipated along the centerline of a plume.

Error Band Application: Tables I and II list plume flowfield parameters and the estimated maximum percentage error imposed upon them by the various items (1 through 10) listed in the preceding discussion. Their application is restricted to locations in the plume specified in Table III and in the preceding discussion of each item. Application of the error bands should be

made considering that each error contribution may only partially exist for a particular plume, and the rms values of the sum should normally be used. In the application of error bands to design data, often a simple means of expressing the error band is needed. As a result, a nominal accuracy (or error band) representation has been devised for use on a general basis. This nominal accuracy should be based upon and reflect, for any particular plume, an rms summation of various error contributions cited in this paper. The rms errors should be resolved into a maximum percent error of combined spatial position and flow parameter value. The spatial accuracy band is arbitrarily assigned as being equal in percentage magnitude to the quantitative accuracy band. Results of numerous plume calculations and experimental calculations indicate that the flowfield structure (shock wave locations, etc.) can be in error as a result of the various factors. Some of the effects which produce flowfield parameter quantitative errors, also produce flowfield structure positional errors. Conversely, a highly accurate plume calculation will necessarily reflect accurate flowfield positional accuracies. Consequently, combining the spatial and quantitative accuracy bands is logical. For example, a plume nominal accuracy band might, by the inspection process, be assessed at ± 20 percent, which means that the calculated location of a particular flow feature (a shock wave for instance) may be in error by ± 20 percent in both the axial and radial position; also, the magnitude of the flowfield parameters may additionally be in error by ± 20 percent.

In summary, the process of defining a nominal plume accuracy should be accomplished by:

1. Assessing the applicability of the various items which contribute errors to the computed plume flow field at various plume locations

2. Determining the rms error band for each flowfield parameter for numerous points in the plume

3. Obtaining a "nominal plume accuracy band" rms value by averaging the rms error bands of the various points in the flow field.

CONCLUSIONS

Factors that affect the accuracy of plume calculations have been categorized, and anticipated ranges of errors associated with each plume parameter have been estimated. This information is provided for reference and is intended to serve as a guide in estimating the overall accuracy of any given plume analysis based upon the assumptions employed for the plume calculation. Absolute values of accuracy are almost impossible to assign to plume calculations. Therefore, the data presented should be used judiciously, and the problem at hand carefully considered, including the fact that the error bands have been somewhat grossly estimated.

SYMBOLS AND NOTATION

Force	force
M	Mach number
$\dot{m}$	mass flow rate
O/F	oxidizer/fuel ratio

P	static pressure
P_T	total pressure
P_{T_2}	pitot total pressure
T	static temperature
T_T	total temperature
V	velocity
σ_i	i^{th} species
γ	isentropic exponent
ρ	density

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TABLE I. ESTIMATED RANGE OF PERCENTAGE OF ERROR FOR VARIOUS PARAMETERS IN PLUME FLOW FIELD FOR A 3-SIGMA DEVIATION AT 95% CONFIDENCE INTERVAL

Item	1	2	3	4	5	6	7	8	9	10
Item Introducing Error Band in Plume Flow-field Parameters / Affected Parameter	Engine Operating Condition (P_c, O/F, $\dot{m}$), ±10% Variation	Chamber Combustion Efficiency and Momentum Loss not Included in Plume Analysis	Fuel Striations (Oxidizer/Fuel Gradients) not Included in Plume Analysis	Reaction Kinetics (Finite Rate Effects) not Included in Plume Analysis	Non-Continuum Flow Effects not Included in Plume Analysis	Computational Accuracy	Viscous Effects (Boundary Layer) Not Included in Plume Analysis	Flow Condensation Not Included In Plume Analysis	Approximate Start Line Used in the Analysis	Shock Waves Not Included in the Analysis
P_{T_2}	± 10	+ 0 / - 20	± 10	0	*	± 5	**	Δ	0	± 25
T_T	± 3	+ 0 / - 20	+ 0 / - 50	+ 0 / - 25	*	± 5	**	Δ	0	± 25
P	± 10	+ 0 / - 20	± 5	± 100	± 10	± 5	**	+1000 / - 0	±100	±100
T	± 3	+ 0 / - 20	+ 0 / - 50	± 100	+ 100 / - 0	± 5	**	+ 0 / -100	±100	±100
ρ	± 10	+ 0 / - 20	+ 100 / - 0	± 100	± 5	± 5	**	±50	±100	±100
V	± 5	+ 0 / - 10	- 40 / + 0	± 5	± 3	± 5	**	± 5	± 10	± 10
γ	± 3	± 3	± 50	± 25	± 40	± 5	**	Δ	± 0	± 10
α_i	± 1	± 25	± 100	± 100	± 1	± 5	**	Δ	± 0	± 5
F (impingement force) & P_{T_2}	± 10	+ 0 / - 20	± 10	± 5	± 20	± 10	**	±20	± 10	± 10
M	± 2	± 5	+ 5 / - 10	± 15	- 0 / + 50	± 5	**	±20	± 10	± 15

* Not meaningful
** Affects mainly the outer 40% of the mass flow (see Discussion)
Δ Not defined

TABLE II. ESTIMATED RANGE OF PERCENTAGE OF ERROR FOR VARIOUS PARAMETERS IN CALCULATED PLUME FLOW FIELDS FOR 1-SIGMA DEVIATIONS AT 95% CONFIDENCE INTERVALS

Item	1	2	3	4	5	6	7	8	9	10
Item Introducing Error Band in Plume Flowfield Parameters / Affected Parameter	Engine Operating Condition (P_c, O/F, $\dot{m}$), ±10% Variation	Chamber Combustion Efficiency and Momentum Loss Not Included in Plume Analysis	Fuel Striations (Oxidizer/Fuel Gradients) Not Included in Plume Analysis	Reaction Kinetics (Finite Rate Effects) Not Included in Plume Analysis	Non-Continuum Flow Effects Not Included in Plume Analysis	Computational Accuracy	Viscous Effects (Boundary Layer) Not Included in Plume Analysis	Flow Condensation Not Included in Plume Analysis	Approximate Start Line Used in the Analysis	Shock Waves Not Included in the Analysis
P_T	± 2	+ 0 - 3	± 2	0	*	± 2	**	Δ	0	± 25
T_T	± 1	+ 0 - 3	+ 0 - 10	+ 0 - 25	*	± 2	**	Δ	0	± 25
P	± 2	+ 0 - 3	± 2	± 15	± 10	± 2	**	+ 50 - 0	± 25	± 100
T	± 1	+ 0 - 3	+ 5 - 10	± 15	+100 - 0	± 2	**	+ 0 - 20	± 25	± 100
ρ	± 2	+ 0 - 3	- 20 - 5	± 15	± 5	± 2	**	± 10	± 25	± 100
V	± 1	+ 0 - 2	- 10 + 5	± 2	± 3	± 2	**	± 2	± 2	± 10
γ	± 1	± 1	± 5	± 5	± 40	± 2	**	Δ	0	± 10
α_i	±0.5	± 4	± 10	± 15	± 1	± 2	**	Δ	0	± 5
F (impingement force) & P_{T_2}	± 2	+ 0 - 3	± 2	± 2	± 20	± 4	**	± 5	± 2	± 10
	± 2	± 2	+ 2 - 5	± 10	- 0 + 50	± 2	**	± 10	± 10	± 50

*Not meaningful

**Affects mainly the outer 40% of the mass flow (see Discussion)

Δ Not defined

TABLE III. REGIONS OF THE PLUME WHERE ERROR BANDS APPLY

Item	Region of Plume Where Error Bands Apply if the Item is Not Included in the Analysis
1. Engine Operating Conditions	Entire Flow Field
2. Chamber Combustion Efficiency and Momentum Loss	Entire Flow Field
3. Flow Striations	Entire Flow Field
4. Reaction Kinetics	Small errors near nozzle exit, progressively larger errors in the far plume.
5. Non-Continuum Effects	Error applies in the transition flow regime. The error is zero at the onset of transition flow, maximum at the sudden freeze point, and decreases as free molecular flow occurs.
6. Calculational Accuracy	Entire Flow Field
7. Viscous Effects	Error increases in the region of the plume outside of approximately the 60% mass flow streamline (where minor errors exists). Major errors occur outside the inviscid plume region.
8. Condensation	Error is zero upstream of the point in the flow field where the equilibrium condensation temperature exists. Downstream, the error can grow with increasing distances from the equilibrium point.
9. Start Line	Error is maximum near the startline, decreases to smaller values 2 to 5 startline diameters (nozzle throat or exit) downstream.
10. Shock Waves	Error is maximum near the centerline and in the regions where the shock should be; decreases away from the centerline.

Appendix C

EMPIRICAL INPUT DATA AND INPUT DATA SUGGESTIONS

Appendix C

The results obtained from the Reacting and Multiphase Computer Program (RAMP) are very sensitive to data which are input. For two-phase cases the mean particle size, distribution of sizes, specific heats, mass density, particle melting temperature, chemistry assumptions and boundary equations are the primary input variables which determine the results. Each of these variables will be discussed in some detail and suggestions will be made as to what values can be used for aluminized propellants. It should be noted, however, that the data presented is not necessarily the best available.

Mean Particle Size

Several different methods have been employed for obtaining mean particle size. Included are techniques which correlate mean size to throat diameter (Ref. C-1), mean motor L^* (Ref. C-2) (chamber volume/throat area), chamber pressure, residence time, particle loading, maximum stable droplet size as well as combinations of each of these parameters. As a simple estimate of mean particle size the correlation of Delaney (Ref. C-1) based on throat diameter can be used:

$$D_m = 4\, D_t^{.3} \qquad \text{(C.1)}$$

where D_m is the mean particle diameter in microns and D_t is the throat diameter in inches.

Particle Size Distribution

For nozzle calculations in which no particle impingement on the wall is anticipated, one particle size at the mean size can be used. However, for plume calculations a knowledge of the particle size distribution is necessary.

Delaney in Ref. C-1 showed that the distribution of particles for smaller motors ($D_t \lesssim 3.5$ in.) followed a log normal distribution (Fig. C-1). For the large motors ($D_t > 3.5$ in.) the data indicate that the size distribution follows a normal distribution (Fig. C-2). To use these distributions: move the curves up or down to the mean size at the 50% coordinate, then divide the curve into 5 or 6 sections and determine the mean size that goes with each of these sections. Table C-1 gives an example of the size distribution (for 6 discrete sizes) which was determined from the curve in Fig. C-1.

Particle Specific Heats, Enthalpies and Melting Temperature

The values for particle specific heats, enthalpies and melting temperature which the authors use are shown in Table C-2. The specific heats shown are used for the ideal approximation of particle enthalpy verses temperature (i.e., the specific heat for liquid and solid phases of the aluminum oxide are constant). The user may find the tables of temperature verses enthalpy in the JANAF Thermochemical Tables (Ref. C-3).

Particle Mass Density

The mass density for aluminum oxide is different for the solid and liquid phases. Reference C-4 shows the mass density of liquid aluminum oxide ($A\ell_2O_3$) to be 188 lbm/ft^3. The mass density of solid $A\ell_2O_3$ is 250 lbm/ft^3. For cases where the particle temperatures will be higher than the melting temperature for most of the flow field, the liquid mass density should be used. In cases where the particle temperature will be below the melting temperature (i.e., plumes) the solid mass density should be used.

Chemistry Assumptions

There are numerous chemistry assumptions which can be employed by the RAMP code. The various assumptions are: (1) ideal gas (constant specific heat ratio and molecular weight); (2) equilibrium; (3) frozen (constant molecular weight, varying specific heat ratio); (4) equilibrium/frozen (equilibrium with the molecular weight constant below a specified pressure) or (5) finite-rate chemistry.

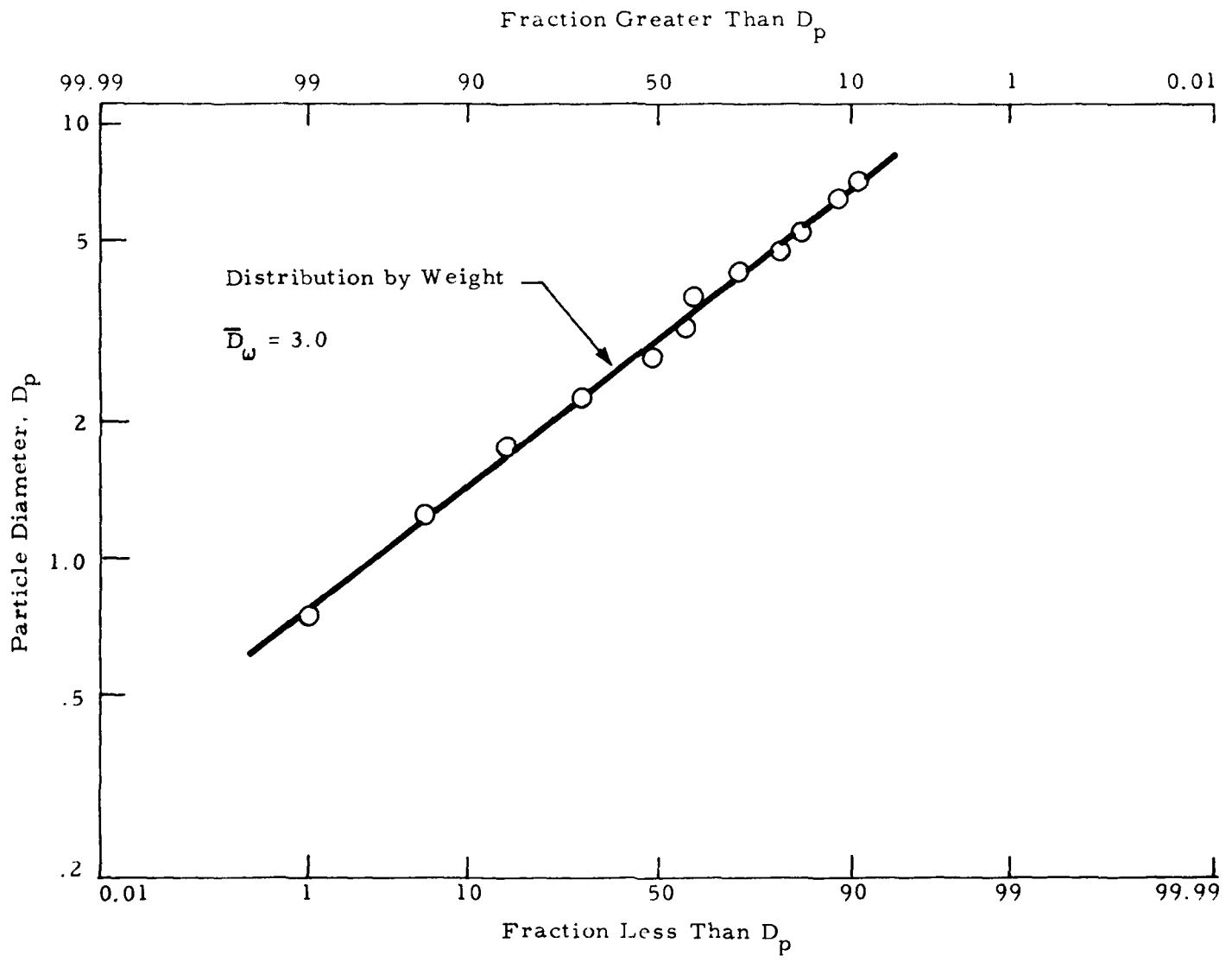


Fig. C-1 - Log Normal Particle Size Distribution from HI 5 PC Motor (Ref. C-1)

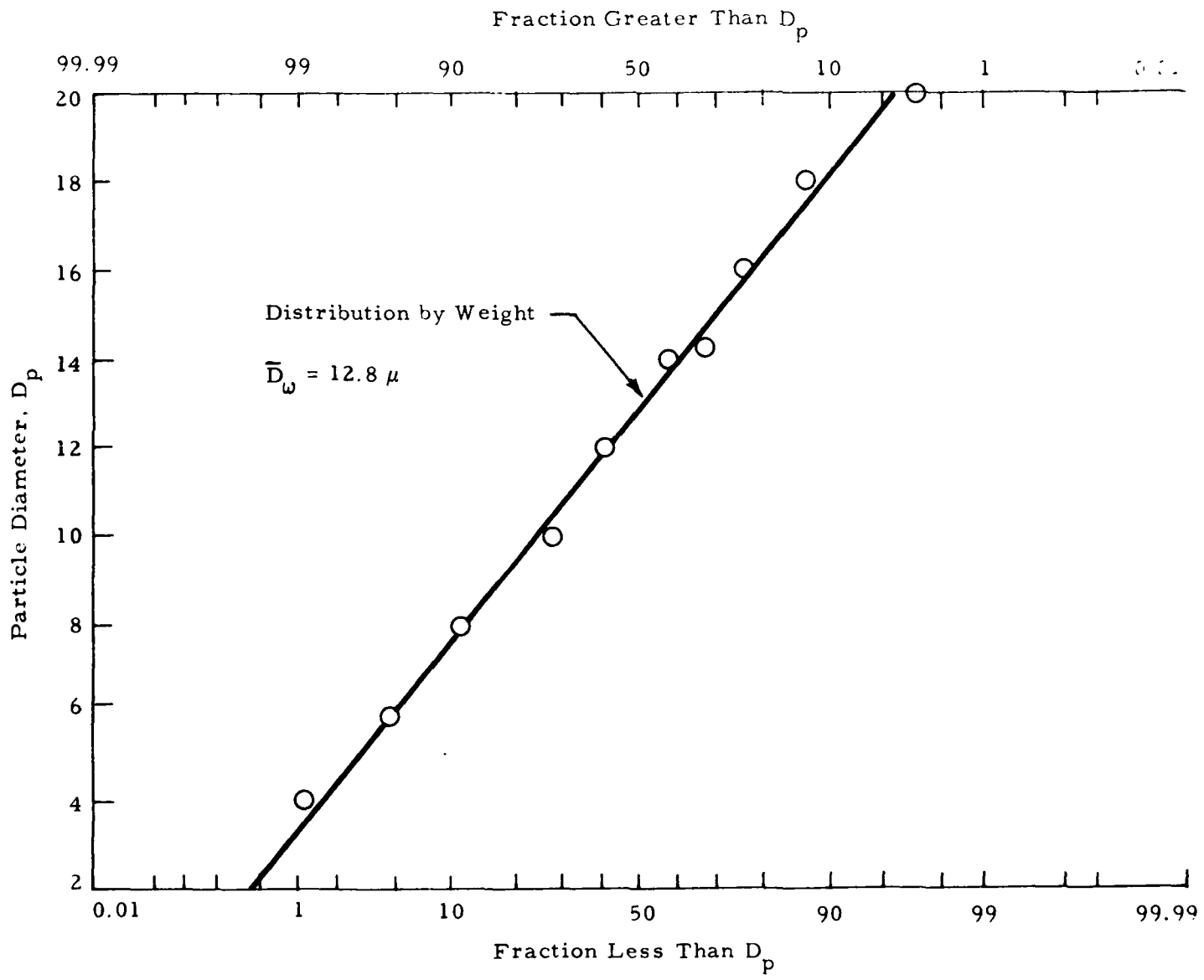


Fig. C-2 - Normal Particle Size Distribution from AGC 260-2 Motor (Ref. C-1)

Table C-1

LOG NORMAL PARTICLE SIZE DISTRIBUTION
FOR HI 5 PC MOTOR

Particle Diameter	Percent Total Particle Mass Flow
1.2	10
1.9	20
2.65	20
3.5	20
5.0	20
8.0	10

Table C-2

$A\ell_2O_3$ THERMODYNAMIC DATA

Liquid $A\ell_2O_3$ Specific Heat (C_{p_ℓ})	–	.34 Btu/lbm°R
Solid $A\ell_2O_3$ Specific Heat (C_{p_s})	–	.32 Btu/lbm°R
Enthalpy of Solid Phase of $A\ell_2O_3$ at Melting Temperature	–	1358.9 Btu/lbm
Enthalpy of Liquid Phase of $A\ell_2O_3$ at Melting Temperature	–	1858.7 Btu/lbm
Melting Temperature	–	4188°R

The type of chemistry assumption is very case dependent and also depends on the use of the flow field. Table C-3 presents various cases and applications, along with suggestions as to the type of chemistry assumptions to be used.

Finite rate cases can generally be started at the nozzle throat assuming the species distribution is in chemical equilibrium since this is valid for most propellant systems. Tables C-4 through C-6 present some reaction mechanisms which may be used for applicable propellant systems. These reaction mechanisms were obtained from data presented in Ref. C-5.

Boundary Equations

The boundary equations which are input to the code should be smooth and not contain discontinuities in either the slopes or coordinates where no discontinuities are physically present. Fictitious discontinuities can result in undesirable mass flow errors showing up during a solution. In Fig. C-3 a description of the boundary equations for the nozzle throat and free boundary are presented.

More complex nozzle contours may be input with discrete points which define the wall as a function of radial position and flow angle versus axial position.

Table C-3

SUGGESTED CHEMISTRY ASSUMPTIONS
FOR VARIOUS APPLICATIONS

Application	Ideal Gas	Equilibrium	Equilibrium/Frozen	Finite Rate
Nozzle Performance		x		
Plume Radiation				x
Plume Impingement			x	
Base Pressure (Initial Plume Expansion)	x*			
Electron Density				x
Contamination				x

*Use specific heat ratio which exists at lip.

Table C-4

REACTION MECHANISM FOR SPACE SHUTTLE SRM PROPELLANT

H	+OH	+M1	=H2O	+M1	22	6.10-26	2.0	0.0
O	+H	+M1	=OH	+M1	21	2.00-32	0.0	0.0
O	+O	+M1	=O2	+M1	24	3.60-30	1.0	-340.0
H	+H	+M2	=H2	+M2	22	2.80-30	1.0	0.0
OH	+H		=H2	+O	14	1.40-14	-1.0	-7000.0
OH	+O		=H	+O2	11	4.00-11	0.0	0.0
OH	+H2		=H2O	+H	14	1.00-17	-2.0	-2900.0
OH	+OH		=H2O	+O	13	1.00-11	0.0	-1100.0
CO	+O	+M3	=CO2	+M3	23	2.00-33	0.0	-4000.0
OH	+CO		=CO2	+H	14	1.10-19	-2.0	1600.0
CL	+CL	+M1	=CL2	+M1	24	4.30-31	1.0	1250.0
H	+CL	+M4	=HCL	+M4	22	3.00-30	1.0	0.0
OH	+HCL		=H2O	+CL	14	1.00-14	-1.0	-1000.0
O	+HCL		=OH	+CL	13	2.00-12	0.0	-4500.0
H	+CL2		=HCL	+CL	13	2.00-10	0.0	-2400.0
CL	+H2		=HCL	+H	13	8.00-11	0.0	-5260.0

Catalytic Species

M_1 = 3 H_2O, 2 CO_2; All others: 1.0

M_2 = 20 H, 10 H_2O, 3 CO_2, 2.5 H_2; All others: 1.0

M_3 = 20 O_2, 10 H_2O, 3 CO_2, 1.5 CO; All others: 1.0

M_4 = 10 H_2O, 5 $HC\ell$, 5 $C\ell$, 5 H, 3 $C\ell_2$, 3 CO_2; All others: 1.0

Table C-5

REACTION MECHANISM FOR H_2-O_2 PROPELLANT SYSTEM

H	+OH	+M1	=H2O	+M1	22	6.10-26	2.0	0.0
O	+H	+M1	=OH	+M1	21	2.00-32	0.0	0.0
O	+O	+M1	=O2	+M1	24	3.80-30	1.0	-340.0
H	+H	+M2	=H2	+M2	22	2.80-30	1.0	0.0
OH	+H		=H2	+O	14	1.40-14	-1.0	-7000.0
OH	+O		=H	+O2	11	4.00-11	0.0	0.0
OH	+H2		=H2O	+H	14	1.00-17	-2.0	-2900.0
OH	+OH		=H2O	+O	13	1.00-11	0.0	-1100.0

Catalytic Species

M_1 = 3 H_2O; All others: 1.0

M_2 = 20 H, 10 H_2O, 2.5 H_2; All others: 1.0

Table C-6

REACTION MECHANISM FOR LOX-RP1 PROPELLANT SYSTEM

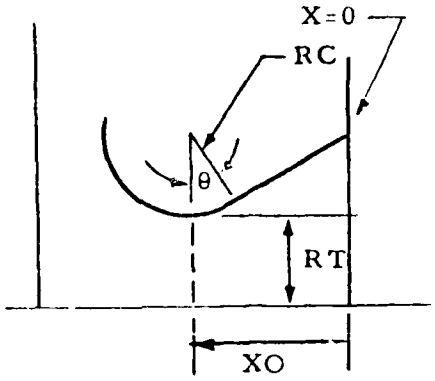
H	+OH	+M1	=H2O	+M1	22	6.10-26	2.0	0.0
O	+H	+M1	=OH	+M1	21	2.00-32	0.0	0.0
O	+O	+M1	=O2	+M1	24	3.80-30	1.0	-340.0
H	+H	+M2	=H2	+M2	22	2.80-30	1.0	0.0
OH	+H		=H2	+O	14	1.40-14	-1.0	-7000.0
OH	+O		=H	+O2	11	4.00-11	0.0	0.0
OH	+H2		=H2O	+H	14	1.00-17	-2.0	-2900.0
OH	+OH		=H2O	+O	13	1.00-11	0.0	-1100.0
CO	+O	+M3	=CO2	+M3	23	2.00-33	0.0	-4000.0
OH	+CO		=CO2	+H	14	1.10-19	-2.0	1600.0

Catalytic Species

M_1 = 3 H_2O, 2 CO_2; All others: 1.0

M_2 = 20 H, 10 H_2O, 3 CO_2, 2.5 H_2; All others: 1.0

M_3 = 20 O_2, 10 H_2O, 3 CO_2, 1.5 CO; All others: 1.0



RC = radius of curvature of the circular arc of the throat
RT = throat radius
XO = axial distance from the origin of the coordinate system to the throat
θ = throat divergence angle corresponding to the maximum value for which the throat conic equation applies

The conic equation for this case would have the following form:

A = -1 for an upper equation, +1 for a lower equation (-1 for this case)

$B = RC^2 - XO^2$

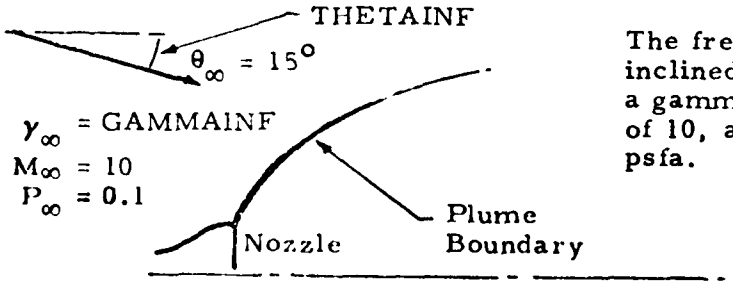
$C = 2XO$

$D = -1$

$E = -(RC + RT)$

$Xmax = RC \sin\theta + XO$

An example of a free boundary is shown in the sketch below.



The freestream approach flow is inclined at 15 deg to the plume with a gamma (γ) of 1.4, a Mach number of 10, and a static pressure of 0.1 psfa.

PINF = 0.1 (psfa)
E = 0 (No pressure variation with axial distance)
GAMMAINF = 1.4
MINF = 10
THETAINF = -15°

Fig. C-3 - Sample of Boundary Equations

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